

# 数值传热学

## 第四章 扩散方程的数值解及其应用(1)



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2016年10月10日, 西安

# Numerical Heat Transfer

## (数值传热学)

### Chapter 4 Numerical Solution of Diffusion Equation and its Applications(1)



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**Xi'an, 2016-Sept.-28**

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## 4.1 1-D Heat Conduction Equation

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## 4.1 1-D Heat Conduction Equation

### 4.1.1 G.E. of 1-D steady heat conduction

#### 1. Two ways of coding for solving engineering problems

**Specific code(专用程序):** FLOWTHERN, POLYFLOW...Having some generality within its application range.

**General code(通用程序):** HT, FF, Combustion, MT, Reaction, etc.; PHOENICS, FLUENT, STAR-CD, CFX....

**Different codes tempt to have some generality.**

**Generality includes: Coordinates; G.E.; B.C. treatment; Source term treatment; Geometry.....**

## 2. General governing equations of 1-D steady heat conduction problem

$$\frac{1}{A(x)} \frac{d}{dx} \left[ \lambda A(x) \frac{dT}{dx} \right] + S = 0$$

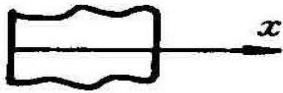
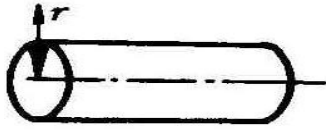
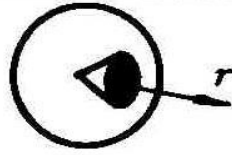
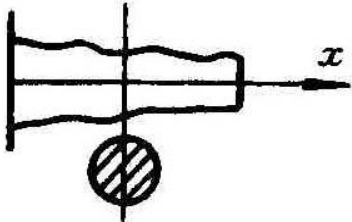
$x$ ----Independent variable (**独立变量**), normal to cross section

$A(x)$ ----Area factor, normal to heat conduction direction

$\lambda$ ----Thermal conductivity

$S$ ---- Source term, may be a function of both  $x$  and  $T$ .

$$\frac{1}{A(x)} \frac{d}{dx} \left[ \lambda A(x) \frac{dT}{dx} \right] + S = 0$$

Mode	Coordinate	Indep. variable	Area factor	Illustration
1	Cartesian	x	1(unit)	
2	Cylindrical	r	r (arc <span style="color: red;">弧度</span> area)	
3	Spherical	r	R <sup>2</sup> (spherical surface)	
4	Variable cross section	x Perpendicular to section	A(x), ⊥ Heat conduction direction	

## 4.1.2 Discretization of G.G.Eq. by CVM

Multiplying two sides by  $A(x)$

$$\frac{1}{A(x)} \frac{d}{dx} \left[ \lambda A(x) \frac{dT}{dx} \right] + S = 0 \quad \longrightarrow \quad \frac{d}{dx} \left[ \lambda A(x) \frac{dT}{dx} \right] + S \cdot A(x) = 0$$

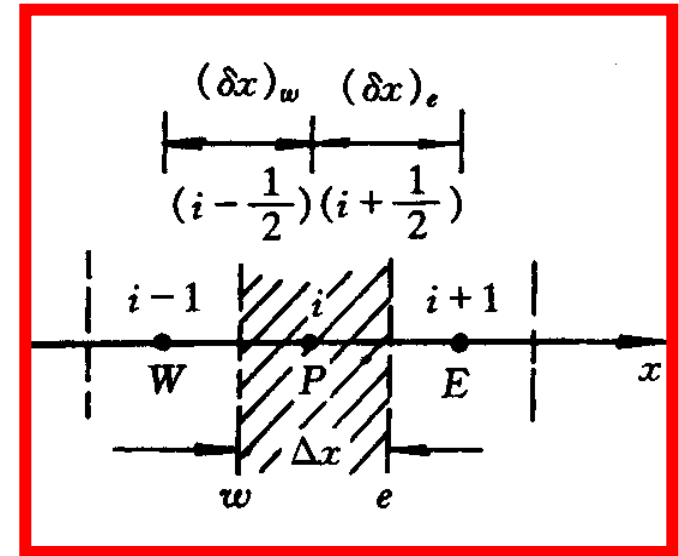
Linearizing (线性化) source term :  $S = S_C + S_P T_P$

Adopting piecewise linear profile:

Integrating over control volume

P, yielding (得)

$$\left[ \lambda A(x) \frac{dT}{dx} \right]_e - \left[ \lambda A(x) \frac{dT}{dx} \right]_w + \int (S_C + S_P T_P) A(x) dx = 0$$





$$\lambda_e A_e(x) \frac{T_E - T_P}{(\delta x)_e} - \lambda_w A_w(x) \frac{T_P - T_W}{(\delta x)_w} + (S_C + S_P T_P) A_P(x) \Delta x = 0$$

**Moving terms with  $T_P$  to left side while those with  $T_E, T_W$  to right side**

$$T_P \left[ \frac{A_e(x) \lambda_e}{(\delta x)_e} + \frac{A_w(x) \lambda_w}{(\delta x)_w} - S_P A_P(x) \Delta x \right] = T_E \left[ \frac{A_e(x) \lambda_e}{(\delta x)_e} \right] + T_W \left[ \frac{A_w(x) \lambda_w}{(\delta x)_w} \right] + S_C A_P(x) \Delta x$$

**We adopt following well-accepted form for discretized eqs.:**

$$a_P T_P = a_E T_E + a_W T_W + b$$

$$a_E = \frac{\lambda_e A(x)_e}{(\delta x)_e}, \quad a_W = \frac{\lambda_w A(x)_w}{(\delta x)_w}, \quad b = S_C A_P(x) \Delta x = S_C \Delta V$$

$$a_P = a_E + a_W - S_P \Delta V$$

# Physical meaning of coefficients $a_E, a_W$

$$a_E = \frac{1}{(\delta x)_e / [\lambda_e A(x)_e]} = \frac{1}{\text{Thermal resistance between P and E}}$$

It represents the effect of point E on point P, and is also called influencing coefficient(影响系数).

## 4.1.3 Determination of interface thermal conductivity

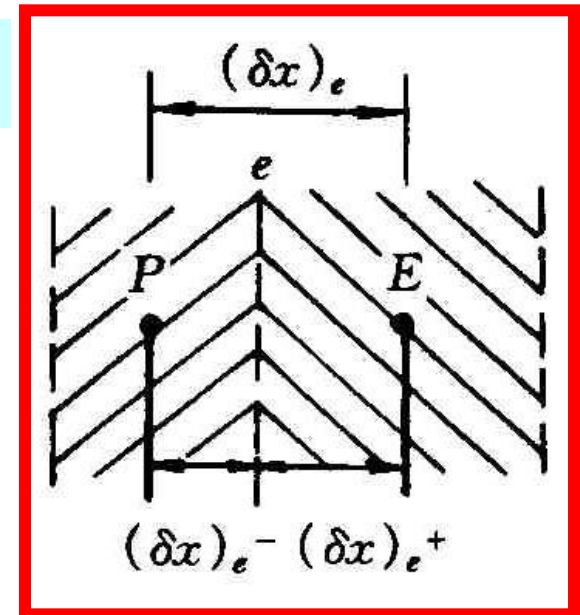
### 1. Arithmetic mean(算术平均法)

$$\lambda_e = \lambda_P \frac{(\delta x)_{e^+}}{(\delta x)_e} + \lambda_E \frac{(\delta x)_{e^-}}{(\delta x)_e}$$

Uniform grid



$$\lambda_e = \frac{\lambda_P + \lambda_E}{2}$$



## 2. Harmonic mean (调和平均法)

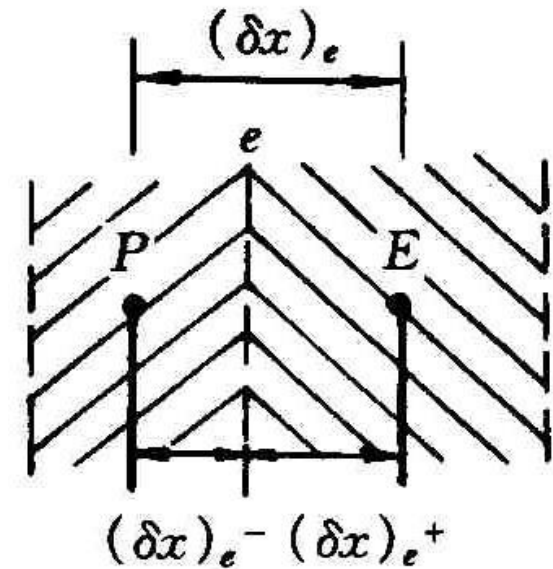
Assuming that conductivities of P, E are different, according to the continuous requirement of heat flux at interface:

$$\frac{T_E - T_e}{(\delta x)_{e^+}} = \frac{T_e - T_P}{(\delta x)_{e^-}} \rightarrow \frac{T_E - T_P}{(\delta x)_{e^+} + (\delta x)_{e^-}}$$

Left side

Right side

Algebraic operation rule



$$\frac{T_E - T_P}{(\delta x)_{e^+} + (\delta x)_{e^-}} = \frac{T_E - T_P}{(\delta x)_e}$$

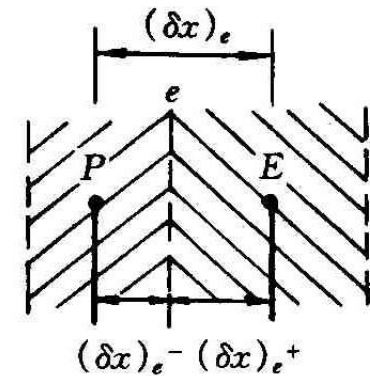
Interface conductivity

$$\frac{(\delta x)_e}{\lambda_e} = \frac{(\delta x)_{e^+}}{\lambda_E} + \frac{(\delta x)_{e^-}}{\lambda_P}$$

Harmonic mean

**For uniform grid:**

$$\lambda_e = \frac{2\lambda_P\lambda_E}{\lambda_P + \lambda_E}$$



### 3. Comparison of two methods

If  $\lambda_P \gg \lambda_E$  major resistance is at E-side, while A.M.:

$$\lambda_e = \frac{\lambda_P + \lambda_E}{2} \xrightarrow{\lambda_P \gg \lambda_E} \lambda_e \cong \frac{\lambda_P}{2} \xrightarrow{\text{Resis.}} \frac{(\delta x)_e}{\frac{\lambda_P}{2}}$$

