

Numerical Heat Transfer (数值传热学)

Chapter 10 General Code for 2D Elliptical Fluid Flow and Heat Transfer (2)



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Chapter 10 General Code for 2D Elliptical Fluid Flow and Heat Transfer Problems (2)

10.6 Methods of application and explanation of Main Program

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10. 6 Methods of Application and Explanation of Main Program

10.6.1 Methods of Code application

1. **Establishing** complete mathematical formulation and **comparing** with the standard equation:

$$\frac{\partial(\rho^* \phi)}{\partial t} + \text{div}(\rho^* \vec{u} \phi) = \text{div}(\Gamma_{\phi} \text{grad} \phi) + S_{\phi}^*$$

Determine S_{ϕ}^* , Γ_{ϕ} , and ρ_{ϕ}^*

2. **Calling (调用)** a USER(will be taught in Chapter 11) similar to the problem studied

3. Using a few nodes, 5~7 in each direction, and setting a **small value of LAST**, say 3–5, to go through grammatical examination; Then gradually increasing the complexity.

4. Making correspondent modifications for the **six-Module in USER**, according to the problem studied, especially for following parts:

(1) **LSOLVE(NF)**—for variable NF to be solved setting :

.TRUE.

(2) **LAST**—Specify iteration number, default value is 5.

(3) **NTIMES(NF)**—Default value equals 1; for steady nonlinear one, setting: 1 to 2; unsteady linear: 5 to 6

(4) **DT**—Time step, default value is 10^{30}

For fully implicit scheme, in the a_p -term there is a term of $a_p^0 = \rho\Delta V / \Delta t$, if $\Delta t \rightarrow \infty$, $a_p^0 \rightarrow 0$, leading to steady state results. **Default value is for steady case.**

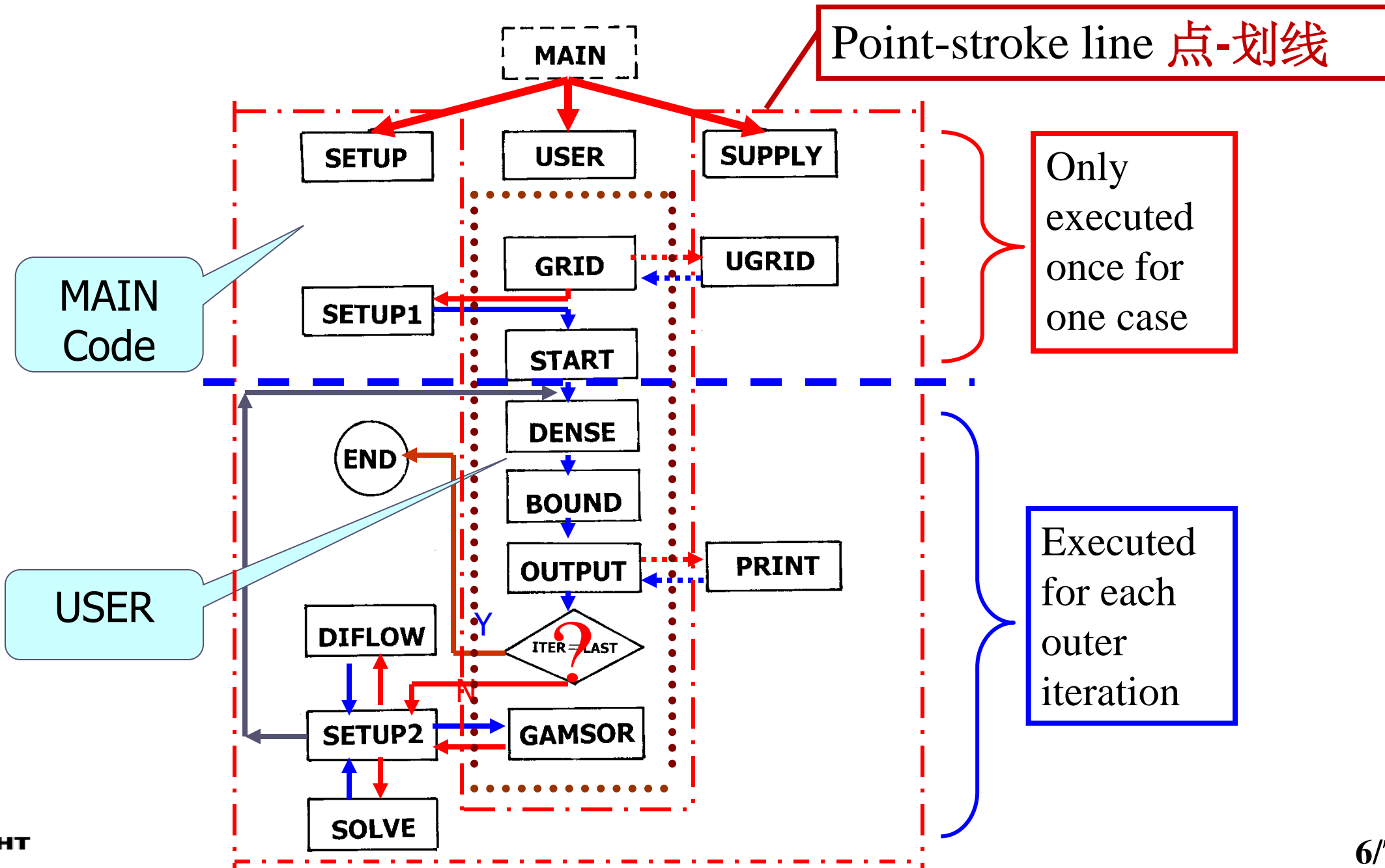
(5) **RELAX(NF)**—Default value is 1.

5 Defining a new dependent variable, say $C(i,j)$, as follows:

First defining $C(NI,NJ)$,

then using **EQUIVALENCE:**

EQUIVALENCE (F(1,1,5), C(1,1)).



For the **Main Program**, these parts will be explained in detail.

1. **MODULE START_L**
2. -----**MAIN** -----
3. **SUBROUTINE DIFLOW**
4. **Structure of SOLVE**
5. **Block correction**
6. **Structure of SETUP**
7. **MODE execution**
8. **Determination of neighbor coefficients**
9. **Determination of AP coefficients**
10. **Structure of SIMPLER**
11. **Temporal storage of coefficients for SIMPLER**
12. **Accumulated addition**
13. **Storage of coefficients of p -equation**
14. **Nominal density for temperature**
15. **Iteration=Marching forward**
16. **Data Format for print out**

10-6-2 Explanation of Main programs

```
CCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCC  
C This computer program was copied from the graduate student course  
C program of the University of Minnesota. Part of it was re-formulated  
C to meet the local computational environment. Some inappropriate  
C expressions were also corrected. The program is used only for the  
C teaching purpose. No part of it may be published. You may use it as a  
C frame to re-develop your own code for research purpose.  
C -----Instructor of Numerical Heat Transfer, XJTU,2013.-----  
CCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCC  
C The current version of the program was updated from Fortran 77 to  
C Fortran 95 by Dr. Yu-Tong Mu , Dr. Li Chen and Dr.Kong Ling of NHT  
C group of XJTU during 2013.01-04  
CCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCC  
C*****
```




毋玉同



凌空



陈黎

10.6.2.1 MODULE START_L

(1)-Explained in detail

MODULE START_L ! Name of Module

PARAMETER (NI=100,NJ=200,NIJ=NI,**NFMAX=10,NFX4=NFMAX+4**)

C*****

CHARACTER*8 TITLE(NFX4)

LOGICAL LSOLVE(NFX4),LPRINT(NFX4),LBLK(NFX4),LSTOP

REAL*8,DIMENSION(NI,NJ,NFX4)::F ! One 3D function

REAL*8,DIMENSION(NI,NJ,6)::COF,COFU,COFV,COFP

REAL*8,DIMENSION(NI,NJ)::P,RHO,GAM,CP,CON,AIP,AIM,AJP,AJM,AP

REAL*8,DIMENSION(NI):: U,V,PC,T,DU,DV,UHAT,VHAT

REAL*8,DIMENSION(NI):: X,XU,XDIF,XCV,XCVS,XCVI,XCVIP

REAL*8,DIMENSION(NJ)::Y,YV,YDIF,YCV,YCVS,YCVR,YCVRS,ARX,ARXJ,

& ARXJP,R,RMN,SX,SXMN

REAL*8,DIMENSION(NI)::FV,FVP,FX,FXM

REAL*8,DIMENSION(NJ)::FY,FYM

REAL*8,DIMENSION(NIJ)::PT,QT

REAL*8 RELAX(NFX3),TIME,DT,XL,YL,RHOCON

INTEGER*4 NF,NP,NRHO,NGAM,NCP,L1,L2,L3,M1,M2,M3,

& IST,JST,ITER,LAST,MODE,NTIMES(NFX4),IPREF,JPREF

REAL*8 SMAX,SSUM

REAL*8 FLOW,DIFF,ACOF

Sc or b

a_e, a_w, a_n, a_s, a_p

- (1) Packaging data (封装数据);
- (2) Initializing data (数据初始化);
- (3) Declaring type of data (声明数据类型).

C*****

**EQUIVALENCE(F(1,1,1),U(1,1)),(F(1,1,2),V(1,1)),(F(1,1,3),PC(1,1))
&, (F(1,1,4),T(1,1))**

**EQUIVALENCE(F(1,1,11),P(1,1)),(F(1,1,12),RHO(1,1)),(F(1,1,13)
&,GAM(1,1),(F(1,1,14),CP(1,1))**

**EQUIVALENCE(COF(1,1,1),CON(1,1)),(COF(1,1,2),AIP(1,1)),
&(COF(1,1,3),AIM(1,1)),(COF(1,1,4),AJP(1,1)),
&(COF(1,1,5),AJM(1,1)),(COF(1,1,6),AP(1,1))**

REAL*8,DIMENSION(NI)::TH,THU,THDIF,THCV,THCVS

REAL*8 THL

**EQUIVALENCE(X,TH),(XU,THU),(XDIF,THDIF),(XCV,THCV),
&(XCVS,THCVS),(XL,THL)**

DATA LSTOP,LSOLVE,LPRINT/.FALSE.,NFX4*.FALSE., NFX4*.FALSE./

DATA LBLK/NFX4*.TRUE./

DATA MODE,LAST,TIME,ITER/1,5,0.,0/

DATA RELAX,NTIMES/NFX4*1.,NFX4*1/

DATA DT,IPREF,JPREF,RHOCON,CPCON/1.E+30, 1,1,1.,1./

END MODULE

MODULE module_name

•••••
•••••
•••••

Module name is composed of two parts,
with a hyphen(-) at bottom in between.

END MODULE

- (1) Packaging data (封装数据);
- (2) Initializing data (数据初始化);
- (3) Declaring type of data (声明数据类型).

**Default
value!!**

Some explains to this most important module

REAL*8,DIMENSION(NI,NJ,NFX4)::F

Real variable 3-D array, array title F, F(NI,NJ,NFX4);
Variable number in three coordinates are NI,NJ and NFX4
respectively;

REAL*8 SMAX,SSUM

Real variable of SMAX and SSUM, with length of eight digits;

INTEGER*4 NF,NP,NRHO

Integer variable of NF,NP,NRHO, with length of four digits;

EQUIVALENCE(F(1,1,1),U(1,1)),(F(1,1,2),V(1,1))

Making the 1st variable of the 3D array F identical to the 2D
array U; the same for (F(1,1,2), V(1,1))

10.6.2.2 PROGRAM MAIN

(2)-Explained
in detail

```

C*****
C-----MAIN-----
C*****
PROGRAM MAIN ! Set up entire flow chart
USE START_L      Share the variables defined in the MODULE
IMPLICIT NONE
C*****
OPEN(8,FILE='RESULT.txt') ! Result file for output
CALL GRID      !Grid generation (setup interface positions)
CALL SETUP1   !Set up 1-D array of geometric parameters
CALL START    !Set up initial field
DO WHILE (.NOT.LSTOP) ! If LSTOP is .F., then do loop
CALL DENSE    !Set up fluid density
CALL BOUND    !Set up boundary condition
CALL OUTPUT   !Print out representative results
CALL SETUP2   !Key module: set coefficients and solve ABEqs.
ENDDO
CALL OUTPUT !Print out some results
CLOSE(8)     !Simulation completed close file RESULT.TXT in Channel 8
STOP        !Terminate computation
END         !End of main program

```

Calling
Module



Only
Executed
once



Executed
Many times



CC

For ABEqs, we determine coefficients using **Subroutine DIFLOW**

For all other scalar variables (including T , etc)

$$\frac{\partial(\rho^* \phi)}{\partial t} + \text{div}(\rho^* \phi \vec{U}) = \text{div}(\Gamma_\phi \text{grad} \phi) + S_\phi^*$$

$$a_P \phi_P = a_E \phi_E + a_W \phi_W + a_N \phi_N + a_S \phi_S + b$$

$$a_E = D_e A(|P_{\Delta e}|) + \llbracket -F_e, 0 \rrbracket \quad a_W = D_w A(|P_{\Delta w}|) + \llbracket F_w, 0 \rrbracket$$

a_E / D_e :

Scheme	Central difference	Upwind difference
Definition	$1 - 0.5 P_{\Delta e}$	$1 + \llbracket -P_{\Delta e}, 0 \rrbracket$
Hybrid	Power-law	Exponential
$\llbracket -P_{\Delta e}, 1 - \frac{1}{2} P_{\Delta e}, 0 \rrbracket$	$\llbracket 0, (1 - 0.1 P_{\Delta e})^5 \rrbracket + \llbracket 0, -P_{\Delta e} \rrbracket$	$\frac{P_{\Delta e}}{\exp(P_{\Delta e}) - 1}$

$$P_{\Delta e} = \frac{F_e}{D_e}$$

10.6.2.3 SUBROUTINE DIFLOW

(3)-Explained
in detail

CC

SUBROUTINE DIFLOW ! Determine $D \cdot A(|P_\Delta|)$ of power law scheme
 !The input variables are DIFF and FLOW

