

# Numerical Heat Transfer

## Chapter 13 Application examples of fluent for basic flow and heat transfer problems



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# 数值传热学

## 第 13 章 求解流动换热问题的Fluent软件基础应用举例



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## 第 13 章 求解流动换热问题的Fluent软件基础应用举例

**13.1 Conductive heat transfer in a heat sink**

**13.2 Unsteady cooling process of a steel ball**

**13.3 Flow and heat transfer in a micro-channel**

**13.4 Flow and heat transfer in chip cooling**

**13.5 Liquid cooling of photovoltaic panel**

**13.6 Phase change material melting with fins**

## 第 13 章 求解流动换热问题的Fluent软件基础应用举例

**13.1 散热装置导热问题**

导热问题

**13.2 非稳态圆球冷却问题**

**13.3 微通道内流动换热问题**

**13.4 芯片冷却流动换热问题**

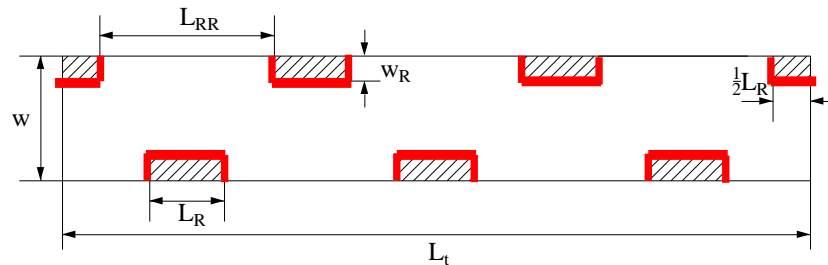
对流传热问题

**13.5 太阳能光伏板水冷问题**

**13.6 肋片强化相变材料融化**

相变传热

## Example 4: Fluid-solid interface

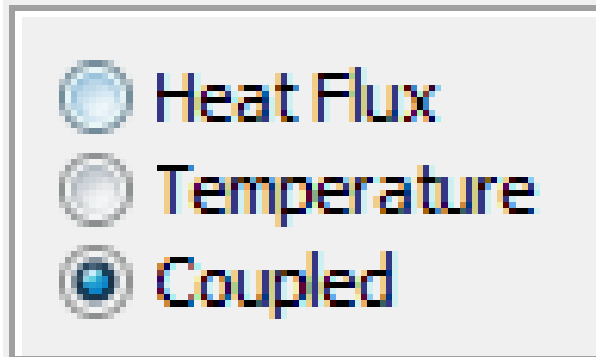


**This wall type has fluid zone and solid zone on each side. This wall is called a “two-sided-wall”.**

**When such kind wall is read into Fluent, a “shadow” (影子) zone is automatically created.**

There are three options for the temperature boundary conditions of such “two-sided-wall”.