From harmonic mean:

$$\lambda_e = \frac{2\lambda_E\lambda_P}{\lambda_E + \lambda_P} \xrightarrow{\lambda_P \gg \lambda_E} \lambda_e \cong 2\lambda_E \xrightarrow{\text{Resis.}} \frac{(\delta x)_e}{2\lambda_E} \xrightarrow{\text{Uniform}} \frac{(\delta x)_e}{\lambda_E} \xrightarrow{\text{Reasonable!}}$$

# Harmonic mean has been widely accepted.

## 4.1.4 Discretization of 1-D transient heat conduction equation(20160928)

**1. Governing eq.**

$$\rho c \frac{\partial T}{\partial t} = \frac{1}{A(x)} \frac{d}{dx} \left[ \lambda A(x) \frac{dT}{dx} \right] + S$$

**2. Integration over CV** Multiplying by  $A(x)$ , assuming

$\rho c$  is independent on time, integrating over CV P within time step  $\Delta t$

$$(\rho c)_P A_P(x) \Delta x (T_P^{n+1} - T_P^n) = \int_t^{t+\Delta t} \left[ \frac{\lambda_e A_e(x) (T_E - T_P)}{(\delta x)_e} - \frac{\lambda_w A_w(x) (T_P - T_W)}{(\delta x)_w} \right] dt$$

Stepwise in space

Needs to select time profile

$$+\Delta x \int_t^{t+\Delta t} (S_C + S_P T_P) dt$$

### 3. Results with a general time profile

$$\int_t^{t+\Delta t} T dt = [fT^{t+\Delta t} + (1-f)T^t] \Delta t, \quad 0 \leq f \leq 1$$

Substituting this profile, integrating, yields:

$$a_P T_P = a_E [fT_E + (1-f)T_E^0] + a_W [fT_W + (1-f)T_W^0] +$$

$$T_P^0 [a_P^0 - (1-f)a_E - (1-f)a_W + (1-f)S_P A_P(x) \Delta x] + S_C A_P(x) \Delta x$$

$$a_E = \frac{\lambda_e A_e(x)}{(\delta x)_e} = \frac{A_e(x)}{\frac{(\delta x)_{e^+}}{\lambda_E} + \frac{(\delta x)_{e^-}}{\lambda_P}}$$

$$a_W = \frac{\lambda_w A_w(x)}{(\delta x)_w} = \frac{A_w(x)}{\frac{(\delta x)_{w^+}}{\lambda_P} + \frac{(\delta x)_{w^-}}{\lambda_W}}$$

$$a_P = fa_E + fa_W + a_P^0 - fS_P A_P(x) \Delta x$$

$$a_P^0 = \frac{\rho c A_P(x) \Delta x}{\Delta t} = \frac{\rho c \Delta V}{\Delta t}$$

Thermal inertia (热惯性)

## 4. Stability analysis

From von Neumann analysis method it can be shown:

$0.5 \leq f \leq 1$ , Absolutely stable;

$0 \leq f < 0.5$ , Conditionally stable:

$$\frac{a\Delta t}{\Delta x^2} \leq \frac{1}{2(1-f)}$$

## 5. Three forms of time level for discretized diffus. term

(1) Explicit(显),  $f = 0$  ; 
$$\frac{T_P - T_P^0}{\Delta t} = a \left( \frac{T_E^0 - 2T_P^0 + T_W^0}{\Delta x^2} \right)$$

(2) Fully implicit(全隐)  $f = 1$  ; 
$$\frac{T_P - T_P^0}{\Delta t} = a \left( \frac{T_E - 2T_P + T_W}{\Delta x^2} \right)$$

(3) C-N scheme,  $f = 0.5$

$$\frac{T_P - T_P^0}{\Delta t} = \frac{a}{2} \left( \frac{T_E - 2T_P + T_W}{\Delta x^2} + \frac{T_E^0 - 2T_P^0 + T_W^0}{\Delta x^2} \right)$$

**No superscript  
for  $t + \Delta t$  time level**

## 4.1.5 Mathematical stability can't guarantee solution physically meaningful

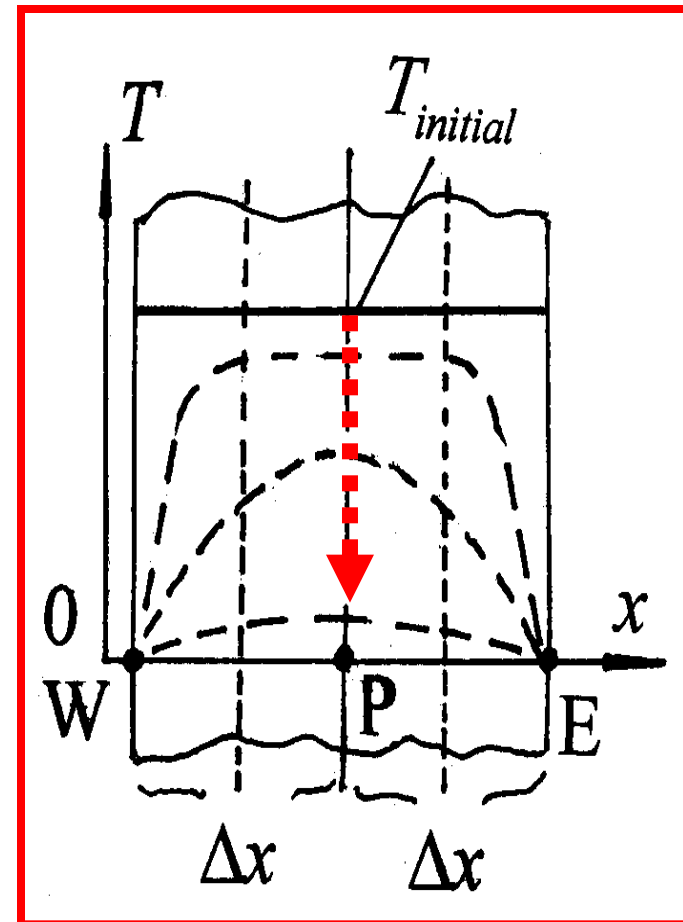
Illustrated by an example.

**[Known]** 1-D transient HC without source term, uniform initial field. Two surfaces were suddenly cooled down to zero.

**[Find]** Variation of inner point temp.

**[Solution]** Discretized by Practice A  
Adopting three grids: W, P, and E.

Physically following variation trend can be expected!





## Analyzing for the 2<sup>nd</sup> time level:

$$T_E = T_E^0 = T_W = T_W^0 = 0 ; S_C = 0, S_P = 0 \quad \text{Substituting:}$$

$$a_P T_P = a_E [f T_E + (1-f) T_E^0] + a_W [f T_W + (1-f) T_W^0] + T_P^0 [a_P^0 - (1-f)a_E - (1-f)a_W + (1-f)S_P A_P(x)\Delta x] + S_C A_P(x)\Delta x$$

**Yields** 
$$a_P T_P = T_P^0 [a_P^0 - (1-f)a_E - (1-f)a_W]$$

**i.e.:** 
$$\frac{T_P}{T_P^0} = \frac{a_P^0 - (1-f)(a_W + a_E)}{a_P} = \frac{a_P^0 - (1-f)(a_W + a_E)}{a_P^0 + f(a_W + a_E)}$$

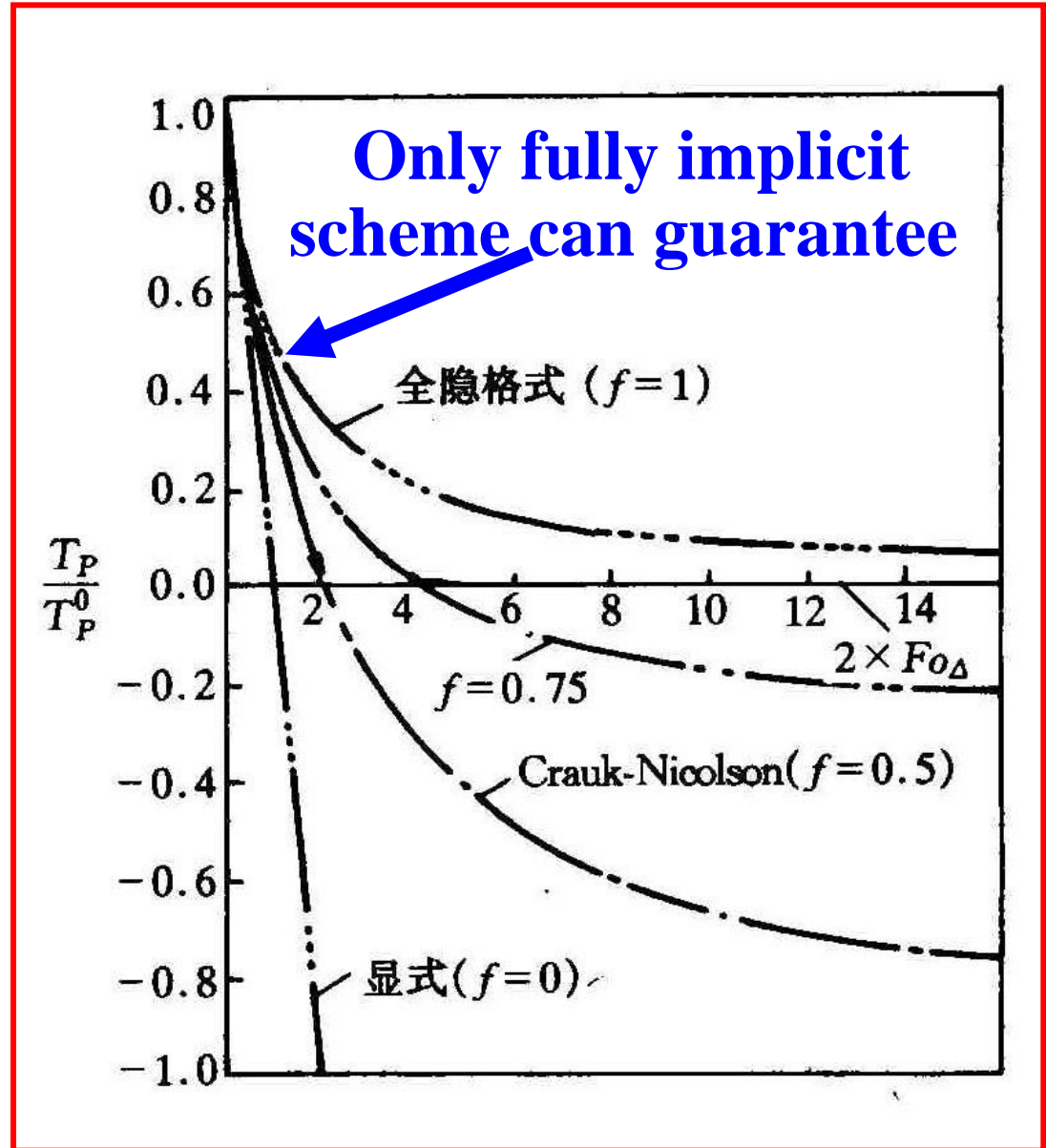
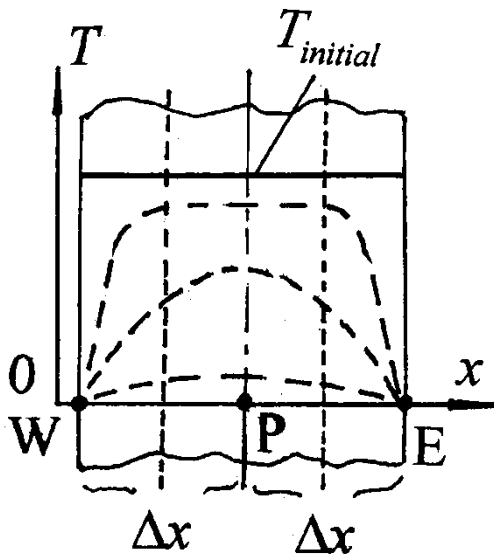
$$a_E = a_W = \frac{\lambda \bullet 1}{\Delta x}, a_P^0 = \frac{\rho c_p \Delta x}{\Delta t}, \frac{a_E}{a_P^0} = \frac{\lambda / \Delta x}{\rho c_p \Delta x / \Delta t} = \left(\frac{\lambda}{\rho c_p}\right) \frac{\Delta t}{\Delta x^2} = \frac{a \Delta t}{\Delta x^2}$$