USE START_L ! Share the variables defined in the MODULE START_L

IMPLICIT NONE

REAL*8 TEMP ! temporal variable

C*****

ACOF=DIFF ! $D \cdot A(|P_\Delta|) = D$ (ACOF represents $D \cdot A(|P_\Delta|)$)

IF(FLOW== 0.) RETURN ! No flow, only diffusion

TEMP=DIFF-ABS(FLOW)*0.1 ! $D - 0.1|F| = D(1 - 0.1|P_\Delta|)$

ACOF=0. ! $\left\{ \begin{array}{l} 0 \quad |P_\Delta| > 10 \\ (1 - 0.1|P_\Delta|)^5 \quad |P_\Delta| < 10 \end{array} \right.$

! 1st return for
diffusion case

! 2nd return for
 $|P_\Delta| > 10$

IF(TEMP <= 0.) RETURN ! $|P_\Delta| > 10$

TEMP=TEMP/DIFF ! $1 - 0.1|P_\Delta|$

! 3rd return for
 $|P_\Delta| < 10$

ACOF=DIFF*TEMP5** ! $D \cdot (1 - 0.1|P_\Delta|)^5 = D \cdot A(|P_\Delta|)$

RETURN

END !In SETUP2: $a_E = D_e A(|P_\Delta|) + [0, -F_e]$

10.6.2.4 SUBROUTINE SOLVE

CC

SUBROUTINE SOLVE ! alternative direction line iteration

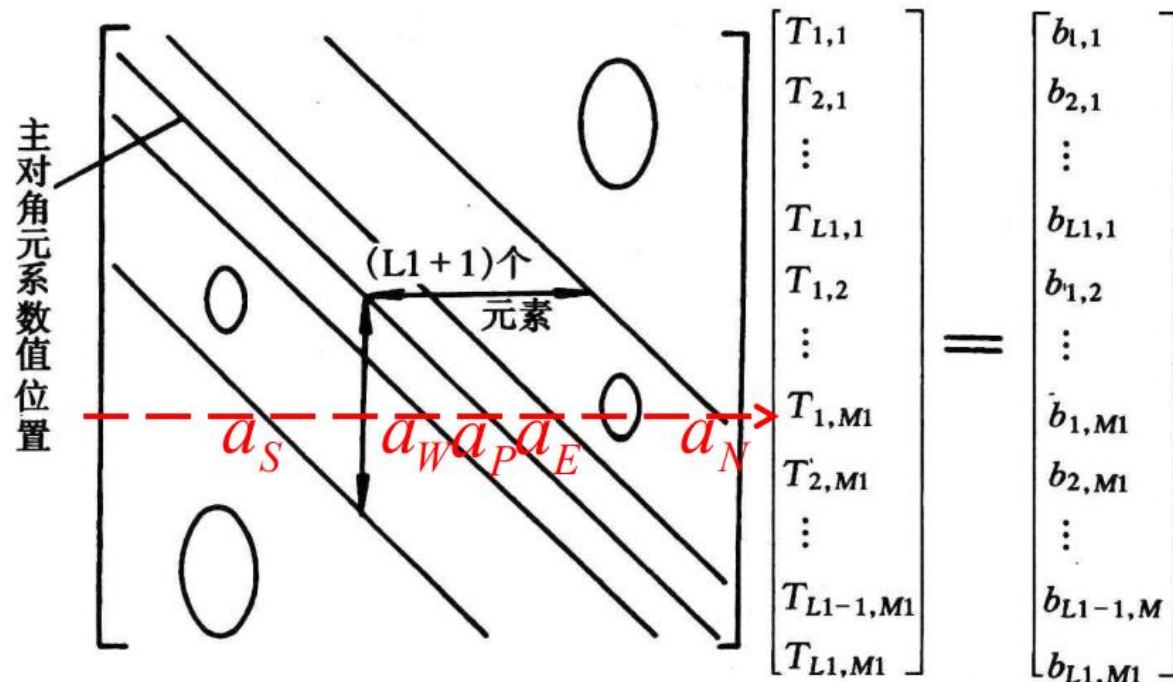
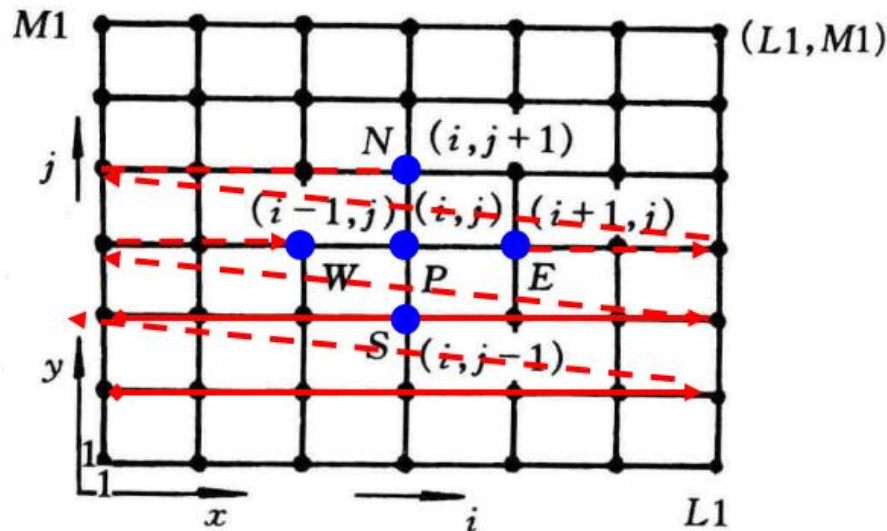
USE START_L + Block correction

IMPLICIT NONE

INTEGER*4 ISTF, JSTF, IT1, IT2, JT1, JT2, NT, N,I,J,II,JJ

REAL*8 BL, BLP, BLM, BLC, DENOM, TEMP

C*****



Structure of SOLVE

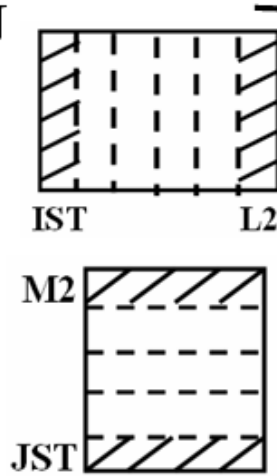
AD---alternative direction

S
O
L
V
E

```

DO 999 NT=1, NTIMES (NF)
N=NF
IF (LBLK(NF)) THEN
PT(ISTF)=0.
.....
13 ENDDO
PT(JSTF)=0.
.....
23 ENDDO
10 ENDIF

```

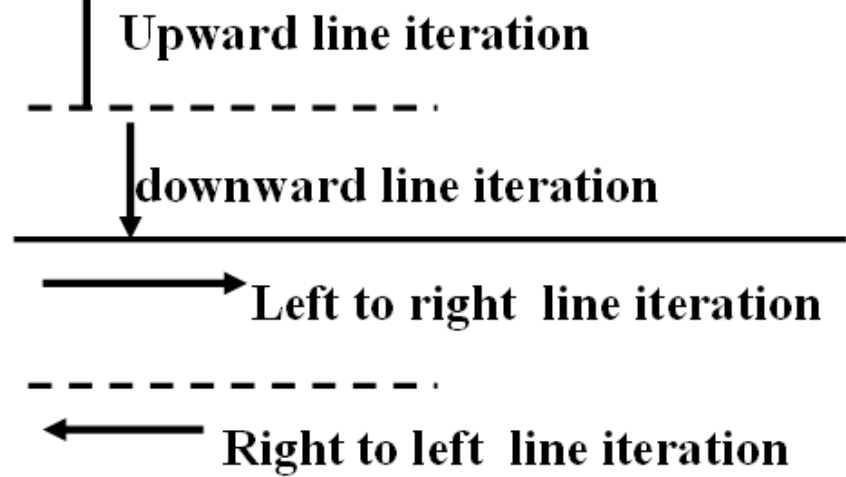


Two times of block corrections

AD Block Correction

Four times of line iterations

AD line Iteration



(4)-Explained in detail

999 ENDDO

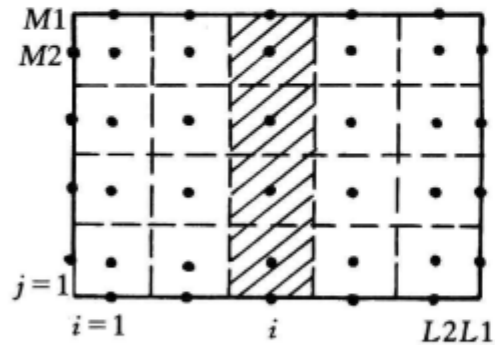
Review on block correction

1. Equation for correction:

It is required that: $(\phi_{i,j}^* + \bar{\phi}_i')$ satisfy following eq.

$$\begin{aligned} \sum_j \underline{AP}(\phi_{i,j}^* + \bar{\phi}_i') &= \sum_j \underline{AIP}(\phi_{i+1,j}^* + \bar{\phi}_{i+1}') + \sum_j \underline{AIM}(\phi_{i-1,j}^* + \bar{\phi}_{i-1}') \\ &+ \sum_j (\underline{AJM})(\phi_{i,j-1}^* + \bar{\phi}_i') \\ &+ \sum_j (\underline{AJP})(\phi_{i,j+1}^* + \bar{\phi}_i') + \sum_j \underline{CON} \end{aligned}$$

$(i = IST, \dots, L2)$



IST-solution starting subscript in X-direction; L2-last but one.

Here AP, AIP, AIM , etc. are the symbols adopted in teaching code

Review on block correction

(5)-Explained
in detail

$$(BL)\bar{\phi}'_i = (BLP)\bar{\phi}'_{i+1} + (BLM)\bar{\phi}'_{i-1} + BLC, i = IST, \dots, L2$$

$$BL = \sum_{j=JST}^{M2} (AP) - \sum_{j \neq M2} (AJP) - \sum_{j \neq JST} (AJM) \quad BLP = \sum_{j=JST}^{M2} (AIP)$$

$$BLM = \sum_{j=JST}^{M2} (AIM) \quad BLC = \sum_{j=JST}^{M2} CON + \sum_{j=JST}^{M2} (AJP)\phi_{i,j+1}^* + \sum_{j=JST}^{M2} (AJM)\phi_{i,j-1}^*$$

$$BL = A, BLP = B, \\ BLM = C$$

$$+ \sum_{j=JST}^{M2} (AIP)\phi_{i+1,j}^* + \sum_{j=JST}^{M2} (AIM)\phi_{i-1,j}^* - \sum_{j=JST}^{M2} (AP)\phi_{i,j}^*$$

$$A_i \bar{\phi}'_i = B_i \bar{\phi}'_{i+1} + C_i \bar{\phi}'_{i-1} + D_i, i = 1, 2, \dots, M1 \rightarrow \bar{\phi}'_{i-1} = P_{i-1} \bar{\phi}'_i + Q_{i-1}$$

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}}; \quad Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}}; \quad P_1 = \frac{B_1}{A_1}; \quad Q_1 = \frac{D_1}{A_1}$$

$$DENOM = BL - PT(I-1) * BLM$$

DENOM

● TDMA

$$A_i T_i = B_i T_{i+1} + C_i T_{i-1} + D_i, \quad i = 1, 2, \dots, M1 \quad (\mathbf{a})$$

(1) Elimination (消元) – Reducing the unknowns at each line from 3 to 2

$$T_{i-1} = P_{i-1} T_i + Q_{i-1} \quad (\mathbf{b})$$

$$P_1 = \frac{B_1}{A_1}; \quad Q_1 = \frac{D_1}{A_1} \quad P_i = \frac{B_i}{A_i - C_i P_{i-1}}; \quad Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}};$$

(2) Back substitution (回代) – Starting from M1 via Eq.(b) to get T_i sequentially

$$T_{M1} = Q_{M1} \quad T_{i-1} = P_{i-1} T_i + Q_{i-1}$$

● Implementation of TDMA for 1st kind B.C.

For 1st kind B.C., the solution region is from $i=2\dots$ to $M1-1=M2$, because T_1 and T_{M1} are known.

Applying Eq.(b) to $i=1$ with given $T_{1,given}$:

$$T_1 = P_1 T_2 + Q_1 \longrightarrow P_1 = 0; Q_1 = T_{1,given}$$

Because T_{M1} is known, back substitution should be started from M_2 :

$$T_{M2} = P_{M2} T_{M1} + Q_2$$

When the ASTM is adopted to deal with B.C. of 2nd and 3rd kind, **the numerical B.C. for all cases is regarded as 1st kind**, and the above treatment should be adopted.

C*****

ISTF=IST-1
 JSTF=JST-1
 IT1=L2+IST
IT2=L3+IST
 JT1=M2+JST
JT2=M3+JST

!Temporal variables for starting points of DO-loop

C*****

DO 999 NT=1,NTIMES(NF) ! Solution of algebraic equation
N=NF ! NF: 1=U, 2=V, 3=P, 4=T.....

C-----

IF(LBLK(NF)) THEN !When LBLK is true, execute Block-correction

PT(ISTF)=0. ! Coefficient in TDMA P_{IST-1}

QT(ISTF)=0. ! Constant in TDMA Q_{IST-1}

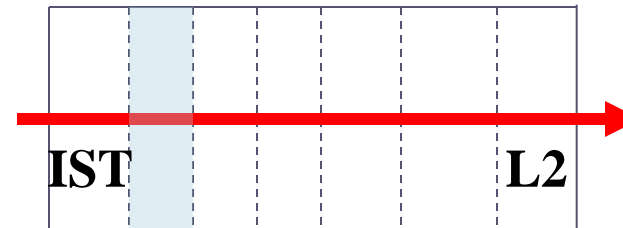
DO 11 I=IST,L2

BL=0. !Initial value in B-correction

BLP=0. !Initial value in B-correction

BLM=0. ! Initial value in B-correction

I-direction B. Correction.