### Thermal Conditions

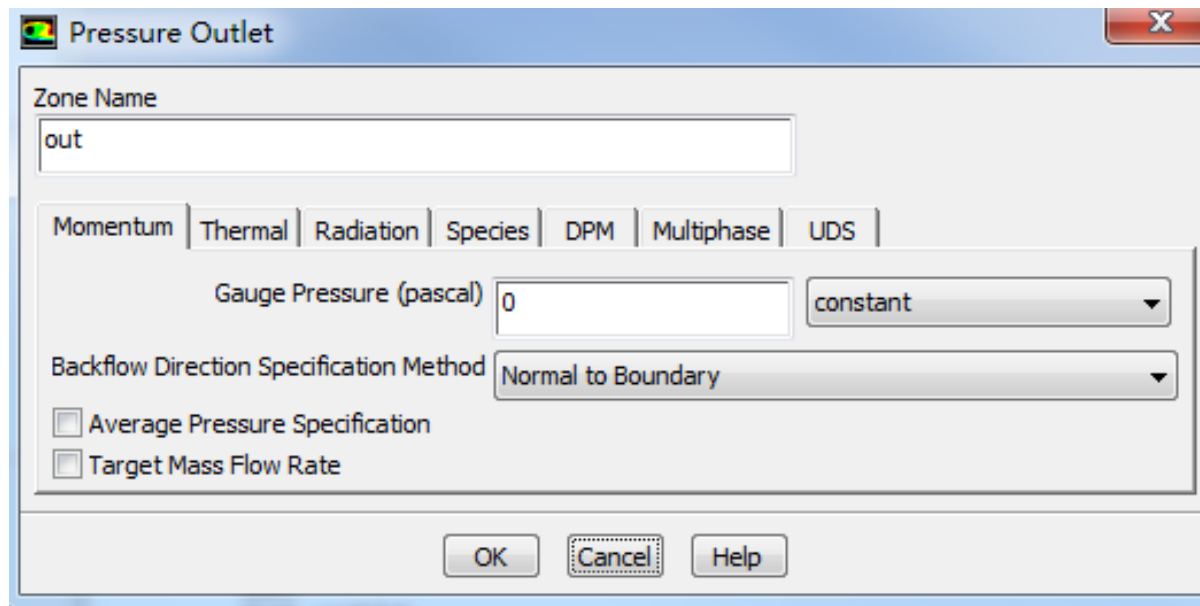


- Heat flux
- Temperature
- **Coupled**

If you choose “**Coupled**”, no additional information is required. The solver will calculate heat transfer directly from the solution of adjacent cells. **Such wall is not a boundary.**



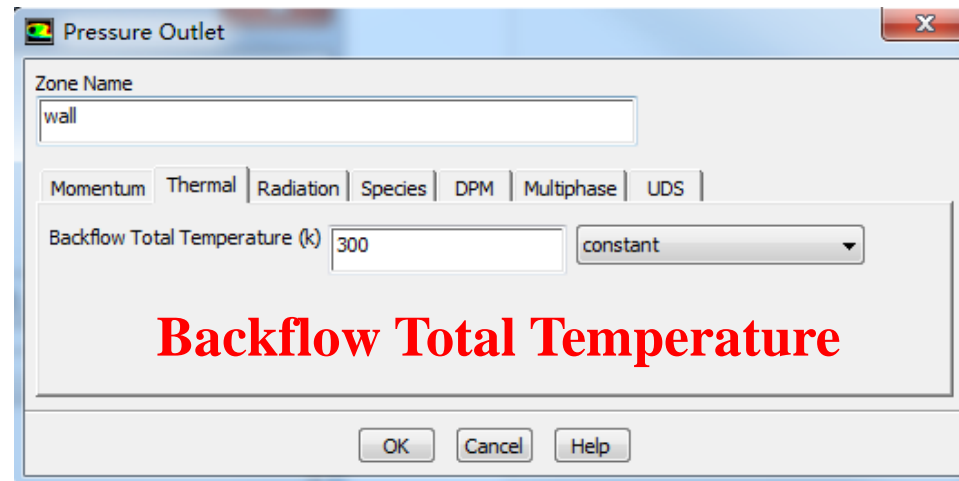
## Pressure outlet boundary condition



Gauge Pressure (表压)