**Finally:** 
$$\frac{T_P}{T_P^0} = \frac{1 - 2(1-f)\left(\frac{a \Delta t}{\Delta x^2}\right)}{1 + 2f\left(\frac{a \Delta t}{\Delta x^2}\right)}$$

$$\frac{T_P}{T_P^0} = \frac{1 - 2(1 - f)Fo_\Delta}{1 + 2fFo_\Delta}$$

Physically it is required :

$$\frac{T_P}{T_P^0} > 0$$



Only when  $f = 1$  (fully imp.) can guarantee

This can be obtained from physical analysis!

The discretized form of transient HC is:

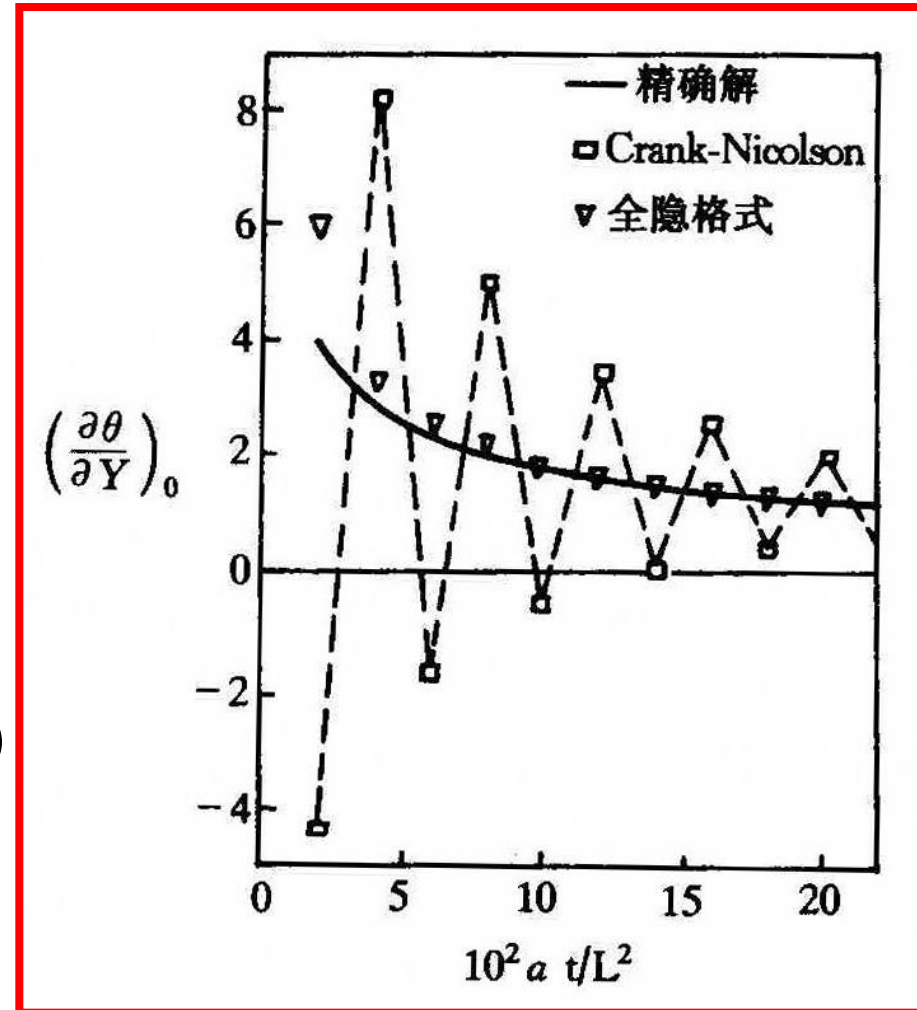
$$a_P T_P = a_E T_E + a_W T_W + a_t T_P^0 + b$$

where all coefficients must be  $\geq 0$

$$a_t = a_P^0 - (1-f)a_E - (1-f)a_W \geq 0$$

$$1 - (1-f)(a_E + a_W) / a_P^0 \geq 0$$

$$\frac{a_E}{a_P^0} = \frac{a\Delta t}{\Delta x^2} = Fo_{\Delta} \quad Fo_{\Delta} \leq \frac{1}{2(1-f)}$$



**Conclusion: mathematical stability can't guarantee solution physically meaningful!**

## **4.2 Fully Implicit Scheme of Multi-dimensional Heat Conduction Equation**

**4.2.1 Fully implicit scheme in three coordinates**

**4.2.2 Comparison between coefficients**

**4.2.3 Uniform expression of discretized form for three coordinates**

# 4.2 Fully Implicit Scheme of Multi-dimensional Heat Conduction Equation

## 4.2.1 Fully implicit scheme in three coordinates

### 1. Cartesian coordinates

#### (1) Governing eq.

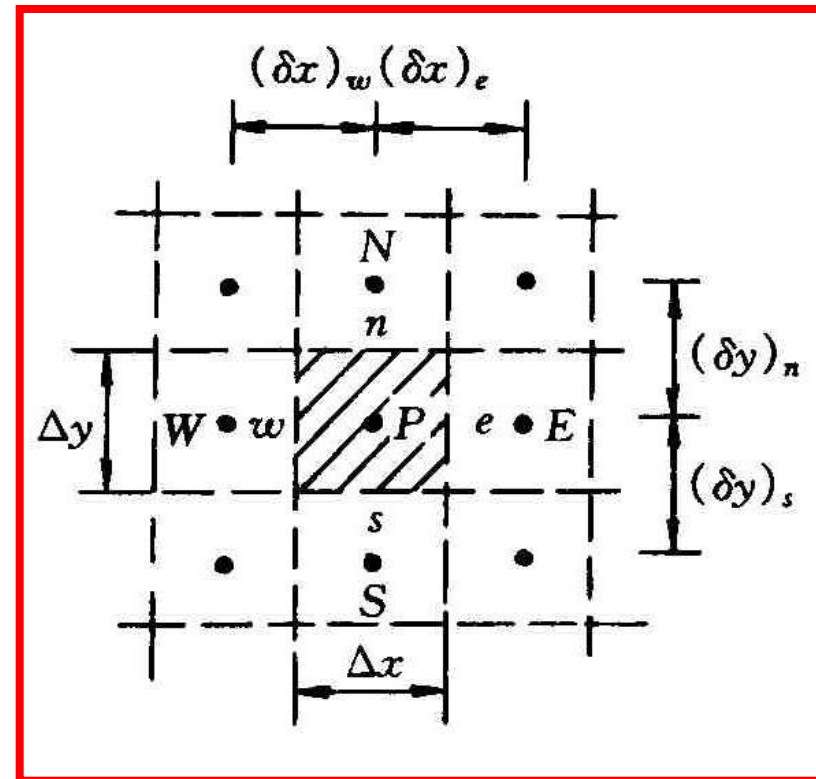
$$\rho c \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left( \lambda \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( \lambda \frac{\partial T}{\partial y} \right) + S$$

#### (2) CV integration

Space profiles are the same as 1-D problem.

Fully implicit for time

Heat flux is uniform at interface.