**(5)-
Explained
in detail**

In discussion of TDMA:

A B C D
 $(BL)\bar{\phi}'_i = (BLP)\bar{\phi}'_{i+1} + (BLM)\bar{\phi}'_{i-1} + BLC, i = IST, ..L2$

BLC=0. !Initial value

DO 12 J=JST,M2

BL=BL+AP(I,J)

IF(J /= M2) BL=BL-AJP(I,J)

IF(J /= JST) BL=BL-AJM(I,J)

BLP=BLP+AIP(I,J)

BLM=BLM+AIM(I,J)

BLC=BLC+CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)

& +AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)-AP(I,J)*F(I,J,N)

12 ENDDO

DENOM=BL-PT(I-1)*BLM

IF(ABS(DENOM/BL) < 1.E-10) DENOM=1.E25

PT(I)=BLP/DENOM

QT(I)=(BLC+BLM*QT(I-1))/DENOM

11 ENDDO

$$BL = \sum_{j=JST}^{M2} (AP) - \sum_{j \neq M2} (AJP) - \sum_{j \neq JST} (AJM)$$

$$BLP = \sum_{j=JST}^{M2} (AIP)$$

$$BLM = \sum_{j=JST}^{M2} (AIM)$$

$$BLC = \sum_{j=JST}^{M2} CON + \sum_{j=JST}^{M2} (AJP)\phi_{i,j+1}^* + \sum_{j=JST}^{M2} (AJM)\phi_{i,j-1}^* + \sum_{j=JST}^{M2} (AIP)\phi_{i+1,j}^* + \sum_{j=JST}^{M2} (AIM)\phi_{i-1,j}^* - \sum_{j=JST}^{M2} (AP)\phi_{i,j}^*$$

$$A_i \bar{\phi}'_i = B_i \bar{\phi}'_{i+1} + C_i \bar{\phi}'_{i-1} + D_i$$

$$\bar{\phi}'_{i-1} = P_{i-1} \bar{\phi}'_i + Q_{i-1}$$

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}}; \quad Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}}$$

DENOM

**Coefficients
calculation**

**Elimination
(消元)**

!Ensure a meaningful correction

Back substitution
(回代)

BL=0. (Initial set up)

DO 13 II=IST,L2

I=IT1-II

BL=BL*PT(I)+QT(I)

DO 14 J=JST,M2

F(I,J,N)=F(I,J,N)+BL!

14 ENDDO

13 ENDDO

C

PT(JSTF)=0.

QT(JSTF)=0.

DO 21 J=JST,M2

BL=0.

BLP=0.

BLM=0.

BLC=0.

DO 22 I=IST,L2

BL=BL+AP(I,J)

IF(I /= L2) BL=BL-AIP(I,J)

IF(I /= IST) BL=BL-AIM(I,J)

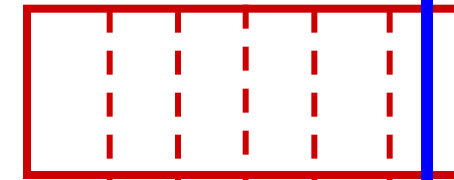
BLP=BLP+AJP(I,J)

IT1=L2+IST

I=IT1-II=L2+IST-IST=L2-Begin

I=IT1-II=L2+IST-L2=IST-End

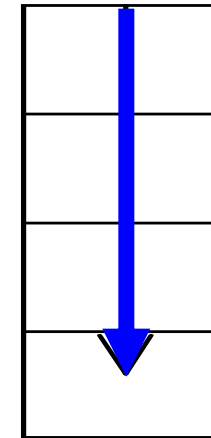
Correcting by BL for the same column



$$T_{i-1} = P_{i-1} T_i + Q_{i-1}$$

BL=BL*PT(I)+QT(I)

TDMA: from L2 to IST



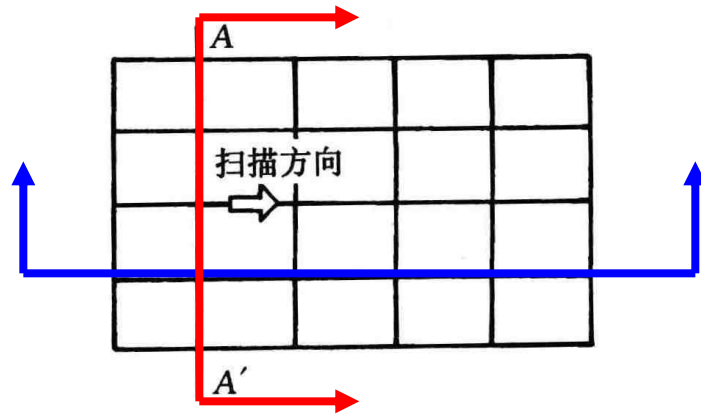
$$(BL)\bar{\phi}_j = (BLP)\bar{\phi}_{j+1} + (BLM)\bar{\phi}_{j-1} + BLC, J = JST, \dots, M2$$

Y-direction
B-correction


```
BLM=BLM+AJM(I,J)
BLC=BLC+CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)
& +AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)-AP(I,J)*F(I,J,N)
22 ENDDO
DENOM=BL-PT(J-1)*BLM
IF(ABS(DENOM/BL)<1.E-10) DENOM=1.E25
PT(J)=BLP/DENOM !
QT(J)=(BLC+BLM*QT(J-1))/DENOM
21 ENDDO
BL=0.
DO 23 JJ=JST,M2
J=JT1-JJ
BL=BL*PT(J)+QT(J)
DO 24 I=IST,L2
F(I,J,N)=F(I,J,N)+BL !Correcting by BL for the same block
24 ENDDO
23 ENDDO
10 ENDIF
```

! Above is block correction, following is AD line iteration

line iteration:



Alternative direction iteration (ADI)

Solving in I-direction, scanning in J direction

$$a_P T_P^{(k+1)} = a_E T_E^{(k+1)} + a_W T_W^{(k+1)} + \underbrace{[a_N T_N^{(k)} + a_S T_S^{(k)} + b]}_{! b'}$$

At the same line, TDMA is used for direct solution, from line to line, iterative method is used.

$$A_i \bar{\phi}_i = B \bar{\phi}_{i+1} + C_i \bar{\phi}_{i-1} + D_i, i = 1, 2, \dots, M1$$

Solving in I-direction, scanning in J direction, from bottom to top

C

DO 90 J=JST,M2 $AP\phi_{i,j}^n = AIP\phi_{i+1,j}^n + AIM\phi_{i-1,j}^n + b + AJP\phi_{i,j+1}^{n-1} + AJM\phi_{i,j-1}^{n-1}; i = IST...L2$

PT(ISTF)=0. ! PT=0, QT=given boundary value, 1st kind boundary condition

QT(ISTF)=F(ISTF,J,N)

DO 70 I=IST,L2

DENOM=AP(I,J)-PT(I-1)*AIM(I,J)

PT(I)=AIP(I,J)/DENOM

TEMP=CON(I,J)+AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)

QT(I)=(TEMP+AIM(I,J)*QT(I-1))/DENOM

70 ENDDO

DO 80 II=IST,L2

I=IT1-II !Recursive

F(I,J,N)=F(I+1,J,N)*PT(I)+QT(I)

80 ENDDO

90 ENDDO

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}};$$

$$Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}};$$

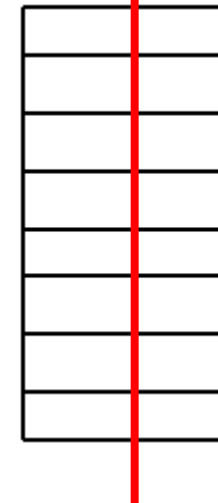
$$T_{i-1} = P_{i-1} T_i + Q_{i-1}$$

$$b + AJP\phi_{i,j+1}^{n-1} + AJM\phi_{i,j-1}^{n-1}$$

Elimination
(消元)

Back substitution
(回代)

Scanning direction



C

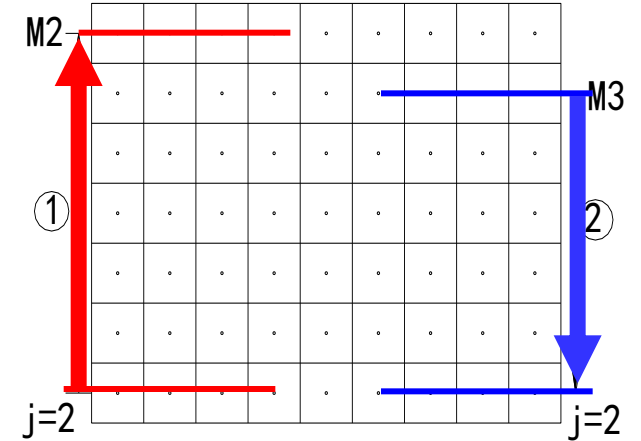
DO 190 JJ=JST,M3 ! Solving in I-direction, scanning from top to bottom

J=JT2-JJ !Starting from M3 ,rather than from M2

PT(ISTF)=0.

QT(ISTF)=F(ISTF,J,N)

} For executing 1st kind B.C.



Elimination
(消元)

DO 170 I=IST,L2

DENOM=AP(I,J)-PT(I-1)*AIM(I,J)

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}};$$

PT(I)=AIP(I,J)/DENOM

TEMP=CON(I,J)+AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)

QT(I)=(TEMP+AIM(I,J)*QT(I-1))/DENOM

$$b + AJP \phi_{i,j+1}^{n-1} + AJM \phi_{i,j-1}^{n-1}$$

170 ENDDO

$$Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}};$$

Back substitution
(回代)

DO 180 II=IST,L2

I=IT1-II !Recursive solution

F(I,J,N)=F(I+1,J,N)*PT(I)+QT(I)

180 ENDDO

190 ENDDO

C

C-----

```
DO 290 I=IST,L2 ! Solving in J-direction, scanning from left to right
DO 270 J=JST,M2
DENOM=AP(I,J)-PT(J-1)*AJM(I,J)
PT(J)=AJP(I,J)/DENOM
TEMP=CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)
QT(J)=(TEMP+AJM(I,J)*QT(J-1))/DENOM !
270 ENDDO
DO 280 JJ=JST,M2
J=JT1-JJ !Recursive solution
F(I,J,N)=F(I,J+1,N)*PT(J)+QT(J)
280 ENDDO
290 ENDDO
```

C-----

C

DO 390 II=IST,L3 ! Solving in J-direction, scanning from right to left

I=IT2-II

PT(JSTF)=0.

QT(JSTF)=F(I,JSTF,N)

DO 370 J=JST,M2

DENOM=AP(I,J)-PT(J-1)*AJM(I,J)

PT(J)=AJP(I,J)/DENOM ,

TEMP=CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)

QT(J)=(TEMP+AJM(I,J)*QT(J-1))/DENOM

370 ENDDO

DO 380 JJ=JST,M2

J=JT1-JJ !Recursive solution

F(I,J,N)=F(I,J+1,N)*PT(J)+QT(J)

380 ENDDO

390 ENDDO

C*****

C*****

999 ENDDO ! (End of solution of ABEqs)

ENTRY RESET ! (CON, AP are accumulatively used, should be reset)

DO 400 J=2,M2

DO 401 I=2,L2

CON(I,J)=0. S_c or b

AP(I,J)=0. S_p or a_p

401 ENDDO

400 ENDDO

RETURN

END

CC

10.6.2.5 SUBROUTINE SETUP

CC

SUBROUTINE SETUP

C*****

USE START_L

IMPLICIT NONE

INTEGRER*4 I, J, K, N

REAL*8 REL, FL, FLM, FLP, GM, GMM, VOL, APT, AREA, SXT,
1 SXB, ARHO

C*****

1 FORMAT(//15X,'COMPUTATION IN CARTESIAN COORDINATES')

! Print out title for Cartesian coordinate

2 FORMAT(//15X,'COMPUTATION FOR AXISYMMETRIC SITUATION')

! Print out title for cylindrical coordinate

3 FORMAT(//15X,'COMPUTATION IN POLAR COORDINATES')

! Print out title for polar coordinate ^

4 FORMAT(14X,40(1H*),//)

C-----

Structure of SETUP

(6)-Explained
in detail

S
E
T
U
P

ENTRY SETUP1

Setup 28 one dimensional geometric parameters;
Setup initial values

RETURN

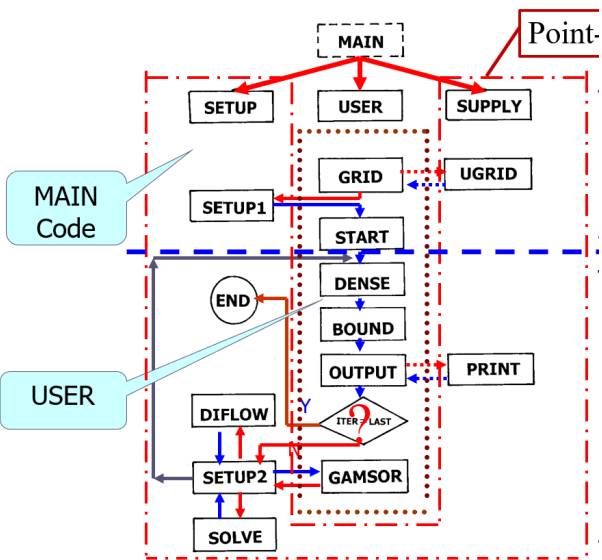
$$a_e u_e = \sum a_{nb} u_{nb} + b + A_e (p_P - p_E)$$

ENTRY SETUP2

Coefficient for u equation
Coefficient for v equation
Calculate UHAT and VHAT
Coefficient for pressure equation and solve pressure
Solve u equation and v equation.
Coefficient for pressure correction equation and solve it.
Correction velocity
Coefficient for other equation and solve it (from NF=4 to 10 in order)

