

Numerical Heat Transfer (数值传热学)

Chapter 10 General Code for 2D Elliptical Fluid Flow and Heat Transfer (2)



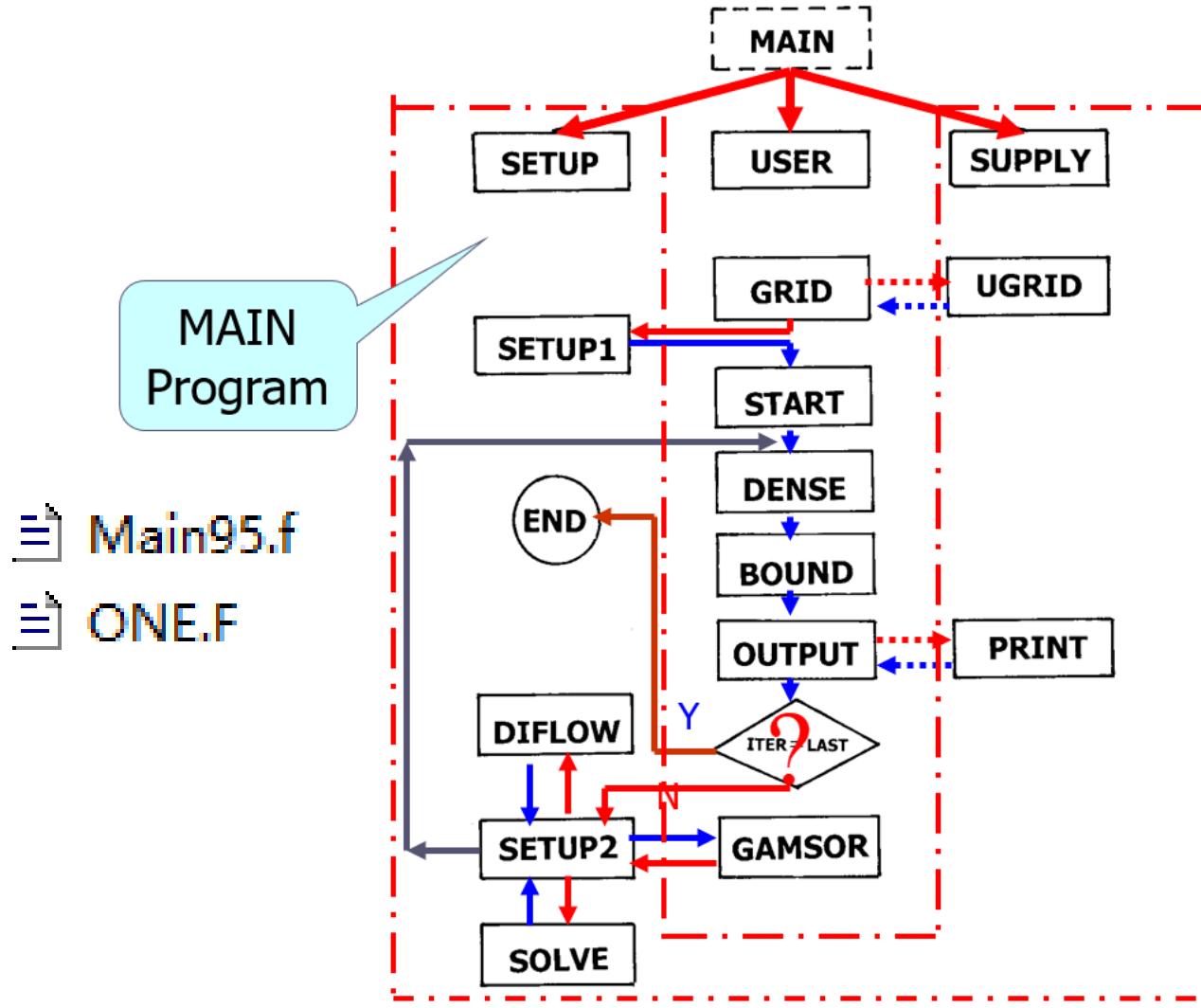
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**Key Laboratory of Thermo-Fluid Science & Engineering
Xi'an Jiaotong University**

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Main Program: 917 sentences



Main95.f
ONE.F

```

C -----MAIN PROGRAM-----
C *****
PROGRAM MAIN
USE START_L
IMPLICIT NONE
C *****
OPEN(8, FILE='RESULT.TXT')
CALL GRID
CALL SETUP1
CALL START
DO WHILE(.NOT.LSTOP)
CALL DENSE
CALL BOUND
CALL OUTPUT
CALL SETUP2
ENDDO
CALL OUTPUT
CLOSE(8)
STOP
END
CCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCC
SUBROUTINE DIFLOW
C *****
USE START_L
IMPLICIT NONE
REAL*8 TEMP
C *****
  
```

Chapter 10 General Code for 2D Elliptical Fluid Flow and Heat Transfer Problems (2)

10.6 Methods of application and explanation of Main Program

10.6.1 Methods of Code application

10.6.2 Explanation of Main Program

10.6.2.1 MODULE START_L

10.6.2.2 PROGRAM MAIN

10.6.2.3 SUBROUTINE DIFLOW

10.6.2.4 SUBROUTINE SOLVE

10.6.2.5 SUBROUTINE SETUP

10.6.2.6 SUBROUTINE SUPPLY

10. 6 Methods of Application and Explanation of Main Program

10.6.1 Methods of Code application

1. **Establishing** complete mathematical formulation and comparing with the standard equation:

$$\frac{\partial(\rho^* \phi)}{\partial t} + \text{div}(\rho^* \vec{u} \phi) = \text{div}(\Gamma_{\phi} \text{grad} \phi) + S_{\phi}^*$$

Determine S_{ϕ}^* , Γ_{ϕ} , and ρ_{ϕ}^*

2. **Calling (调用)** a USER(will be taught in Chapter 11) similar to the problem studied

3. Using a few nodes, 5~7 in each direction, and setting a small value of LAST, say 3–5, to go through grammatical examination; Then gradually increasing the complexity. For example, for turbulent heat transfer simulation, computing laminar flow first .

4. Making correspondent modifications for the six-ENTRY in USER, according to the problem studied, especially for following parts:

**(1) LSOLVE(NF)—for variable NF to be solved setting :
.TRUE.**

**(2) LPRINT(NF)—for variable NF to be printed out setting:
.TRUE.**

- (3) **TITLE(NF)**—for variable NF to be printed out specifying its title (within eight letters).
- (4) **LBLK(NF)**—for variable NF to be solved by block correction setting: **.TRUE.**, otherwise **.FALSE.**, Its default value is **.T. .**
- (5) **LAST**—Specify iteration number, default value is 5.
- (6) **NTIMES(NF)**—Default value equals 1; for steady nonlinear one, setting: 1 to 2; unsteady linear: 5 to 6

(7) **DT**—Time step, default value is 10^{30}

For fully implicit scheme, in the a_p -term there is a term of $a_p^0 = \rho \Delta V / \Delta t$, if $\Delta t \rightarrow \infty$, $a_p^0 \rightarrow 0$, leading to steady state results. Default value is for steady case.

(8) **RELAX(NF)**—Default value is 1.

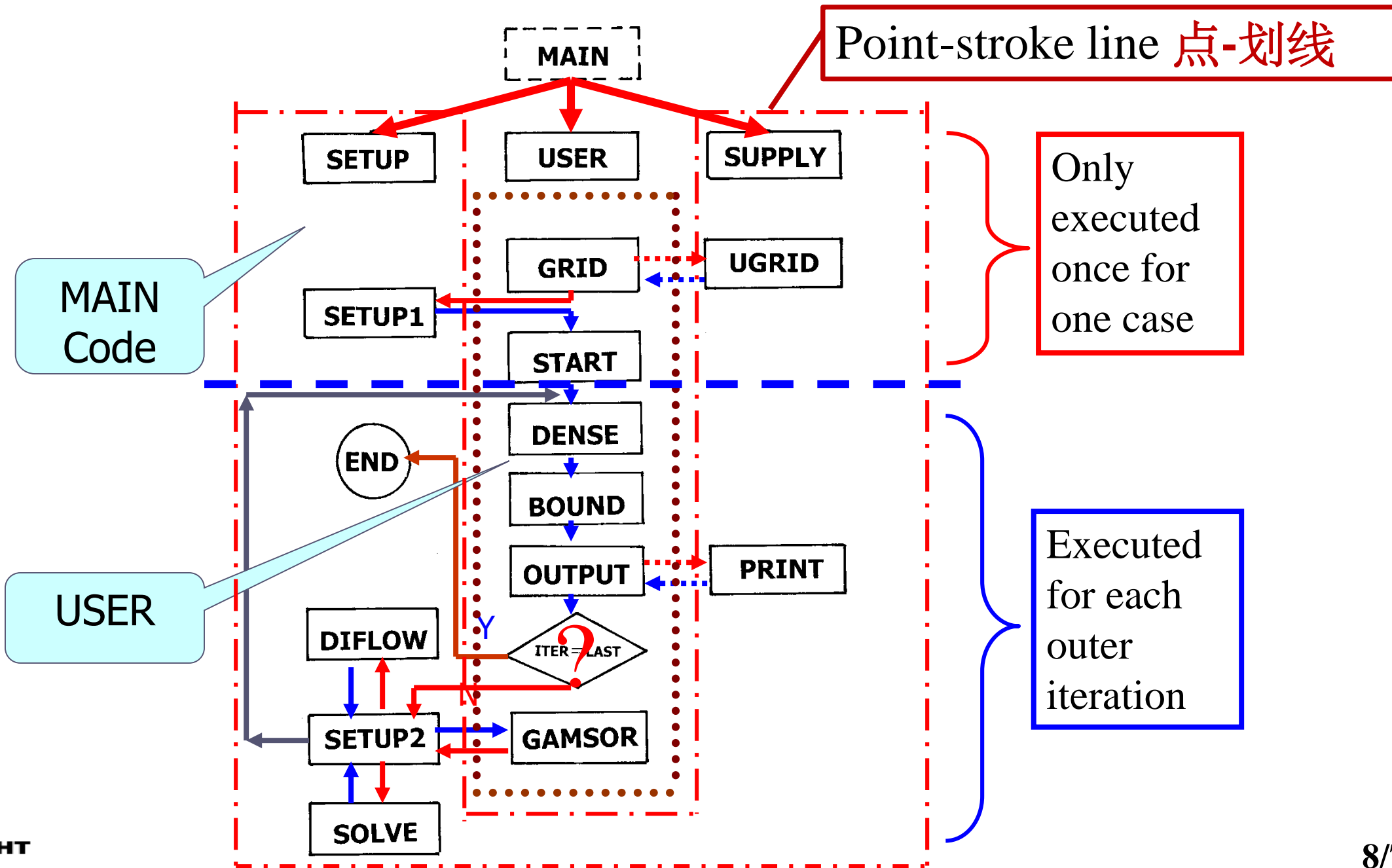
(9) **IPREF, JPREF**: I, J of pressure reference point, their default values are 1,1;

5 Defining a new dependent variable, say $C(i,j)$, as follows:

First defining **C(NI,NJ)**,

then using **EQUIVALENCE**:

EQUIVALENCE (F(1,1,5), C(1,1)).



**For the Main Program,
these parts will
be explained in
detail.**

- 1. MODULE START_L**
- 2.-----MAIN-----**
- 3. SUBROUTINE DIFLOW**
- 4. Structure of SOLVE**
- 5. Block correction**
- 6. Structure of SETUP**
- 7. MODE execution**
- 8. Determination of neighbor coefficients**
- 9. Determination of AP coefficients**
- 10. Structure of SIMPLER**
- 11. Temporal storage of coefficients for SIMPLER**
- 12. Accumulated addition**
- 13. Storage of coefficients of p-equation**
- 14. Nominal density for temperature**
- 15. Iteration=Marching forward**
- 16. Data Format for print out**
- 17. Stream function computation**
- 18. Data print out procedure**

10-6-2 Explanation of Main programs

CC

**C This computer program was copied from the graduate student course
C program of the University of Minnesota. Part of it was re-formulated
C to meet the local computational environment. Some inappropriate
C expressions were also corrected. The program is used only for the
C teaching purpose. No part of it may be published. You may use it as a
C frame to re-develop your own code for research purpose.**

C -----Instructor of Numerical Heat Transfer, XJTU,2013.-----

CC

**C The current version of the program was updated from Fortran 77 to
C Fortran 95 by Dr. Yu-Tong Mu , Dr. Li Chen and Dr.Kong Ling of NHT
C group of XJTU during 2013.01-04**

CC

C*****



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凌空



陈黎

10.6.2.1 MODULE START_L

(1)-Explained in detail

MODULE START_L

PARAMETER (NI=100,NJ=200,NIJ=NI,NFMAX=10,NFX4=NFMAX+4)

CHARACTER*8 TITLE(NFX4)

LOGICAL LSOLVE(NFX4),LPRINT(NFX4),LBLK(NFX4),LSTOP

REAL*8,DIMENSION(NI,NJ,NFX4)::F ! One 3D function

REAL*8,DIMENSION(NI,NJ,6)::COF,COFU,COFV,COFP ! Four 3D functions

REAL*8,DIMENSION(NI,NJ)::P,RHO,GAM,CP,CON,AIP,AIM,AJP,AJM,AP

REAL*8,DIMENSION(NI):: U,V,PC,T,DU,DV,UHAT,VHAT

REAL*8,DIMENSION(NI):: X,XU,XDIF,XCV,XCVS,XCVI,XCVIP

REAL*8,DIMENSION(NJ)::Y,YV,YDIF,YCV,YCVS,YCVR,YCVRS,ARX,ARXJ,

& ARXJP,R,RMN,SX,SXMN

REAL*8,DIMENSION(NI)::FV,FVP,FX,FXM

REAL*8,DIMENSION(NJ)::FY,FYM

REAL*8,DIMENSION(NIJ)::PT,QT For TDMA in Block correction

REAL*8 RELAX(NFX3),TIME,DT,XL,YL,RHOCON

INTEGER*4 NF,NP,NRHO,NGAM,NCP,L1,L2,L3,M1,M2,M3,

& IST,JST,ITER,LAST,MODE,NTIMES(NFX4),IPREF,JPREF

REAL*8 SMAX,SSUM

REAL*8 FLOW,DIFF,ACOF

Sc or b

a_e, a_w, a_n, a_s, a_p

- (1) Packaging data (封装数据);
- (2) Initializing data (数据初始化);
- (3) Declaring type of data (声明数据类型).