## Integration of transient term =

$$\int_s^n \int_w^e \int_t^{t+\Delta t} \rho c \frac{\partial T}{\partial t} dx dy dt \xrightarrow{\text{stepwise}} (\rho c)_P (T_P - T_P^0) \Delta x \Delta y$$

$$\text{Diffusion term (1)} = \int_s^n \int_w^e \int_t^{t+\Delta t} \frac{\partial}{\partial x} \left( \lambda \frac{\partial T}{\partial x} \right) dx dy dt =$$

**Space linear wise**  
**Heat flux uniform,**  
**Time fully implicit**

$$\int_s^n \int_t^{t+\Delta t} \left[ \left( \lambda \frac{\partial T}{\partial x} \right)_e - \left( \lambda \frac{\partial T}{\partial x} \right)_w \right] dy dt$$

$$= \left( \lambda_e \frac{T_E - T_P}{(\delta x)_e} - \lambda_w \frac{T_P - T_W}{(\delta x)_w} \right) \Delta y \Delta t$$

**No superscript for  
(n+1) time level**

**Diffusion term (2) =** 
$$\int_s^n \int_w^e \int_t^{t+\Delta t} \frac{\partial}{\partial y} \left( \lambda \frac{\partial T}{\partial y} \right) dx dy dt =$$

$$\int_w^e \int_t^{t+\Delta t} \left[ \left( \lambda \frac{\partial T}{\partial y} \right)_n - \left( \lambda \frac{\partial T}{\partial y} \right)_s \right] dx dt$$

**Space linear wise**  
**Heat flux uniform,**  
**Time fully implicit**

$$= \left( \lambda_n \frac{T_N - T_P}{(\delta y)_n} - \lambda_s \frac{T_P - T_S}{(\delta y)_s} \right) \Delta x \Delta t$$

**Source term =** 
$$\int_w^e \int_s^n \int_t^{t+\Delta t} S dx dy dt \xrightarrow{\text{Linealization}} (S_C + S_P T_P) \Delta x \Delta y \Delta t$$

**Fully implicit**

**Substituting and rearranging:**

$$a_P T_P = a_E T_E + a_W T_W + a_N T_N + a_S T_S + b$$

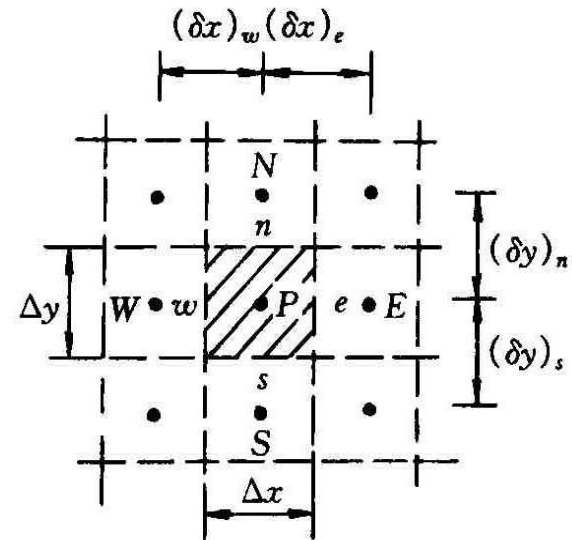
$$a_E = \frac{\Delta y}{(\delta x)_e / \lambda_e}, a_W = \frac{\Delta y}{(\delta x)_w / \lambda_w}, a_N = \frac{\Delta x}{(\delta y)_n / \lambda_n}, a_S = \frac{\Delta x}{(\delta y)_s / \lambda_s}$$

$$a_P = a_E + a_W + a_N + a_S + a_P^0 - S_P \Delta x \Delta y$$

$$a_P^0 = \frac{\rho c \Delta V}{\Delta t}, b = S_C \Delta V + a_P^0 T_P^0$$

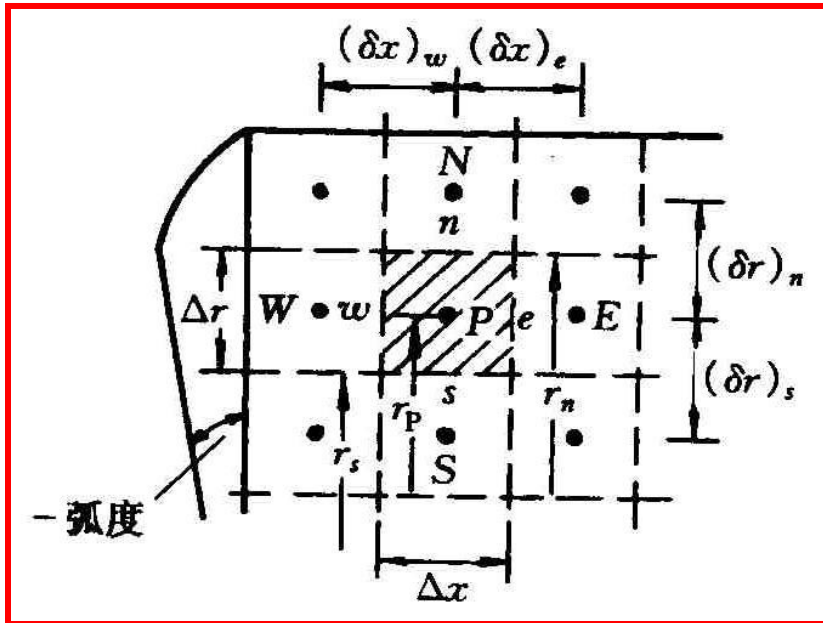
**Physical meaning of coefficients:**  
**heat conductance (热导) between**  
**neighboring grids.**

$$a_E = \frac{\Delta y}{(\delta x)_e / \lambda_e} = \frac{\lambda_e \Delta y}{(\delta x)_e}$$

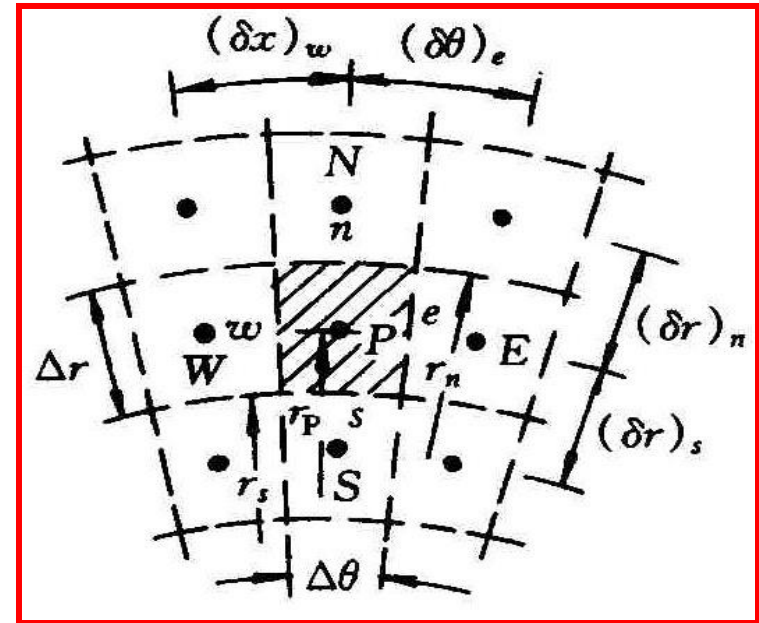




## 2. Cylindrical symmetry



## 3. Polar coordinates



$$a_P T_P = a_E T_E + a_W T_W + a_N T_N + a_S T_S + b$$

$$a_E = \frac{r_P \Delta r}{(\delta x)_e} \lambda_e$$

$$a_E = \frac{\Delta r}{r_P (\delta \theta)_e} \lambda_e$$

## 4.2.2 Comparison between coefficients

Coefficients  $a_E$  of the three 2-D coordinates can be expressed as

$$a_E = \frac{\text{Interface conductivity} \times \text{E-W HC area}}{\text{Distance between Nodes E and P}}$$

**It is the thermal conductance!**

### 1. What's the difference between 3 coordinates

- (1) In polar coordi.  $\theta$  is the arc (弧度), dimensionless, while in  $x - y, x - r, x$  is dimensional!
- (2) In polar and cylindrical coordinates there are radius, while in Cartesian coordinate no any radius at all.

## 2. One way to unify the expression of coefficients

For this purpose we introduce two auxiliary (辅助的) parameters

### (1) Scaling factor (x-方向标尺因子)

Distance in x direction is expressed by  $s_x \bullet \delta x$

For Cartesian and cylindrical coordinates:  $s_x \equiv 1$ ;

For polar coordinate:  $s_x = r$ ;

(2) In y-direction, a normal(名义上的) radius, R, is introduced.

For Cartesian coordi.  $R=1$  For Cy. & Po.  $R= r$

Then: E-W conduction distance:  $s_x \bullet \delta x$

E-W conduction area:  $R\Delta y / s_x$

## 4.2.3 Unified expressions for three 2-D coordinates

Coordinate	Cartes.	Cy.Sym	Polar	Generalized
E-W Coord.	$x$	$x$	$\theta$	$X$
S-N Coord.	$y$	$r$	$r$	$Y$
Radius	$1$	$r$	$r$	$R$
Scaling factor in $x$	$1$	$1$	$r$	$SX$
E-W distance	$\delta x$	$\delta x$	$r\delta\theta$	$(\delta x)(SX)$
S-N distance	$\delta y$	$\delta r$	$\delta r$	$\delta Y$
E-W Conduct.area	$\Delta y$	$r\Delta r$	$\Delta r$	$R\Delta Y / SX$

S-N Conduct.area	$\Delta x$	$r\Delta x$	$r\delta\theta$	$R(\Delta X)$
Volume of CV	$\Delta x\Delta y$	$r\Delta x\Delta r$	$r\Delta\theta\Delta r$	$R\Delta X\Delta Y$
$a_E$	$\frac{\Delta y}{(\Delta x)_e / \lambda_e}$	$\frac{r\Delta r}{(\Delta x)_e / \lambda_e}$	$\frac{\Delta r}{(\Delta\theta)_e r / \lambda_e}$	$\frac{R\Delta Y}{(SX)^2 (\Delta X)_e / \lambda_e}$
$a_N$	$\frac{\Delta x}{(\Delta y)_n / \lambda_n}$	$\frac{r\Delta x}{(\Delta r)_n / \lambda_n}$	$\frac{r\Delta\theta}{(\Delta r)_n / \lambda_n}$	$\frac{R\Delta X}{(\delta Y)_n / \lambda_n}$
$a_P^0$	$\rho c R\Delta X\Delta Y / \Delta t$			
$b$	$S_c R\Delta X\Delta Y$			

If coding by this way, then by setting up a variable, **MODE**, computer will automatically deal with the three coordinates according to **MODE**:

<b>MODE</b>	<b>1(x-y)</b>	<b>2(x-r)</b>	<b>3(theta-r)</b>
<b>R</b>	<b>1</b>	<b>r</b>	<b>r</b>
<b>SX</b>	<b>1</b>	<b>1</b>	<b>r</b>

Commercial software usually adopts the similar method to deal with coefficients in different coordinates.

## 4.3 Treatments of Source Term and B.C.

### 4.3.1 Linearization of non-constant source term

1. Linearization (线性化) method

2. Discussion

3. Examples of linearization method

### 4.3.2 Treatments of 2<sup>nd</sup> and 3<sup>rd</sup> kind of B.C. for closing algebraic equations

1. Supplementing(补充) equations for  
boundary points

2. Additional source term method (ASTM)

## 4.3 Treatments of Source Term and B.C.

### 4.3.1 Linearization of non-constant source term

#### 1. Linearization (线性化)

Importance of source term in the present method--"Ministry of portfolio(不管部长)": refer to (指) any terms which can not be classified as one of the transient, diffusion or convection terms.

