

# Numerical Heat Transfer

## Chapter 13 Application examples of fluent for basic flow and heat transfer problems



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# 数值传热学

## 第 13 章 求解流动换热问题的Fluent软件基础应用举例



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## 第 13 章 求解流动换热问题的Fluent软件基础应用举例

**13.1 Heat transfer with source term**

**13.2 Unsteady cooling process of a steel ball**

**13.3 Lid-driven flow and heat transfer**

**13.4 Flow and heat transfer in a micro-channel**

**13.5 Flow and heat transfer in chip cooling**

**13.6 Phase change material melting with fins**

## 第 13 章 求解流动换热问题的Fluent软件基础应用举例

**13.1 有内热源的导热问题**

导热问题

**13.2 非稳态圆球冷却问题**

**13.3 顶盖驱动流动换热问题**

混合对流问题

**13.4 微通道内流动换热问题**

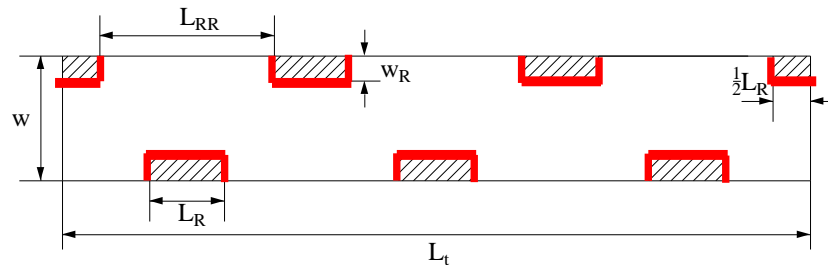
**13.5 芯片冷却流动换热问题**

微通道问题

**13.6 肋片强化相变材料融化**

相变传热

## Example 4: Fluid-solid interface



**This wall type has fluid zone and solid zone on each side. This wall is called a “two-sided-wall”.**

**When such kind wall is read into Fluent, a “shadow” (影子) zone is automatically created.**

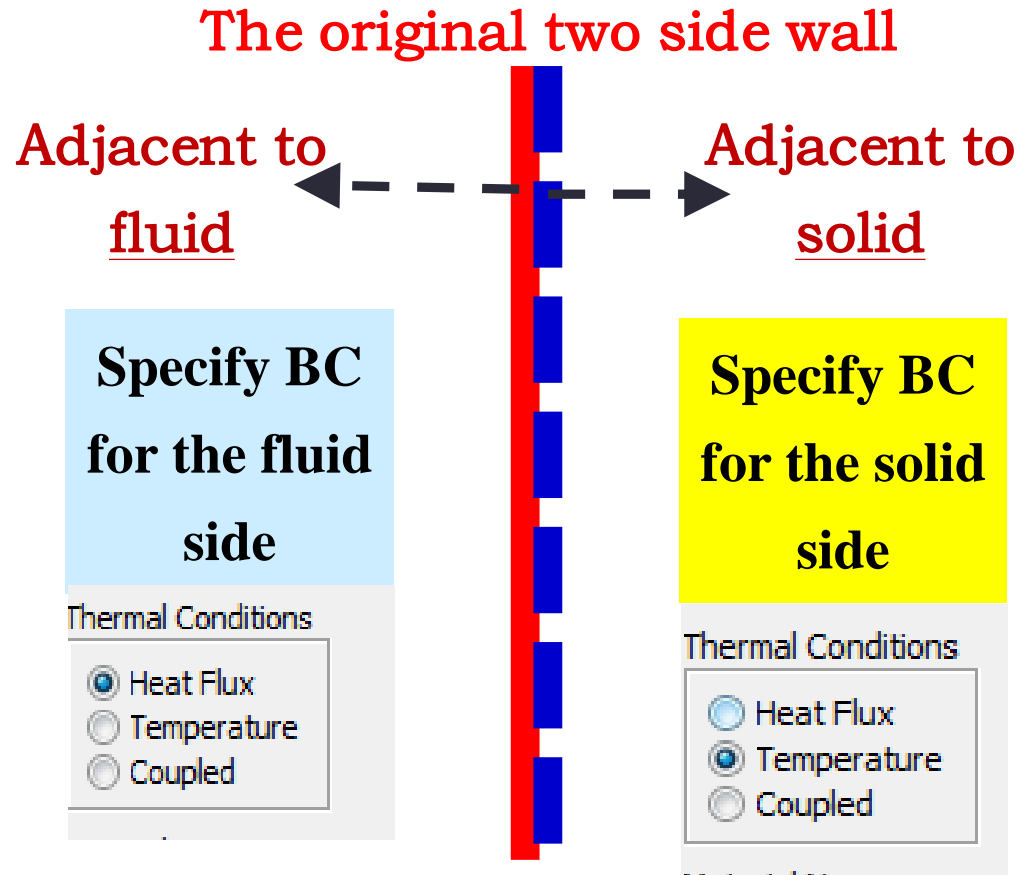
There are three options for the temperature boundary conditions of such “two-sided-wall”.