RETURN

SIMPLER



MAIN Code

USER

C

ENTRY SETUP1 !Set up 1D arrays, not changed during iteration

NP=NFMAX+1 ! NFMAX=10, NP=11

NRHO=NP +1 ! NRHO=12

NGAM=NRHO+1 ! NGAM=13

NCP=NGAM+1 ! NCP=14

L2=L1-1 ! Set up L2,L3,M2,M3

L3=L2-1

M2=M1-1

M3=M2-1

X(1)=XU(2) ! X(1)=XU(2)=0

DO 5 I=2,L2

X(I)=0.5*(XU(I+1)+XU(I))

5 ENDDO

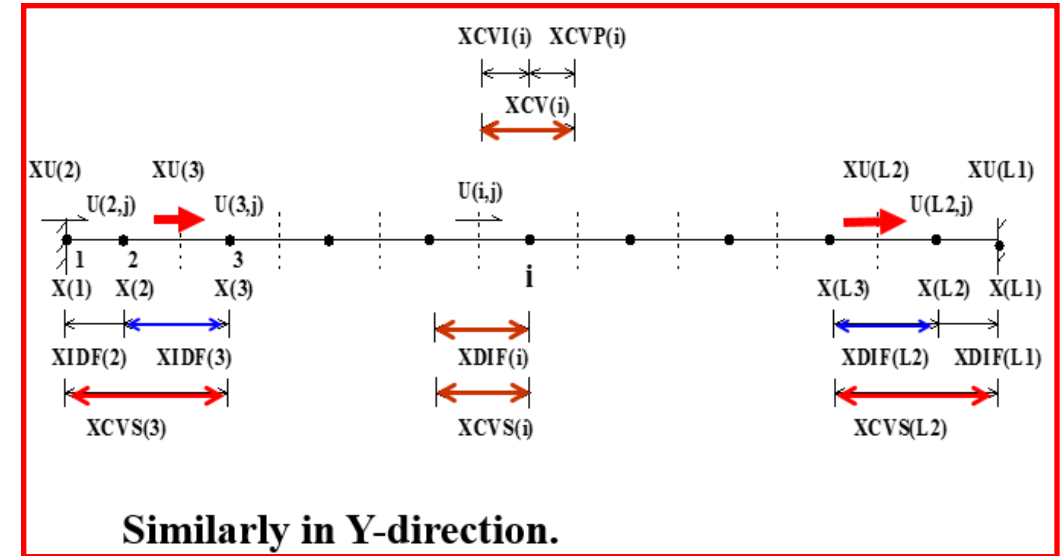
X(L1)=XU(L1)

Y(1)=YV(2) !Y(1)=YV(2)=0

DO 10 J=2,M2

Y(J)=0.5*(YV(J+1)+YV(J)) !Practice B

10 ENDDO

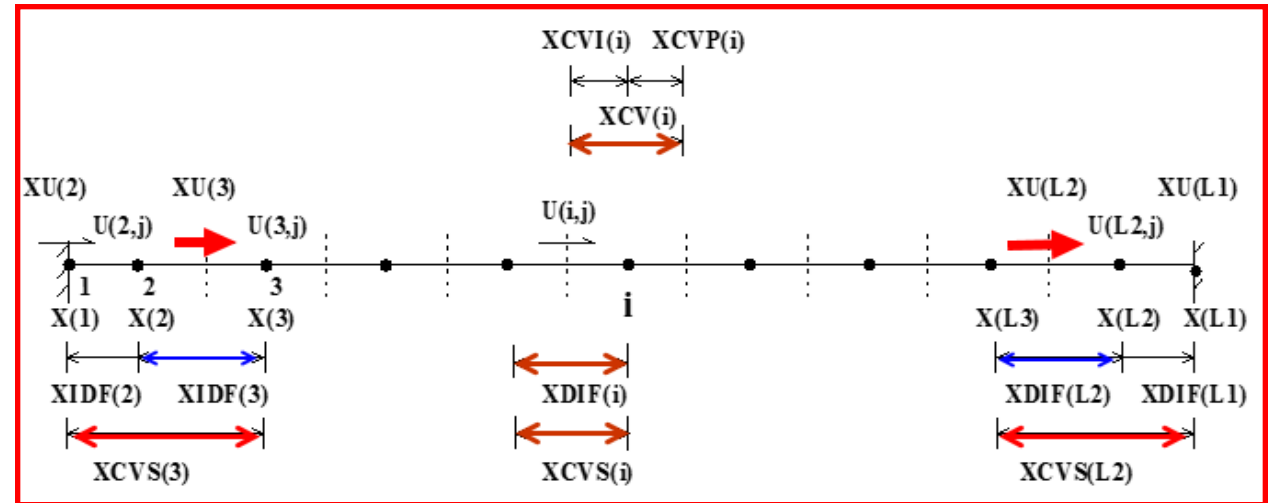


**! Practice B:
XU(I) has been
set in GRID**

```

Y(M1)=YV(M1)
DO 15 I=2,L1
XDIF(I)=X(I)-X(I-1)
15 ENDDO
DO 18 I=2,L2
XCV(I)=XU(I+1)-XU(I)
18 ENDDO
DO 20 I=3,L3

```



```

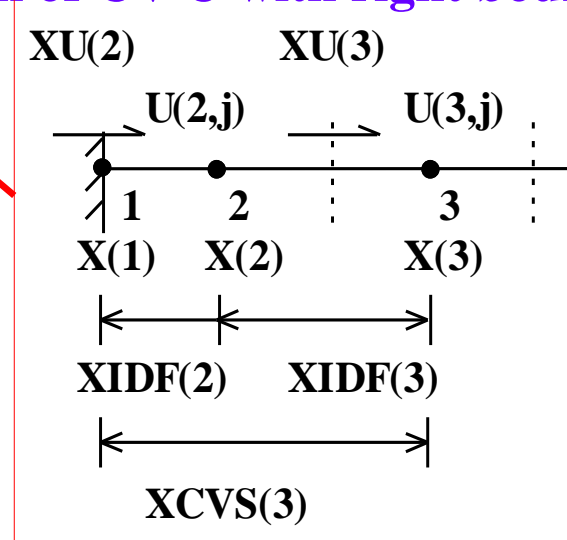
XCVS(I)=XDIF(I) ! Width of CV U (I,J) in x direction
20 ENDDO
XCVS(3)=XCVS(3)+XDIF(2) ! Width of CV U connected with left boundary
XCVS(L2)=XCVS(L2)+XDIF(L1) ! Width of CV U with right boundary

```

```

DO 22 I=3,L3
XCVI(I)=0.5*XCV(I) !  $(\delta x)_{e^-}$ 
XCVIP(I)=XCVI(I) !  $(\delta x)_{e^+}$ 
22 ENDDO

```



```

XCVIP(2)=XCV(2)
XCVI(L2)=XCV(L2)
DO 35 J=2,M1
YDIF(J)=Y(J)-Y(J-1)
35 ENDDO

```

(7a)---
Explained
in detail

```

DO 40 J=2,M2
YCV(J)=YV(J+1)-YV(J) !Width of main CV in y-direction
40 ENDDO
DO 45 J=3,M2
YCVS(J)=YDIF(J) ! Width of V (I,J) in y-direction
45 ENDDO
YCVS(3)=YCVS(3)+YDIF(2)
YCVS(M2)=YCVS(M2)+YDIF(M1)
IF(MODE= =1) THEN
DO 52 J=1,M1
RMN(J)=1.0 ! Nominal radius=1
R(J)=1.0 ! for Cartesian coordinate
52 ENDDO
ELSE
DO 50 J=2,M1 !Cylindrical and polar coordinates
R(J)=R(J-1)+YDIF(J) !R(1) has defined
50 ENDDO
RMN(2)=R(1)
DO 60 J=3,M2
60 RMN(J)=RMN(J-1)+YCV(J-1) ! Radius of position of V(I,J)
60 ENDDO
RMN(M1)=R(M1)
ENDIF

```

R = 1 for both nodes and interfaces in Cartesian coordinate

(7b)---
Explained
in detail

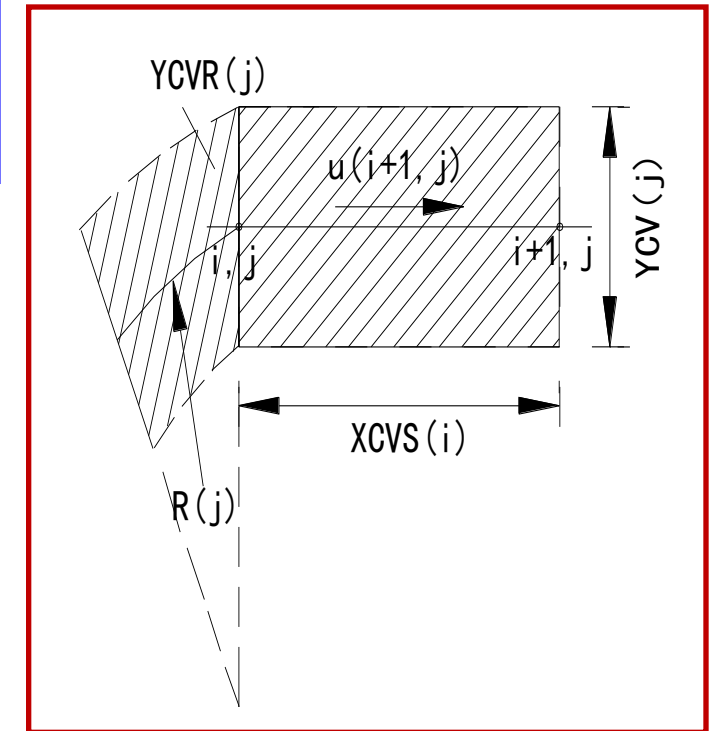
```

DO 57 J=1,M1
SX(J)=1.
SXMN(J)=1.
IF(MODE.== 3) THEN
SX(J)=R(J)
IF(J /= 1) SXMN(J)=RMN(J)
ENDIF
57 ENDDO
DO 62 J=2,M2
YCVR(J)=R(J)*YCV(J)
ARX(J)=YCVR(J)
IF(MODE = = 3) THEN
ARX(J)=YCV(J)
62 ENDDO
    
```

Set up scaling
Factor for polar
coordinate

Interface starts from J=2

!E-W conduction area of
CV for three cases, for
Cartesian R=1



DO 64 J=4,M3
 $YCVRS(J)=0.5*(R(J)+R(J-1))*YDIF(J)$ $ARXJ(J)=\frac{1}{2}(R(j)+RMN(j))\cdot\frac{YCV(j)}{2} =$

64 ENDDO

$YCVRS(3)=0.5*(R(3)+R(1))*YCVS(3)$ $0.25[1+\frac{RMN(j)}{R(j)}]\cdot R(j)\cdot YCV(j) =$
 $YCVRS(M2)=0.5*(R(M1)+R(M3))*YCVS(M2)$

(7c)---

Explained
in detail

IF(MODE == 2) THEN

DO 65 J=3,M3

$ARXJ(J)=0.25*(1+RMN(J)/R(J))*ARX(J)$

$ARXJP(J)=ARX(J)-ARXJ(J)$

65 ENDDO

ELSE

DO 66 J=3,M3

$ARXJ(J)=0.5*ARX(J)$

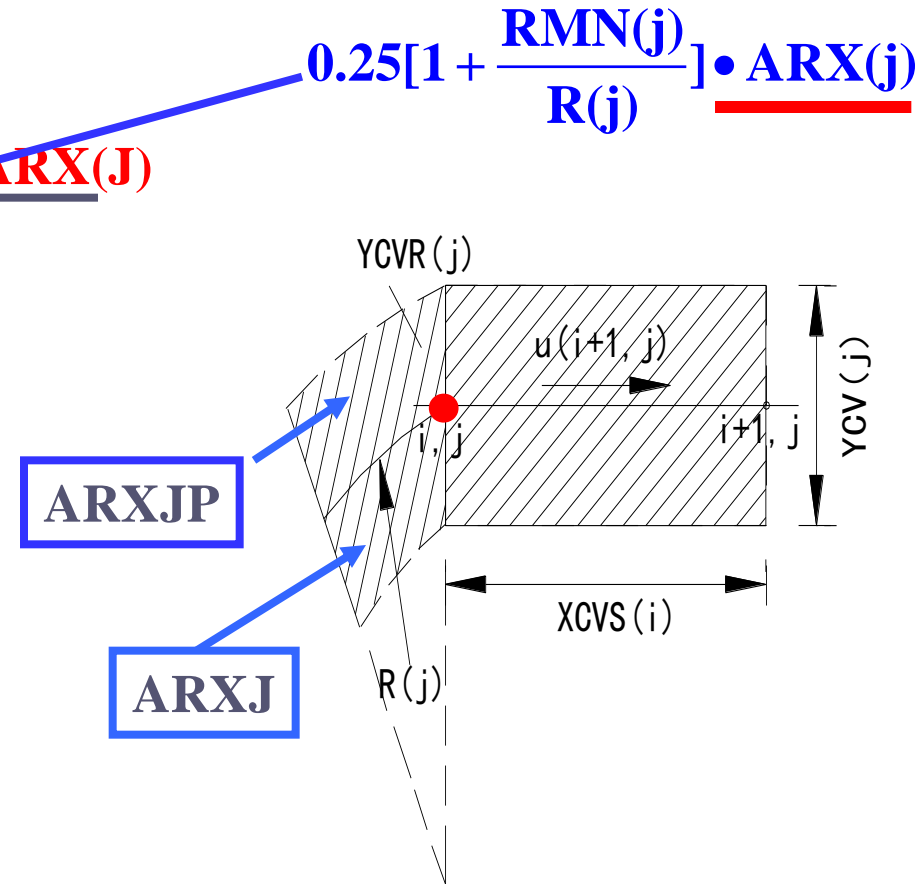
$ARXJP(J)=ARXJ(J)$

66 ENDDO

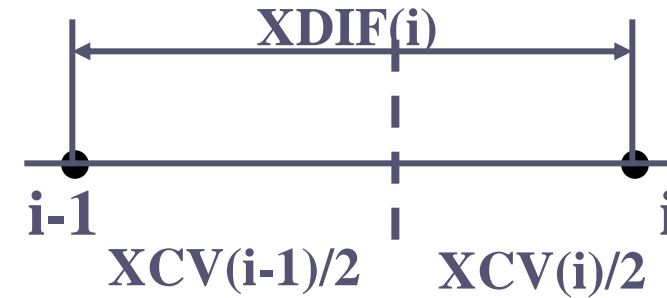
ENDIF

$ARXJP(2)=ARX(2)$

$ARXJ(M2)=ARX(M2)$



```
DO 70 J=3,M3
FV(J)=ARXJP(J)/ARX(J)
FVP(J)=1.-FV(J) !Interpolation coefficient
70 ENDDO
```



```
DO 85 I=3,L2
FX(I)=0.5*XCV(I-1)/XDIF(I) !Interpolation in x-direction
FXM(I)=1.-FX(I)
```

```
85 ENDDO
```

```
FX(2)=0.
FXM(2)=1.
FX(L1)=1.
FXM(L1)=0.
```

$$\begin{aligned} \phi_{i-1/2} &= \phi_{i-1} \frac{XCV(i)/2}{XDIF(i)} + \phi_i \frac{XCV(i-1)/2}{XDIF(i)} \\ &= \phi_{i-1} FXM(i) + \phi_i FX(i) \end{aligned}$$

```
DO 90 J=3,M2
FY(J)=0.5*YCV(J-1)/YDIF(J) ! Interpolation in y-direction
FYM(J)=1.-FY(J)
```

```
90 ENDDO
```

```
FYM(2)=1.
FY(M1)=1.
FYM(M1)=0.
```