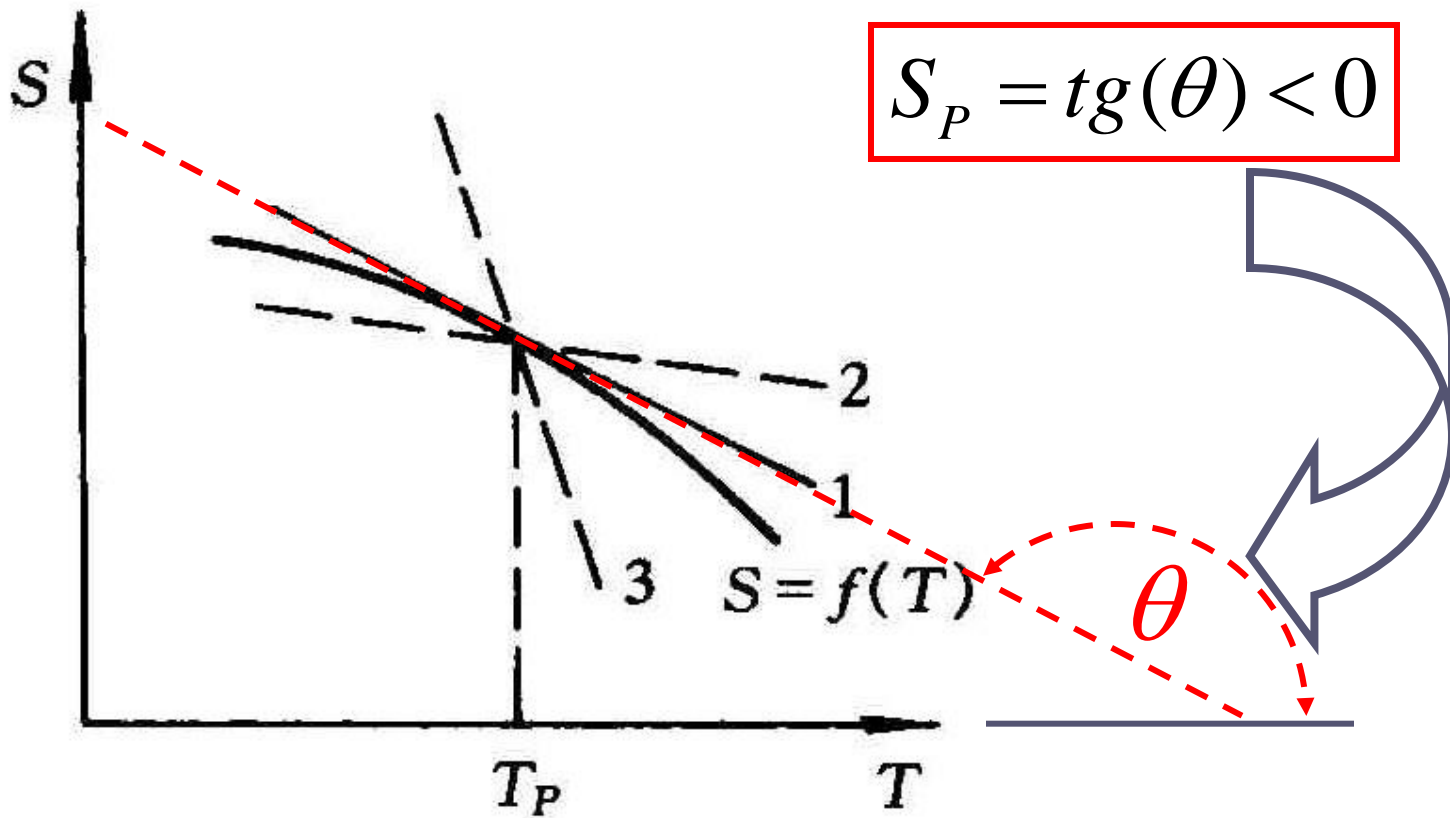
Linearization: for CV. P its source term is expressed as:

$$S = S_C + S_P \phi_P, \quad S_P \leq 0$$

$S_C, S_P$  are constants for each CV,  $S_P$  is the slope(斜率) of the curve  $S = f(\phi)$



For the curve  $S = f(T)$



## 2. Discussion on linearization of source term

**(1)** For variable source term ,  $S = f(T)$  , **linearization is better than taking previous value**,  $S = f(T_P^*)$  .

There is one time step lag (迟后) between

$$S = S_C + S_P T_P \text{ and } S = f(T^*) .$$

**(2)** Any complicated function can be approximated by a linear function, and **linearity is also required by deriving linear algebraic equations.**

**(3)**  $S_P \leq 0$  is required by the convergence condition for solving the algebraic equations.

**The sufficient condition for iterative solution of the algebraic equations like:**

$$a_P \phi_P = \sum a_{nb} \phi_{nb} + b$$

is that:  $a_P \geq \sum a_{nb}$

**Since in our method:**

$$a_P = \sum a_{nb} - S_P \Delta V$$

Thus  $S_P \leq 0$  will ensure(确保) the above sufficient condition.

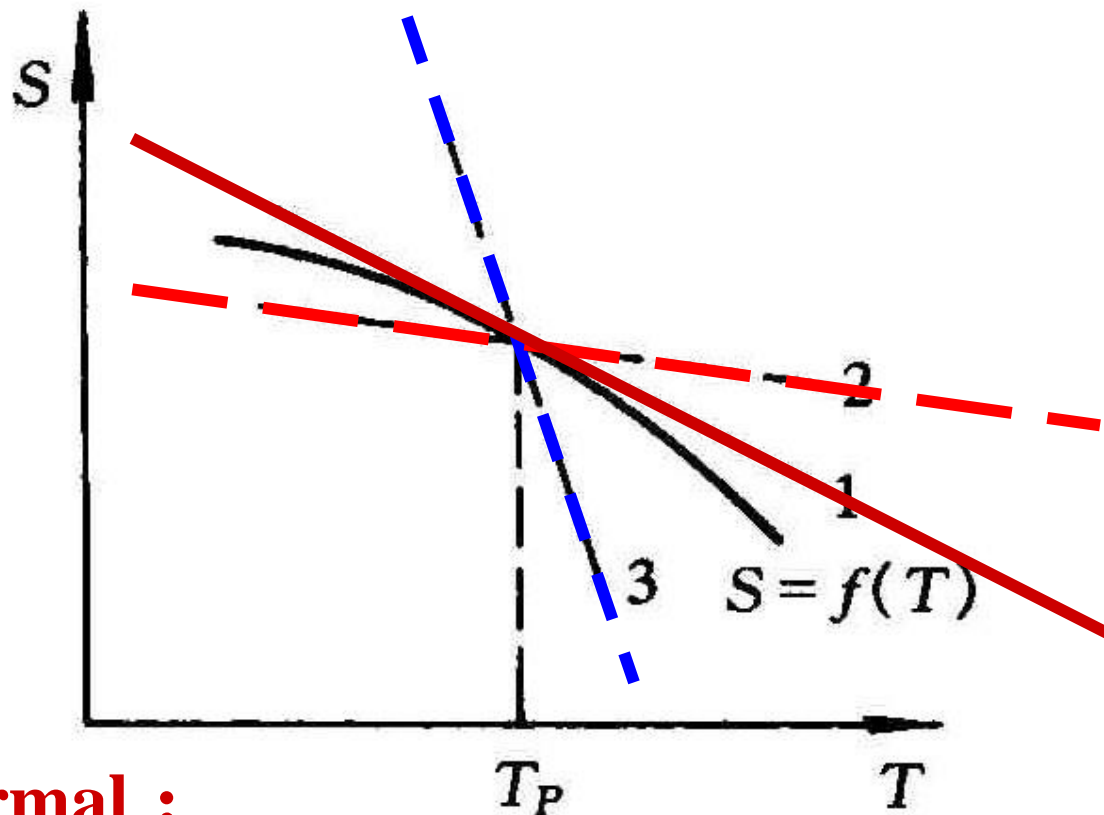
**(4)** If a practical problem has  $S_P > 0$ , then  
**an artificial(人为的) negative  $S_p$  may be introduced.**

**(5)** Effect of the absolute value of  $S_p$  on the  
 convergence speed

Iteration equation: 
$$\phi_P = \frac{\sum a_{nb} \phi_{nb} + b}{\sum a_{nb} - S_P \Delta V}$$

$|S_P|$   **Denominator(分母) increases, difference  
 between two successive iterations decreases;  
 hence convergence speed decreases;**

With given iteration number, it is favorable (利于) to get  
 the converged solution for **highly nonlinear problem.**



Curve 1--**normal** ;

Curve 3-- Absolute value of  $S_p$  increases — It is in favor of getting a converged solution for nonlinear case, while **speed of convergence decreases**.

Curve 2 --Absolute value of  $S_p$  decreases, it is in favor of speed up iteration, but **takes a risk(风险) of divergence!**

### 3. Examples of linearization

(1)  $S = 3 - 5T$ ;  $S_C = 3$ ,  $S_P = -5$

(2)  $S = 3 + 5T$ ;

**Different practices:**

$$\left\{ \begin{array}{l} S_C = 3 + 5T^*, S_P = 0 \\ S_C = 3 + 7T^*, S_P = -2 \\ \dots\dots\dots \end{array} \right.$$

(3)  $S = 4 - 2T^2$ ;

$$S = S^* + \left(\frac{dS}{dT}\right)^* (T - T^*) = [4 - (2T^*)^2] + (-4T^*)(T - T^*)$$

$$= 4 - 2T^{*2} + 4T^{*2} - 4T^*T = \underbrace{4 + 2T^{*2}}_{S_C} - \underbrace{4T^*T}_{S_P}$$

**Recommended**

## 4.3.2 Treatments of 2nd and 3rd kind of B.C. for closing algebraic equations

For 2<sup>nd</sup> and 3<sup>rd</sup> kinds of B.C., the boundary temperatures are not known, while they are involved in the inner node equations. Thus the resulted algebraic equations are not closed (方程组不封闭).