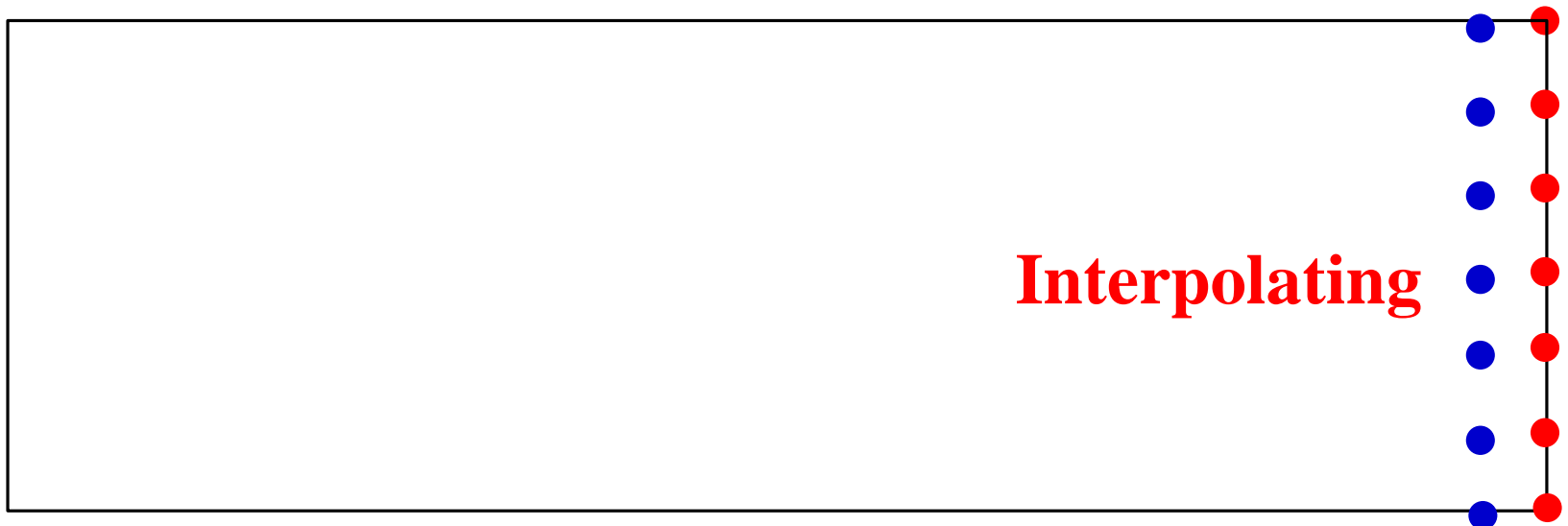


For pressure outlet boundary condition, Fluent asks you to input a **Backflow (回流) Total Temperature**. However, it will play a role only if there is backflow. There is **no information provided by Fluent Help File** about what is the actual boundary condition for heat transfer.



**The problem has been asked by many users.**

Someone indicate online that the actual value of temperature is calculated using **the value of last time step**, or by **interpolating methods** from values of neighboring nodes.



## Pressure in Fluent

**Atmospheric pressure (大气压)**

**Gauge pressure (表压):** the difference between the true pressure and the Atmospheric pressure.

**Absolute pressure (真实压力):** the true pressure

**= Atmospheric pressure + Gauge pressure**

**Operating pressure (操作压力) :** the reference pressure (参考压力)

In our teaching code, a reference pressure point is defined.

## Pressure in Fluent

**Absolute pressure (真实压力):** the true pressure

**= Reference Pressure + Relative Pressure**

**Static pressure (静压):** the difference between true pressure and operating pressure.

**The same as relative pressure.**

**Dynamic pressure (动压):** calculated by  $0.5\rho U^2$

**Is related to the velocity.**

**Total pressure (总压):**

**= Static pressure + dynamic pressure**

## 13.5 Flow and heat transfer in chip cooling

### 芯片冷却流动换热问题

**Focus:** compared with previous examples, this example is a relatively realistic problem. The domain of this Example contains fluid, board (电路板) and chip (芯片) .

## 13.5 Flow and heat transfer in chip cooling

**Known:** Steady laminar flow and convective heat transfer around a board on top of which is a chip with source term. The domain and size is shown in **Fig. 1**. The boundary conditions are as follows:

- Inlet:  $u=0.5\text{m/s}$  (constant)  
 $T=298\text{K}$
- Pressure outlet: Gauge pressure (表压) : 0 Pa.
- Top and bottom boundary: 3<sup>rd</sup> boundary condition  
Heat transfer coefficient:  $h=1.5\text{ W}/(\text{m}^2\text{K})$ ;  
Free stream temperature:  $T_f=298\text{K}$ .

- Chip-- a constant source term,  $904055 \text{ W/m}^3$
- Front surface and back surface---symmetry