### Thermal Conditions

- Heat Flux
- Temperature
- Coupled

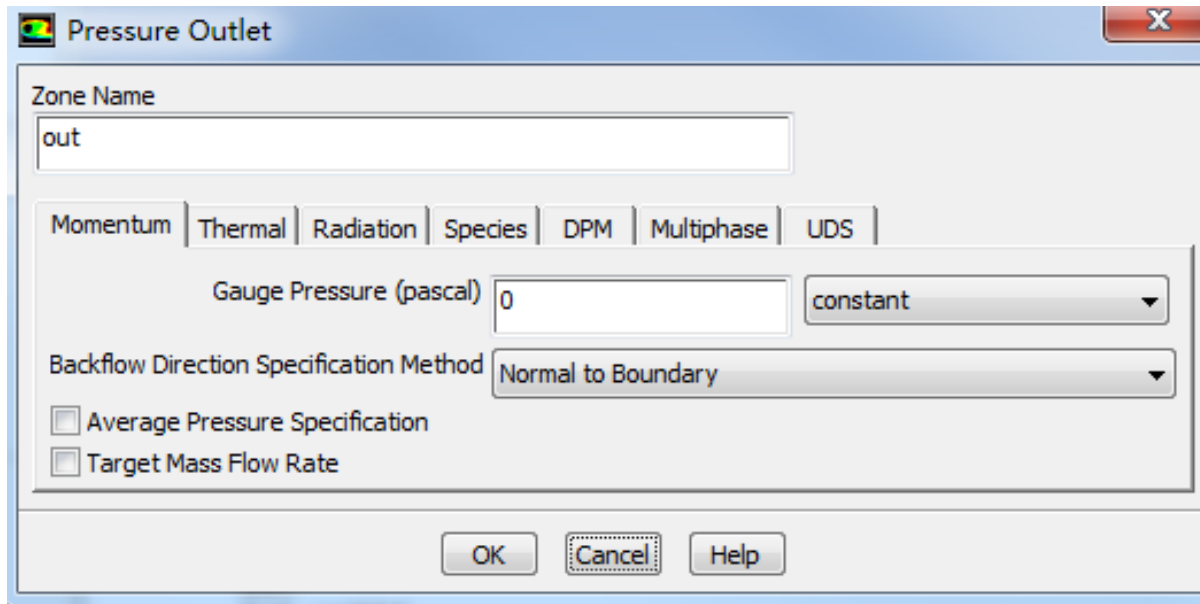
- Heat flux
- Temperature
- **Coupled**

If you choose “**Coupled**”, no additional information is required. The solver will calculate heat transfer directly from the solution of adjacent cells. **Such wall is not a boundary.**



Its shadow created by Fluent

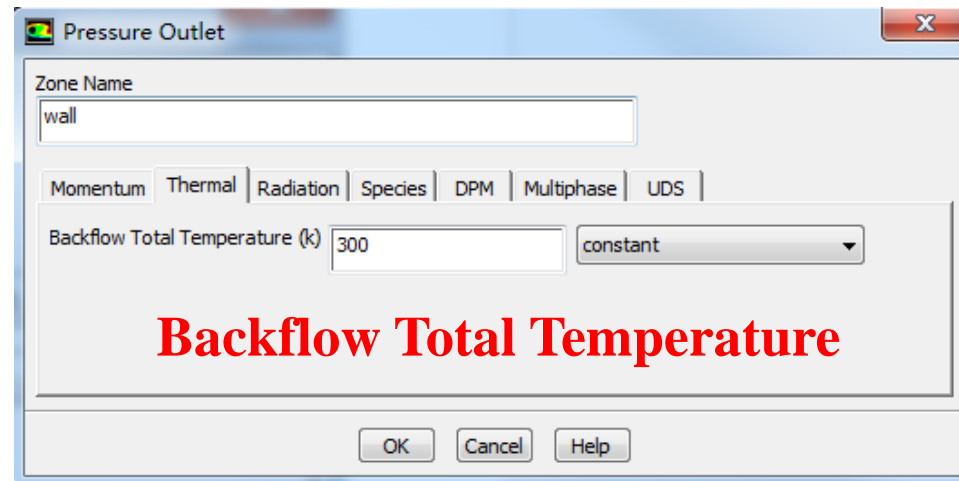
## Pressure outlet boundary condition



Gauge Pressure (表压)

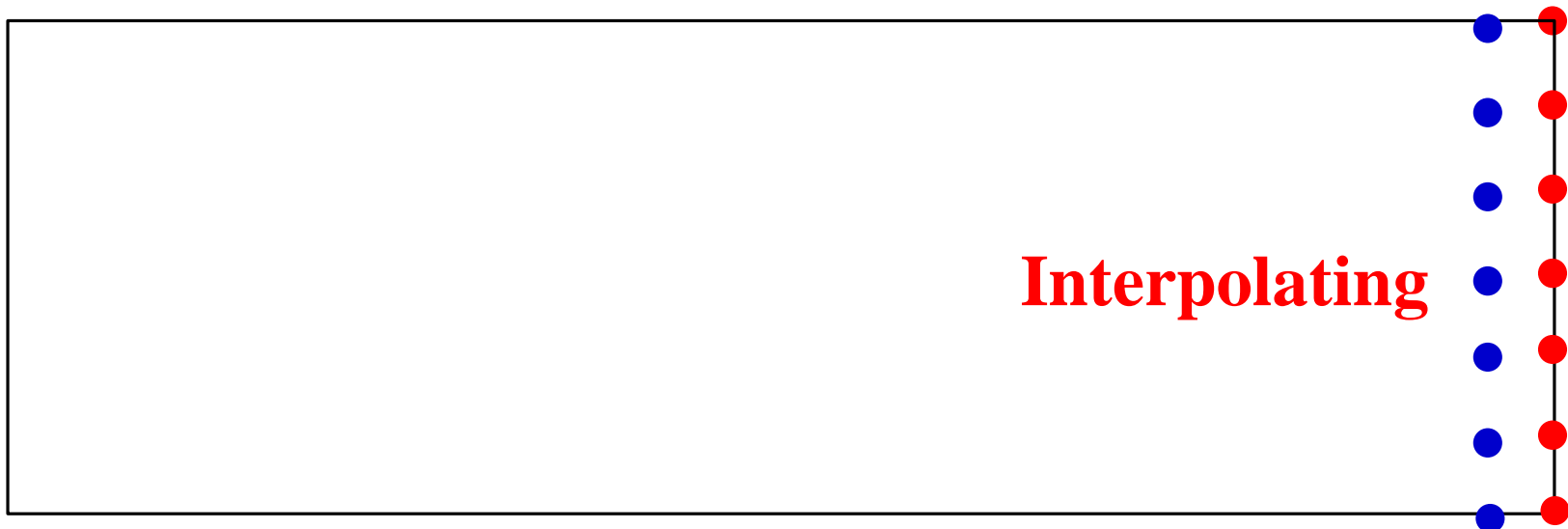


For pressure outlet boundary condition, Fluent asks you to input a **Backflow (回流) Total Temperature**. However, it will play a role only if there is backflow. There is **no information provided by Fluent Help File** about what is the actual boundary condition for heat transfer.



The problem has been asked by many users.

Someone indicate online that the actual value of temperature is calculated using the value of last time step, or by interpolating methods from values of neighboring nodes.