C*****

**EQUIVALENCE(F(1,1,1),U(1,1)),(F(1,1,2),V(1,1)),(F(1,1,3),PC(1,1))
&, (F(1,1,4),T(1,1))**

**EQUIVALENCE(F(1,1,11),P(1,1)),(F(1,1,12),RHO(1,1)),(F(1,1,13)
&,GAM(1,1),(F(1,1,14),CP(1,1))**

**EQUIVALENCE(COF(1,1,1),CON(1,1)),(COF(1,1,2),AIP(1,1)),
&(COF(1,1,3),AIM(1,1)),(COF(1,1,4),AJP(1,1)),
&(COF(1,1,5),AJM(1,1)),(COF(1,1,6),AP(1,1))**

REAL*8,DIMENSION(NI)::TH,THU,THDIF,THCV,THCVS

REAL*8 THL

**EQUIVALENCE(X,TH),(XU,THU),(XDIF,THDIF),(XCV,THCV),
&(XCVS,THCVS),(XL,THL)**

DATA LSTOP,LSOLVE,LPRINT/.FALSE.,NFX4*.FALSE., NFX4*.FALSE./

DATA LBLK/NFX4*.TRUE./

DATA MODE,LAST,TIME,ITER/1,5,0.,0/

DATA RELAX,NTIMES/NFX4*1.,NFX4*1/

DATA DT,IPREF,JPREF,RHOCON,CPCON/1.E+30, 1,1,1.,1./

END MODULE

MODULE module_name

•••••
•••••
•••••

Module name is composed of two parts,
with a hyphen(-) at bottom in between.

END MODULE

- (1) Packaging data (封装数据);
- (2) Initializing data (数据初始化);
- (3) Declaring type of data (声明数据类型).

**Default
value!!**

Some explains to this most important module

REAL*8,DIMENSION(NI,NJ,NFX4)::F

Real variable 3-D array, array title F, F(NI,NJ,NFX4);
Variable number in three coordinates are NI,NJ and NFX4
respectively;
:: ---is the symbol for separation, separator, to make the
declaration of variable type clear;

REAL*8 SMAX,SSUM

Real variable of SMAX and SSUM, with length of eight digits;

INTEGER*4 NF,NP,NRHO

Integral variable of NF,NP,NRHO, with length of four digits;

EQUIVALENCE(F(1,1,1),U(1,1)),(F(1,1,2),V(1,1))

Making the 1st variable of the 3D array F identical to the 2D
array U; the same for (F(1,1,2), V(1,1)))

10.6.2.2 PROGRAM MAIN

(2)-Explained
in detail

```

C*****
C-----MAIN-----
C*****

PROGRAM MAIN !Name of main program
USE START_L   Share the variables defined in the MODULE
IMPLICIT NONE

C*****

OPEN(8,FILE='RESULT.txt') ! Result file for output
CALL GRID !Grid generation (setup interface positions)
CALL SETUP1 !Set up 1-D array, not changed in iteration
CALL START !Set up initial field
DO WHILE (.NOT.LSTOP) ! If LSTOP is .F., the NOT .F. is .T., following
CALL DENSE !Set up fluid density four CALLs are executed
CALL BOUND !Set up boundary condition
CALL OUTPUT !Print out present results
CALL SETUP2 !Key module: set coefficients and solve ABEqs.
ENDDO
CALL OUTPUT !Print out some results
CLOSE(8) !Simulation completed close file RESULT.TXT in Channel 8
STOP !Terminate computation
END !End of main program

```

Calling
Module



Only
Executed
once



Executed
Many times



For all other scalar variables (including T , etc)

$$\frac{\partial(\rho^* \phi)}{\partial t} + \text{div}(\rho^* \phi \vec{U}) = \text{div}(\Gamma_\phi \text{grad} \phi) + S_\phi^*$$

$$a_P \phi_P = a_E \phi_E + a_W \phi_W + a_N \phi_N + a_S \phi_S + b$$

$$a_E = D_e A(|P_{\Delta e}|) + \llbracket -F_e, 0 \rrbracket \quad a_W = D_w A(|P_{\Delta w}|) + \llbracket F_w, 0 \rrbracket$$

$\frac{a_E}{D_e}$	Scheme	Central difference	Upwind difference
	Definition		$1 - 0.5 P_{\Delta e}$
Hybrid		Power-law	Exponential
$P_{\Delta e} = \frac{F_e}{D_e}$	$\llbracket -P_{\Delta e}, 1 - \frac{1}{2} P_{\Delta e}, 0 \rrbracket$	$\llbracket 0, (1 - 0.1 P_{\Delta e})^5 \rrbracket + \llbracket 0, -P_{\Delta e} \rrbracket$	$\frac{P_{\Delta e}}{\exp(P_{\Delta e}) - 1}$

Determine coefficients using **Subroutine DIFLOW**

10.6.2.3 SUBROUTINE DIFLOW

(3)-Explained
in detail

CC

Calling
Module



```

SUBROUTINE DIFLOW ! Determine  $D \cdot A(|P_{\Delta}|)$  of power law scheme
USE START_L ! Share the variables defined in the MODULE START_L
IMPLICIT NONE ! The input variables are DIFF and FLOW
REAL*8 TEMP ! Declaration of a temporal real variable TEMP
    
```

C*****

! 1st return for
diffusion case

```

ACOF=DIFF !  $D \cdot A(|P_{\Delta}|) = D$  (ACOF finally represents  $D \cdot A(|P_{\Delta}|)$ )
IF(FLOW== 0.) RETURN ! No flow, only diffusion
TEMP=DIFF-ABS(FLOW)*0.1 !  $D - 0.1|F| = D(1 - 0.1|P_{\Delta}|)$ 
    
```

! 2nd return for
 $|P_{\Delta e}| > 10$

```

ACOF=0. !  $\left\{ \begin{array}{l} 0 \quad |P_{\Delta e}| > 10 \\ (1 - 0.1|P_{\Delta e}|)^5 \quad |P_{\Delta e}| < 10 \end{array} \right.$ 
IF(TEMP.<= 0.) RETURN !  $|P_{\Delta e}| > 10$ 
TEMP=TEMP/DIFF !  $1 - 0.1|P_{\Delta e}|$ 
    
```

! 3rd return for
 $|P_{\Delta e}| < 10$

```

ACOF=DIFF*TEMP**5 !  $D \cdot (1 - 0.1|P_{\Delta e}|)^5 = D \cdot A(|P_{\Delta e}|)$ 
RETURN
    
```

END !In SETUP2: $a_E = D_e A(|P_{\Delta e}|) + [0, -F_e]$

CC

10.6.2.4 SUBROUTINE SOLVE

CC

SUBROUTINE SOLVE !ADI line iteration+Block correction

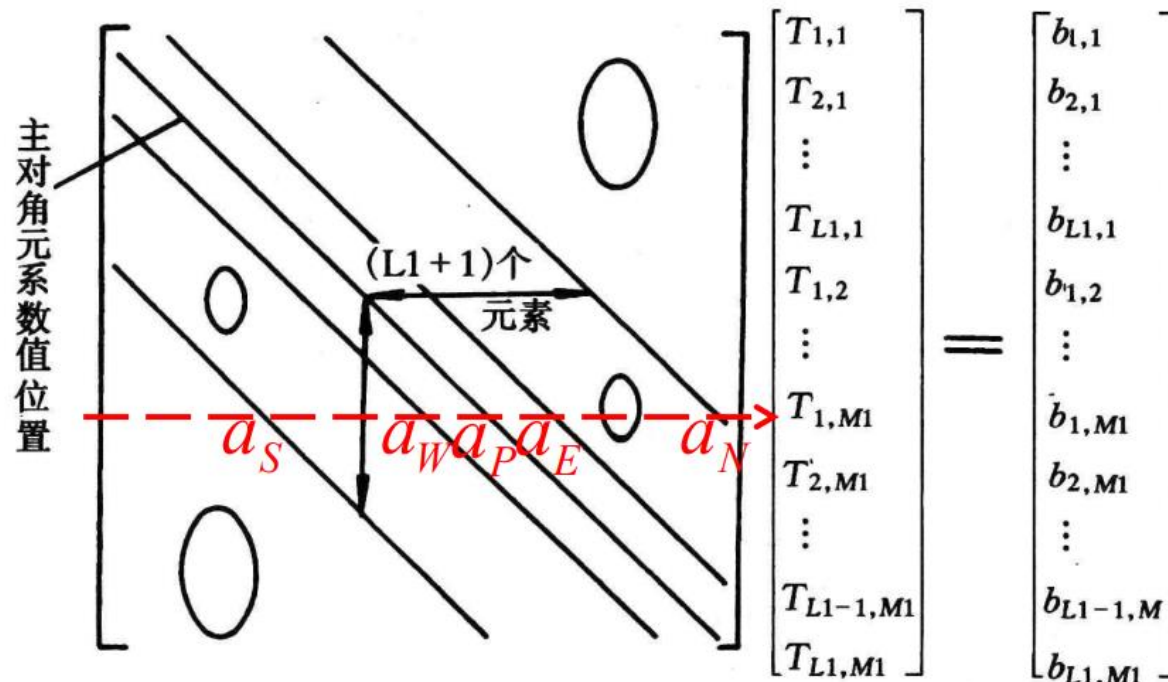
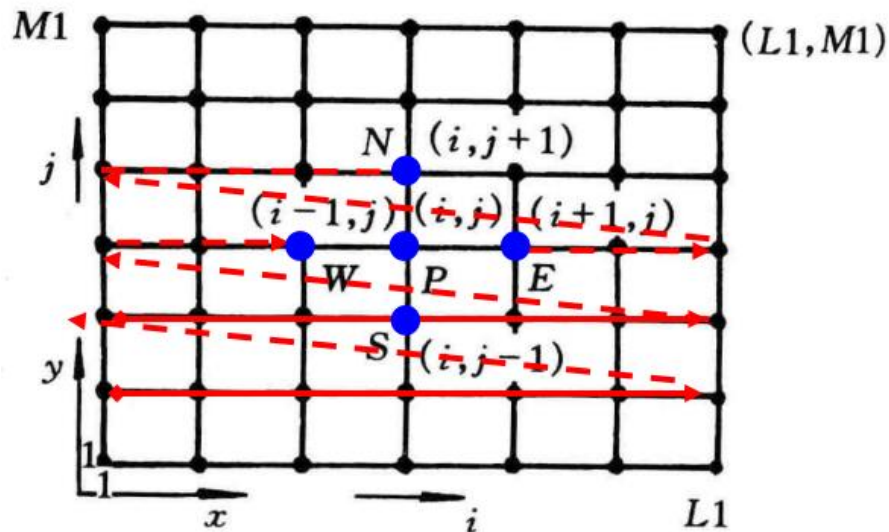
Calling
Module

USE START_L
IMPLICIT NONE

Declaration of
variable type

INTEGER*4 ISTF, JSTF, IT1, IT2, JT1, JT2, NT, N,I,J,II,JJ
REAL*8 BL, BLP, BLM, BLC, DENOM, TEMP

C*****



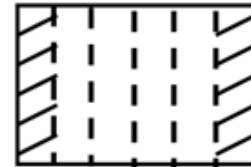
Structure of SOLVE

AD---alternative direction

S
O
L
V
E

```

DO 999 NT=1, NTIMES (NF)
N=NF
IF (LBLK(NF)) THEN
PT(ISTF)=0.
.....
13 ENDDO
PT(JSTF)=0.
.....
23 ENDDO
10 ENDIF
999 ENDDO
    
```



IST L2



M2 JST

Upward line iteration

downward line iteration

Left to right line iteration

Right to left line iteration

Two times of block corrections

Correction

Four times of line iterations

AD line Iteration

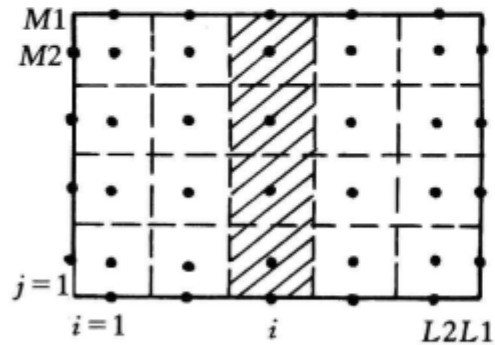
(4)-Explained in detail

Review on block correction

1. Equation for correction:

It is required that: $(\phi_{i,j}^* + \bar{\phi}_i')$ satisfy following eq.

$$\begin{aligned} \sum_j \underline{AP}(\phi_{i,j}^* + \bar{\phi}_i') &= \sum_j \underline{AIP}(\phi_{i+1,j}^* + \bar{\phi}_{i+1}') + \sum_j \underline{AIM}(\phi_{i-1,j}^* + \bar{\phi}_{i-1}') \\ &+ \sum_j (\underline{AJM})(\phi_{i,j-1}^* + \bar{\phi}_i') \\ &+ \sum_j (\underline{AJP})(\phi_{i,j+1}^* + \bar{\phi}_i') + \sum_j CON \\ &(i = IST, \dots, L2) \end{aligned}$$



IST-solution starting subscript in X-direction; L2-last but one.