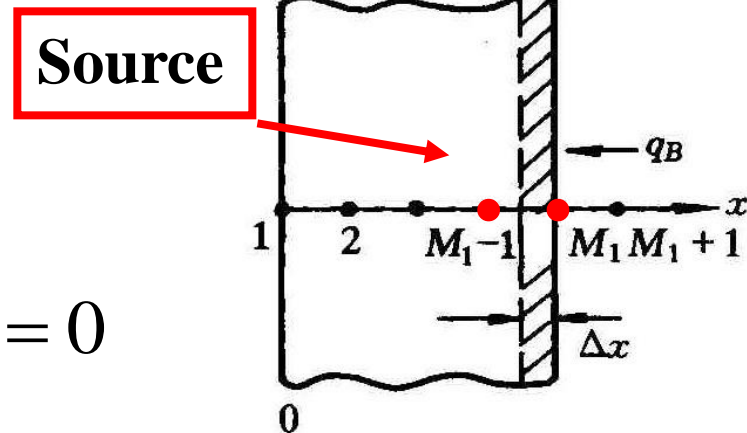
### 1. Supplementing (增补) equations for boundary nodes.

Adopting the CV to obtain boundary nodes equation.

#### (1) Practice A

Taking the heat into the solution region as positive.

$$q_B + \lambda \frac{T_{M_1-1} - T_{M_1}}{\delta x} + \Delta x \cdot S = 0$$



**Yields:**

$$T_{M1} = T_{M1-1} + \frac{\delta x \cdot \Delta x \cdot S}{\lambda} + \frac{q_B \cdot \delta x}{\lambda}$$

**The T.E. of this discretized equation is:  $O(\Delta x^2)$**

**For 3rd kind B.C., according to Newton's law of cooling:**

$$q_B = h(T_f - T_{M1}) \quad \text{(Heat into the region as + )}$$

**Substituting  $q_B$  into the above equation, and rearranging:**

$$T_{M1} = \frac{T_{M1-1} + \frac{\delta x \cdot \Delta x \cdot S}{\lambda} + \left(\frac{h \cdot \delta x}{\lambda}\right)T_f}{\frac{h \cdot \delta x}{\lambda} + 1}$$

## (2) Practice B



The **volume of boundary node in Practice B is zero**, thus setting zero volume of the boundary nodes in the above equation:

$$q_B + \lambda \frac{T_{M1-1} - T_{M1}}{\delta x} + \Delta x \bullet S = 0$$

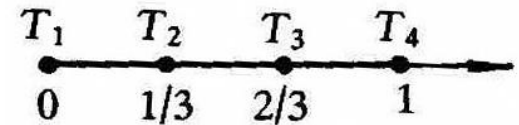
yields:

for 2<sup>nd</sup> kind boundary —

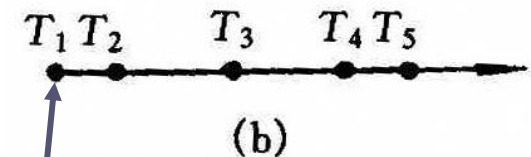
$$T_{M1} = T_{M1-1} + \frac{q_B \bullet \delta x}{\lambda}$$

for 3<sup>rd</sup> kind boundary —

$$T_{M1} = \frac{T_{M1-1} + \left(\frac{h \bullet \delta x}{\lambda}\right) T_f}{1 + \frac{h \bullet \delta x}{\lambda}}$$



(a)



(b)

Zero boundary CV

The above discretized forms have 2<sup>nd</sup> order accuracy.

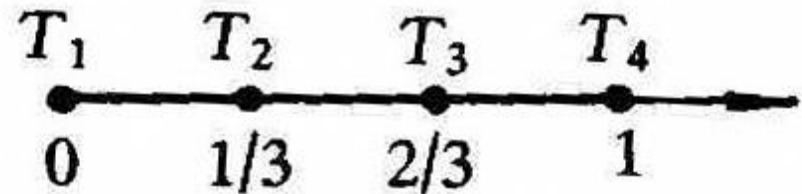
### (3) Example

**[Known]**  $\frac{d^2T}{dx^2} - T = 0; x = 0, T = 0; x = 1, \frac{dT}{dx} = 1$

**[Find]** Temperatures of 2-3 nodes in the region

**[Solution]**

Practice A, 2 inner nodes,



$T_2, T_3$  Adopting 2<sup>nd</sup> order accuracy

$T_4$  Adopting 1<sup>st</sup> order :  $\frac{T_4 - T_3}{1/3} = 1 \longrightarrow T_4 - T_3 = 1/3$

$T_4$  Adopting 2<sup>nd</sup> order:  $T_{M1} = T_{M1-1} + \frac{\delta x \cdot \Delta x \cdot S}{\lambda} + \frac{q_B \cdot \delta x}{\lambda}$

**Question 1: what is the source term?**

Boundary node has a half CV,  
From  $\frac{d^2T}{dx^2} - T = 0$   $S = -T_4$

**Question 2: what is the heat flux?**

Then from  $T_{M1} = T_{M1-1} + \frac{\delta x \cdot \Delta x \cdot S}{\lambda} + \frac{q_B \cdot \delta x}{\lambda}$

$$q = \lambda \frac{dT}{dx} = 1 \times 1 = 1$$

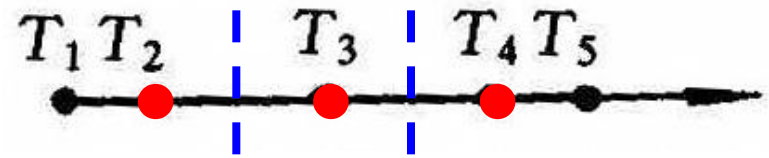
We have

$$T_4 = T_3 - \frac{\frac{1}{3} \cdot \frac{1}{6} \cdot T_4}{1} + \frac{1 \cdot \frac{1}{3}}{1} \rightarrow \frac{19}{18} T_4 - T_3 = \frac{1}{3}$$

**Effect of order of accuracy of B.C. on the numerical solution**

Scheme	$T_2$	$T_3$	$T_4$
Analytical	0.2200	0.4648	0.7616
First order	0.2477	0.5229	0.8563
2nd order	<u>0.2164</u>	<u>0.4570</u>	<u>0.7408</u>

**Practice B, three CVs,  
three inner nodes**



For inner nodes  $T_2, T_3, T_4$  adopting 2<sup>nd</sup> order;

$T_5$  can be calculated from  $T_{M1} = T_{M1-1} + \frac{q_B \cdot \delta x}{\lambda}$

**Numerical results are much closer to exact solution!**

Scheme	$T_2$	$T_3$	$T_4$	$T_5$
Exact	0.1085	0.3377	0.6408	0.7616
Practice B	<u>0.1084</u>	<u>0.3372</u>	<u>0.6035</u>	<u>0.7702</u>

**Question:** How to get the discretized eqs. for 2, 4 ?

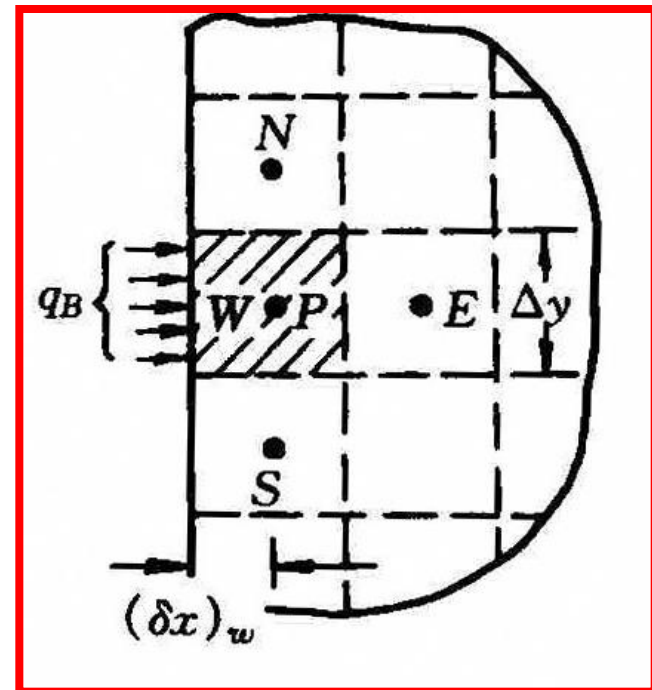
## 2. Additional source term method (ASTM 附加源项法)

### (1) Basic idea

Regarding the heat going into the region by 2<sup>nd</sup> or 3<sup>rd</sup> kind B.C. as the **source term** of the first inner CV; Cutting the connection between inner node and boundary, i.e, regarding the boundary as adiabatic, Hence eliminating (消除) the wall temp. from discretized eqs. of inner nodes.

### (2) Analysis for 2<sup>nd</sup> kind B.C.

$$a_P T_P = a_E T_E + a_W T_W + a_N T_N + a_S T_S + b$$



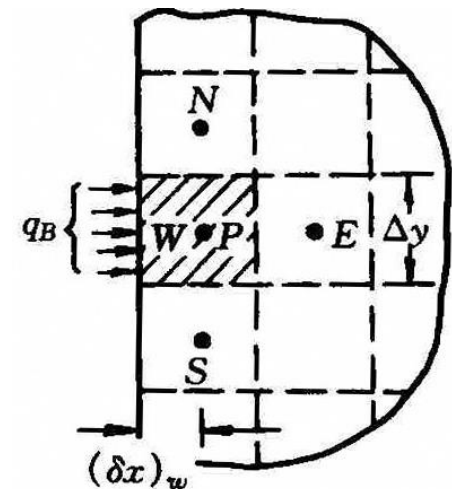
where  $a_W = \frac{\lambda_B \Delta y}{(\delta x)_B}$ . Subtracting  $a_W T_P$  from above eq.