## Pressure in Fluent

**Atmospheric pressure (大气压)**

**Gauge pressure (表压):** the difference between the true pressure and the Atmospheric pressure.

**Absolute pressure (真实压力):** the true pressure

**= Atmospheric pressure + Gauge pressure**

**Operating pressure (操作压力) :** the reference pressure (参考压力)

In our teaching code, a reference pressure point is defined.

## Pressure in Fluent

**Absolute pressure (真实压力):** the true pressure

**= Reference Pressure + Relative Pressure**

**Static pressure (静压):** the difference between true pressure and operating pressure.

**The same as relative pressure.**

**Dynamic pressure (动压):** calculated by  $0.5\rho U^2$

**Is related to the velocity.**

**Total pressure (总压):**

**= Static pressure + dynamic pressure**

## 13.5 Flow and heat transfer in chip cooling

### 芯片冷却流动换热问题

**Focus:** compared with previous examples, this example is a relatively realistic problem. The domain of this Example contains fluid, board (电路板) and chip (芯片) .

## 13.5 Flow and heat transfer in chip cooling

**Known:** Steady laminar flow and convective heat transfer around a board on top of which is a chip with source term. The domain and size is shown in **Fig. 1**. The boundary conditions are as follows:

- Inlet:  $u=0.5\text{m/s}$  (constant)  
 $T=298\text{K}$
- Pressure outlet: Gauge pressure (表压) : 0 Pa.
- Top and bottom boundary: 3<sup>rd</sup> boundary condition  
Heat transfer coefficient:  $H=1.5\text{ W}/(\text{m}^2\text{K})$ ;  
Free stream temperature:  $T_f=298\text{K}$ .

- Chip-- a constant source term,  $904055 \text{ W/m}^3$
- Front surface and back surface---symmetry

Pressure outlet

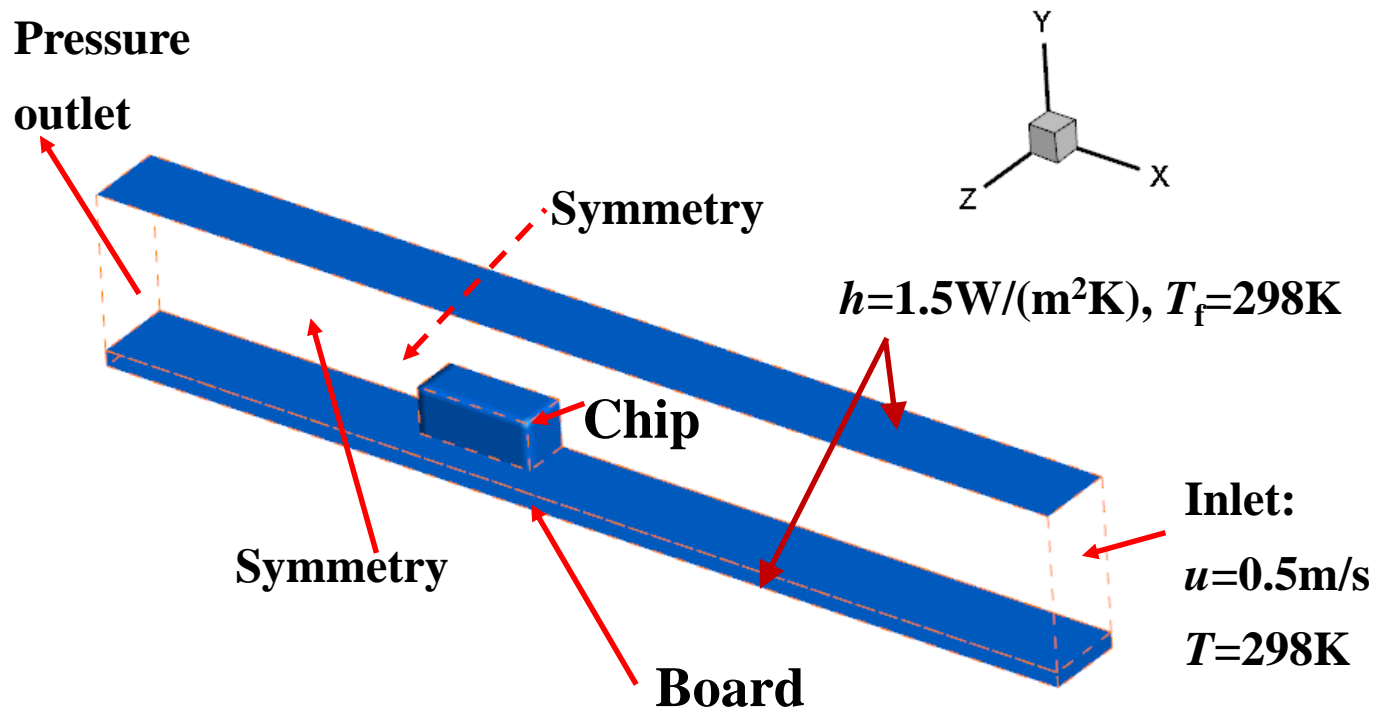


Fig.1 Computational domain

**Find:** Temperature distribution in the domain.

**Solution:**

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho_f} \frac{\partial p}{\partial x} + \frac{\mu_f}{\rho_f} \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{1}{\rho_f} \frac{\partial p}{\partial y} + \frac{\mu_f}{\rho_f} \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

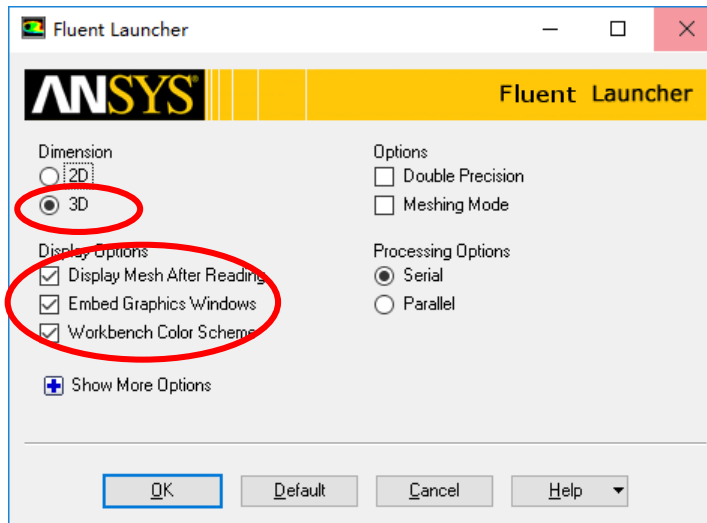
$$u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{1}{\rho_f} \frac{\partial p}{\partial z} + \frac{\mu_f}{\rho_f} \left( \frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right)$$