Here AP, AIP, AIM , etc. are the symbols adopted in teaching code

Review on block correction

(5)-Explained
in detail

$$(BL)\bar{\phi}'_i = (BLP)\bar{\phi}'_{i+1} + (BLM)\bar{\phi}'_{i-1} + BLC, i = IST, \dots, L2$$

$$BL = \sum_{j=JST}^{M2} (AP) - \sum_{j \neq M2} (AJP) - \sum_{j \neq JST} (AJM) \quad BLP = \sum_{j=JST}^{M2} (AIP)$$

$$BLM = \sum_{j=JST}^{M2} (AIM) \quad BLC = \sum_{j=JST}^{M2} CON + \sum_{j=JST}^{M2} (AJP)\phi_{i,j+1}^* + \sum_{j=JST}^{M2} (AJM)\phi_{i,j-1}^*$$

$$+ \sum_{j=JST}^{M2} (AIP)\phi_{i+1,j}^* + \sum_{j=JST}^{M2} (AIM)\phi_{i-1,j}^* - \sum_{j=JST}^{M2} (AP)\phi_{i,j}^*$$

$$BL=A, BLP = B,$$

$$BLM = C$$

$$A_i \bar{\phi}'_i = B_i \bar{\phi}'_{i+1} + C_i \bar{\phi}'_{i-1} + D_i, i = 1, 2, \dots, M1 \rightarrow \bar{\phi}'_{i-1} = P_{i-1} \bar{\phi}'_i + Q_{i-1}$$

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}}; \quad Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}}; \quad P_1 = \frac{B_1}{A_1}; \quad Q_1 = \frac{D_1}{A_1}$$

DENOM=BL-PT(I-1)*BLM

DENOM

C*****

ISTF=IST-1
 JSTF=JST-1
 IT1=L2+IST
IT2=L3+IST
 JT1=M2+JST
JT2=M3+JST

!Temporal integral variables for starting points of DO-loop

C*****

DO 999 NT=1,NTIMES(NF) ! Solution of algebraic equation
N=NF ! NF: 1=U, 2=V, 3=P,

C-----

IF(LBLK(NF)) THEN !When LBLK is true, execute Block-correction

PT(ISTF)=0. ! Coefficient in TDMA P_{IST-1}

QT(ISTF)=0. ! Constant in TDMA Q_{IST-1}

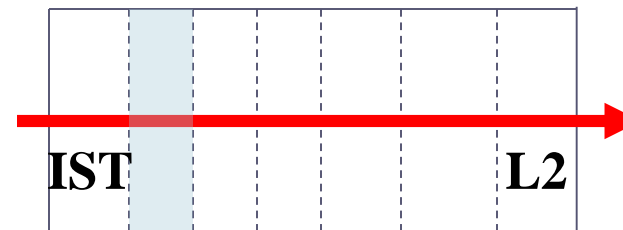
DO 11 I=IST,L2

BL=0. !Initial value in B-correction

BLP=0. !Initial value in B-correction

BLM=0. ! Initial value in B-correction

I -direction B.Correction.



**(5)-
Explained
in detail**

In discussion of TDMA:

A B C D
 $(BL)\bar{\phi}'_i = (BLP)\bar{\phi}'_{i+1} + (BLM)\bar{\phi}'_{i-1} + BLC, i = IST, \dots, L2$

BLC=0. !Initial value

DO 12 J=JST,M2

BL=BL+AP(I,J)

IF(J /= M2) BL=BL-AJP(I,J)

IF(J /= JST) BL=BL-AJM(I,J)

BLP=BLP+AIP(I,J)

BLM=BLM+AIM(I,J)

BLC=BLC+CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)

& +AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)-AP(I,J)*F(I,J,N)

12 ENDDO

DENOM=BL-PT(I-1)*BLM

IF(ABS(DENOM/BL) < 1.E-10) DENOM=1.E25

PT(I)=BLP/DENOM

QT(I)=(BLC+BLM*QT(I-1))/DENOM

11 ENDDO

$$BL = \sum_{j=JST}^{M2} (AP) - \sum_{j \neq M2} (AJP) - \sum_{j \neq JST} (AJM)$$

$$BLP = \sum_{j=JST}^{M2} (AIP)$$

$$BLM = \sum_{j=JST}^{M2} (AIM)$$

$$BLC = \sum_{j=JST}^{M2} CON + \sum_{j=JST}^{M2} (AJP)\phi_{i,j+1}^* + \sum_{j=JST}^{M2} (AJM)\phi_{i,j-1}^* + \sum_{j=JST}^{M2} (AIP)\phi_{i+1,j}^* + \sum_{j=JST}^{M2} (AIM)\phi_{i-1,j}^* - \sum_{j=JST}^{M2} (AP)\phi_{i,j}^*$$

$$A_i \bar{\phi}'_i = B \bar{\phi}'_{i+1} + C_i \bar{\phi}'_{i-1} + D_i$$

$$\bar{\phi}'_{i-1} = P_{i-1} \bar{\phi}'_i + Q_{i-1}$$

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}}; \quad Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}}$$

DENOM

**Coefficients
calculation**

**Elimination
(消元)**

!Ensure a meaningful correction

Back substitution
(回代)

BL=0. (Initial set up)

DO 13 II=IST,L2

I=IT1-II

BL=BL*PT(I)+QT(I)

DO 14 J=JST,M2

F(I,J,N)=F(I,J,N)+BL!

14 ENDDO

13 ENDDO

C

PT(JSTF)=0.

QT(JSTF)=0.

DO 21 J=JST,M2

BL=0.

BLP=0.

BLM=0.

BLC=0.

DO 22 I=IST,L2

BL=BL+AP(I,J)

IF(I /= L2) BL=BL-AIP(I,J)

IF(I /= IST) BL=BL-AIM(I,J)

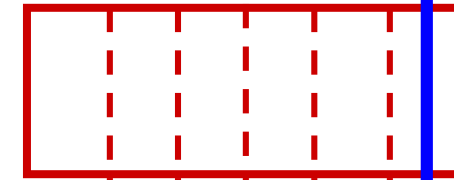
BLP=BLP+AJP(I,J)

IT1=L2+IST

I=IT1-II=L2+IST-IST=L2-Begin

I=IT1-II=L2+IST-L2=IST-End

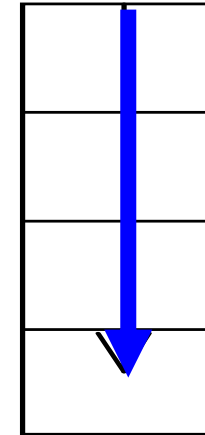
Correcting by BL for the same column



$$T_{i-1} = P_{i-1} T_i + Q_{i-1}$$

BL=BL*PT(I)+QT(I)

TDMA: from L2 to IST



$$(BL)\bar{\phi}'_j = (BLP)\bar{\phi}'_{j+1} + (BLM)\bar{\phi}'_{j-1} + BLC, J = JST, \dots, M2$$

Y-direction
B-correction

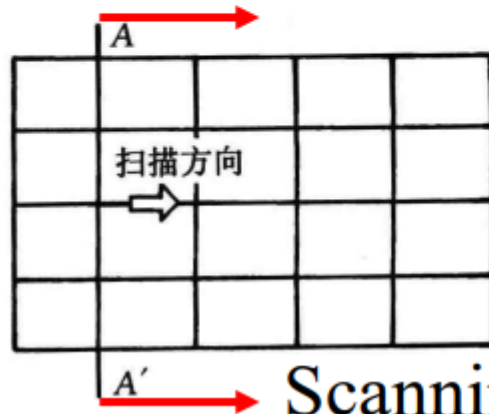

```
BLM=BLM+AJM(I,J) !
BLC=BLC+CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)
& +AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)-AP(I,J)*F(I,J,N)
22 ENDDO
DENOM=BL-PT(J-1)*BLM !
IF(ABS(DENOM/BL)<1.E-10) DENOM=1.E25
PT(J)=BLP/DENOM !
QT(J)=(BLC+BLM*QT(J-1))/DENOM
21 ENDDO
BL=0.
DO 23 JJ=JST,M2
J=JT1-JJ
BL=BL*PT(J)+QT(J)
DO 24 I=IST,L2
F(I,J,N)=F(I,J,N)+BL !Correcting by BL for the same block
24 ENDDO
23 ENDDO
10 ENDIF
```

! Above is block correction, following is ADI line iteration

line iteration:

$$\text{Jakob: } a_P \phi_P^{(k+1)} = a_N \phi_N^{(k+1)} + a_S \phi_S^{(k+1)} + [a_E \phi_E^{(k)} + a_W \phi_W^{(k)} + b]$$

$$\text{G-S: } a_P \phi_P^{(k+1)} = a_N \phi_N^{(k+1)} + a_S \phi_S^{(k+1)} + [a_E \phi_E^{(k)} - a_W \phi_W^{(k+1)} + b]$$



Scanning (扫描) in E-W direction

New b term, b'

At the same line, TDMA is used for direct solution, from line to line iterative method is used.

$$A_i \bar{\phi}_i = B_i \bar{\phi}_{i+1} + C_i \bar{\phi}_{i-1} + D_i, i = 1, 2, \dots, M1$$

Solving in I-direction, scanning in J direction

C

DO 90 J=JST,M2 $AP\phi_{i,j}^n = AIP\phi_{i+1,j}^n + AIM\phi_{i-1,j}^n + b + AJP\phi_{i,j+1}^{n-1} + AJM\phi_{i,j-1}^{n-1}; i = IST...L2$

PT(ISTF)=0. ! PT=0, QT=given boundary value, 1st kind boundary condition

QT(ISTF)=F(ISTF,J,N)

DO 70 I=IST,L2

DENOM=AP(I,J)-PT(I-1)*AIM(I,J)

PT(I)=AIP(I,J)/DENOM

TEMP=CON(I,J)+AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)

QT(I)=(TEMP+AIM(I,J)*QT(I-1))/DENOM

70 ENDDO

DO 80 II=IST,L2

I=IT1-II !Recursive

F(I,J,N)=F(I+1,J,N)*PT(I)+QT(I)

80 ENDDO

90 ENDDO

Elimination
(消元)

Back
substitution
(回代)

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}};$$

$$Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}};$$

$$T_{i-1} = P_{i-1} T_i + Q_{i-1}$$

$$b + AJP\phi_{i,j+1}^{n-1} + AJM\phi_{i,j-1}^{n-1}$$

Scanning
direction



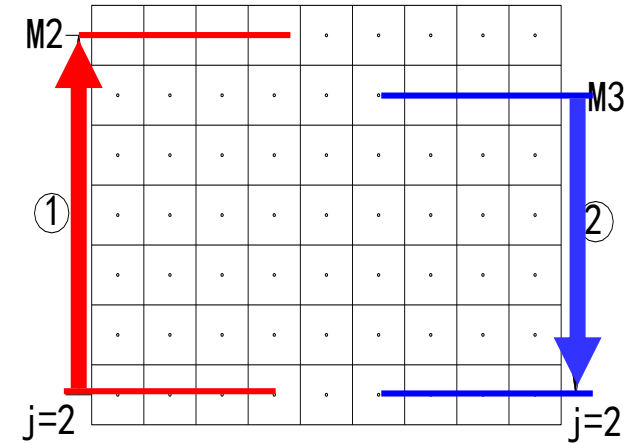
C

DO 190 JJ=JST,M3 ! Solving in I-direction, scanning from t
J=JT2-JJ !Starting from JT2 ,rather than from JT1

PT(ISTF)=0.

QT(ISTF)=F(ISTF,J,N)

} For executing 1st kind B.C.



Elimination
(消元)

DO 170 I=IST,L2

DENOM=AP(I,J)-PT(I-1)*AIM(I,J)

PT(I)=AIP(I,J)/DENOM

$$P_i = \frac{B_i}{A_i - C_i P_{i-1}};$$

TEMP=CON(I,J)+AJP(I,J)*F(I,J+1,N)+AJM(I,J)*F(I,J-1,N)

QT(I)=(TEMP+AIM(I,J)*QT(I-1))/DENOM

$$b + AJP \phi_{i,j+1}^{n-1} + AJM \phi_{i,j-1}^{n-1}$$

170 ENDDO

$$Q_i = \frac{D_i + C_i Q_{i-1}}{A_i - C_i P_{i-1}};$$

Back
substitution
(回代)

DO 180 II=IST,L2

I=IT1-II !Recursive solution

F(I,J,N)=F(I+1,J,N)*PT(I)+QT(I)

180 ENDDO

190 ENDDO

C

C-----

```
DO 290 I=IST,L2 ! Solving in J-direction, scanning from left to right
DO 270 J=JST,M2
DENOM=AP(I,J)-PT(J-1)*AJM(I,J)
PT(J)=AJP(I,J)/DENOM
TEMP=CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)
QT(J)=(TEMP+AJM(I,J)*QT(J-1))/DENOM !
270 ENDDO
DO 280 JJ=JST,M2
J=JT1-JJ !Recursive solution
F(I,J,N)=F(I,J+1,N)*PT(J)+QT(J) ! P100(a),
280 ENDDO
290 ENDDO
```

C-----

C

DO 390 II=IST,L3 ! Solving in J-direction, scanning from right to left

I=IT2-II

PT(JSTF)=0.

QT(JSTF)=F(I,JSTF,N)

DO 370 J=JST,M2

DENOM=AP(I,J)-PT(J-1)*AJM(I,J)

PT(J)=AJP(I,J)/DENOM ,

TEMP=CON(I,J)+AIP(I,J)*F(I+1,J,N)+AIM(I,J)*F(I-1,J,N)

QT(J)=(TEMP+AJM(I,J)*QT(J-1))/DENOM

370 ENDDO

DO 380 JJ=JST,M2

J=JT1-JJ !Recursive solution

F(I,J,N)=F(I,J+1,N)*PT(J)+QT(J) ! P100(a),

380 ENDDO

390 ENDDO

C*****

C*****

999 ENDDO ! (End of solution of ABEqs)

ENTRY RESET ! (CON, AP are accumulatively used, should be reset)

DO 400 J=2,M2

DO 401 I=2,L2

CON(I,J)=0.

AP(I,J)=0.