$$(a_P - a_W)T_P = a_E T_E + a_N T_N + a_S T_S + \underline{a_W (T_W - T_P)} + b$$

$$a_W (T_W - T_P) = \Delta y \frac{\lambda_B (T_W - T_P)}{\underline{(\delta x)_B}} = q_B \Delta y \quad (\text{entering as } +)$$

$$a'_P T_P = a_E T_E + a_N T_N + a_S T_S + \frac{q_B \Delta y}{\underline{\Delta V}} \Delta V + S_C \Delta V$$

$$a'_P = a_P - a_W$$

$$S_{C,ad}$$


**Summary of ASTM for 2<sup>nd</sup> kind B.C.:**

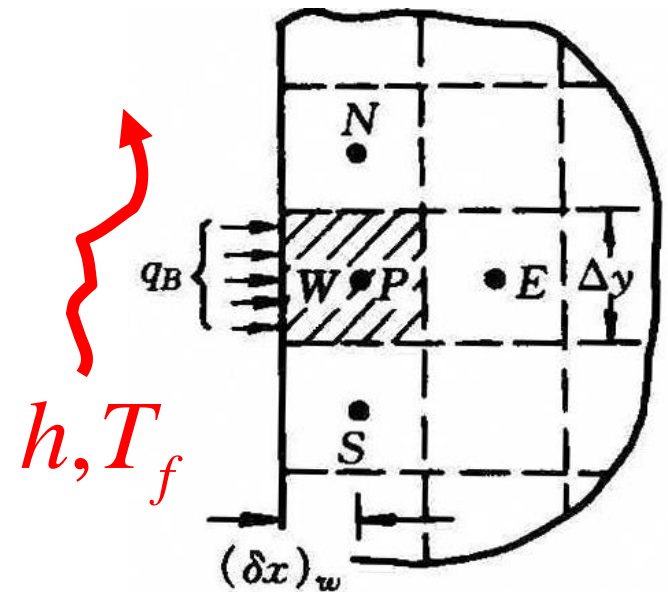
- (1) Adding a source term in discretized eq.  $S_{C,ad} = \frac{q_B \Delta y}{\Delta V}$
- (2) Setting the conductivity of boundary node to be zero, leading to:  $a_W = 0$
- (3) Discretizing inner nodes as usual.

### (3) Analysis for 3<sup>rd</sup> kind B.C.

$$q_B = h(T_f - T_W) \quad (\text{Entering as } +)$$

$$q_B = \frac{T_f - T_W}{\frac{1}{h}} = \frac{T_W - T_P}{\frac{(\delta x)_B}{\lambda_B}} = \frac{T_f - T_P}{\frac{1}{h} + \frac{(\delta x)_B}{\lambda_B}}$$

Substituting the result to the source term for 2<sup>nd</sup> kind B.C.,



$$a'_P T_P = a_E T_E + a_N T_N + a_S T_S + \frac{q_B \Delta y}{\Delta V} \Delta V + S_C \Delta V$$

$$q_B = \frac{T_f - T_P}{\frac{1}{h} + \frac{(\delta x)_B}{\lambda_B}}$$

Substituting  $q_B$

Moving  $T_P$  to left hand,  $T_f$  kept as is, yields:

$$\left\{ a'_P + \frac{\Delta y}{\Delta V \cdot \left[ \frac{1}{h} + \frac{(\delta x)_B}{\lambda_B} \right]} \Delta V \right\} T_P = a_E T_E + a_N T_N + a_S T_S + \left\{ S_C + \frac{\Delta y \cdot T_f}{\Delta V \left[ \frac{1}{h} + \frac{(\delta x)_B}{\lambda_B} \right]} \right\} \Delta V$$

From  $q_B$



$$S_{P,ad} = - \frac{\Delta y}{\Delta V \bullet [1/h + (\delta x)_B / \lambda_B]}$$

$$S_{C,ad} = \frac{\Delta y \bullet T_f}{\Delta V \left[ \frac{1}{h} + \frac{(\delta x)_B}{\lambda_B} \right]}$$

## (4) Implementing procedure of ASTM

- Determining ASTs for CV neighboring to boundary

$$S_{C,ad}, S_{P,ad},$$

- Adding them into source term of related CV

$$S_C \leftarrow S_C + S_{C,ad}$$

Accumulative  
addition (累加)

- **Setting the conductivity of the boun. node to be zero;**
- **Deriving the discretized eqs. of inner nodes as usual,  
Solving the algebraic eqs. for inner nodes;**
- **Using Newton' law of cooling or Fourier eq. to get  
the boundary temperatures from the converged  
solution of inner nodes.**

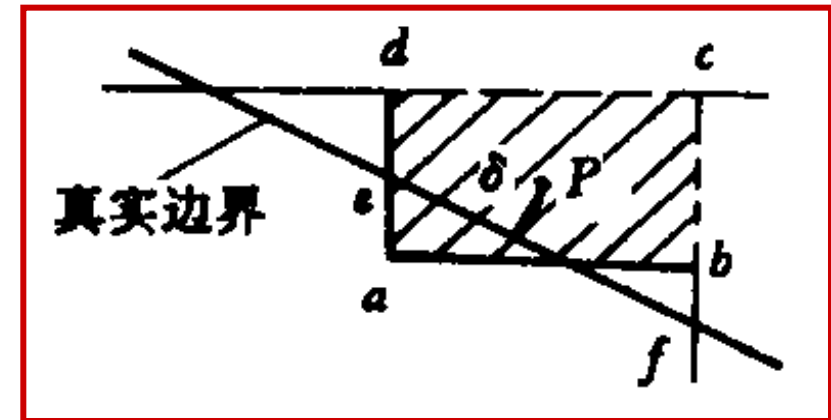
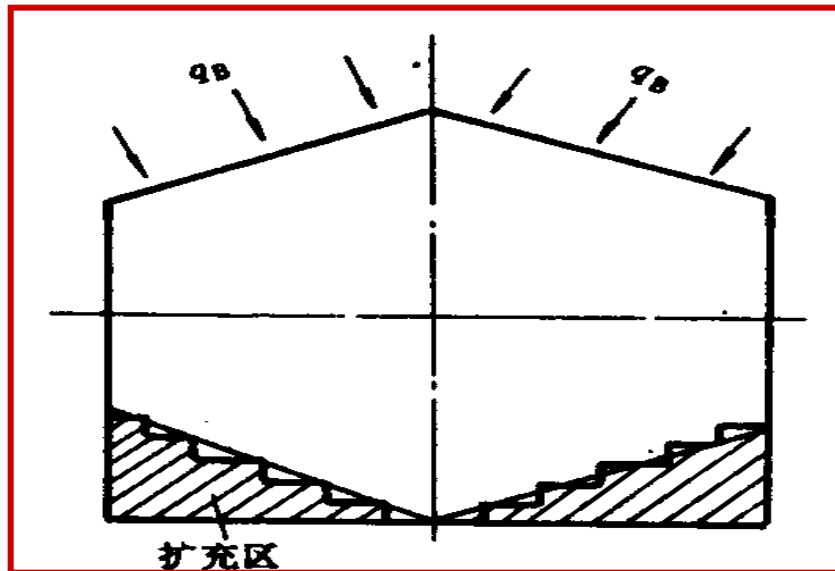
## **(5) Application examples of ASTM**

**In FVM when Practice B is adopted to discretize space, the 2<sup>nd</sup> and 3<sup>rd</sup> kinds of B.C. can be treated by ASTM, which can greatly accelerate(加速) the solution process.**

# Extended applications of ASTM

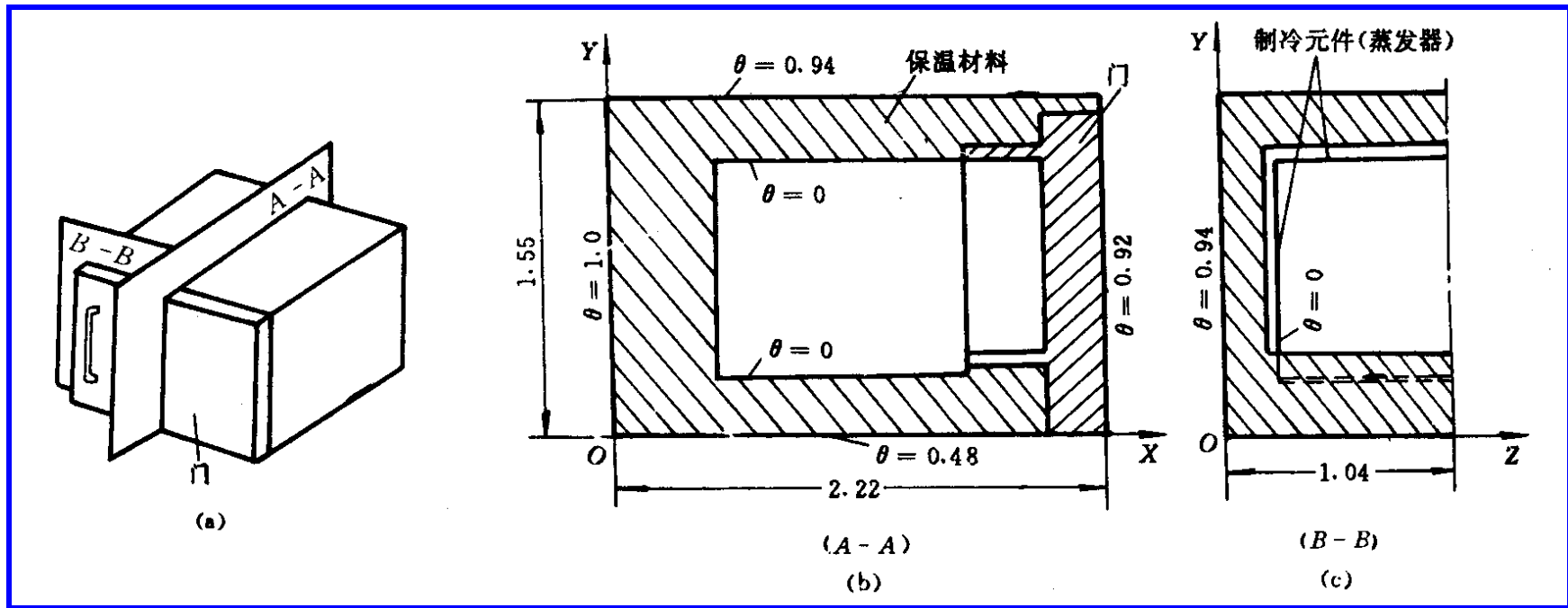
## (1) Dealing with irregular(不规则) boundary

When the code designed for regular region is used to simulated irregular domain, ASTM can be used to treat the B.C.