$$\frac{\partial(\rho_f C_{pf} u_f T_f)}{\partial x} + \frac{\partial(\rho_f C_{pf} v_f T_f)}{\partial y} + \frac{\partial(\rho_f C_{pf} w_f T_f)}{\partial z} = \lambda_f \left( \frac{\partial^2 T_f}{\partial x^2} + \frac{\partial^2 T_f}{\partial y^2} + \frac{\partial^2 T_f}{\partial z^2} \right)$$

$$0 = \lambda_s \left( \frac{\partial^2 T_s}{\partial x^2} + \frac{\partial^2 T_s}{\partial y^2} + \frac{\partial^2 T_s}{\partial z^2} \right) + s$$



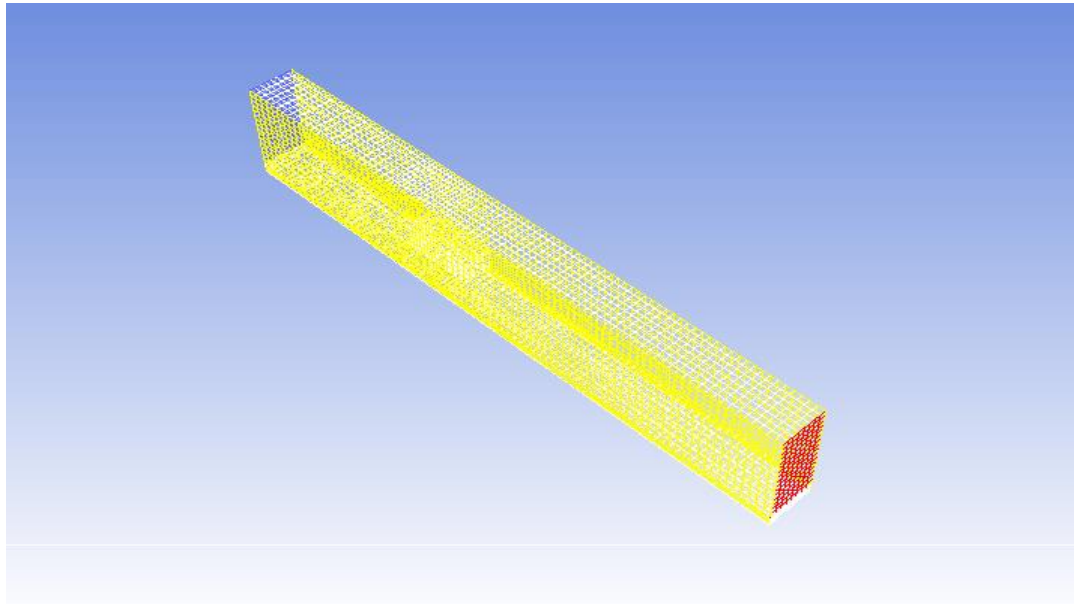
## 13.5.1 Start the Fluent software



1. Choose **3-Dimension**
2. Choose display options
3. Choose Serial processing option

## 1st step: **Read** and check the mesh

- The mesh is generated by pre-processing software such as **ICEM** and **GAMBIT**. The document is with suffix (后缀名) “**xx.msh**”





## 1st step: Read and **check** the mesh

### Mesh→Check

- Check the **quality and topological information** of the mesh

#### Mesh Check

##### Domain Extents:

x-coordinate: min (m) = 0.000000e+00, max (m) = 1.651000e-01

y-coordinate: min (m) = 0.000000e+00, max (m) = 2.794000e-02

z-coordinate: min (m) = -2.540000e-07, max (m) = 1.270000e-02

##### Volume statistics:

minimum volume (m3): 1.119834e-09

maximum volume (m3): 7.845747e-09

total volume (m3): 5.858386e-05

##### Face area statistics:

minimum face area (m2): 8.370037e-07

maximum face area (m2): 4.194085e-06

Checking mesh.....

Done.