401 ENDDO

400 ENDDO

RETURN

END

CC

10.6.2.5 SUBROUTINE SETUP

CC

SUBROUTINE SETUP

C*****

USE START_L

IMPLICIT NONE

INTEGRER*4 I, J,K,N

REAL*8 REL, FL, FLM, FLP, GM, GMM, VOL, APT, AREA, SXT,

1 SXB, ARHO

C*****




```
C*****
```

```
1 FORMAT(//15X,'COMPUTATION IN CARTESIAN COORDINATES'
```

```
! Print out title for Cartesian coordinate
```

```
2 FORMAT(//15X,'COMPUTATION FOR AXISYMMETRIC SITUATION')
```

```
! Print out title for cylindrical coordinate
```

```
3 FORMAT(//15X,'COMPUTATION IN POLAR COORDINATES')
```

```
! Print out title for polar coordinate
```

```
4 FORMAT(14X,40(1H*),//)
```

```
C-----
```

Structure of SETUP

(6)-Explained
in detail

S
E
T
U
P

ENTRY SETUP1

Setup 28 one dimensional geometric parameters;
Setup initial values

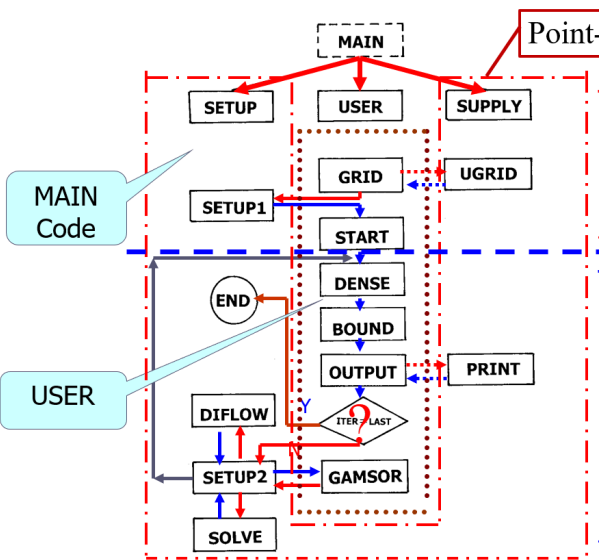
RETURN

ENTRY SETUP2

Coefficient for u equation
Coefficient for v equation
Calculate UHAT and VHAT
Coefficient for pressure equation and solve pressure
Solve u equation and v equation.
Coefficient for pressure correction equation and solve it.
Correction velocity
Coefficient for other equation and solve it (from NF=5 to 10 in order)

RETURN

SIMPLER



C-----

ENTRY SETUP1 !Set up 1D arrays, not changed during iteration

NP=NFMAX+1 ! NFMAX=10, NP=11

NRHO=NP +1 ! NRHO=12

NGAM=NRHO+1 ! NGAM=13

NCP=NGAM+1 ! NCP=14

L2=L1-1 ! Set up L2,L3,M2,M3

L3=L2-1

M2=M1-1

M3=M2-1

X(1)=XU(2) ! X(1)=XU(2)=0

DO 5 I=2,L2

X(I)=0.5*(XU(I+1)+XU(I))

5 ENDDO

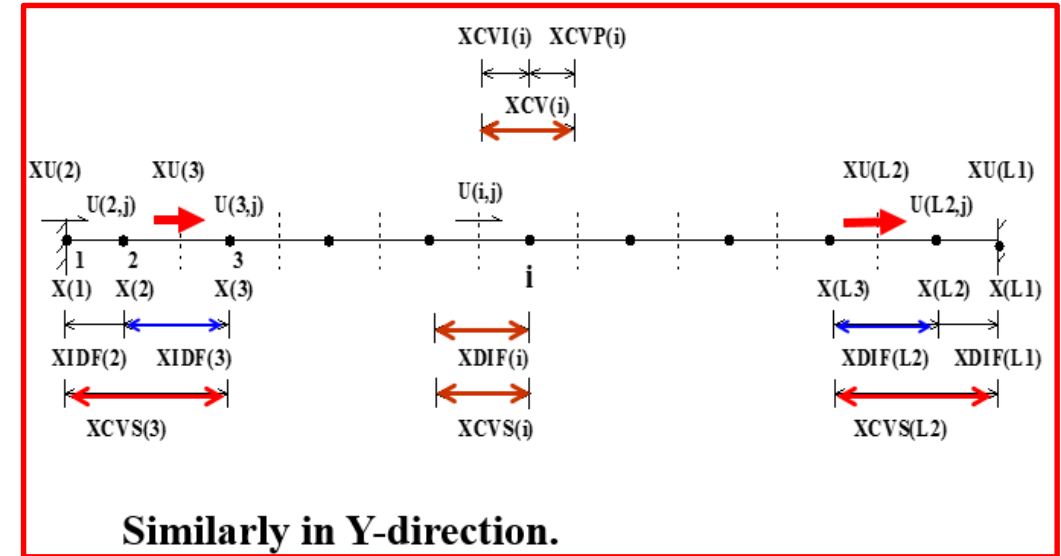
X(L1)=XU(L1)

Y(1)=YV(2) !Y(1)=YV(2)=0

DO 10 J=2,M2

Y(J)=0.5*(YV(J+1)+YV(J)) !Practice B

10 ENDDO

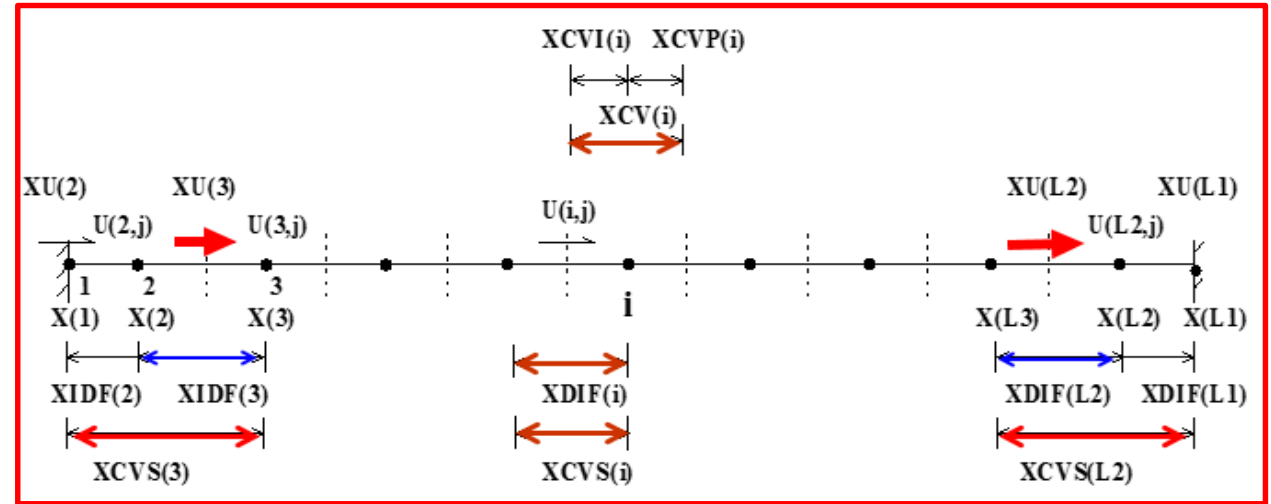


**! Practice B:
XU(I) has been
set in GRID**

```

Y(M1)=YV(M1)
DO 15 I=2,L1
XDIF(I)=X(I)-X(I-1)
15 ENDDO
DO 18 I=2,L2
XCV(I)=XU(I+1)-XU(I)
18 ENDDO
DO 20 I=3,L3

```



```

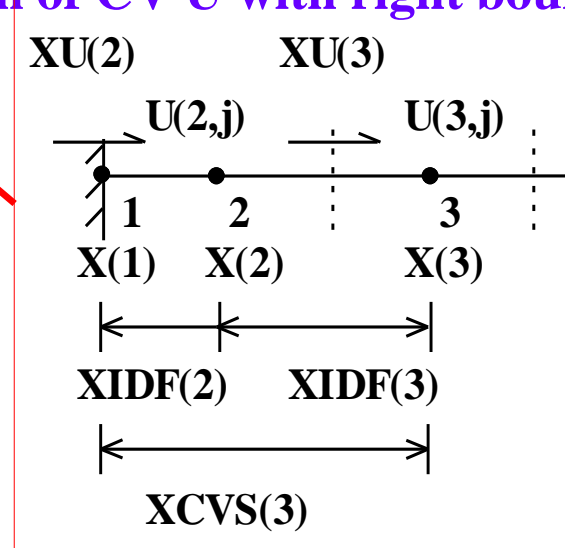
XCVS(I)=XDIF(I) ! Width of CV U (I,J) in x direction
20 ENDDO
XCVS(3)=XCVS(3)+XDIF(2) ! Width of CV U connected with left boundary
XCVS(L2)=XCVS(L2)+XDIF(L1) ! Width of CV U with right boundary

```

```

DO 22 I=3,L3
XCVI(I)=0.5*XCV(I) !  $(\delta x)_{e^-}$ 
XCVIP(I)=XCVI(I) !  $(\delta x)_{e^+}$ 
22 ENDDO

```



```

XCVI(2)=XCV(2)
XCVI(L2)=XCV(L2)
DO 35 J=2,M1
YDIF(J)=Y(J)-Y(J-1)

```

```

35 ENDDO

```

(7a)---
Explained
in detail

```

DO 40 J=2,M2
YCV(J)=YV(J+1)-YV(J) !Width of main CV in y-direction
40 ENDDO
DO 45 J=3,M2
YCVS(J)=YDIF(J) ! Width of V (I,J) in y-direction
45 ENDDO
YCVS(3)=YCVS(3)+YDIF(2)
YCVS(M2)=YCVS(M2)+YDIF(M1)
IF(MODE= =1) THEN
DO 52 J=1,M1
RMN(J)=1.0 ! Nominal radius=1
R(J)=1.0 ! for Cartesian coordinate
52 ENDDO
ELSE
DO 50 J=2,M1 !Cylindrical and polar coordinates
R(J)=R(J-1)+YDIF(J) !R(1) has defined
50 ENDDO
RMN(2)=R(1)
DO 60 J=3,M2
60 RMN(J)=RMN(J-1)+YCV(J-1) ! Radius of position of V(I,J)
60 ENDDO
RMN(M1)=R(M1)
ENDIF

```

R = 1 for both nodes and interfaces in Cartesian coordinate

(7b)---
Explained
in detail

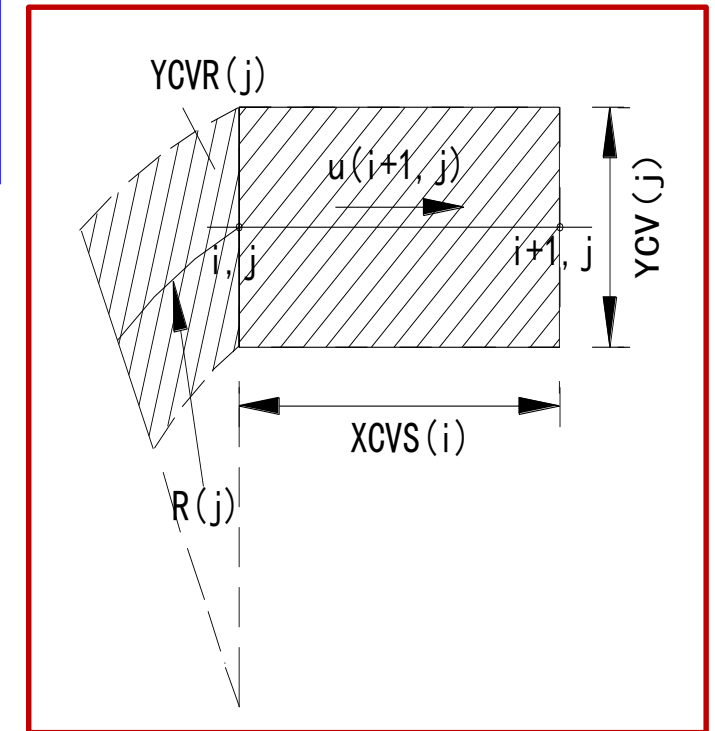
```

DO 57 J=1,M1
SX(J)=1.
SXMN(J)=1.
IF(MODE.== 3) THEN
SX(J)=R(J)
IF(J /= 1) SXMN(J)=RMN(J)
ENDIF
57 ENDDO
DO 62 J=2,M2
YCVR(J)=R(J)*YCV(J)
ARX(J)=YCVR(J)
IF(MODE = = 3) THEN
ARX(J)=YCV(J)
62 ENDDO
    
```

Set up scaling
Factor for polar
coordinate

Interface starts from J=2

!E-W conduction area of
CV for three cases, for
Cartesian R=1



```
DO 64 J=4,M3
YCVRS(J)=0.5*(R(J)+R(J-1))*YDIF(J)
```

$$ARXJ(J) = \frac{1}{2} (R(j) + RMN(j)) \cdot \frac{YCV(j)}{2} =$$

```
64 ENDDO
```

```
YCVRS(3)=0.5*(R(3)+R(1))*YCVS(3)
```

$$0.25 \left[1 + \frac{RMN(j)}{R(j)} \right] \cdot \underline{R(j)} \cdot \underline{YCV(j)} =$$

```
YCVRS(M2)=0.5*(R(M1)+R(M3))*YCVS(M2)
```

(7c)---
Explained
in detail

```
IF(MODE == 2) THEN
```

```
DO 65 J=3,M3
```

```
ARXJ(J)=0.25*(1.+RMN(J)/R(J))*ARX(J)
```

$$0.25 \left[1 + \frac{RMN(j)}{R(j)} \right] \cdot \underline{ARX(j)}$$

```
ARXJP(J)=ARX(J)-ARXJ(J)
```

```
65 ENDDO
```

```
ELSE
```

```
DO 66 J=3,M3
```

```
ARXJ(J)=0.5*ARX(J)
```