The first letter C is also used to indicate that this is an explanation line

CGN,AP,U,V,RHO,PC AND P ARRAYS ARE INITIALIZED HERE

```
DO 96 J=1,M1
```

```
DO 95 I=1,L1
```

```
PC(I,J)=0.
```

```
U(I,J)=0.
```

```
V(I,J)=0.
```

```
CON(I,J)=0.
```

```
AP(I,J)=0.
```

```
RHO(I,J)=RHOCON
```

```
CP (I,J)=CPCON
```

```
P(I,J)=0.
```

```
95 ENDDO
```

```
96 ENDDO
```

```
IF(MODE= =1) PRINT 1
```

```
IF(MODE= =1) WRITE(8,1)
```

```
IF(MODE= =2) PRINT 2
```

```
IF(MODE= =2) WRITE(8,2)
```

```
IF(MODE= =3) PRINT 3
```

```
IF(MODE= =3) WRITE(8,3)
```

```
PRINT 4
```

```
WRITE(8,4)
```

```
RETURN
```

Set up initial fields for iteration

Print out coordinate title of output data

C-----

ENTRY SETUP2

CCC

COEFFICIENTS FOR THE U EQUATION

NF=1 !NF=1: U; NF=2: V; NF=3: P', P; NF=NP: P

IF(LSOLVE(NF)) THEN !

IST=3

JST=2

CALL GAMSOR

REL=1.-RELAX(NF) ! (U) under-relaxation

DO 102 I=3,L2 !Coefficient of south boundary

FL=XCVI(I)*V(I,2)*RHO(I,1)

FLM=XCVIP(I-1)*V(I-1,2)*RHO(I-1,1)

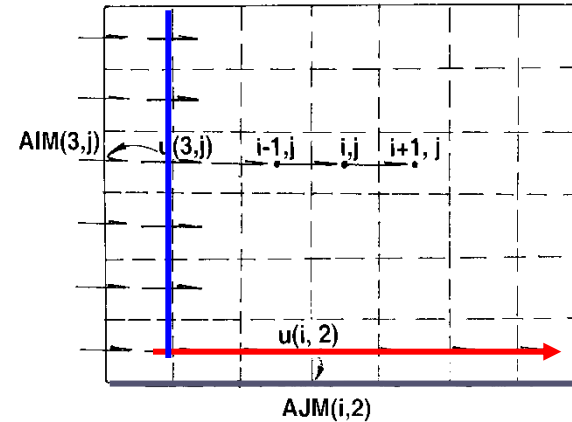
FLOW=R(1)*(FL+FLM) ! Flow rate through south interface

DIFF=R(1)*(XCVI(I)*GAM(I,1)+XCVIP(I-1)*GAM(I-1,1))/YDIF(2)

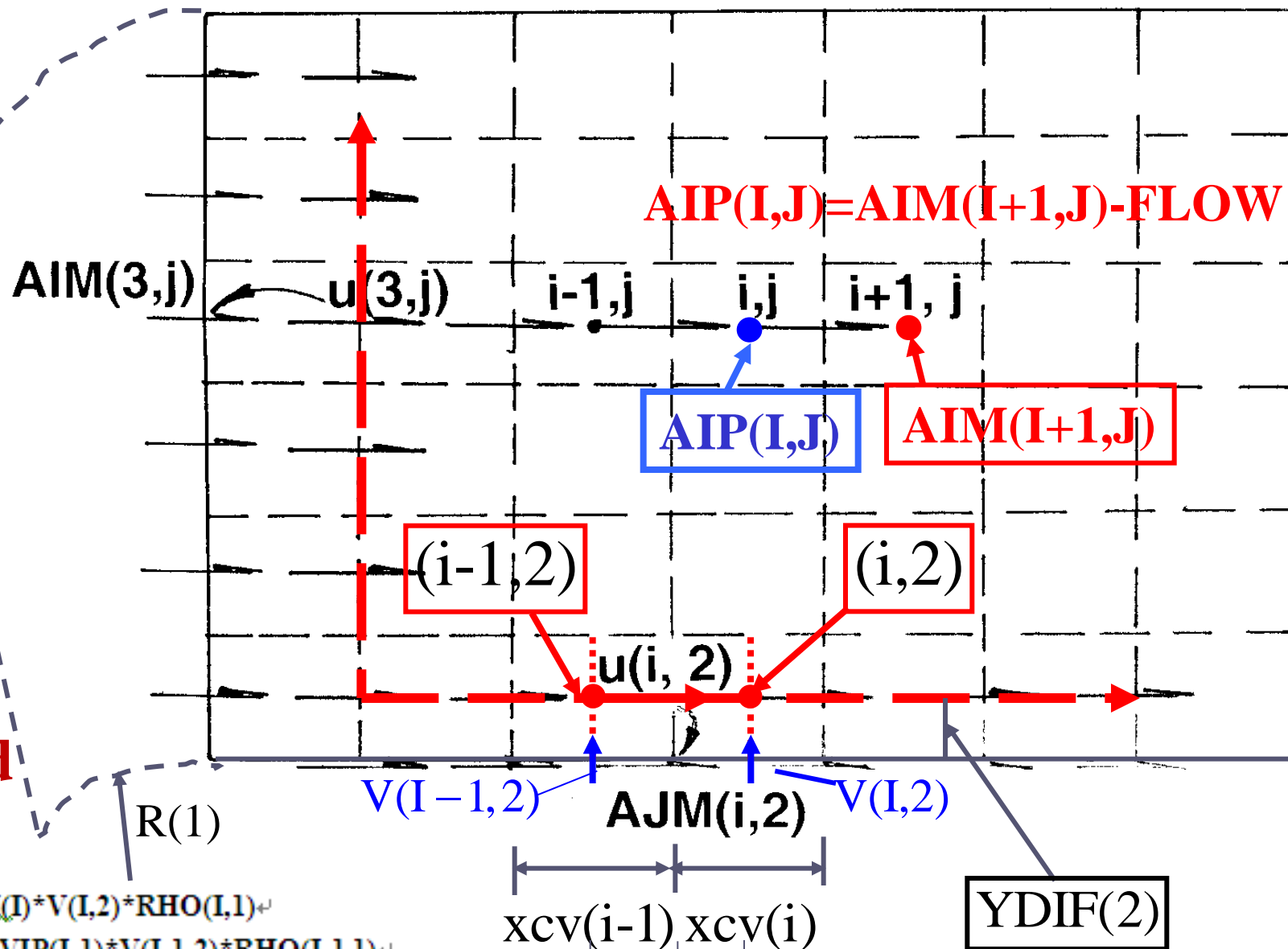
CALL DIFLOW !With DIFF and FLOW at hand, CALL DIFLOW to get D·A(|P|);

AJM(I,2)=ACOF+AMAX1(0.,FLOW) Coefficient a_s

102 ENDDO



$$a_s = D_s A(|P_\Delta|) + [0, -F_s]$$



(8)---Explained in detail

$$\begin{aligned}
 FL &= X_{CVI}(I) * V(I,2) * RHO(I,1) \leftarrow \\
 FLM &= X_{CVIP}(I-1) * V(I-1,2) * RHO(I-1,1) \leftarrow \\
 FLOW &= R(1) * (FL + FLM) \leftarrow \\
 \underline{DIFF} &= R(1) * (X_{CVI}(I) * GAM(I,1) + X_{CVIP}(I-1) * GAM(I-1,1)) / YDIF(2) \leftarrow
 \end{aligned}$$

```

DO 103 J=2,M2
FLOW=ARX(J)*U(2,J)*RHO(1,J)
DIFF=ARX(J)*GAM(1,J)/(XCV(2)*SX(J))
CALL DIFLOW      ! Get A(|P|)
AIM(3,J)=ACOF+AMAX1(0.,FLOW) !Coefficient  $a_w$ 
DO 104 I=3,L2
IF(I == L2) THEN
FLOW=ARX(J)*U(L1,J)*RHO(L1,J)
DIFF=ARX(J)*GAM(L1,J)/(XCV(L2)*SX(J)) ! DW
ELSE
FL=U(I,J)*(FX(I)*RHO(I,J)+FXM(I)*RHO(I-1,J))
FLP=U(I+1,J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
FLOW=ARX(J)*0.5*(FL+FLP)
DIFF=ARX(J)*GAM(I,J)/(XCV(I)*SX(J))
ENDIF
CALL DIFLOW ! A(|P|)
AIM(I+1,J)=ACOF+AMAX1(0.,FLOW)  $D \cdot A(|P_\Delta|) + 0, F$ 
AIP(I,J)=AIM(I+1,J)-FLOW ! Relationship between coefficients
    
```

```

IF(J = = M2) THEN
FL=XCVI(I)*V(I,M1)*RHO(I,M1)
FLM=XCVIP(I-1)*V(I-1,M1)*RHO(I-1,M1)
DIFF=R(M1)*(XCVI(I)*GAM(I,M1)+XCVIP(I-1)*GAM(I-1,M1))/YDIF(M1)
ELSE
FL=XCVI(I)*V(I,J+1)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))
FLM=XCVIP(I-1)*V(I-1,J+1)*(FY(J+1)*RHO(I-1,J+1)+FYM(J+1)*
& RHO(I-1,J))
GM=GAM(I,J)*GAM(I,J+1)/(YCV(J)*GAM(I,J+1)+YCV(J+1)*GAM(I,J)+
& 1.0E-30)*XCVI(I)
GMM=GAM(I-1,J)*GAM(I-1,J+1)/(YCV(J)*GAM(I-1,J+1)+YCV(J+1)*
& GAM(I-1,J)+1.E-30)*XCVIP(I-1)
DIFF=RMN(J+1)*2.*(GM+GMM)
ENDIF
FLOW=RMN(J+1)*(FL+FLM)
CALL DIFLOW ! A(|P|)
AJM(I,J+1)=ACOF+AMAX1(0.,FLOW) ! Coefficient  $a_s$ 
AJP(I,J)=AJM(I,J+1)-FLOW ! Relationship between coefficients
    
```

(9)---
Explained
in detail

VOL=YCVR(J)*XCVS(I) !Volume of velocity CV
APT=(RHO(I,J)*XCVI(I)+RHO(I-1,J)*XCVIP(I-1))
&/((XCVS(I)*DT) ! Unsteady term $\rho/\Delta t$; DT--- Δt ;
AP(I,J)=AP(I,J)-APT ! AP (I,J) at right side is S_p
CON(I,J)=CON(I,J)+APT*U(I,J)
AP(I,J)=(-AP(I,J)*VOL+AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J))
&/RELAX(NF) !Underrelaxation is organized during solution procedure
CON(I,J)=CON(I,J)*VOL+REL*AP(I,J)*U(I,J) ! REL=1 - α
DU(I,J)=VOL/(XDIF(I)*SX(J)) ! To get flow area
DU(I,J)=DU(I,J)/AP(I,J) ! d_e in velocity correction

$$a_p^0 = \frac{\rho_P \Delta V}{\Delta t}$$

$$! d_e = A_e / a_e$$

104 ENDDO

103 ENDDO

! Come here we have finished the coefficients calculation for u velocity and should store them temporary to leave COF empty to calculate coefficients for velocity v .

$$b = S_c \Delta V + a_p^0 \phi_p^0 + (1 - \alpha) \frac{a_p}{\alpha} \phi_p^0$$

$$a_p = \left(\sum a_{nb} + \rho_P \Delta V / \Delta t - S_p \Delta V \right) / \alpha$$

-----Review of SIMPLER algorithm-----

1. Assuming initial fields, determine coefficients of discretized u, v eqs.;
2. Calculating pseudo-velocity u, \tilde{v} ;