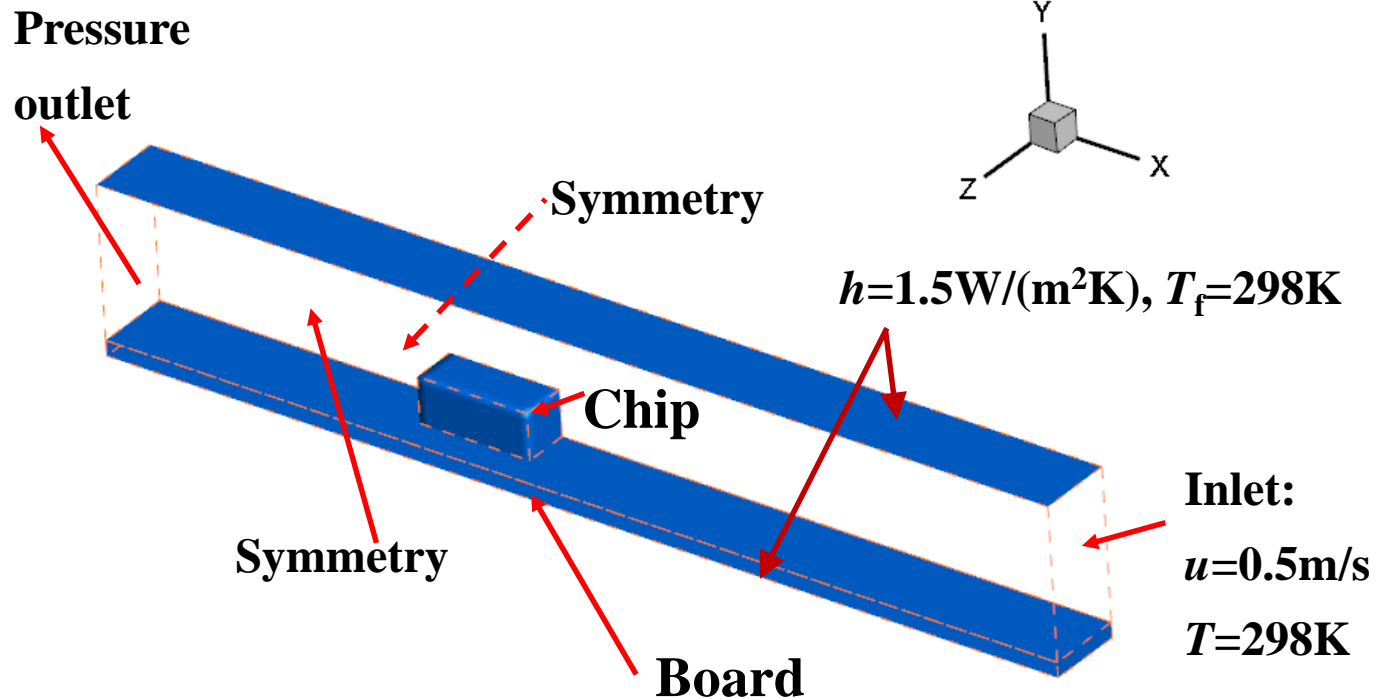


Fig.1 Computational domain

**Find:** Temperature distribution in the domain.

**Solution:**

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho_f} \frac{\partial p}{\partial x} + \frac{\mu_f}{\rho_f} \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{1}{\rho_f} \frac{\partial p}{\partial y} + \frac{\mu_f}{\rho_f} \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

$$u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{1}{\rho_f} \frac{\partial p}{\partial z} + \frac{\mu_f}{\rho_f} \left( \frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right)$$

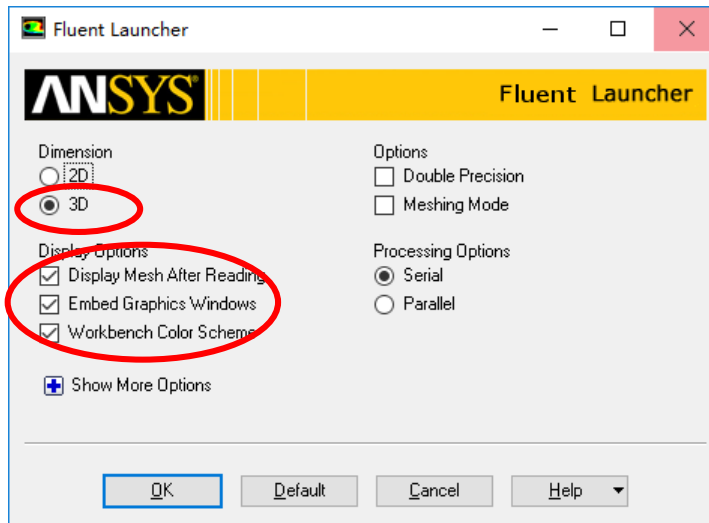
$$\frac{\partial(\rho_f C_{pf} u_f T_f)}{\partial x} + \frac{\partial(\rho_f C_{pf} v_f T_f)}{\partial y} + \frac{\partial(\rho_f C_{pf} w_f T_f)}{\partial z} = \lambda_f \left( \frac{\partial^2 T_f}{\partial x^2} + \frac{\partial^2 T_f}{\partial y^2} + \frac{\partial^2 T_f}{\partial z^2} \right)$$