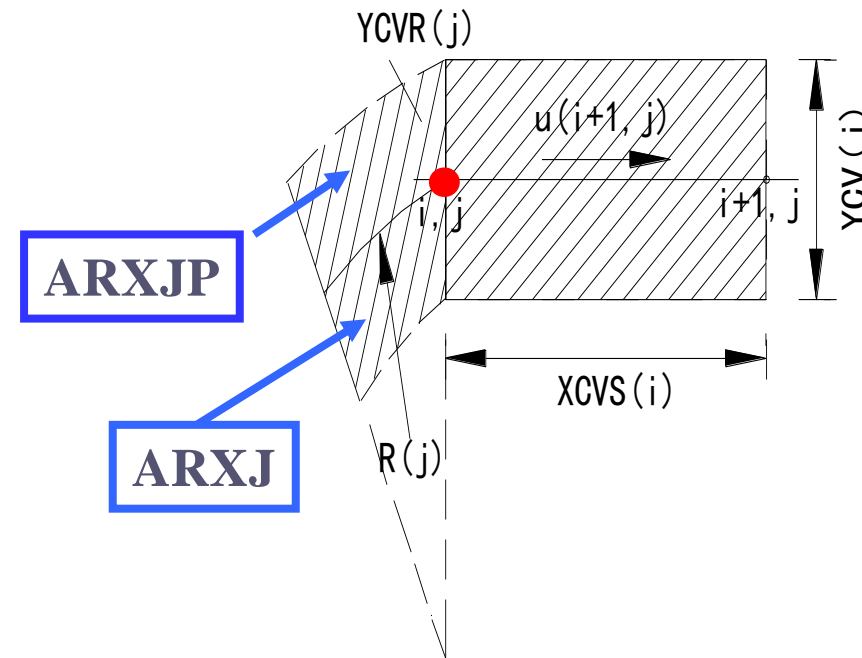
```
ARXJP(J)=ARXJ(J)
```

```
66 ENDDO
```

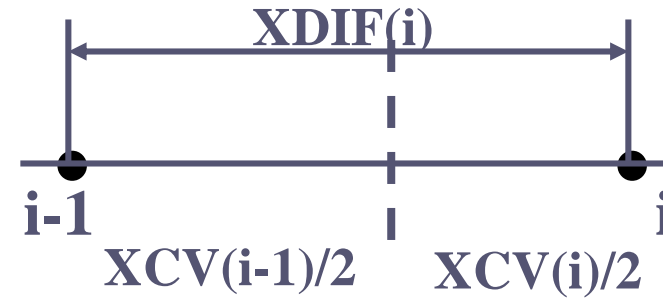
```
ENDIF
```

```
ARXJP(2)=ARX(2)
```

```
ARXJ(M2)=ARX(M2)
```



```
DO 70 J=3,M3
FV(J)=ARXJP(J)/ARX(J)
FVP(J)=1.-FV(J) !Interpolation coefficient
70 ENDDO
```



```
DO 85 I=3,L2
FX(I)=0.5*XCV(I-1)/XDIF(I) !Interpolation in x-direction
FXM(I)=1.-FX(I)
```

```
85 ENDDO
```

$$\phi_{i-1/2} = \phi_{i-1} \frac{XCV(i)/2}{XDIF(i)} + \phi_i \frac{XCV(i-1)/2}{XDIF(i)}$$

$$= \phi_{i-1} FXM(i) + \phi_i FX(i)$$

```
FX(2)=0.
FXM(2)=1.
FX(L1)=1.
FXM(L1)=0.
DO 90 J=3,M2
FY(J)=0.5*YCV(J-1)/YDIF(J) ! Interpolation in y-direction
FYM(J)=1.-FY(J)
```

```
90 ENDDO
```

```
FYM(2)=1.
FY(M1)=1.
FYM(M1)=0.
```

The first letter C is also used to indicate that this is an explanation line

CGN,AP,U,V,RHO,PC AND P ARRAYS ARE INITIALIZED HERE


```
DO 96 J=1,M1
```

```
DO 95 I=1,L1
```

```
PC(I,J)=0.
```

```
U(I,J)=0.
```

```
V(I,J)=0.
```

```
CON(I,J)=0.
```

```
AP(I,J)=0.
```

```
RHO(I,J)=RHOCON
```

```
CP (I,J)=CPCON
```

```
P(I,J)=0.
```

```
95 ENDDO
```

```
96 ENDDO
```

```
IF(MODE= =1) PRINT 1
```

```
IF(MODE= =1) WRITE(8,1)
```

```
IF(MODE= =2) PRINT 2
```

```
IF(MODE= =2) WRITE(8,2)
```

```
IF(MODE= =3) PRINT 3
```

```
IF(MODE= =3) WRITE(8,3)
```

```
PRINT 4
```

```
WRITE(8,4)
```

```
RETURN
```

Set up initial fields for iteration

Print out coordinate title of out put data

C-----

ENTRY SETUP2

CC

COEFFICIENTS FOR THE U EQUATION

NF=1 !NF=1: U; NF=2: V; NF=3: P', P; NF=NP: P

IF(LSOLVE(NF)) THEN !

IST=3

JST=2

CALL GAMSOR

REL=1.-RELAX(NF) ! (U) underrelaxation

DO 102 I=3,L2 !Coefficient of south boundary

FL=XCVI(I)*V(I,2)*RHO(I,1)

FLM=XCVIP(I-1)*V(I-1,2)*RHO(I-1,1)

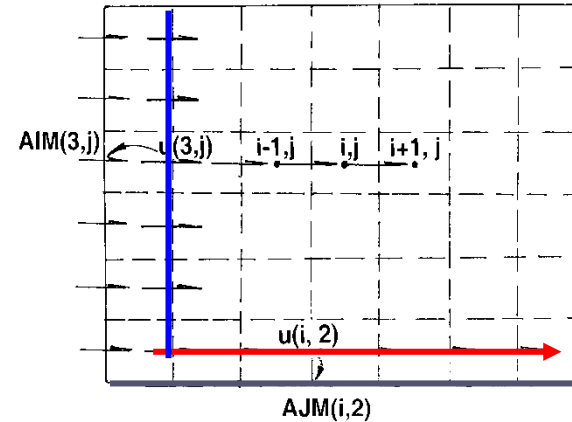
FLOW=R(1)*(FL+FLM) ! Flow rate through south interface

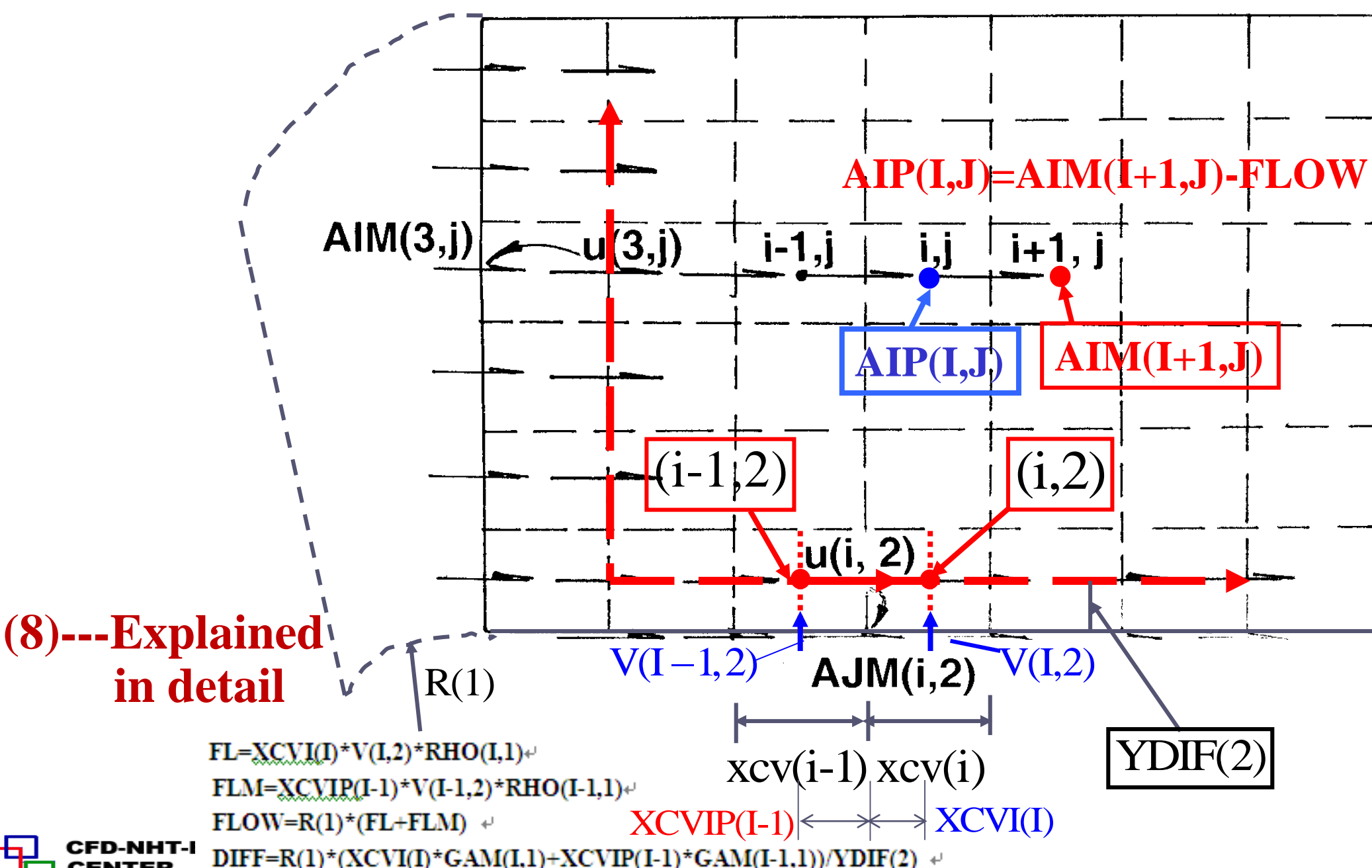
DIFF=R(1)*(XCVI(I)*GAM(I,1)+XCVIP(I-1)*GAM(I-1,1))/YDIF(2)

CALL **DIFLOW** !With DIFF and FLOW at hand, CALL DIFLOW to get D.A(|P|);

AJM(I,2)=ACOF+AMAX1(0.,FLOW) Coefficient a_s

102 ENDDO





Explanation of DIFF(Diffusion conductance)

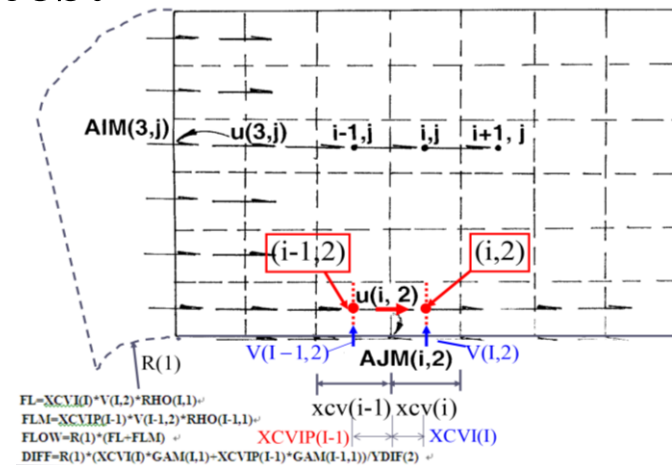
$$DIFF=R(1)*(XCVI(I)*GAM(I,1)+XCVIP(I-1)*GAM(I-1,1))/YDIF(2)$$

For Cartesian coordinates:

$$D_{n-e} = \frac{(\delta x)_{e^-}}{(\delta y)_n} + \frac{(\delta x)_{e^+}}{(\delta y)_n} = \frac{(\delta x)_{e^-} \Gamma_n + (\delta x)_{e^+} \Gamma_{ne}}{(\delta y)_n}$$

For Cylindrical coordinates:

$$D_{n-e} = R1 \left[\frac{(\delta x)_{e^-} \Gamma_n + (\delta x)_{e^+} \Gamma_{ne}}{(\delta y)_n} \right]$$



```

DO 103 J=2,M2
FLOW=ARX(J)*U(2,J)*RHO(1,J)
DIFF=ARX(J)*GAM(1,J)/(XCV(2)*SX(J))
CALL DIFLOW ! Get A(|P|)
AIM(3,J)=ACOF+AMAX1(0.,FLOW) !Coefficient  $a_w$ 
DO 104 I=3,L2
IF(I == L2) THEN
FLOW=ARX(J)*U(L1,J)*RHO(L1,J)
DIFF=ARX(J)*GAM(L1,J)/(XCV(L2)*SX(J)) ! DW
ELSE
FL=U(I,J)*(FX(I)*RHO(I,J)+FXM(I)*RHO(I-1,J))
FLP=U(I+1,J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
FLOW=ARX(J)*0.5*(FL+FLP)
DIFF=ARX(J)*GAM(I,J)/(XCV(I)*SX(J))
ENDIF
CALL DIFLOW ! A(|P|)
AIM(I+1,J)=ACOF+AMAX1(0.,FLOW)  $D \bullet A(|P_\Delta|) + 0, F$ 
AIP(I,J)=AIM(I+1,J)-FLOW ! Relationship between coefficients
    
```

```

IF(J == M2) THEN
FL=XCVI(I)*V(I,M1)*RHO(I,M1)
FLM=XCVIP(I-1)*V(I-1,M1)*RHO(I-1,M1)
DIFF=R(M1)*(XCVI(I)*GAM(I,M1)+XCVIP(I-1)*GAM(I-1,M1))/YDIF(M1)
ELSE
FL=XCVI(I)*V(I,J+1)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))
FLM=XCVIP(I-1)*V(I-1,J+1)*(FY(J+1)*RHO(I-1,J+1)+FYM(J+1)*
& RHO(I-1,J))
GM=GAM(I,J)*GAM(I,J+1)/(YCV(J)*GAM(I,J+1)+YCV(J+1)*GAM(I,J)+
& 1.0E-30)*XCVI(I)
GMM=GAM(I-1,J)*GAM(I-1,J+1)/(YCV(J)*GAM(I-1,J+1)+YCV(J+1)*
& GAM(I-1,J)+1.E-30)*XCVIP(I-1)
DIFF=RMN(J+1)*2.*(GM+GMM)
ENDIF
FLOW=RMN(J+1)*(FL+FLM)
CALL DIFLOW ! A(|P|)
AJM(I,J+1)=ACOF+AMAX1(0.,FLOW) ! Coefficient  $a_s$ 
AJP(I,J)=AJM(I,J+1)-FLOW ! Relationship between coefficients
    
```