(10)---Explained in detail

$$a_e u_e = \sum a_{nb} u_{nb} + b + A_e (p_P - p_E)$$

$$u_e = \sum \frac{a_{nb} u_{nb} + b}{a_e} + \frac{A_e}{a_e} (p_P - p_E) \quad \longrightarrow$$

$$u_e = \tilde{u}_e + \frac{A_e}{a_e} (p_P - p_E)$$

and **Solving pressure equation**, obtaining p^* ;

$$a_P p_P = a_E p_E + a_W p_W + a_N p_N + a_S p_S + b$$

$$a_P = a_E + a_W + a_N + a_S$$

$$a_E = d_e A_e \rho_e \quad a_W = d_w A_w \rho_w \quad a_n = d_n A_n \rho_n \quad a_S = d_s A_s \rho_s$$

$$b = [(\rho u)_w - (\rho u)_s] A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n] A_n$$

Coefficients of u, v momentum equations are needed for determining coefficients of pressure equation. $d_e = \frac{A_e}{a_e}$

3. Solving **momentum equations** based on p^* ,
 obtaining u^*, v^*

$$a_e u_e = \sum a_{nb} u_{nb} + b + A_e (p_P - p_E)$$

4. Solving **pressure correction equation** based on u^*, v^* ,
 obtaining p'

In pressure equation: $b = [(\rho u)_w - (\rho u)_s] A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n] A_n$

In pressure correction equation: $b = [(\rho u^*)_w - (\rho u^*)_s] A_e + [(\rho v^*)_s - (\rho v^*)_n] A_n$

5. Correcting velocity $u = u^* + u'$; $v = v^* + v'$, where u' and v' are determined based on p'

$$u'_e = \frac{A_e}{a_e} (p'_P - p'_E) = d_e (p'_P - p'_E)$$

6. Taking the updated velocity , repeating steps 1-6, until convergence is reached.

-----End of Review of SIMPLER algorithm-----

MODULE START_L

PARAMETER (NI=100,NJ=200,NIJ=NI,NFMAX=10,NFX4=NFMAX+4)

C*****

CHARACTER*8 TITLE(NFX4)

LOGICAL LSOLVE(NFX4),LPRINT(NFX4),LBLK(NFX4),LSTOP

REAL*8,DIMENSION(NI,NJ,NFX4)::F

REAL*8,DIMENSION(NI,NJ,6)::COF,COFU,COFV,COFP

REAL*8,DIMENSION(NI,NJ)::P,RHO,GAM,CP,CON,AIP,AIM,AJP,AJM,AP

C*****

EQUIVALENCE(F(1,1,1),U(1,1)),(F(1,1,2),V(1,1)),(F(1,1,3),PC(1,1))
1, (F(1,1,4),T(1,1))

EQUIVALENCE(F(1,1,11),P(1,1)),(F(1,1,12),RHO(1,1)),(F(1,1,13))
1,GAM(1,1),(F(1,1,14),CP(1,1))

EQUIVALENCE(COF(1,1,1),CON(1,1)),(COF(1,1,2),AIP(1,1)),
1(COF(1,1,3),AIM(1,1)),(COF(1,1,4),AJP(1,1)),
2(COF(1,1,5),AJM(1,1)),(COF(1,1,6),AP(1,1))

REAL*8,DIMENSION(NI)::TH,THU,THDIF,THCV,THCVS

REAL*8 THL

EQUIVALENCE(X,TH),(XU,THU),(XDIF,THDIF),(XCV,THCV),
1(XCVS,THCVS),(XL,THL)

DATA LSTOP,LSOLVE,LPRINT/.FALSE.,NFX4*.FALSE., NFX4*.FALSE./

DATA LBLK/NFX4*.TRUE./

DATA MODE,LAST,TIME,ITER/1,5,0.,0/

DATA RELAX,NTIMES/NFX4*1.,NFX4*1/

DATA DT,IPREF,JPREF,RHOCON,CPCON/1.E+30, 1,1,1.,1./

END MODULE

COFU(IST:L2, JST:M2, 1:6)=COF(IST:L2,JST:M2,1:6) ! Transfer the coefficients

! Store coefficients of U temporary as follows:

COF(I,J,1)	COF(I,J,2)	COF(I,J,3)	COF(I,J,4)	COF(I,J,5)	COF(I,J,6)
CON (I,J)	AIP(I,J)	AIM(I,J)	AJP(I,J)	AJM(I,J)	AP(I,J)

Explain

! In SIMPLER to solve pressure eq., coefficients of both u -eq. and v -eq. are needed. Only u -coefficients are not enough. Thus, u -coefficients are temporary stored, and v -eq. coefficients are computed by using array **COF(I,J)**

COEFFICIENTS FOR THE V EQUATION- (Determine coefficients of V)

NF=2 !

CALL RESET !Set zero values for AP(I,J),CON(I,J)

IST=2

JST=3

CALL GAMSOR

REL=1.-RELAX(NF)

**(11)---Explained
in detail**

```

DO 202 I=2,L2
AREA=R(1)*XCV(I)
FLOW=AREA*V(I,2)*RHO(I,1)
DIFF=AREA*GAM(I,1)/YCV(2)
CALL DIFLOW
AJM(I,3)=ACOF+AMAX1(0.,FLOW) !  $a_s$ 

```

202 ENDO

```

DO 203 J=3,M2
FL=ARXJ(J)*U(2,J)*RHO(1,J)
FLM=ARXJP(J-1)*U(2,J-1)*RHO(1,J-1)
FLOW=FL+FLM
DIFF=(ARXJ(J)*GAM(1,J)+ARXJP(J-1)*GAM(1,J-1))/(XDIF(2)*SXMN(J))
CALL DIFLOW

```

```

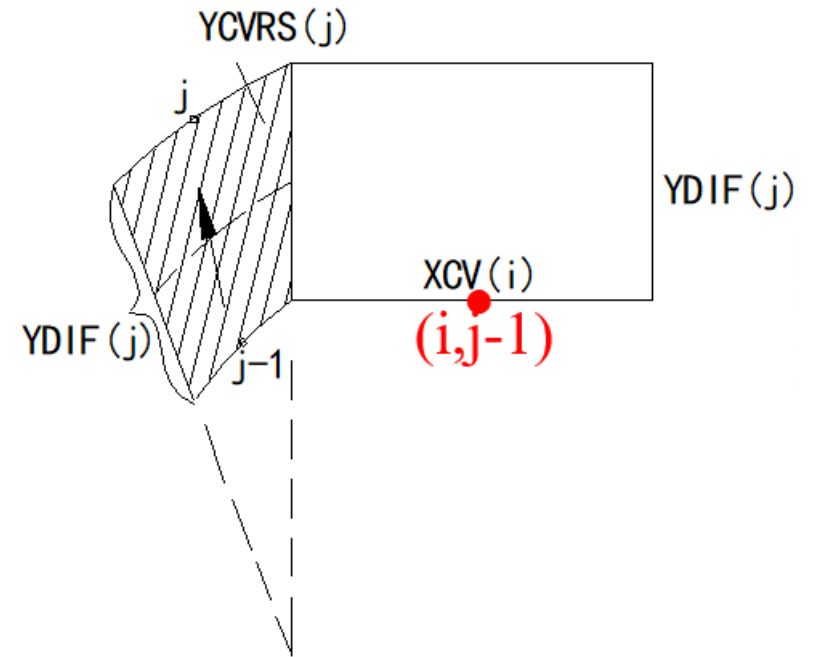
AIM(2,J)=ACOF+AMAX1(0.,FLOW) !  $a_w$ 

```

```

DO 204 I=2,L2
IF(I= L2) THEN
FL=ARXJ(J)*U(L1,J)*RHO(L1,J)
FLM=ARXJP(J-1)*U(L1,J-1)*RHO(L1,J-1)
DIFF=(ARXJ(J)*GAM(L1,J)+ARXJP(J-1)*GAM(L1,J-
& -1))/(XDIF(L1)*SXMN(J))

```



```
ELSE
FL=ARXJ(J)*U(I+1,J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
FLM=ARXJP(J-1)*U(I+1,J-1)*(FX(I+1)*RHO(I+1,J-1)+FXM(I+1)*RHO(I,J-1))
GM=GAM(I,J)*GAM(I+1,J)/(XCV(I)*GAM(I+1,J)+XCV(I+1)*GAM(I,J)+
& 1.E-30)*ARXJ(J)
GMM=GAM(I,J-1)*GAM(I+1,J-1)/(XCV(I)*GAM(I+1,J-1)+XCV(I+1)*
& GAM(I,J-1)+1.0E-30)*ARXJP(J-1)
DIFF=2.*(GM+GMM)/SXMN(J)
ENDIF
FLOW=FL+FLM
CALL DIFLOW
AIM(I+1,J)=ACOF+AMAX1(0.,FLOW) ! aw
AIP(I,J)=AIM(I+1,J)-FLOW ! Relationship between coefficients
IF (J= =M2) THEN
AREA=R(M1)*XCV(I)
FLOW=AREA*V(I,M1)*RHO(I,M1)
```

```
DIFF=AREA*GAM(I,M1)/YCV(M2)
ELSE
AREA=R(J)*XCV(I)
FL=V(I,J)*(FY(J)*RHO(I,J)+FYM(J)*RHO(I,J-1))*RMN(J)
FLP=V(I,J+1)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))*RMN(J+1)
FLOW=(FV(J)*FL+FVP(J)*FLP)*XCV(I)
DIFF=AREA*GAM(I,J)/YCV(J)
ENDIF
CALL DIFLOW
AJM(I,J+1)=ACOF+AMAX1(0.,FLOW) ! as
AJP(I,J)=AJM(I,J+1)-FLOW !Relationship
VOL=YCVRS(J)*XCV(I) !Volume of V- CV
SXT=SX(J)
```

```

    APT=(ARXJ(J)*RHO(I,J)*0.5*(SXT+SXMN(J))+ARXJP(J-1)*RHO(I,J-1)*
    &0.5*(SXB+SXMN(J)))/(YCVRS(J)*DT)
    AP(I,J)=AP(I,J)-APT
    CON(I,J)=CON(I,J)+APT*V(I,J)
    AP(I,J)=(-AP(I,J)*VOL+AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J))
    &/RELAX(NF)
    CON(I,J)=CON(I,J)*VOL+REL*AP(I,J)*V(I,J)
    DV(I,J)=VOL/YDIF(J)
    DV(I,J)=DV(I,J)/AP(I,J)
    
```

204 ENDDO

203 ENDDO

COFV(IST:L2,JST:M2,1:6)=COF(IST:L2,JST:M2,1,6)

! Store coefficients of V-eq. to compute coefficients of P-equation

CALCULATE UHAT AND VHAT !

DO 150 J=2,M2

DO 151 I=3,L2

UHAT(I,J)=(COFU(I,J,2)*U(I+1,J)+COFU(I,J,3)*U(I-1,J)+COFU(I,J,4)

& *U(I,J+1)+COFU(I,J,5)*U(I,J-1)+COFU(I,J,1))/COFU(I,J,6)

! Compute u, \tilde{v}

$$u_e = \sum \frac{a_{nb} u_{nb} + b}{a_e}$$

```

151 ENDDO
150 ENDDO
    DO 250 J=3,M2
    DO 251 I=2,L2
    VHAT(I,J)=(COFV(I,J,2)*V(I+1,J)+COFV(I,J,3)*V(I-1,J)+COFV(I,J,4)
    & *V(I,J+1)+COFV(I,J,5)*V(I,J-1)+COFV(I,J,1))/COFV(I,J,6)
251 ENDDO
250 ENDDO
    
```

COEFFICIENTS FOR THE PRESSURE EQUATION-----

```

NF=3
CALL RESET
IST=2
JST=2
CALL GAMSOR
DO 410 J=2,M2,
DO 411 I=2,L2
VOL=YCVR(J)*XCV(I)
CON(I,J)=CON(I,J)*VOL
411 ENDDO
410 ENDDO
    
```

!In the discretized pressure equation, the source term is

$$! b = [(\rho u)_w - (\rho u)_e]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$$
!This term has to be computed for every interface of a CV!

!Volume of main CV.
!Pressure has no inherent source term, here setting this
!operation just for general purpose .Usually CON(I,J)=0

! For boundary CV, actual velocity is used.

**(12)
Explained
in detail**

DO 402 I=2,L2

ARHO=R(1)*XCV(I)*RHO(I,1)

累加 ! $b = [(\rho u)_w - (\rho u)_e]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$

CON(I,2)=CON(I,2)+ARHO*V(I,2) ! Accumulative add

AJM(I,2)=0 ! $a_s = 0$, Adiabatic boundary

402 ENDDO

DO 403 J=2,M2

ARHO=ARX(J)*RHO(1,J)

CON(2,J)=CON(2,J)+ARHO*U(2,J) ! Accumulative addition

AIM(2,J)=0. ! $a_w = 0$, Adiabatic boundary

DO 404 I=2,L2

IF(I= =L2) THEN **! For boundary CV, actual velocity is used.**

ARHO=ARX(J)*RHO(L1,J)

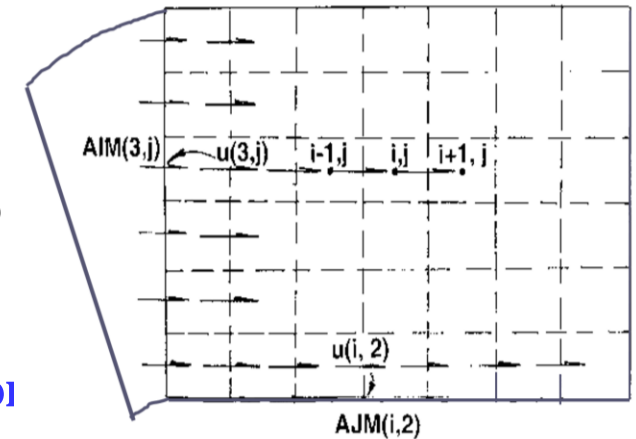
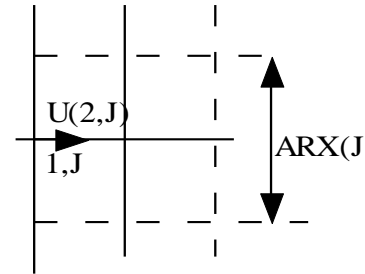
CON(I,J)=CON(I,J)-ARHO*U(L1,J) ! Accumulative addition

AIP(I,J)=0. ! $a_E = 0$

! $b = [(\rho u)_w - (\rho u)_e]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$

ELSE

ARHO=ARX(J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))



FLOW=ARHO*UHAT(I+1,J) ! For inner CV, UHAT is used.