$$0 = \lambda_c \left( \frac{\partial^2 T_c}{\partial x^2} + \frac{\partial^2 T_c}{\partial y^2} + \frac{\partial^2 T_c}{\partial z^2} \right) + s$$

$$0 = \lambda_b \left( \frac{\partial^2 T_b}{\partial x^2} + \frac{\partial^2 T_b}{\partial y^2} + \frac{\partial^2 T_b}{\partial z^2} \right)$$



### 13.5.1 Start the Fluent software



1. Choose **3-Dimension**

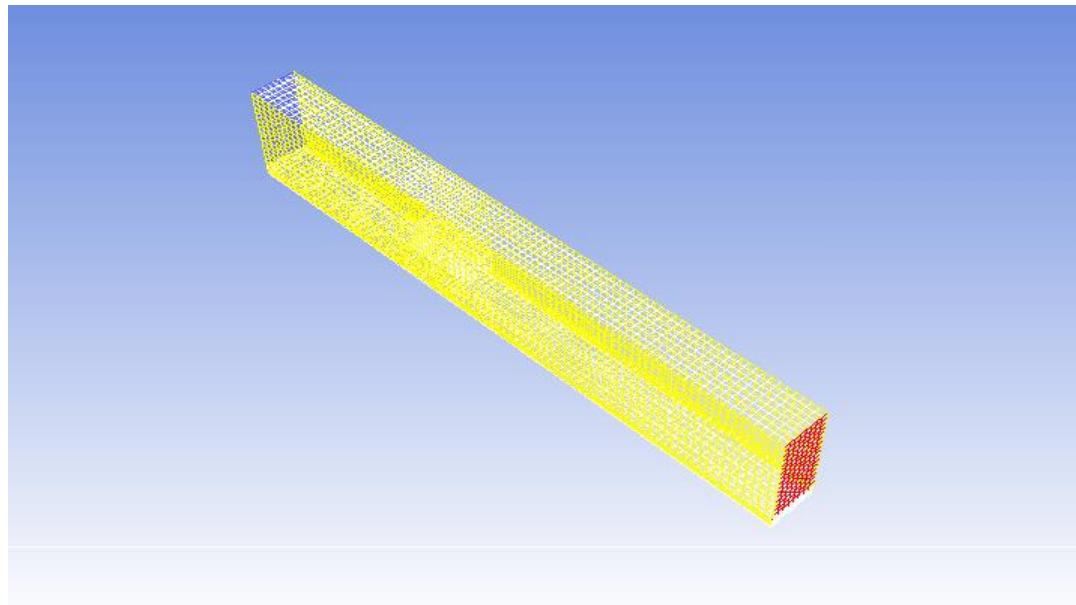
2. Choose display options

3. Choose Serial

← processing option

## 1st step: **Read** and check the mesh

- The mesh is generated by pre-processing software such as **ICEM**, **GAMBIT** and **MESHING**. The document is with suffix (后缀名) “**xx.msh**”





## 1st step: Read and **check** the mesh

Mesh→Check

- Check the **quality and topological information** of the mesh

### Mesh Check

#### Domain Extents:

x-coordinate: min (m) = 0.000000e+00, max (m) = 1.651000e-01

y-coordinate: min (m) = 0.000000e+00, max (m) = 2.794000e-02

z-coordinate: min (m) = -2.540000e-07, max (m) = 1.270000e-02

#### Volume statistics:

minimum volume (m3): 1.119834e-09

maximum volume (m3): 7.845747e-09

total volume (m3): 5.858386e-05

#### Face area statistics:

minimum face area (m2): 8.370037e-07

maximum face area (m2): 4.194085e-06

Checking mesh.....