(9)---
Explained
in detail

VOL=YCVR(J)*XCVS(I) !Volume of velocity CV
APT=(RHO(I,J)*XCVI(I)+RHO(I-1,J)*XCVIP(I-1))
&/((XCVS(I)*DT) ! Unsteady term $\rho/\Delta t$; DT--- Δt ;
AP(I,J)=AP(I,J)-APT ! AP (I,J) at right side is S_p
CON(I,J)=CON(I,J)+APT*U(I,J)
AP(I,J)=(-AP(I,J)*VOL+AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J))
&/RELAX(NF) !Underrelaxation is organized during solution procedure
CON(I,J)=CON(I,J)*VOL+REL*AP(I,J)*U(I,J) ! REL=1 - α
DU(I,J)=VOL/(XDIF(I)*SX(J)) ! To get flow area
DU(I,J)=DU(I,J)/AP(I,J) ! d_e in velocity correction

$$a_p^0 = \frac{\rho_P \Delta V}{\Delta t}$$

$$! d_e = A_e / a_e$$

104 ENDDO

103 ENDDO

! Come here we have finished the coefficients calculation for **u velocity** and should store them temporary to leave COF empty for calculation coefficients for **velocity v**.

$$b = S_c \Delta V + a_p^0 \phi_p^0 + (1 - \alpha) \frac{a_p}{\alpha} \phi_p^0$$

$$a_p = \left(\sum a_{nb} + \rho_P \Delta V / \Delta t - S_p \Delta V \right) / \alpha$$

-----Review of SIMPLER algorithm-----

1. Assuming initial fields, determine coefficients of discretized u, v eqs.;
2. Calculating pseudo-velocity u, \tilde{v} ;

(10)---Explained in detail

$$a_e u_e = \sum a_{nb} u_{nb} + b + A_e (p_P - p_E)$$

$$u_e = \sum \frac{a_{nb} u_{nb} + b}{a_e} + \frac{A_e}{a_e} (p_P - p_E) \quad \longrightarrow \quad u_e = \tilde{u}_e + \frac{A_e}{a_e} (p_P - p_E)$$

and **Solving pressure equation**, obtaining p^* ;

$$a_P p_P = a_E p_E + a_W p_W + a_N p_N + a_S p_S + b$$

$$a_P = a_E + a_W + a_N + a_S$$

$$a_E = d_e A_e \rho_e \quad a_W = d_w A_w \rho_w \quad a_n = d_n A_n \rho_n \quad a_S = d_s A_s \rho_s$$

$$b = [(\rho u)_w - (\rho u)_s] A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n] A_n$$

Coefficients of u, v momentum equations are needed for determining coefficients of pressure equation.

3. Solving momentum equations based on p^* , obtaining u^*, v^*

4. Solving pressure correction equation based on u^*, v^* , obtaining p'

In pressure equation:
$$b = [(\rho u)_w - (\rho u)_s]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$$

In pressure correction equation:
$$b = [(\rho u^*)_w - (\rho u^*)_s]A_e + [(\rho v^*)_s - (\rho v^*)_n]A_n$$

5. Correcting velocity $u = u^* + u'$; $v = v^* + v'$, where u' and v' are determined based on p'

$$u'_e = \frac{A_e}{a_e} (p'_P - p'_E) = d_e (p'_P - p'_E)$$

6. Taking the updated velocity , repeating steps 1-6, until convergence is reached.

-----End of Review of SIMPLER algorithm-----

MODULE START_L

PARAMETER (NI=100,NJ=200,NIJ=NI,NFMAX=10,NFX4=NFMAX+4)

C*****

CHARACTER*8 TITLE(NFX4)

LOGICAL LSOLVE(NFX4),LPRINT(NFX4),LBLK(NFX4),LSTOP

REAL*8,DIMENSION(NI,NJ,NFX4)::F

REAL*8,DIMENSION(NI,NJ,6)::COF,COFU,COFV,COFP

REAL*8,DIMENSION(NI,NJ)::P,RHO,GAM,CP,CON,AIP,AIM,AJP,AJM,AP

C*****

EQUIVALENCE(F(1,1,1),U(1,1)),(F(1,1,2),V(1,1)),(F(1,1,3),PC(1,1))
1, (F(1,1,4),T(1,1))

EQUIVALENCE(F(1,1,11),P(1,1)),(F(1,1,12),RHO(1,1)),(F(1,1,13))
1,GAM(1,1),(F(1,1,14),CP(1,1))

EQUIVALENCE(COF(1,1,1),CON(1,1)),(COF(1,1,2),AIP(1,1)),
1(COF(1,1,3),AIM(1,1)),(COF(1,1,4),AJP(1,1)),
2(COF(1,1,5),AJM(1,1)),(COF(1,1,6),AP(1,1))

REAL*8,DIMENSION(NI)::TH,THU,THDIF,THCV,THCVS

REAL*8 THL

EQUIVALENCE(X,TH),(XU,THU),(XDIF,THDIF),(XCV,THCV),
1(XCVS,THCVS),(XL,THL)

DATA LSTOP,LSOLVE,LPRINT/.FALSE.,NFX4*.FALSE., NFX4*.FALSE./

DATA LBLK/NFX4*.TRUE./

DATA MODE,LAST,TIME,ITER/1,5,0.,0/

DATA RELAX,NTIMES/NFX4*1.,NFX4*1/

DATA DT,IPREF,JPREF,RHOCON,CPCON/1.E+30, 1,1,1.,1./

END MODULE

COFU(IST:L2, JST:M2, 1:6)=COF(IST:L2,JST:M2,1:6) ! Transfer the coefficients

! Store coefficients of U temporary as follows:

COF(I,J,1)	COF(I,J,2)	COF(I,J,3)	COF(I,J,4)	COF(I,J,5)	COF(I,J,6)
CON (I,J)	AIP(I,J)	AIM(I,J)	AJP(I,J)	AJM(I,J)	AP(I,J)

Explain

! In SIMPLER to solve pressure eq., coefficients of both u -eq. and v -eq. are needed. Only u -coefficients are not enough. Thus, u -coefficients are temporary stored, and v -eq. coefficients are computed by using array **COF(I,J)**

COEFFICIENTS FOR THE V EQUATION- (Determine coefficients of V)

NF=2 !

CALL RESET !Set zero values for AP(I,J),CON(I,J)

IST=2

JST=3

CALL GAMSOR

REL=1.-RELAX(NF)

**(11)---Explained
in detail**

```

DO 202 I=2,L2
AREA=R(1)*XCV(I)
FLOW=AREA*V(I,2)*RHO(I,1)
DIFF=AREA*GAM(I,1)/YCV(2)
CALL DIFLOW
AJM(I,3)=ACOF+AMAX1(0.,FLOW) !  $a_s$ 

```

202 ENDO

```

DO 203 J=3,M2
FL=ARXJ(J)*U(2,J)*RHO(1,J)
FLM=ARXJP(J-1)*U(2,J-1)*RHO(1,J-1)
FLOW=FL+FLM
DIFF=(ARXJ(J)*GAM(1,J)+ARXJP(J-1)*GAM(1,J-1))/(XDIF(2)*SXMN(J))
CALL DIFLOW

```

```

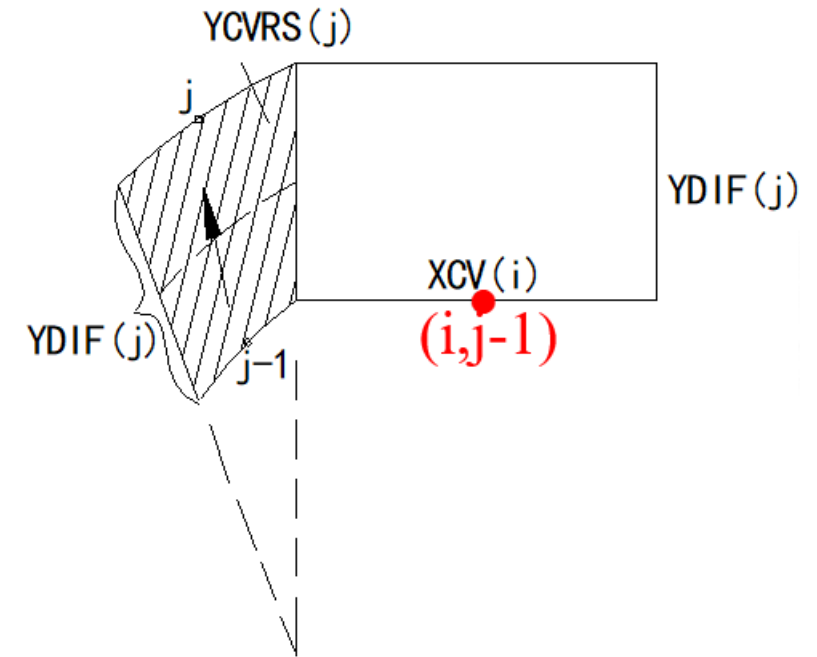
AIM(2,J)=ACOF+AMAX1(0.,FLOW) !  $a_w$ 

```

```

DO 204 I=2,L2
IF(I= L2) THEN
FL=ARXJ(J)*U(L1,J)*RHO(L1,J)
FLM=ARXJP(J-1)*U(L1,J-1)*RHO(L1,J-1)
DIFF=(ARXJ(J)*GAM(L1,J)+ARXJP(J-1)*GAM(L1,J-
& -1))/(XDIF(L1)*SXMN(J))

```



```
ELSE
FL=ARXJ(J)*U(I+1,J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
FLM=ARXJP(J-1)*U(I+1,J-1)*(FX(I+1)*RHO(I+1,J-1)+FXM(I+1)*RHO(I,J-1))
GM=GAM(I,J)*GAM(I+1,J)/(XCV(I)*GAM(I+1,J)+XCV(I+1)*GAM(I,J)+
& 1.E-30)*ARXJ(J)
GMM=GAM(I,J-1)*GAM(I+1,J-1)/(XCV(I)*GAM(I+1,J-1)+XCV(I+1)*
& GAM(I,J-1)+1.0E-30)*ARXJP(J-1)
DIFF=2.*(GM+GMM)/SXMN(J)
ENDIF
FLOW=FL+FLM
CALL DIFLOW
AIM(I+1,J)=ACOF+AMAX1(0.,FLOW) ! aw
AIP(I,J)=AIM(I+1,J)-FLOW ! Relationship between coefficients
IF (J= =M2) THEN
AREA=R(M1)*XCV(I)
FLOW=AREA*V(I,M1)*RHO(I,M1)
```

```
DIFF=AREA*GAM(I,M1)/YCV(M2)
ELSE
AREA=R(J)*XCV(I)
FL=V(I,J)*(FY(J)*RHO(I,J)+FYM(J)*RHO(I,J-1))*RMN(J)
FLP=V(I,J+1)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))*RMN(J+1)
FLOW=(FV(J)*FL+FVP(J)*FLP)*XCV(I)
DIFF=AREA*GAM(I,J)/YCV(J)
ENDIF
CALL DIFLOW
AJM(I,J+1)=ACOF+AMAX1(0.,FLOW) ! as
AJP(I,J)=AJM(I,J+1)-FLOW !Relationship
VOL=YCVRS(J)*XCV(I) !Volume of V- CV
SXT=SX(J)
```

$$APT=(ARXJ(J)*RHO(I,J)*0.5*(SXT+SXMN(J))+ARXJP(J-1)*RHO(I,J-1)*$$

$$\&0.5*(SXB+SXMN(J)))/(YCVRS(J)*DT)$$

$$AP(I,J)=AP(I,J)-APT$$

$$CON(I,J)=CON(I,J)+APT*V(I,J)$$

$$AP(I,J)=(-AP(I,J)*VOL+AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J))$$

&/RELAX(NF)

$$CON(I,J)=CON(I,J)*VOL+REL*AP(I,J)*V(I,J)$$

$$DV(I,J)=VOL/YDIF(J)$$

$$DV(I,J)=DV(I,J)/AP(I,J)$$

204 ENDDO

203 ENDDO

$$COFV(IST:L2,JST:M2,1:6)=COF(IST:L2,JST:M2,1,6)$$

! Store coefficients of V-eq. to compute coefficients of P-equation

CALCULATE UHAT AND VHAT !

DO 150 J=2,M2

DO 151 I=3,L2

$$UHAT(I,J)=(COFU(I,J,2)*U(I+1,J)+COFU(I,J,3)*U(I-1,J)+COFU(I,J,4)$$

$$\&*U(I,J+1)+COFU(I,J,5)*U(I,J-1)+COFU(I,J,1))/COFU(I,J,6)$$

! Compute u, \tilde{v}

$$u_e = \sum \frac{a_{nb} u_{nb} + b}{a_e}$$


```

151 ENDDO
150 ENDDO
    DO 250 J=3,M2
    DO 251 I=2,L2
    VHAT(I,J)=(COFV(I,J,2)*V(I+1,J)+COFV(I,J,3)*V(I-1,J)+COFV(I,J,4)
    & *V(I,J+1)+COFV(I,J,5)*V(I,J-1)+COFV(I,J,1))/COFV(I,J,6)
251 ENDDO
250 ENDDO
    
```

COEFFICIENTS FOR THE PRESSURE EQUATION-----

```

NF=3
CALL RESET
IST=2
JST=2
CALL GAMSOR
DO 410 J=2,M2,
DO 411 I=2,L2
VOL=YCVR(J)*XCV(I)
CON(I,J)=CON(I,J)*VOL
411 ENDDO
410 ENDDO
    
```

!In the discretized pressure equation, the source term is

$$! \quad b = [(\rho u)_w - (\rho u)_e]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$$
!This term has to be computed for every interface of a CV!