Prata A T. and Sparrow EM. Heat transfer and fluid flow characteristics for an annulus of periodically varying cross section. **Num Heat Transfer**, 1984, 7:285-304

## (2) Simulating combined conduction, convection and radiation problem

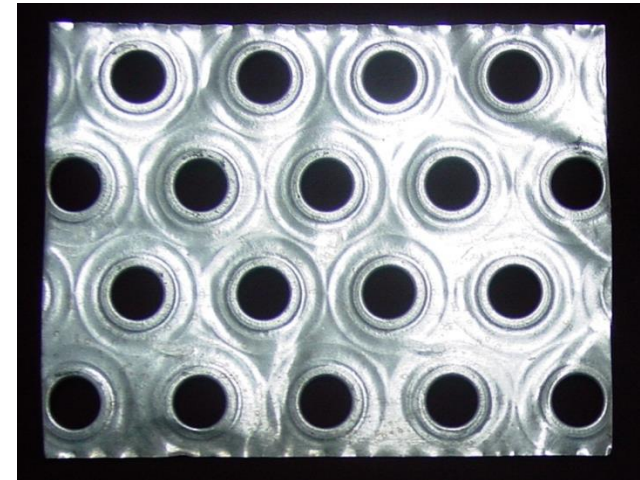
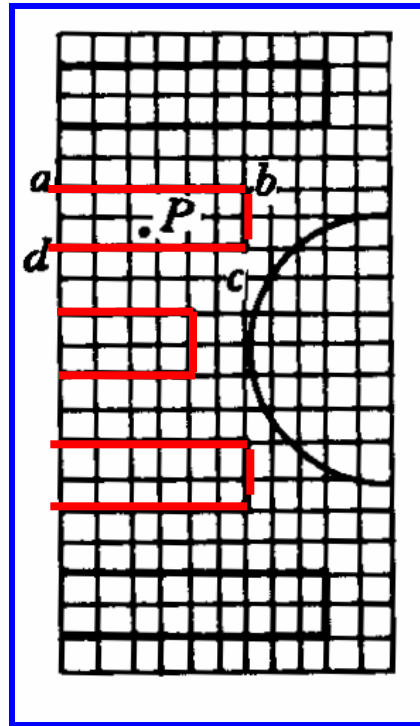
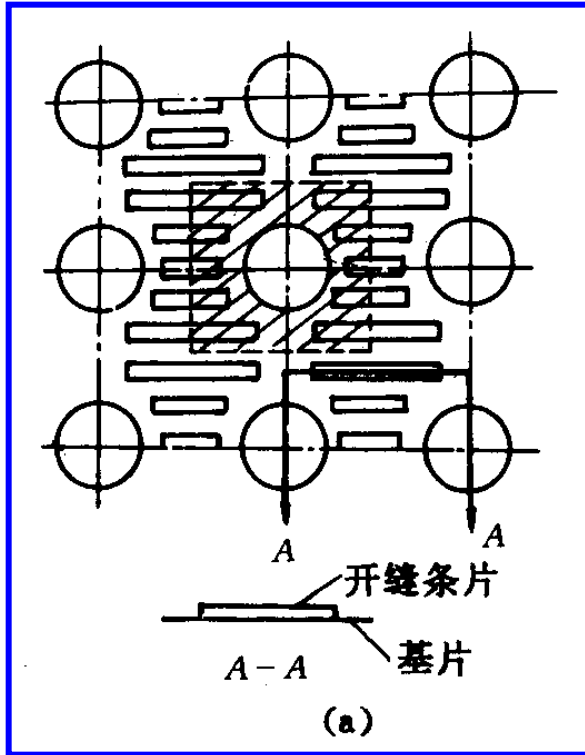


[1] 陶文铨, 李茏. 处理区域内部导热与辐射联合作用的数值方法. **西安交通大学学报**, 1983, 19 (3) : 65-76

[2] 杨沫 王育清 傅燕弘 陶文铨. 家用冰箱冷冻冷藏室温度场的数值模拟. **制冷学报**, 1991年, (4):1-8

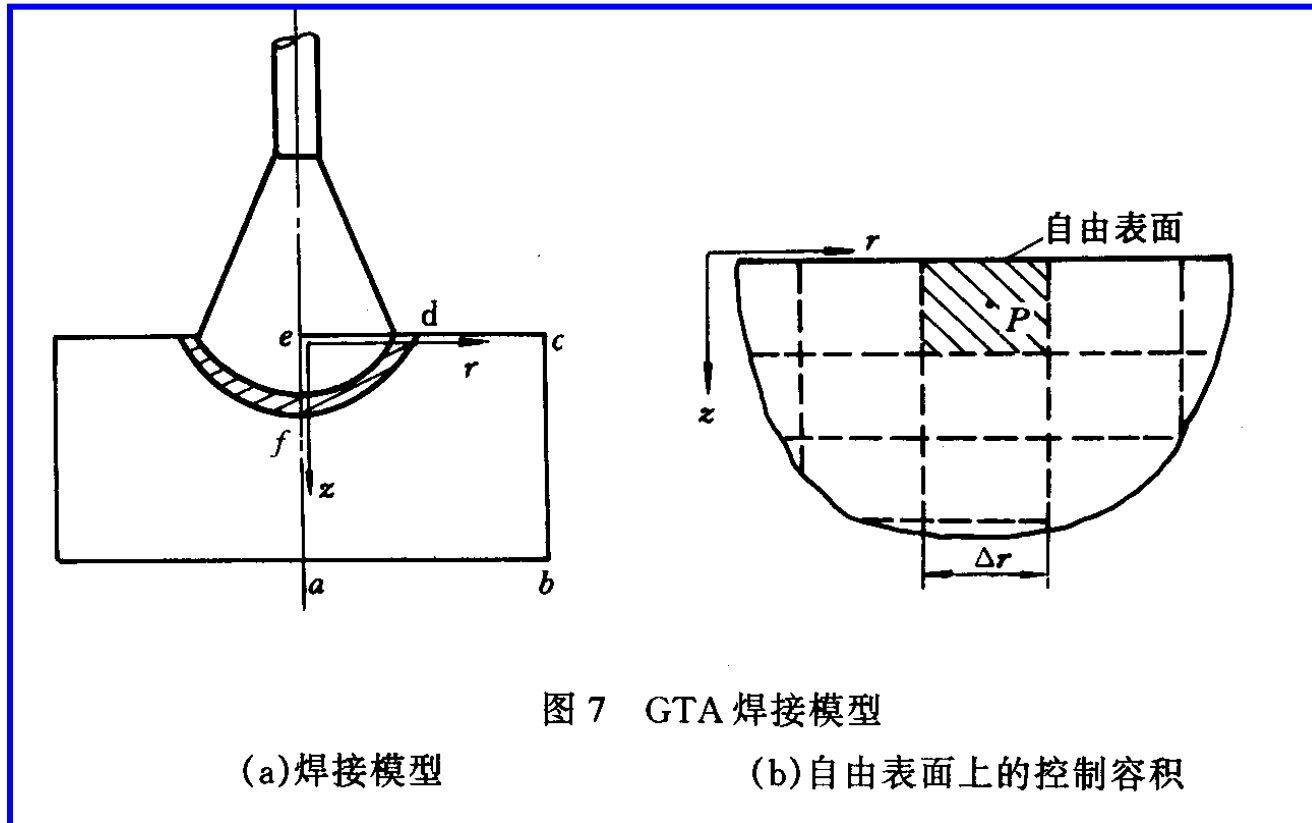
[3] Zhao CY, Tao WQ. Natural convections in conjugated single and double enclosures. **Heat Mass Transfer**, 1995, 30 (3): 175-182

### (3) Determining the efficiency of slotted (开缝) fin

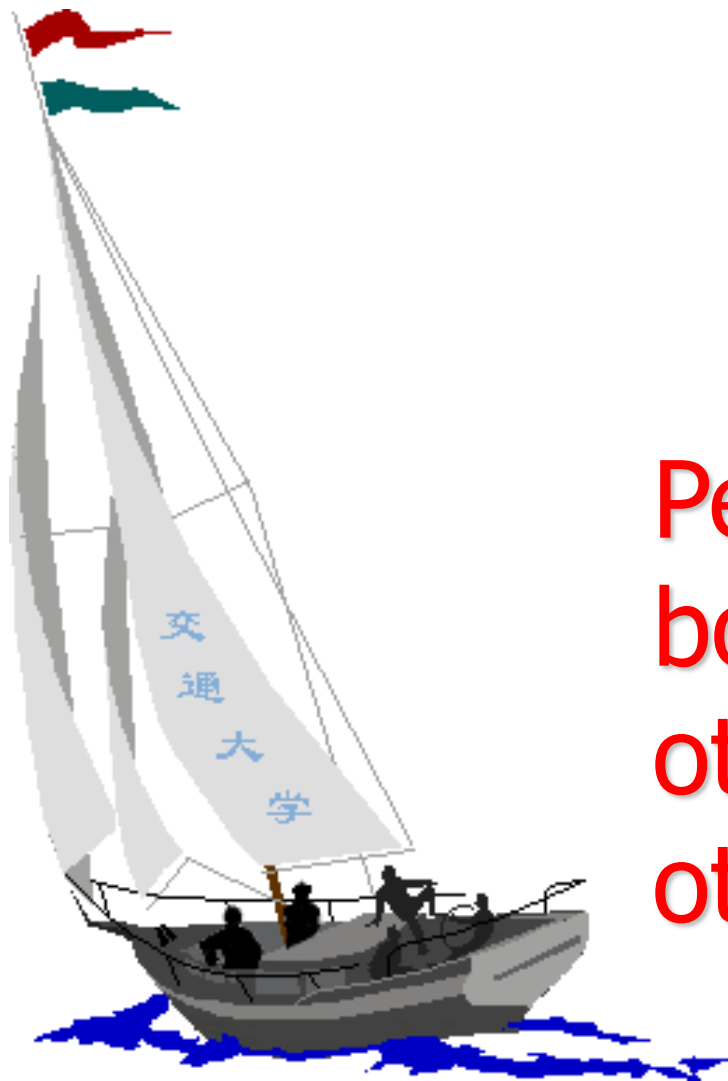


Tao WQ, Lue SS .Numerical method for calculation of slotted fin efficiency in dry condition. **Numerical Heat Transfer, Part A, 1994, 26 (3): 351-362**

# (4) Simulating heat transfer and fluid flow in a welding pool (焊池)



Lei Y P, Shi Y W. Numerical treatment of the boundary conditions and source term of a spot welding process with combining buoyancy – Marangoni flow. **Numerical Heat Transfer, Part b, 1994, 26 : 455-471**



# 同舟共济 渡彼岸!

People in the same  
boat help each  
other to cross to the  
other bank, where....