## 2st step: Scale the domain size

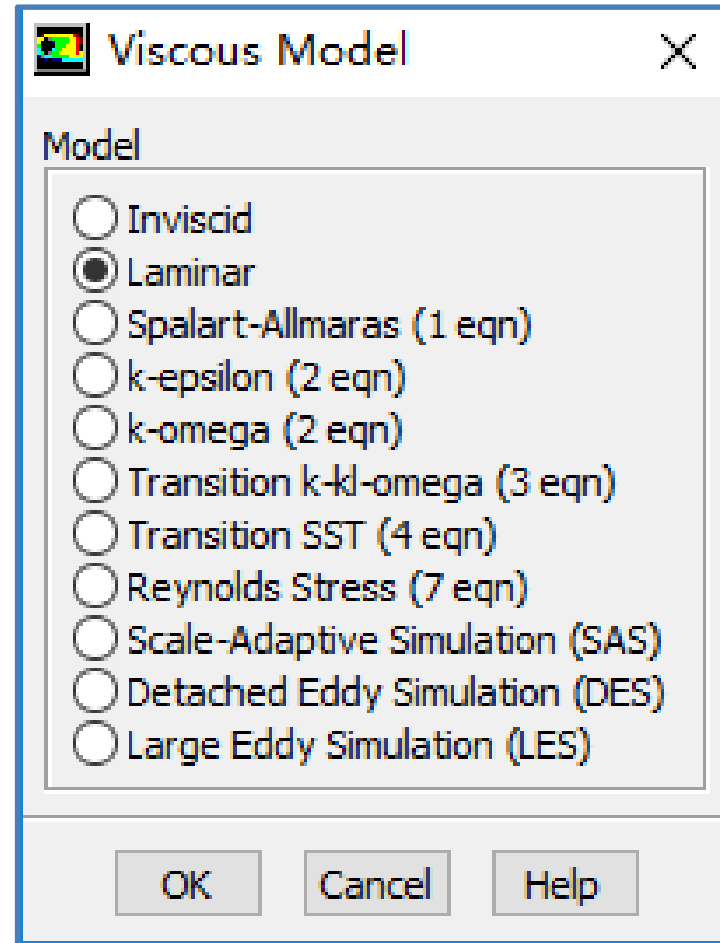
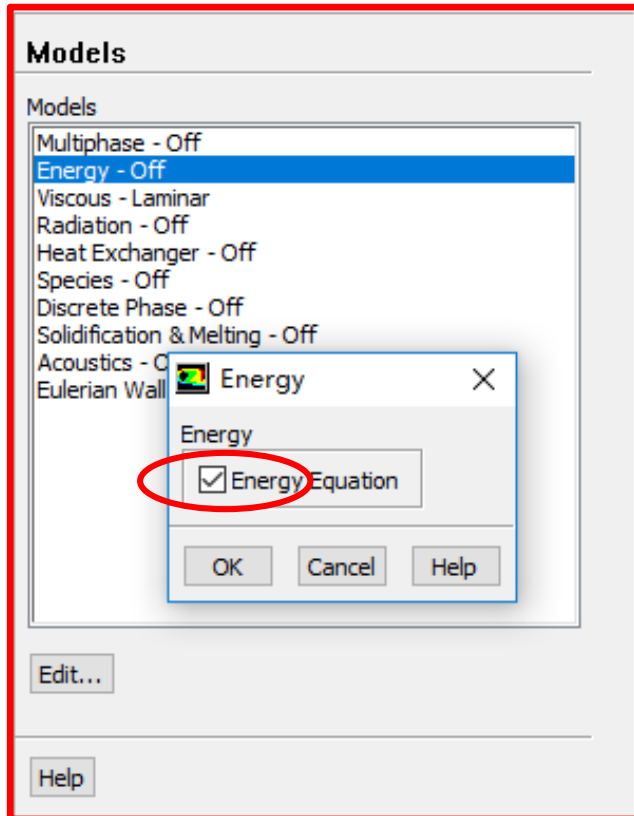
General → Scale

## 3st step: Choose the physicochemical model

*Re* number is calculated to determine the fluid state (laminar or turbulent)

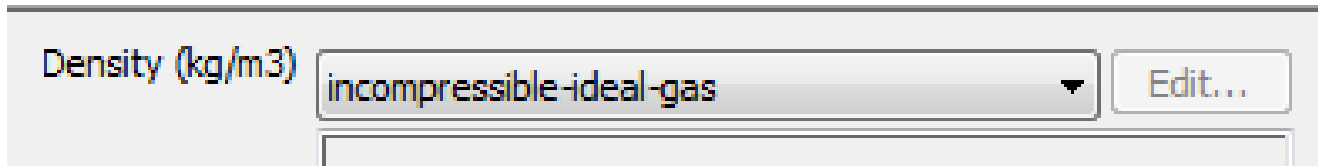
$$Re = \frac{\rho u l}{\mu}$$

The density of air is 1.29 Kg/m<sup>3</sup>, the inlet velocity is 0.5 m/s, characteristic length is about 2 cm, and kinetic viscosity of air is 1.7894E-05. *Re* is 720 and thus flow is **laminar**.



## Step 4: Define the material properties

If you calculate the density using the **ideal gas law**, the solver will compute the density according to **ideal gas state equation**.



### Define a new material as Chip:

density  $1000 \text{ kg/m}^3$ ,  $C_p$   $500 \text{ J/(kg K)}$  and thermal conductivity  $1 \text{ W/(mK)}$

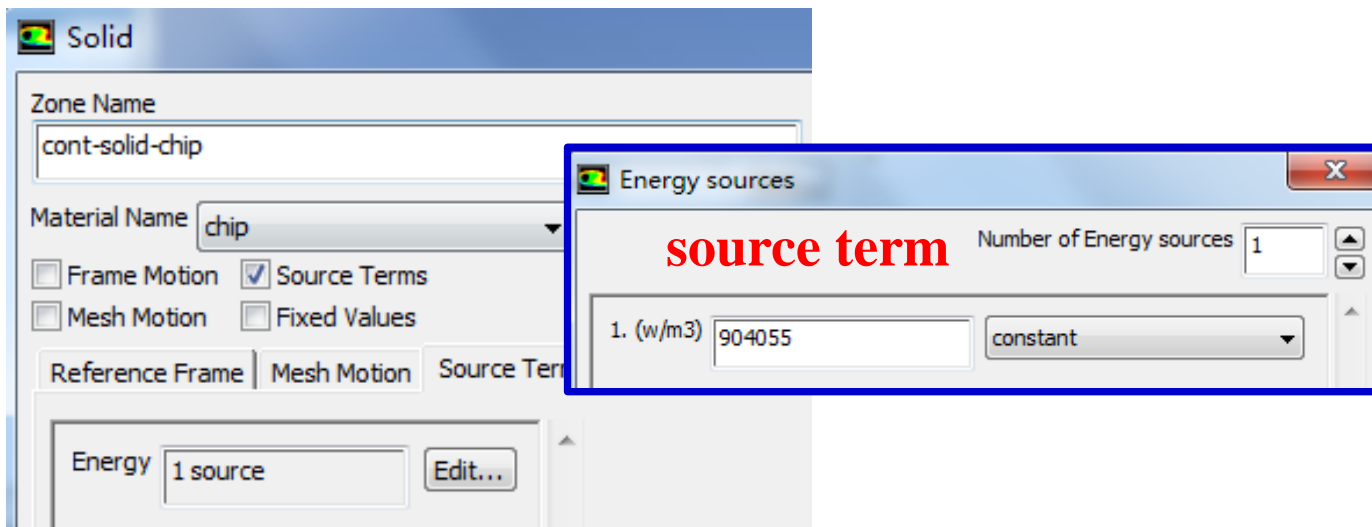
### Define a new material as Board:

density  $2000 \text{ kg/m}^3$ ,  $C_p$   $600 \text{ J/(kg K)}$  and thermal conductivity  $0.1 \text{ W/(mK)}$