!Volume of main CV.
!Pressure has no inherent source term, here setting this
!operation just for general purpose .Usually CON(I,J)=0

! For boundary CV, actual velocity is used.

**(12)
Explained
in detail**

DO 402 I=2,L2

ARHO=R(1)*XCV(I)*RHO(I,1)

累加 ! $b = [(\rho u)_w - (\rho u)_e]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$

CON(I,2)=CON(I,2)+ARHO*V(I,2) ! Accumulative add

AJM(I,2)=0 ! $a_s = 0$, Adiabatic boundary

402 ENDDO

DO 403 J=2,M2

ARHO=ARX(J)*RHO(1,J)

CON(2,J)=CON(2,J)+ARHO*U(2,J) ! Accumulative addition

AIM(2,J)=0. ! $a_w = 0$, Adiabatic boundary

DO 404 I=2,L2

IF(I= =L2) THEN ! For boundary CV, actual velocity is used.

ARHO=ARX(J)*RHO(L1,J)

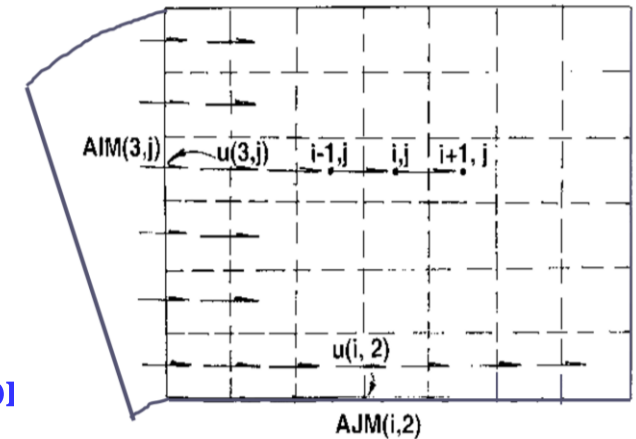
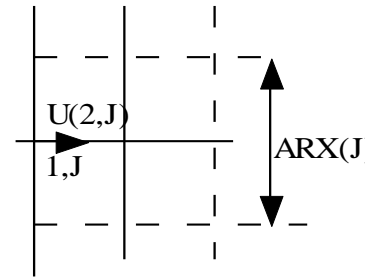
CON(I,J)=CON(I,J)-ARHO*U(L1,J) ! Accumulative addition

AIP(I,J)=0. ! $a_E = 0$

! $b = [(\rho u)_w - (\rho u)_e]A_e + [(\rho \tilde{v})_s - (\rho \tilde{v})_n]A_n$

ELSE

ARHO=ARX(J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))



FLOW=ARHO*UHAT(I+1,J) ! For inner CV, UHAT is used.

CON(I,J)=CON(I,J)-FLOW

CON(I+1,J)=CON(I+1,J)+FLOW !

AIP(I,J)=ARHO*DU(I+1,J) ! a_E

AIM(I+1,J)=AIP(I,J) ! Relationship between (a_w) and $(a_E)_{i+1}$

ENDIF

IF(J= =M2) THEN

ARHO=RMN(M1)*XCV(I)*RHO(I,M1)

CON(I,J)=CON(I,J)-ARHO*V(I,M1) ! Accumulative addition

AJP(I,J)=0. ! North coefficient of M2

ELSE

ARHO=RMN(J+1)*XCV(I)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))

FLOW=ARHO*VHAT(I,J+1) ! For inner CV, VHAT is used.

CON(I,J)=CON(I,J)-FLOW

CON(I,J+1)=CON(I,J+1)+FLOW

AJP(I,J)=ARHO*DV(I,J+1)

AJM(I,J+1)=AJP(I,J) ! Relationship between coefficients

ENDIF

```
AP(I,J)=AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J)
404 ENDDO
403 ENDDO
DO 421 J=2,M2
DO 422 I=2,L2
AP(I,J)=AP(I,J)/RELAX(NP) ! Pressure underrelaxation
CON(I,J)=CON(I,J)+(1.0-RELAX(NP))*AP(I,J)*P(I,J)
422 ENDDO
421 ENDDO
COFP(IST:L2,JST:M2,2:5)=COF(IST:L2,JST:M2,2:5)
```

(13)

Explained
in detail

!Store a_E, a_W, a_N, a_S for p -correction equation

! while CON (b) and AP (a_p) are not stored; Because AP has been
! underrelaxed, and the velocity in b term of p -correction eq. is different.

NF=NP !NFMAX+1; P(I,J) is one member of F(I,J,NF)

CALL **SOLVE** ! Solving P-equation

COMPUTE U AND V! Pressure has been solved

NF=1

IST=3

JST=2

COF(IST:L2,JST:M2,1:6)=COFU(IST:L2,JST:M2,1:6) ! Coefficients of U

DO 551 J=JST,M2

DO 552 I=IST,L2

CON(I,J)=CON(I,J)+DU(I,J)*AP(I,J)*(P(I-1,J)-P(I,J))

522 ENDDO

521 ENDDO

CALL **SOLVE** !Solving U equation

C-----

NF=2

IST=2

JST=3

COF(IST:L2,JST:M2,1:6)=COFV(IST:L2,JST:M2,1:6) !Coefficients of V

DO 553 J=JST,M2

DO 554 I=IST,L2

CON(I,J)=CON(I,J)+DV(I,J)*AP(I,J)*(P(I,J-1)-P(I,J))

```
CON(I,J)=CON(I,J)+DV(I,J)*AP(I,J)*(P(I,J-1)-P(I,J))
554 ENDDO
553 ENDDO
```

CALL **SOLVE** ! Solving V-equation. Such U V are temporary, need to be
! improved

COEFFICIENTS FOR THE PRESSURE CORRECTION EQUATION

```
NF=3 ! P-correction equation
CALL RESET ! Zero of CON(I,j) and AP(i,j)
IST=2
JST=2
COF(IST:L2,JST:M2,2:5)=COFP(IST:L2,JST:M2,2:5)
! Transfer coefficients of P-eq. to P-correction equation.
CALL GAMSOR
SMAX=0.
SSUM=0.
```

$$! b = [(\rho u^*)_w - (\rho u^*)_e]A_e + [(\rho v^*)_s - (\rho v^*)_n]A_n$$

! The velocities just solved are u^* and v^*

```

DO 510 J=2,M2
DO 511 I=2,L2
VOL=YCVR(J)*XCV(I)      ! Volume of PCV
CON(I,J)=CON(I,J)*VOL
511 ENDDO
510 ENDDO                !  $b = [(\rho u^*)_w - (\rho u^*)_e]A_e + [(\rho v^*)_s - (\rho v^*)_n]A_n$ 
DO 502 I=2,L2
ARHO=R(1)*XCV(I)*RHO(I,1)
CON(I,2)=CON(I,2)+ARHO*V(I,2) ! Source term b
502 ENDDO
DO 503 J=2,M2
ARHO=ARX(J)*RHO(1,J)
CON(2,J)=CON(2,J)+ARHO*U(2,J)
DO 504 I=2,L2
IF(I= =L2) THEN
ARHO=ARX(J)*RHO(L1,J)
CON(I,J)=CON(I,J)-ARHO*U(L1,J) ! Calculate b-term
ELSE
ARHO=ARX(J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
FLOW=ARHO*U(I+1,J) ! Adopt U*,V* to solve P'
CON(I,J)=CON(I,J)-FLOW
CON(I+1,J)=CON(I+1,J)+FLOW
    
```

Do loop
502—
504 for
mass
source
of each
CV

```
ENDIF
IF(J= =M2) THEN
ARHO=RMN(M1)*XCV(I)*RHO(I,M1)
CON(I,J)=CON(I,J)-ARHO*V(I,M1)
ELSE
ARHO=RMN(J+1)*XCV(I)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))
FLOW=ARHO*V(I,J+1)
CON(I,J)=CON(I,J)-FLOW
CON(I,J+1)=CON(I,J+1)+FLOW
ENDIF
AP(I,J)=AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J) ← For AP
PC(I,J)=0. ! Initial field
SMAX=AMAX1(SMAX,ABS(CON(I,J))) ! Take the maximum
SSUM=SSUM+CON(I,J) ! Summation of b
504 ENDDO
503 ENDDO
CALL SOLVE ! Solving p-correction equation
```


COME HERE TO CORRECT THE VELOCITIES

```
DO 521 J=2,M2
DO 522 I=2,L2
IF(I/=2) U(I,J)=U(I,J)+DU(I,J)*(PC(I-1,J)-PC(I,J)) ! Correcting velocity u
IF(J/=2) V(I,J)=V(I,J)+DV(I,J)*(PC(I,J-1)-PC(I,J)) ! Correcting velocity v
522 ENDDO
521 ENDDO
500 ENDIF
```

COEFFICIENTS FOR OTHER EQUATIONS-----

```
IST=2
JST=2
DO 600 N=4,NFMAX !NF>=4
NF=N
IF(LSOLVE(NF)) THEN
CALL GAMSOR
IF(LSOLE(4)) THEN
DO I=1,L1
DO J=1,M1
RHO(I,J)=RHO(I,J)*CP(I,J) ! Nominal density for temperature
ENDDO
ENDDO
REL=1.-RELAX(NF)
```

(14) Explain
in detail

```
DO 602 I=2,L2
AREA=R(1)*XCV(I)
FLOW=AREA*V(I,2)*RHO(I,1)
DIFF=AREA*GAM(I,1)/YDIF(2)
CALL DIFLOW
AJM(I,2)=ACOF+AMAX1(0.,FLOW)
```

```
602 ENDDO
```

```
DO 603 J=2,M2
FLOW=ARX(J)*U(2,J)*RHO(1,J)
DIFF=ARX(J)*GAM(1,J)/(XDIF(2)*SX(J))
CALL DIFLOW
AIM(2,J)=ACOF+AMAX1(0.,FLOW)
DO 604 I=2,L2
IF(I==L2) THEN
FLOW=ARX(J)*U(L1,J)*RHO(L1,J)
DIFF=ARX(J)*GAM(L1,J)/(XDIF(L1)*SX(J))
ELSE
FLOW=ARX(J)*U(I+1,J)*(FX(I+1)*RHO(I+1,J)+FXM(I+1)*RHO(I,J))
DIFF=ARX(J)*2.*GAM(I,J)*GAM(I+1,J)/((XCV(I)*GAM(I+1,J)+
```

```
& XCV(I+1)*GAM(I,J)+1.0E-30)*SX(J)
ENDIF
CALL DIFLOW
AIM(I+1,J)=ACOF+AMAX1(0.,FLOW)
AIP(I,J)=AIM(I+1,J)-FLOW
AREA=RMN(J+1)*XCV(I)
IF(J= = M2) THEN
FLOW=AREA*V(I,M1)*RHO(I,M1)
DIFF=AREA*GAM(I,M1)/YDIF(M1)
ELSE
FLOW=AREA*V(I,J+1)*(FY(J+1)*RHO(I,J+1)+FYM(J+1)*RHO(I,J))
DIFF=AREA*2.*GAM(I,J)*GAM(I,J+1)/(YCV(J)*GAM(I,J+1)+
& YCV(J+1)*GAM(I,J)+1.0E-30)
ENDIF
CALL DIFLOW
```

```

AJM(I,J+1)=ACOF+AMAX1(0.,FLOW)
AJP(I,J)=AJM(I,J+1)-FLOW
VOL=YCVR(J)*XCV(I)
APT=RHO(I,J)/DT ! Transient term  $\rho/\Delta t$  without volume
AP(I,J)=AP(I,J)-APT
CON(I,J)=CON(I,J)+APT*F(I,J,NF)
AP(I,J)=(-AP(I,J)*VOL+AIP(I,J)+AIM(I,J)+AJP(I,J)+AJM(I,J))
&/RELAX(NF)
CON(I,J)=CON(I,J)*VOL+REL*AP(I,J)*F(I,J,NF)
604 ENDO
603 ENDO
CALL SOLVE !
IF (LSLVE(4)) THEN ! If the temp. eq. is solved ,then Reset density back to rho
DO I=I,L1
DO J=1,M1
RHO(I,J)=RHO(I,J)/CP(I,J) ! Reset density back to rho
ENDDO
ENDDO
ENDIF
ENDIF
600 ENDDO (End of the solving process)
TIME=TIME+DT ! Forward time
ITER=ITER+1 ! Increase the indicator
IF(ITER>= LAST) LSTOP=.TRUE. RETURN
END

```

$$a_p = (\sum a_{nb} + \rho_p \Delta V / \Delta t - S_p \Delta V) / \alpha$$

$$b = S_c \Delta V + a_p^0 \phi_p^0 + (1 - \alpha) \frac{a_p}{\alpha} \phi_p^0$$

Transient,
Linear----
Steady,
nonlinear

(15)---Explained
in detail

C*****

```
10 FORMAT(1X,26(1H*),3X,A10,3X,26(1H*))
20 FORMAT(1X,4H I =,I6,6I9)
30 FORMAT(1X,' J')
40 FORMAT(1X,I3,2X,1P7E9.2)
50 FORMAT(1X,1H )
51 FORMAT(2X,'I =',2X,7(I4,5X))
52 FORMAT(2X,'X =',1P7E9.2)
53 FORMAT(1X,' TH =',1P7E9.2)
54 FORMAT(2X,'J =',2X,7(I4,5X))
55 FORMAT(2X,'Y =',1P7E9.2)
```

!1P7E9.2

!1P---1 integral digit of each data;

!7E---7 data in scientific expression

! 9.2---Each data contains 9 places, and there are two decimal places (小数2位)

C*****

```
ENTRY UGRID
XU(2)=0.
DX=XL/FLOAT(L1-2)
DO 1 I=3,L1
XU(I)=XU(I-1)+DX
1 ENDDO
YV(2)=0.
DY=YL/FLOAT(M1-2)

DO 2 J=3,M1
YV(J)=YV(J-1)+DY
2 ENDDO
RETURN
```

2.00E+00	2.30E+00	2.90E+00	3.50E+00	4.10E+00	4.70E+00	5.00E+00
1.80E+00	2.08E+00	2.64E+00	3.20E+00	3.76E+00	4.32E+00	4.60E+00
1.40E+00	1.64E+00	2.12E+00	2.60E+00	3.08E+00	3.56E+00	3.80E+00
1.00E+00	1.20E+00	1.60E+00	2.00E+00	2.40E+00	2.80E+00	3.00E+00
6.00E-01	7.60E-01	1.08E+00	1.40E+00	1.72E+00	2.04E+00	2.20E+00
2.00E-01	3.20E-01	5.60E-01	8.00E-01	1.04E+00	1.28E+00	1.40E+00
0.00E+00	1.00E-01	3.00E-01	5.00E-01	7.00E-01	9.00E-01	1.00E+00

(16)---Explained in detail

C*****

ENTRY **PRINT**

! For print out, NF=3
represents stream function

DO 82 J=3,M1

IF(LPRINT(3)) THEN

CALCULATE THE STREAM FUNCTION

F(2,2,3)=0.