CON(I,J)=CON(I,J)-FLOW

CON(I+1,J)=CON(I+1,J)+FLOW !

AIP(I,J)=ARHO*DU(I+1,J) ! a_E

AIM(I+1,J)=AIP(I,J) ! Relationship between (a_w) and $(a_E)_{i+1}$

ENDIF

IF(J= =M2) THEN

ARHO=RMN(M1)*XCV(I)*RHO(I,M1)

CON(I,J)=CON(I,J)-ARHO*V(I,M1) ! Accumulative addition

AJP(I,J)=0. ! North coefficient of M2

ELSE

ARHO=RMN(J+1)*XCV(I)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))

FLOW=ARHO*VHAT(I,J+1) ! For inner CV, VHAT is used.

CON(I,J)=CON(I,J)-FLOW

CON(I,J+1)=CON(I,J+1)+FLOW

AJP(I,J)=ARHO*DV(I,J+1)

AJM(I,J+1)=AJP(I,J) ! Relationship between coefficients

ENDIF

```
AP(I,J)=AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J)
404 ENDDO
403 ENDDO
DO 421 J=2,M2
DO 422 I=2,L2
AP(I,J)=AP(I,J)/RELAX(NP) ! Pressure underrelaxation
CON(I,J)=CON(I,J)+(1.0-RELAX(NP))*AP(I,J)*P(I,J)
422 ENDDO
421 ENDDO
COFP(IST:L2,JST:M2,2:5)=COF(IST:L2,JST:M2,2:5)
```

(13)

Explained
in detail

! Store a_E, a_W, a_N, a_S for p -correction equation

! while CON (b) and AP (a_p) are not stored; Because AP has been
! underrelaxed, and the velocity in b term of p -correction eq. is different.

NF=NP !NFMAX+1; P(I,J) is one member of F(I,J,NF)

CALL **SOLVE** ! Solving P-equation

COMPUTE U AND V! Pressure has been solved

NF=1

IST=3

JST=2

COF(IST:L2,JST:M2,1:6)=COFU(IST:L2,JST:M2,1:6) ! Coefficients of U

DO 551 J=JST,M2

DO 552 I=IST,L2

CON(I,J)=CON(I,J)+DU(I,J)*AP(I,J)*(P(I-1,J)-P(I,J))

522 ENDDO

521 ENDDO

CALL **SOLVE** !Solving U equation

C-----

NF=2

IST=2

JST=3

COF(IST:L2,JST:M2,1:6)=COFV(IST:L2,JST:M2,1:6) !Coefficients of V

DO 553 J=JST,M2

DO 554 I=IST,L2

CON(I,J)=CON(I,J)+DV(I,J)*AP(I,J)*(P(I,J-1)-P(I,J))

```
CON(I,J)=CON(I,J)+DV(I,J)*AP(I,J)*(P(I,J-1)-P(I,J))
554 ENDDO
553 ENDDO
```

CALL **SOLVE** ! Solving V-equation. Such U V do not satisfy mass
! conservation, need to be improved

COEFFICIENTS FOR THE PRESSURE CORRECTION EQUATION

```
NF=3 ! P-correction equation
CALL RESET ! Zero of CON(I,j) and AP(i,j)
IST=2
JST=2
COF(IST:L2,JST:M2,2:5)=COFP(IST:L2,JST:M2,2:5)
! Transfer coefficients of P-eq. to P-correction equation.
CALL GAMSOR
SMAX=0.
SSUM=0.
```

$$! b = [(\rho u^*)_w - (\rho u^*)_e]A_e + [(\rho v^*)_s - (\rho v^*)_n]A_n$$

! The velocities just solved are u^* and v^*

```

DO 510 J=2,M2
DO 511 I=2,L2
VOL=YCVR(J)*XCV(I)      ! Volume of PCV
CON(I,J)=CON(I,J)*VOL
511 ENDDO
510 ENDDO                !  $b = [(\rho u^*)_w - (\rho u^*)_e]A_e + [(\rho v^*)_s - (\rho v^*)_n]A_n$ 
DO 502 I=2,L2
ARHO=R(1)*XCV(I)*RHO(I,1)
CON(I,2)=CON(I,2)+ARHO*V(I,2) ! Source term b
502 ENDDO
DO 503 J=2,M2
ARHO=ARX(J)*RHO(1,J)
CON(2,J)=CON(2,J)+ARHO*U(2,J)
DO 504 I=2,L2
IF(I= =L2) THEN
ARHO=ARX(J)*RHO(L1,J)
CON(I,J)=CON(I,J)-ARHO*U(L1,J) ! Calculate b-term
ELSE
ARHO=ARX(J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
FLOW=ARHO*U(I+1,J) ! Adopt U*,V* to solve P'
CON(I,J)=CON(I,J)-FLOW
CON(I+1,J)=CON(I+1,J)+FLOW
    
```

Do loop
502—
504 for
mass
source
of each
CV

```
ENDIF
IF(J= =M2) THEN
ARHO=RMN(M1)*XCV(I)*RHO(I,M1)
CON(I,J)=CON(I,J)-ARHO*V(I,M1)
ELSE
ARHO=RMN(J+1)*XCV(I)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))
FLOW=ARHO*V(I,J+1)
CON(I,J)=CON(I,J)-FLOW
CON(I,J+1)=CON(I,J+1)+FLOW
ENDIF
AP(I,J)=AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J) ← For AP
PC(I,J)=0. ! Initial field
SMAX=AMAX1(SMAX,ABS(CON(I,J))) ! Take the maximum
SSUM=SSUM+CON(I,J) ! Summation of b
504 ENDDO
503 ENDDO
CALL SOLVE ! Solving p-correction equation
```

COME HERE TO CORRECT THE VELOCITIES

```
DO 521 J=2,M2
DO 522 I=2,L2
IF(I/=2) U(I,J)=U(I,J)+DU(I,J)*(PC(I-1,J)-PC(I,J)) ! Correcting velocity u
IF(J/=2) V(I,J)=V(I,J)+DV(I,J)*(PC(I,J-1)-PC(I,J)) ! Correcting velocity v
522 ENDDO
521 ENDDO
500 ENDIF
```

COEFFICIENTS FOR OTHER EQUATIONS-----

```
IST=2
JST=2
DO 600 N=4,NFMAX !NF>=4
NF=N
IF(LSOLVE(NF)) THEN
CALL GAMSOR
IF(LSOLE(4)) THEN
DO I=1,L1
DO J=1,M1
RHO(I,J)=RHO(I,J)*CP(I,J) ! Nominal density for temperature
ENDDO
ENDDO
REL=1.-RELAX(NF)
```

$$\rho^* = \rho c_p$$

(14) Explain
in detail

```
DO 602 I=2,L2
AREA=R(1)*XCV(I)
FLOW=AREA*V(I,2)*RHO(I,1)
DIFF=AREA*GAM(I,1)/YDIF(2)
CALL DIFLOW
AJM(I,2)=ACOF+AMAX1(0.,FLOW)
```

```
602 ENDDO
```

```
DO 603 J=2,M2
FLOW=ARX(J)*U(2,J)*RHO(1,J)
DIFF=ARX(J)*GAM(1,J)/(XDIF(2)*SX(J))
CALL DIFLOW
AIM(2,J)=ACOF+AMAX1(0.,FLOW)
DO 604 I=2,L2
IF(I==L2) THEN
FLOW=ARX(J)*U(L1,J)*RHO(L1,J)
DIFF=ARX(J)*GAM(L1,J)/(XDIF(L1)*SX(J))
ELSE
FLOW=ARX(J)*U(I+1,J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
DIFF=ARX(J)*2.*GAM(I,J)*GAM(I+1,J)/((XCV(I)*GAM(I+1,J)+
```



```
& XCV(I+1)*GAM(I,J)+1.0E-30)*SX(J)
ENDIF
CALL DIFLOW
AIM(I+1,J)=ACOF+AMAX1(0.,FLOW)
AIP(I,J)=AIM(I+1,J)-FLOW
AREA=RMN(J+1)*XCV(I)
IF(J= = M2) THEN
FLOW=AREA*V(I,M1)*RHO(I,M1)
DIFF=AREA*GAM(I,M1)/YDIF(M1)
ELSE
FLOW=AREA*V(I,J+1)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))
DIFF=AREA*2.*GAM(I,J)*GAM(I,J+1)/(YCV(J)*GAM(I,J+1)+
& YCV(J+1)*GAM(I,J)+1.0E-30)
ENDIF
CALL DIFLOW
```

```

AJM(I,J+1)=ACOF+AMAX1(0.,FLOW)
AJP(I,J)=AJM(I,J+1)-FLOW
VOL=YCVR(J)*XCV(I)
APT=RHO(I,J)/DT ! Transient term  $\rho/\Delta t$  without volume
AP(I,J)=AP(I,J)-APT
CON(I,J)=CON(I,J)+APT*F(I,J,NF)
AP(I,J)=(-AP(I,J)*VOL+AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J))
&/RELAX(NF)
CON(I,J)=CON(I,J)*VOL+REL*AP(I,J)*F(I,J,NF)
604 ENDO
603 ENDO
CALL SOLVE !
IF (LSLVE(4)) THEN ! If the temp. eq. is solved ,then Reset density back to rho
DO I=I,L1
DO J=1,M1
RHO(I,J)=RHO(I,J)/CP(I,J) ! Reset density back to rho
ENDDO
ENDDO
ENDIF
ENDIF
600 ENDDO (End of the solving process)
TIME=TIME+DT ! Forward time
ITER=ITER+1 ! Increase the indicator
IF(ITER>= LAST) LSTOP=.TRUE. RETURN
END

```

$$a_p = (\sum a_{nb} + \rho_P \Delta V / \Delta t - S_p \Delta V) / \alpha$$

$$b = S_c \Delta V + a_p^0 \phi_p^0 + (1 - \alpha) \frac{a_p}{\alpha} \phi_p^0$$

Transient,
Linear----
Steady,
nonlinear

(15)---Explained
in detail

10.6.2.6 SUBROUTINE SUPPLY

SUBROUTINE SUPPLY ! main function: for printing

C*****

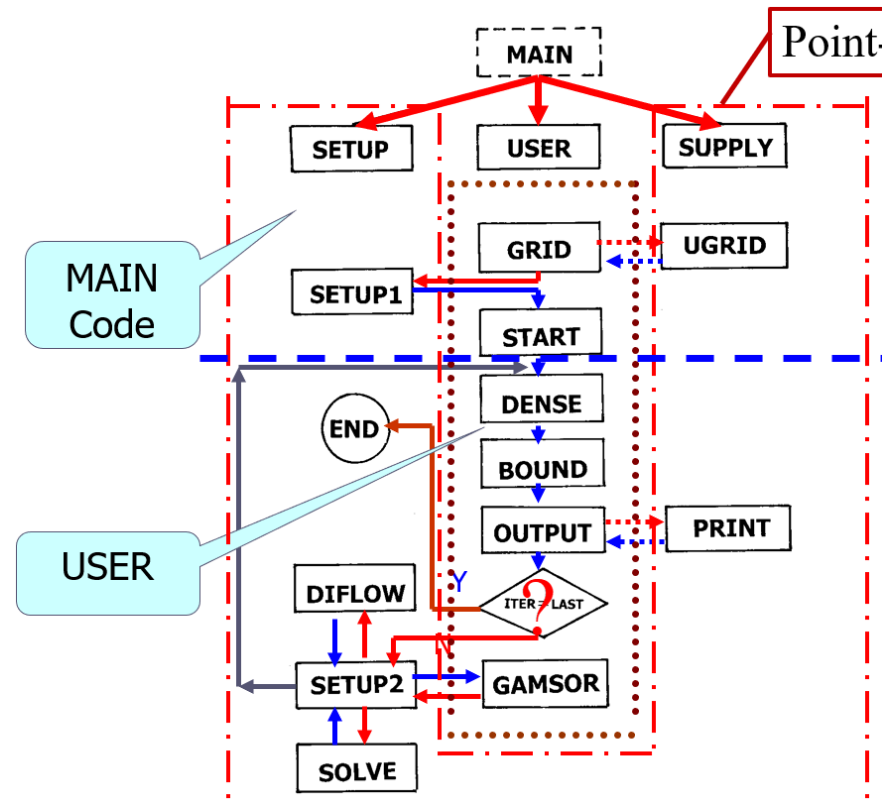
USE START_L

IMPLICIT NONE

REAL*8 DX,DY,RHOM,PREF

INTEGER*4 I,J,N,JJ,IEND,JEND,IBEG,JBEG,IFST,JFST,JFL

C*****



C*****

```
10 FORMAT(1X,26(1H*),3X,A10,3X,26(1H*))
20 FORMAT(1X,4H I =,I6,6I9)
30 FORMAT(1X,' J')
40 FORMAT(1X,I3,2X,1P7E9.2)
50 FORMAT(1X,1H )
51 FORMAT(2X,'I =',2X,7(I4,5X))
52 FORMAT(2X,'X =',1P7E9.2)
53 FORMAT(1X,' TH =',1P7E9.2)
54 FORMAT(2X,'J =',2X,7(I4,5X))
55 FORMAT(2X,'Y =',1P7E9.2)
```

!1P7E9.2

!1P---1 integer digit of each data;

!7E---7 data in scientific expression

! 9.2---Each data contains 9 places, and there are two decimal places (小数2位)

C*****

```
ENTRY UGRID
XU(2)=0.
DX=XL/FLOAT(L1-2)
DO 1 I=3,L1
XU(I)=XU(I-1)+DX
1 ENDDO
YV(2)=0.
DY=YL/FLOAT(M1-2)

DO 2 J=3,M1
YV(J)=YV(J-1)+DY
2 ENDDO
RETURN
```

2.00E+00	2.30E+00	2.90E+00	3.50E+00	4.10E+00	4.70E+00	5.00E+00
1.80E+00	2.08E+00	2.64E+00	3.20E+00	3.76E+00	4.32E+00	4.60E+00
1.40E+00	1.64E+00	2.12E+00	2.60E+00	3.08E+00	3.56E+00	3.80E+00
1.00E+00	1.20E+00	1.60E+00	2.00E+00	2.40E+00	2.80E+00	3.00E+00
6.00E-01	7.60E-01	1.08E+00	1.40E+00	1.72E+00	2.04E+00	2.20E+00
2.00E-01	3.20E-01	5.60E-01	8.00E-01	1.04E+00	1.28E+00	1.40E+00
0.00E+00	1.00E-01	3.00E-01	5.00E-01	7.00E-01	9.00E-01	1.00E+00

(16)---Explained in detail

C*****

ENTRY PRINT

! For print out, NF=3
represents stream function

DO 82 J=3,M1

IF(LPRINT(3)) THEN

CALCULATE THE STREAM FUNCTION

F(2,2,3)=0.