## Step 5: Define zone condition

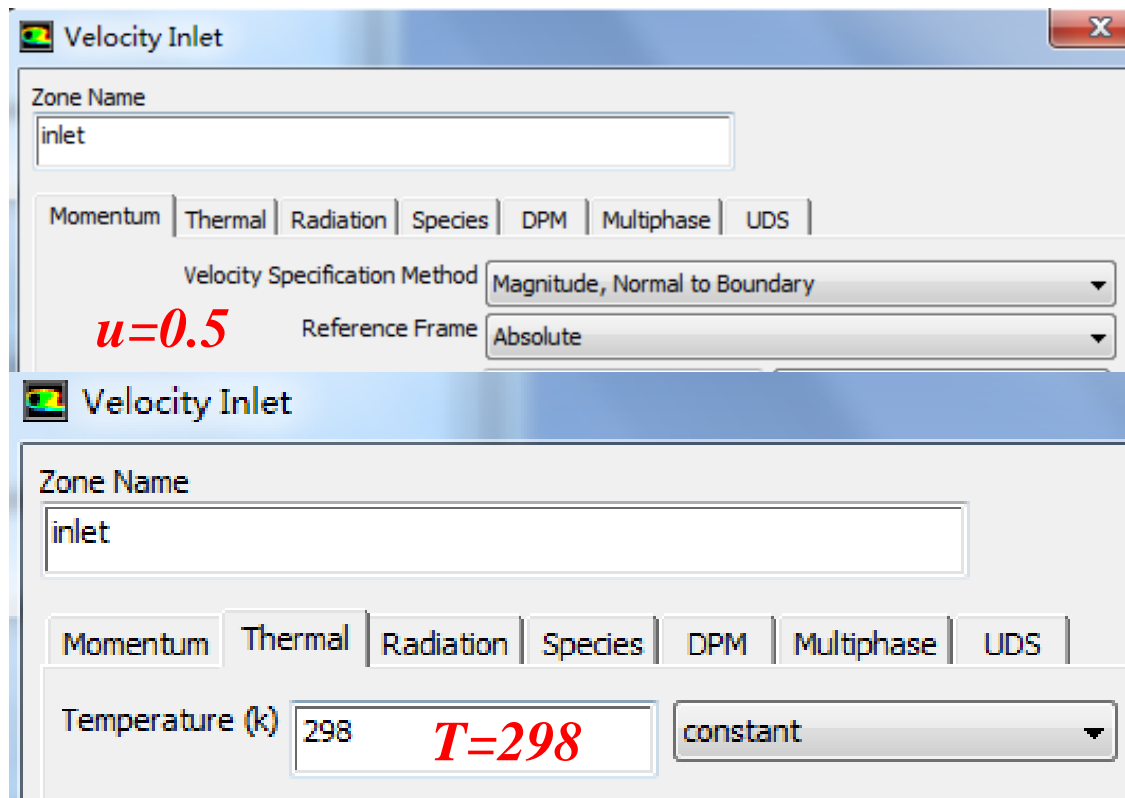
Assign different regions with the corresponding materials.

For the chip, there is a source term with value of  $904055 \text{ W/m}^3$



## Step 6: Define the boundary condition

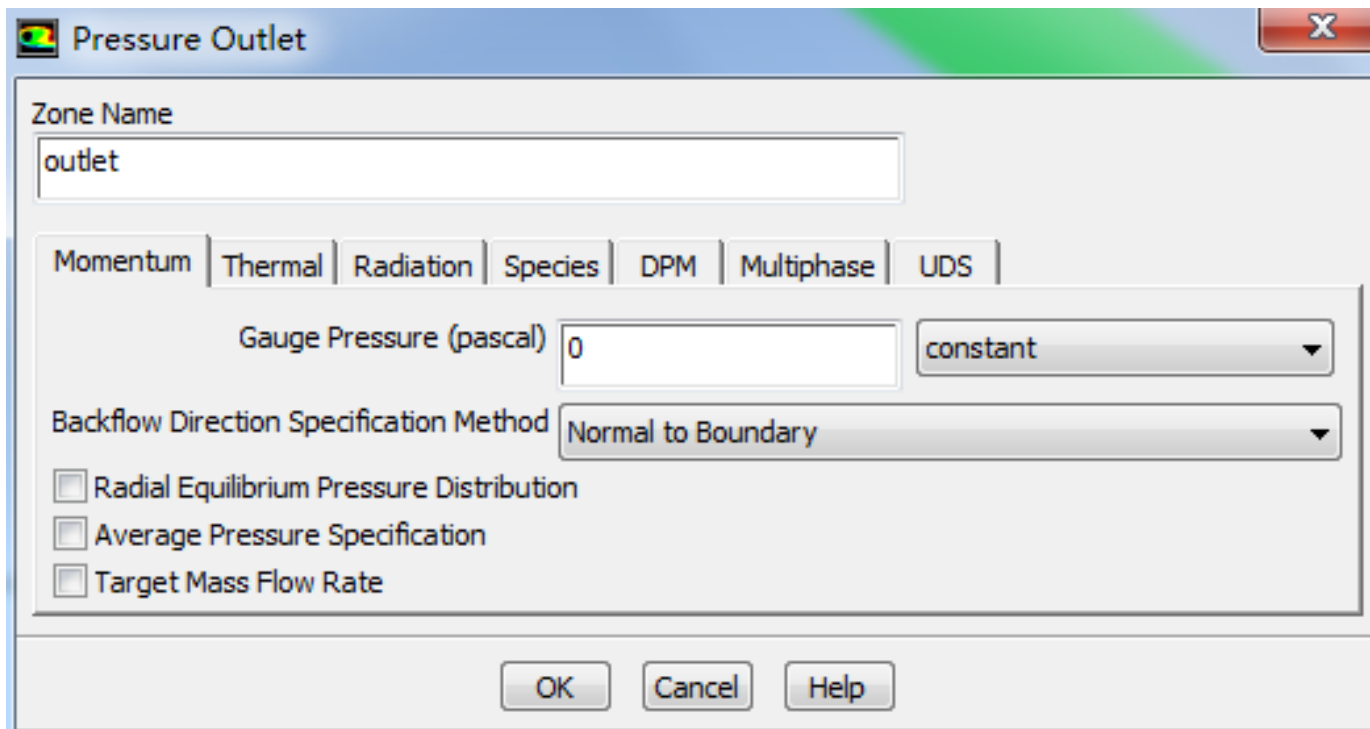
Inlet:  $u$  and  $T$  are specified.