DO 81 I=2,L1

IF(I.NE.2) F(I,2,3)=F(I-1,2,3)-RHO(I-1,1)*V(I-1,2)

&*R(1)*XCV(I-1) ! I=2, F(2,2,3)=0;

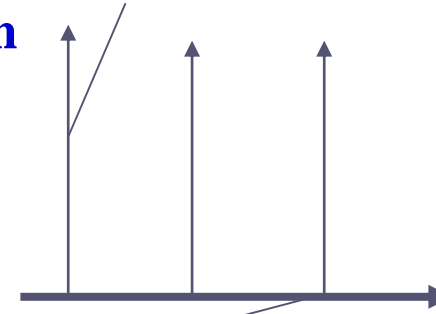
DO 82 J=3,M1

RHOM=FX(I)*RHO(I,J-1)+FXM(I)*RHO(I-1,J-1)

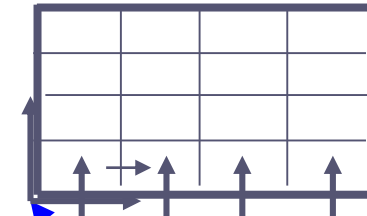
F(I,J,3)=F(I,J-1,3)+RHOM*U(I,J-1)*ARX(J-1) !

82 ENDDO

81 ENDDO



DO 82 I=2,L1



F(2,2,3)=0

$$\rho u r = \frac{\partial \psi}{\partial y}; \rho v r = -\frac{\partial \psi}{\partial x} \quad \psi = -\int \rho v r dx \quad \psi = \int \rho u r dy$$

(17)---

Explained
in detail

For bottom, from left to right

$$\psi_{i,2} = \psi_{i-1,2} - \sum_{i=3} \rho_{i-1,1} v_{i-1,2} r(1) \Delta x_i$$

For vertical, from bottom to top

$$\psi_{i,j} = \psi_{i,j-1} + \rho_m u_{i,j-1} r(j) \Delta y_j$$

```
IF(LPRINT(NP)) THEN
CONSTRUCT BOUNDARY PRESSURES BY EXTRAPOLATION
DO 91 J=2,M2
P(1,J)=(P(2,J)*XCVS(3)-P(3,J)*XDIF(2))/XDIF(3)
P(L1,J)=(P(L2,J)*XCVS(L2)-P(L3,J)*XDIF(L1))/XDIF(L2)
91 ENDDO
DO 92 I=2,L2
P(I,1)=(P(I,2)*YCVS(3)-P(I,3)*YDIF(2))/YDIF(3)
P(I,M1)=(P(I,M2)*YCVS(M2)-P(I,M3)*YDIF(M1))/YDIF(M2)
92 ENDDO
P(1,1)=P(2,1)+P(1,2)-P(2,2)
P(L1,1)=P(L2,1)+P(L1,2)-P(L2,2)
P(1,M1)=P(2,M1)+P(1,M2)-P(2,M2)
P(L1,M1)=P(L2,M1)+P(L1,M2)-P(L2,M2)
PREF=P(IPREF,JPREF) ! Reference point of pressure
DO 93 J=1,M1
DO 93 I=1,L1
P(I,J)=P(I,J)-PREF ! Relative pressure
94ENDDO
93ENDDO
ENDIF
```


**(17a)---Explained
in detail**

```
PRINT 50 ! Print out to screen
WRITE(8,50) ! Output into file
IEND=0
DO WHILE (IEND/=L1)
IBEG=IEND+1
IEND=IEND+7 ! !7 data in each line
IEND=MIN0(IEND,L1) ! Take minimum
PRINT 50
WRITE(8,50)
PRINT 51,(I,I=IBEG,IEND) !From IBEG to IEND for printing
WRITE(8,51) (I,I=IBEG,IEND)
IF(MODE/=3) THEN
PRINT 52,(X(I),I=IBEG,IEND)
WRITE(8,52) (X(I),I=IBEG,IEND)
ELSE ! Print out x-coordinates
PRINT 53,(X(I),I=IBEG,IEND)
WRITE(8,53) (X(I),I=IBEG,IEND)
ENDIF
ENDDO
IF(IEND= =L1) THEN
```

```
JEND=0
PRINT 50
WRITE(8,50)
DO WHILE(JEND/=M1) THEN
JBEG=JEND+1
JEND=JEND+7
JEND=MIN0(JEND,M1)
PRINT 50
WRITE(8,50)
PRINT 54,(J,J=JBEG,JEND)
WRITE(8,54) (J,J=JBEG,JEND)
PRINT 55,(Y(J),J=JBEG,JEND) ! Print out y-coordinates
WRITE(8,55) (Y(J),J=JBEG,JEND) GO TO 311
ENDDO
ENDIF
```

```
DO 999 N=1,NCP      ! NCP has been defined as 14 in SETUP1
NF=N
IF(LPRINT(NF)) THEN      ! Print out F(I,J,NF) field
PRINT 50
WRITE(8,50)
PRINT 10,TITLE(NF)
WRITE(8,10) TITLE(NF)      ! Print out title of variable F(I,J,NF)
IFST=1
JFST=1
IF(NF==1.OR.NF==3) IFST=2
IF(NF==2.OR.NF==3) JFST=2
IBEG=IFST-7
DO WHILE ( IEND<L1.OR.IBEG== -5.OR.IBRG== -6)
IBEG=IBEG+7 ! Starting point for each line (7data)
IEND=IBEG+6 ! Ending point of the line
IEND=MIN0(IEND,L1)
PRINT 50 WRITE(8,50)
```

```

PRINT 20,(I,I=IBEG,IEND)
WRITE(8,20) (I,I=IBEG,IEND)
PRINT 30
WRITE(8,30)
JFL=JFST+M1 .
DO 115 JJ=JFST,M1
J=JFL-JJ
PRINT 40, J, (F(I,J,NF),I=IBEG,IEND)
WRITE(8,40) J,(F(I,J,NF),I=IBEG,IEND)
115 ENDDO
ENDDO
ENDIF
999 END (End of print do-loop)
    
```

```

***** .TEMP. *****
I=  1      2      3      4      5      6      7
J
7  2.00E+00 2.30E+00 2.90E+00 3.50E+00 4.10E+00 4.70E+00 5.00E+00
6  1.80E+00 2.08E+00 2.64E+00 3.20E+00 3.76E+00 4.32E+00 4.60E+00
5  1.40E+00 1.64E+00 2.12E+00 2.60E+00 3.08E+00 3.56E+00 3.80E+00
4  1.00E+00 1.20E+00 1.60E+00 2.00E+00 2.40E+00 2.80E+00 3.00E+00
3  6.00E-01 7.60E-01 1.08E+00 1.40E+00 1.72E+00 2.04E+00 2.20E+00
2  2.00E-01 3.20E-01 5.60E-01 8.00E-01 1.04E+00 1.28E+00 1.40E+00
1  0.00E+00 1.00E-01 3.00E-01 5.00E-01 7.00E-01 9.00E-01 1.00E+00
    
```

**(17b) —
Explained
in detail**

115 ENDDO
ENDDO
ENDIF

999 END (End of print do-loop)

Transformation of data format for Tecplot

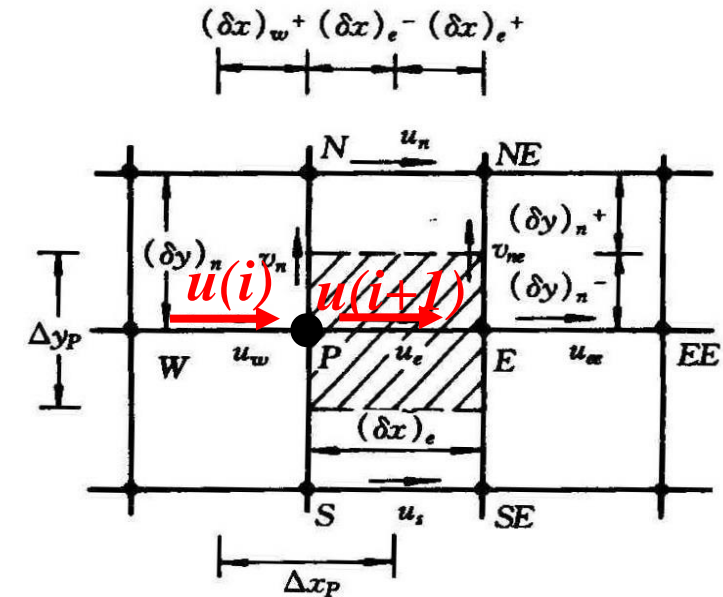
```

OPEN(9,FILE="RESULT.DAT")
WRITE(9,('"VARIABLES=X,Y",$',))
DO NF=1,NCP
IF(LPRINT(NF)) WRITE(9,('",",A7,$')) TITLE(NF)
ENDDO
WRITE(9,('/',"ZONE I=",I4,",J=",I4,",T=T",,$')) L1,M1
DO J=1,M1
DO I=1,L1
WRITE(9,('/',E11.3,E11.3,$')) X(I),Y(J)
DO NF=1,NCP
IF(LPRINT(NF)) THEN
FSHOW=F(I,J,NF)
IF(NF==1) THEN
IF(I==1) FSHOW=U(2,J)
IF(I>=2.AND.I<=L2) FSHOW=(U(I,J)+U(I+1,J))/2
IF(I==L1) FSHOW=U(L1,J)
ENDIF

```

Data format of TECPLOT

Data format of TECPLOT



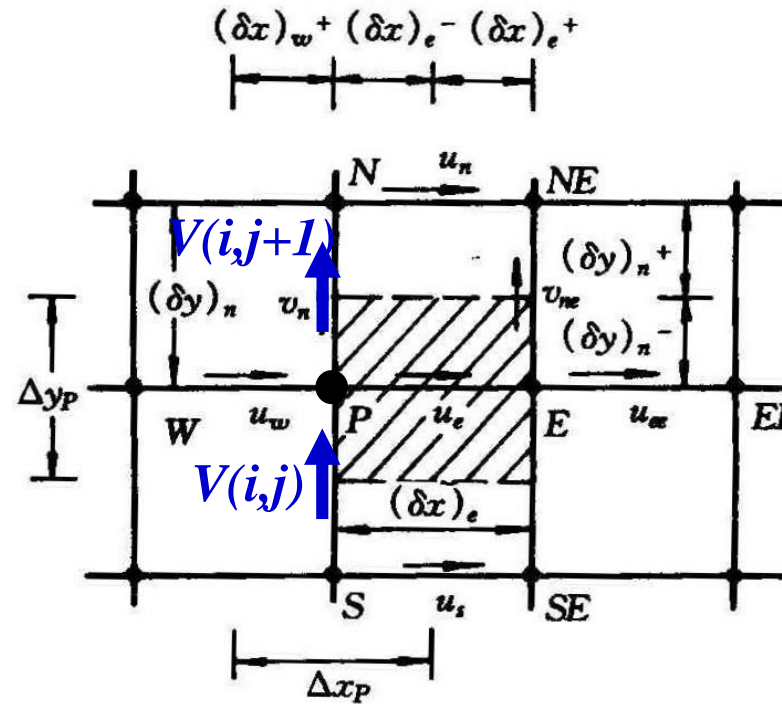
}

For u

```

IF(NF==2) THEN
  IF(J==1) FSHOW=V(I,2)
  IF(J>=2.AND.J<=M2) FSHOW=(V(I,J)+V(I,J+1))/2
  IF(J==M1) FSHOW=V(I,M1)
ENDIF
WRITE(9,'(E11.3,$)') FSHOW
ENDIF
ENDDO
      ENDDO
ENDDO
CLOSE(9)
RETURN
END
    
```

} For v



Comments and Recommendations for Teaching Code Study

1. It is the students' responsibility to study the code line by line to completely understanding the function of each line and the numerical techniques included.

You should understand every detail included in each line, for example:

```
IF(MODE.== 3) THEN  
SX(J)=R(J)  
IF(J /= 1) SXMN(J)=RMN(J)  
ENDIF
```

why here J=1 should not be included?

2. You can understand a numerical algorithm, say SIMPLER, completely only when you know how to implementing the algorithm by code.

3. If you meet some difficulty in understanding the teaching code you may contact me by email (fangwenzhen@mail.xjtu.edu.cn) at any time. I will be happy to communicate with you.

4. Our teaching assistants will give you instruction on how to run the code.

本组网页地址: <http://nht.xjtu.edu.cn> 欢迎访问!
Teaching PPT will be loaded on our website



同舟共济
渡彼岸!

People in the
same boat help
each other to
cross to the other
bank, where....