Done.



## 2st step: Scale the domain size

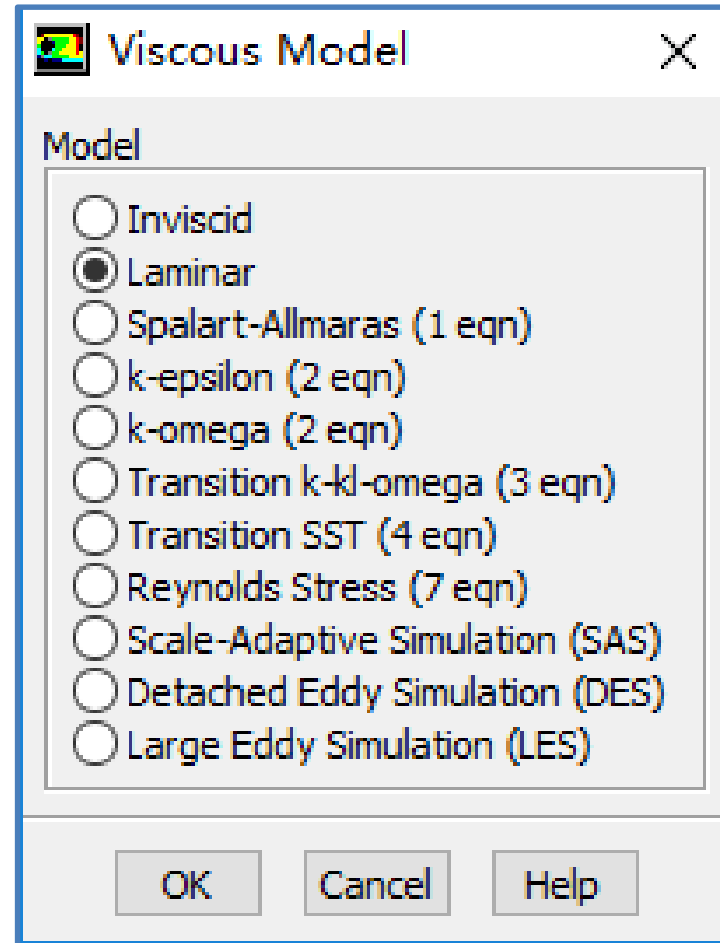
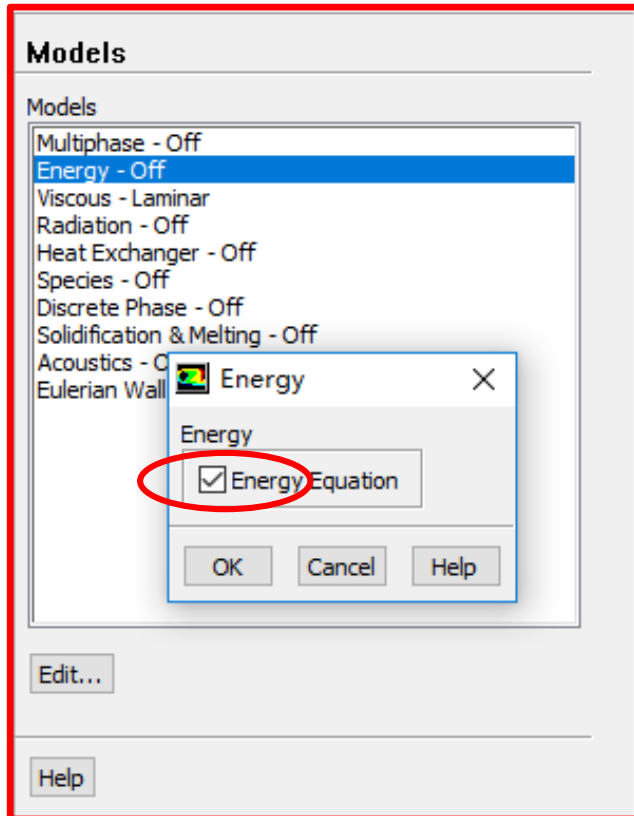
General → Scale