## Step 6: Define the boundary condition

**Outlet: pressure outlet, Gauge pressure as 0.**



Pressure Outlet

Zone Name  
outlet

Momentum | Thermal | Radiation | Species | DPM | Multiphase | UDS

Gauge Pressure (pascal) 0 constant

Backflow Direction Specification Method Normal to Boundary

Radial Equilibrium Pressure Distribution  
 Average Pressure Specification  
 Target Mass Flow Rate

OK Cancel Help

## Step 6: Define the boundary condition

### Top and bottom wall: convective boundary condition

The screenshot shows a 'Wall' dialog box with the following settings:

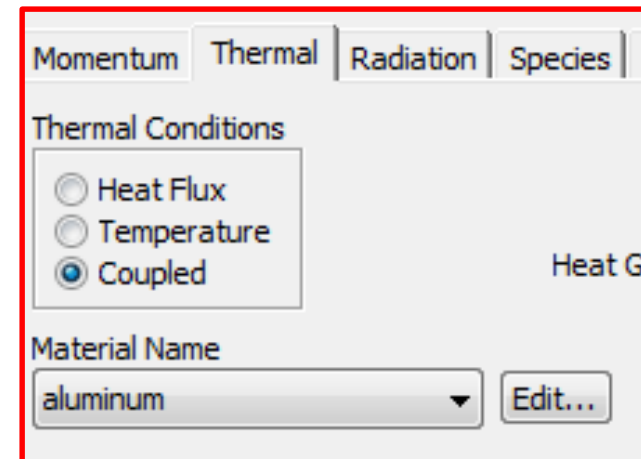
- Zone Name: wall-board-bottom
- Adjacent Cell Zone: cont-solid-board
- Thermal Conditions:  Convection
- Heat Transfer Coefficient (w/m<sup>2</sup>-k): 1.5, constant
- Free Stream Temperature (k): 298, constant
- Wall Thickness (in): 0
- Material Name: aluminum
- Heat Generation Rate (w/m<sup>3</sup>): 0, constant
- Shell Conduction:  Shell Conduction Define...

Buttons: OK, Cancel, Help

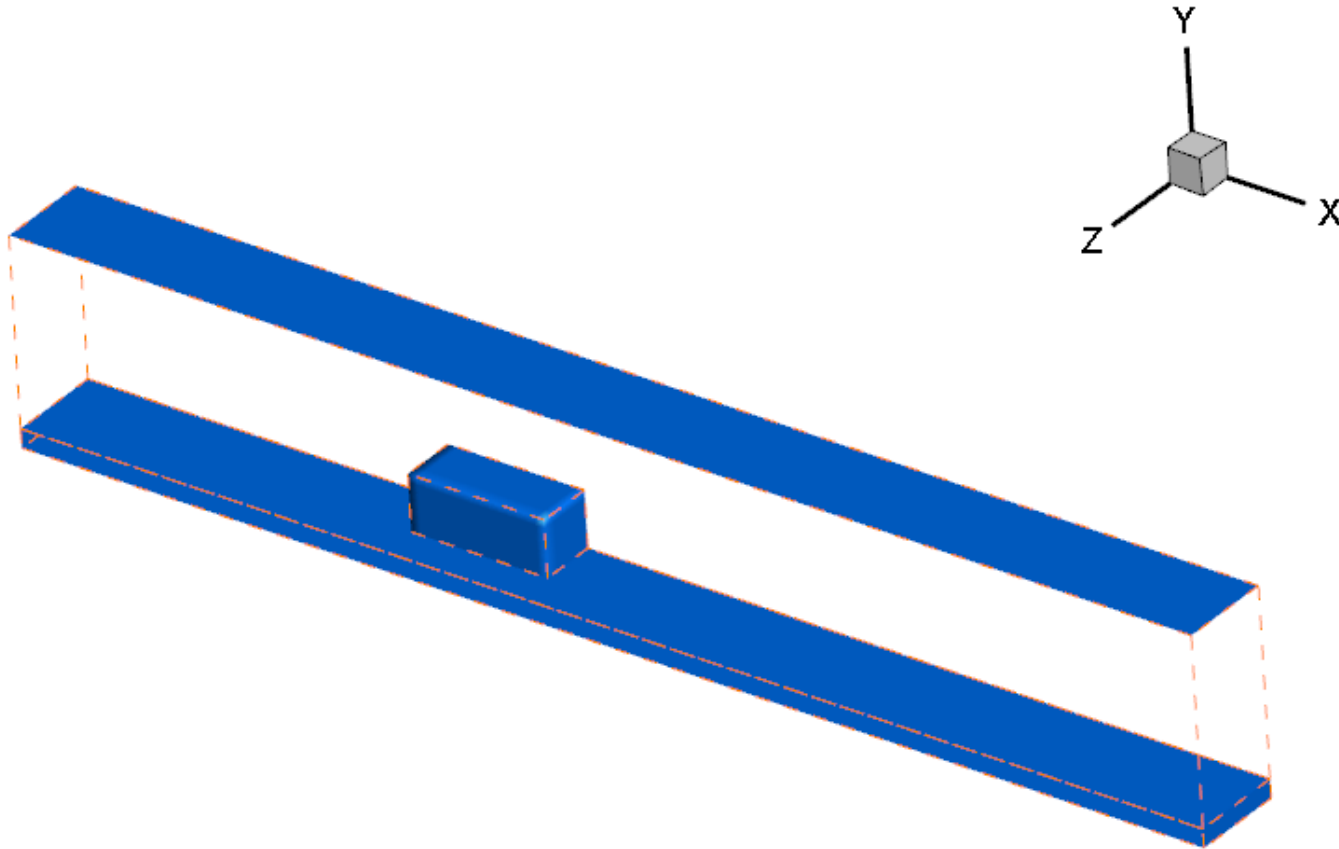
## Step 6: Define the boundary condition

For the front and back boundaries, keep the default set up of **Symmetry**.