DO 81 I=2,L1

IF(I.NE.2) F(I,2,3)=F(I-1,2,3)-RHO(I-1,1)*V(I-1,2)

&*R(1)*XCV(I-1) ! I=2, F(2,2,3)=0;

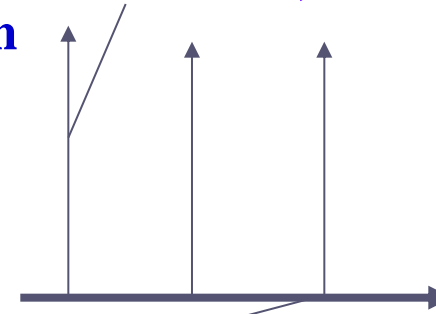
DO 82 J=3,M1

RHOM=FX(I)*RHO(I,J-1)+FXM(I)*RHO(I-1,J-1)

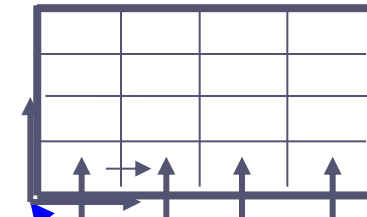
F(I,J,3)=F(I,J-1,3)+RHOM*U(I,J-1)*ARX(J-1) !

82 ENDDO

81 ENDDO



DO 82 I=2,L1



F(2,2,3)=0

$$\rho u r = \frac{\partial \psi}{\partial y}; \rho v r = -\frac{\partial \psi}{\partial x} \quad \psi = -\int \rho v r dx \quad \psi = \int \rho u r dy$$

For bottom, from left to right $\psi_{i,2} = \psi_{i-1,2} - \sum_{i=3} \rho_{i-1,1} v_{i-1,2} r(1) \Delta x_i$

For vertical, from bottom to top $\psi_{i,j} = \psi_{i,j-1} + \rho_m u_{i,j-1} r(j) \Delta y_j$

```
IF(LPRINT(NP)) THEN
CONSTRUCT BOUNDARY PRESSURES BY EXTRAPOLATION
DO 91 J=2,M2
P(1,J)=(P(2,J)*XCVS(3)-P(3,J)*XDIF(2))/XDIF(3)
P(L1,J)=(P(L2,J)*XCVS(L2)-P(L3,J)*XDIF(L1))/XDIF(L2)
91 ENDDO
DO 92 I=2,L2
P(I,1)=(P(I,2)*YCVS(3)-P(I,3)*YDIF(2))/YDIF(3)
P(I,M1)=(P(I,M2)*YCVS(M2)-P(I,M3)*YDIF(M1))/YDIF(M2)
92 ENDDO
P(1,1)=P(2,1)+P(1,2)-P(2,2)
P(L1,1)=P(L2,1)+P(L1,2)-P(L2,2)
P(1,M1)=P(2,M1)+P(1,M2)-P(2,M2)
P(L1,M1)=P(L2,M1)+P(L1,M2)-P(L2,M2)
PREF=P(IPREF,JPREF) ! Reference point of pressure
DO 93 J=1,M1
DO 93 I=1,L1
P(I,J)=P(I,J)-PREF ! Relative pressure
94ENDDO
93ENDDO
ENDIF
```

```
PRINT 50 ! Print out to screen
WRITE(8,50) ! Output into file
IEND=0
DO WHILE (IEND/=L1)
IBEG=IEND+1
IEND=IEND+7 ! !7 data in each line
IEND=MIN0(IEND,L1) ! Take minimum
PRINT 50
WRITE(8,50)
PRINT 51,(I,I=IBEG,IEND) !From IBEG to IEND for printing
WRITE(8,51) (I,I=IBEG,IEND)
IF(MODE/=3) THEN
PRINT 52,(X(I),I=IBEG,IEND)
WRITE(8,52) (X(I),I=IBEG,IEND)
ELSE ! Print out x-coordinates
PRINT 53.(X(I),I=IBEG,IEND)
WRITE(8,53) (X(I),I=IBEG,IEND)
ENDIF
ENDDO
IF(IEND= =L1) THEN
```

```
JEND=0
PRINT 50
WRITE(8,50)
DO WHILE(JEND/=M1) THEN
JBEG=JEND+1
JEND=JEND+7
JEND=MIN0(JEND,M1)
PRINT 50
WRITE(8,50)
PRINT 54,(J,J=JBEG,JEND)
WRITE(8,54) (J,J=JBEG,JEND)
PRINT 55,(Y(J),J=JBEG,JEND) ! Print out y-coordinates
WRITE(8,55) (Y(J),J=JBEG,JEND) GO TO 311
ENDDO
ENDIF
```



```
DO 999 N=1,NCP      ! NCP has been defined as 14 in SETUP1
NF=N
IF(LPRINT(NF)) THEN      ! Print out F(I,J,NF) field
PRINT 50
WRITE(8,50)
PRINT 10,TITLE(NF)
WRITE(8,10) TITLE(NF)      ! Print out title of variable F(I,J,NF)
IFST=1
JFST=1
IF(NF==1.OR.NF==3) IFST=2
IF(NF==2.OR.NF==3) JFST=2
IBEG=IFST-7
DO WHILE ( IEND<L1.OR.IBEG== -5.OR.IBRG== -6)
IBEG=IBEG+7 ! Starting point for each line (7data)
IEND=IBEG+6 ! Ending point of the line
IEND=MIN0(IEND,L1)
PRINT 50 WRITE(8,50)
```

```

PRINT 20,(I,I=IBEG,IEND)
WRITE(8,20) (I,I=IBEG,IEND)
PRINT 30
WRITE(8,30)
JFL=JFST+M1 .
DO 115 JJ=JFST,M1
J=JFL-JJ
PRINT 40, J, (F(I,J,NF),I=IBEG,IEND)
WRITE(8,40) J,(F(I,J,NF),I=IBEG,IEND)
115 ENDDO
ENDDO
ENDIF
999 END (End of print do-loop)
    
```

```

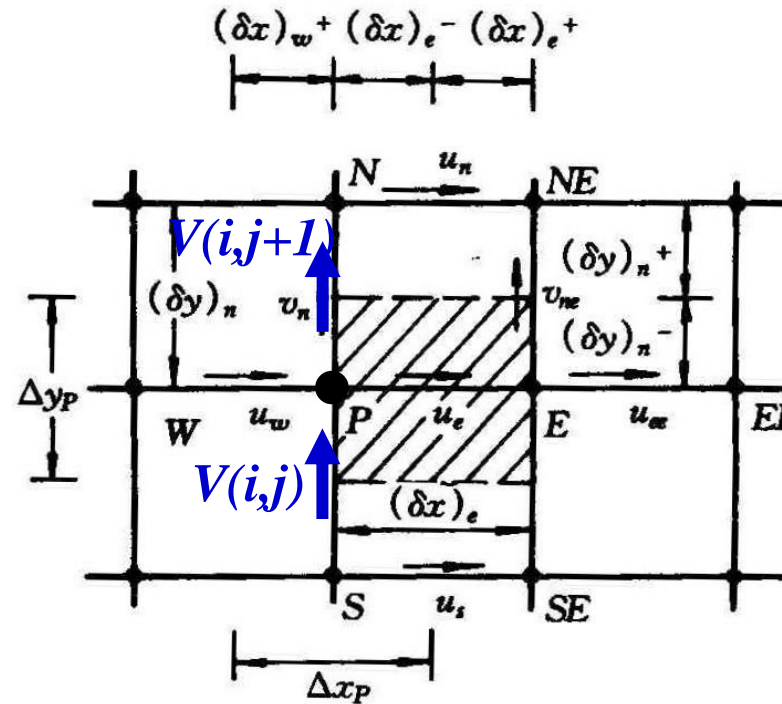
***** .TEMP. *****
I=  1      2      3      4      5      6      7
J
7  2.00E+00 2.30E+00 2.90E+00 3.50E+00 4.10E+00 4.70E+00 5.00E+00
6  1.80E+00 2.08E+00 2.64E+00 3.20E+00 3.76E+00 4.32E+00 4.60E+00
5  1.40E+00 1.64E+00 2.12E+00 2.60E+00 3.08E+00 3.56E+00 3.80E+00
4  1.00E+00 1.20E+00 1.60E+00 2.00E+00 2.40E+00 2.80E+00 3.00E+00
3  6.00E-01 7.60E-01 1.08E+00 1.40E+00 1.72E+00 2.04E+00 2.20E+00
2  2.00E-01 3.20E-01 5.60E-01 8.00E-01 1.04E+00 1.28E+00 1.40E+00
1  0.00E+00 1.00E-01 3.00E-01 5.00E-01 7.00E-01 9.00E-01 1.00E+00
    
```



```

IF(NF==2) THEN
  IF(J==1) FSHOW=V(I,2)
  IF(J>=2.AND.J<=M2) FSHOW=(V(I,J)+V(I,J+1))/2
  IF(J==M1) FSHOW=V(I,M1)
ENDIF
WRITE(9,'(E11.3,$)') FSHOW
ENDIF
ENDDO
      ENDDO
ENDDO
CLOSE(9)
RETURN
END
    
```

For v



Comments and Recommendations for Teaching Code Study

1. We should study the code line by line to completely understanding the function of each line and the numerical techniques included.

You should understand every detail included in each line, for example:

```
IF(MODE.== 3) THEN  
SX(J)=R(J)  
IF(J /= 1) SXMN(J)=RMN(J)  
ENDIF
```

why here J=1 should not be included?

2. You can understand a numerical algorithm, say **SIMPLER**, completely only when you know how to implementing the algorithm by code.

3. If you meet some difficulty in understanding the teaching code you may contact me by email (fangwenzhen@mail.xjtu.edu.cn) at any time.

4. Our teaching assistants will give you instruction on how to run the code.

Announcement

The lessons On **Dec. 2 (Monday)** and **Dec. 9 (Monday)**, the class will be cancelled Since the class time is conflicted with another course. **Next class will be on Dec. 3 (Thursday)** .

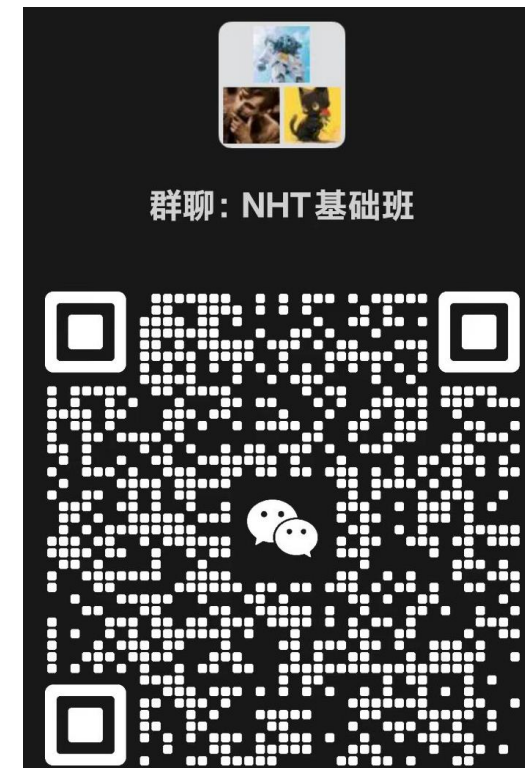
下周一（12月2日）和下下周一（12月9日）停课两次，下周二（12月3日）和下下周二的（12月10日）课不停课，谢谢大家！

Announcement

In the study of application of **FLUENT**, our class will be divided into two teaching groups: **Fundamental and Intermediate**. They are presented at the same time. Every student should make your choice. Please send your choice to the teaching assistance group **in this week**. We have to arrange an additional classroom from the graduate school.



Fill the table



Following students are invited for the office hour of this afternoon (2024.11.26)

Tuesday, Venue: 1-5080, 2:30 pm - 4:00 pm

3124101202	王百川	3124103149	范志泽楷
3124103037	宋岳轩	3124103150	吴诗帆
3124103039	王基惠	3124103151	全帅宇
3124103042	徐昊	3124103233	虎登科
3124103072	杨泽峰	3124103234	余顺杰
3124103073	李鸿鹏	3124103235	武文浩
3124103075	马继军	3124103236	左梦成
3124103146	王楠	3124103237	黄文玥
3124103147	董梦芸	3124103238	李家乐
3124103148	王林业	3124103239	卢堉浩

本组网页地址: <http://nht.xjtu.edu.cn> 欢迎访问!
Teaching PPT will be loaded on our website



同舟共济
渡彼岸!

People in the
same boat help
each other to
cross to the other
bank, where....