For all the other “two-side-walls” boundaries in the domain, keep the default set up for thermal conditions, namely “**Coupled**”. *For details of “Coupled” and “uncoupled” conditions, refer to Example 4 in Chapter 13.*

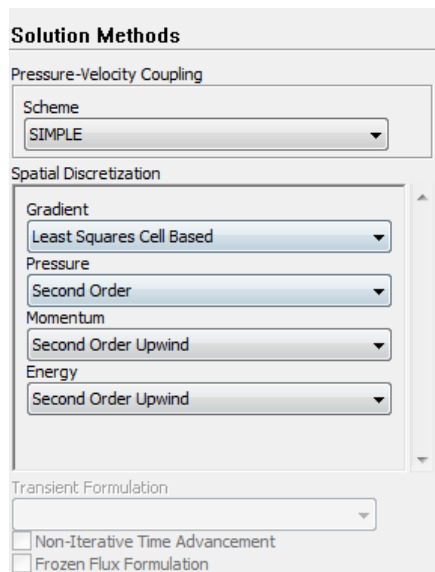


There are many **two-sided-wall** in this Example.



## 7st step: Define the solution

For algorithm and schemes, keep it as default. For more details of this step, one can refer to **Example 1** of Chapter 13.



**Algorithm:** simple

**Gradient:** Least Square Cell Based

**Pressure:** second order

**Momentum:** second order upwind

**Energy:** second order Upwind



## 7st step: **Define the solution**

For under-relaxation factor, keep it default. For more details, refer to **Example 1**.

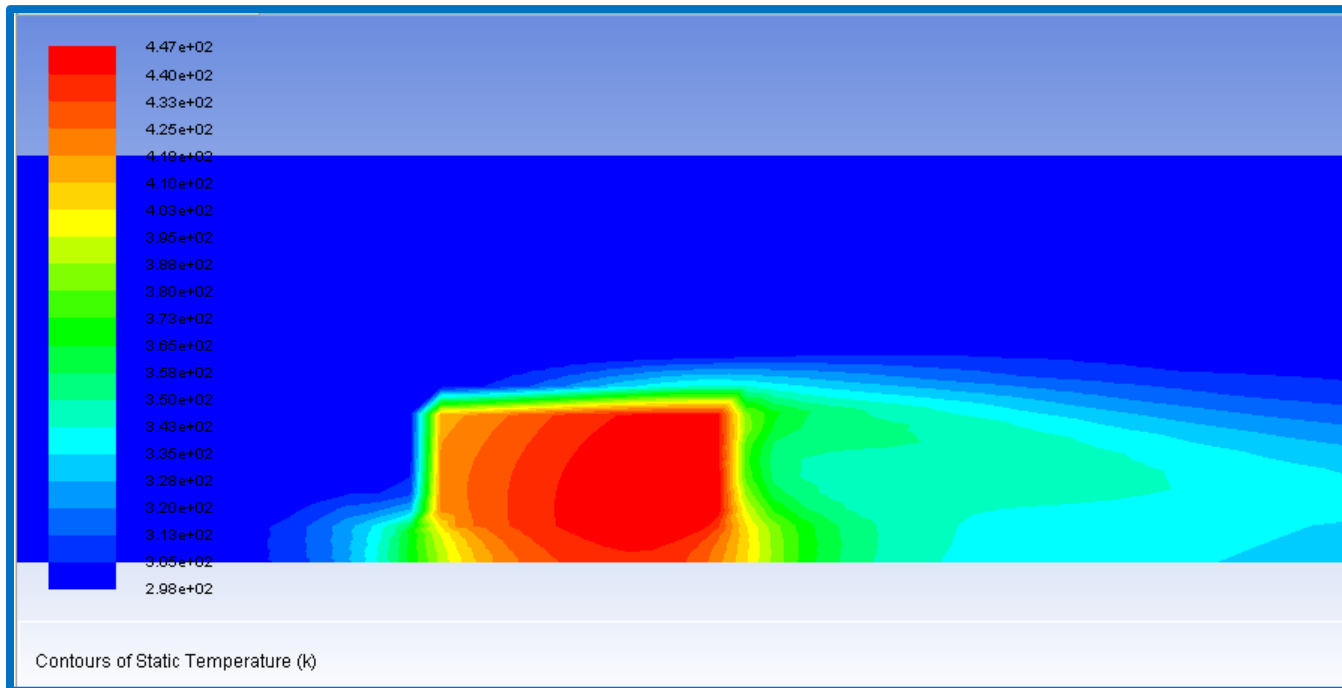
## 8st step: Initialization

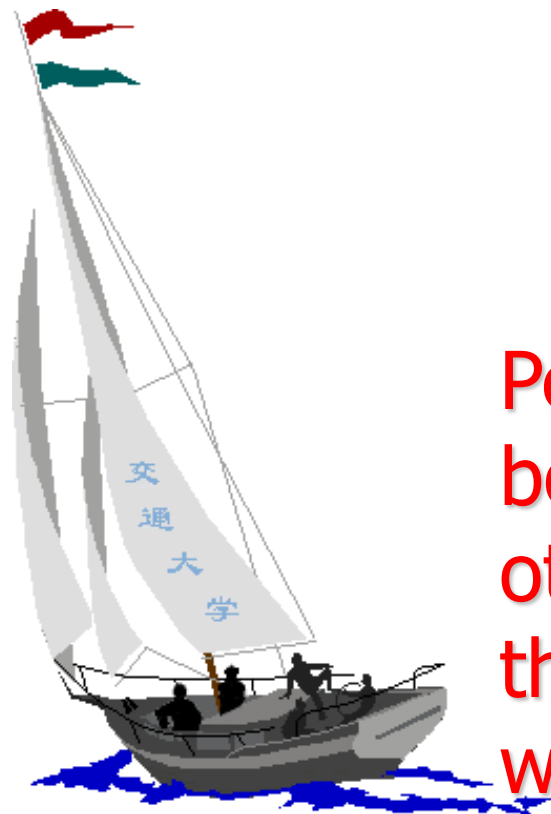
Use the standard initialization, for more details of Hybrid initialization, refer to Example 1.

## Step 9: Run the simulation

## Step 10: Post-processing results

## Static Temperature(K) of back boundary





# 同舟共济 渡彼岸!

People in the same  
boat help each  
other to cross to  
the other bank,  
where....