## 3st step: Choose the physicochemical model

*Re* number is calculated to determine the fluid state (laminar or turbulent)

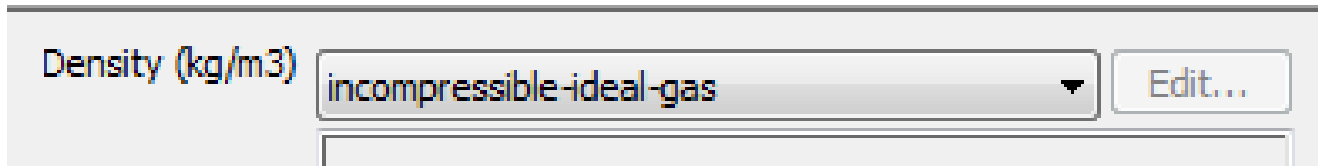
$$Re = \frac{\rho u l}{\mu}$$

The density of air is 1.29 kg/m<sup>3</sup>, the inlet velocity is 0.5 m/s, characteristic length is about 2 cm, and kinetic viscosity of air is 1.7894E-05. *Re* is 720 and thus flow is **laminar**.



## Step 4: Define the material properties

If you calculate the density using the **ideal gas law**, the solver will compute the density according to **ideal gas state equation**.



### Define a new material as Chip:

density  $1000 \text{ kg/m}^3$ ,  $C_p$   $500 \text{ J/(kg K)}$  and thermal conductivity  $1 \text{ W/(mK)}$

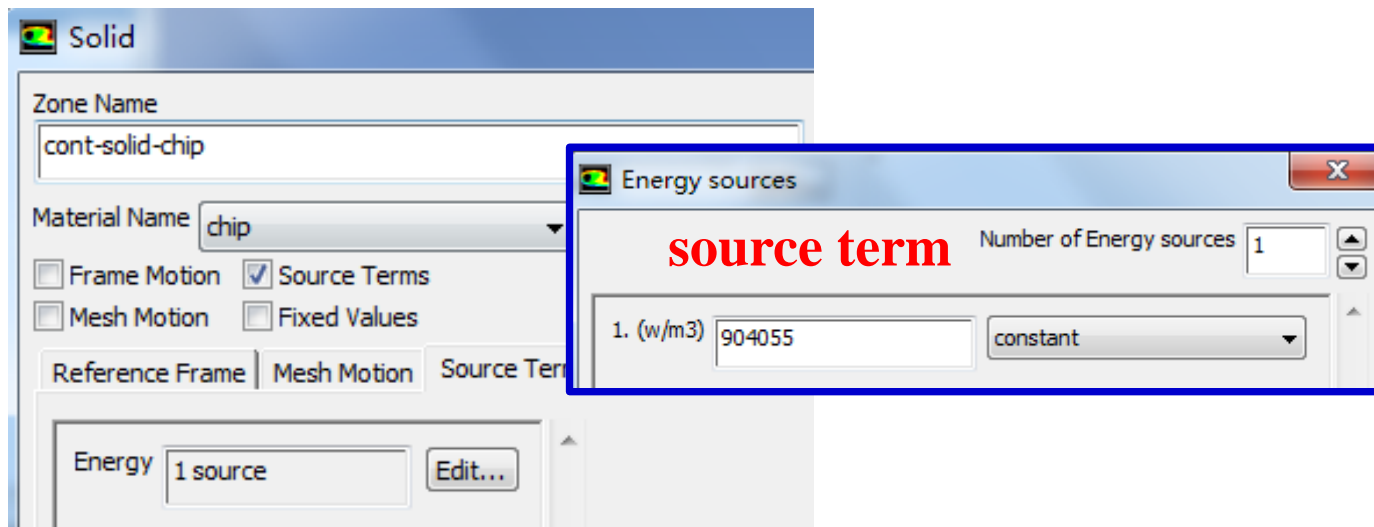
### Define a new material as Board:

density  $2000 \text{ kg/m}^3$ ,  $C_p$   $600 \text{ J/(kg K)}$  and thermal conductivity  $0.1 \text{ W/(mK)}$

## Step 5: Define zone condition

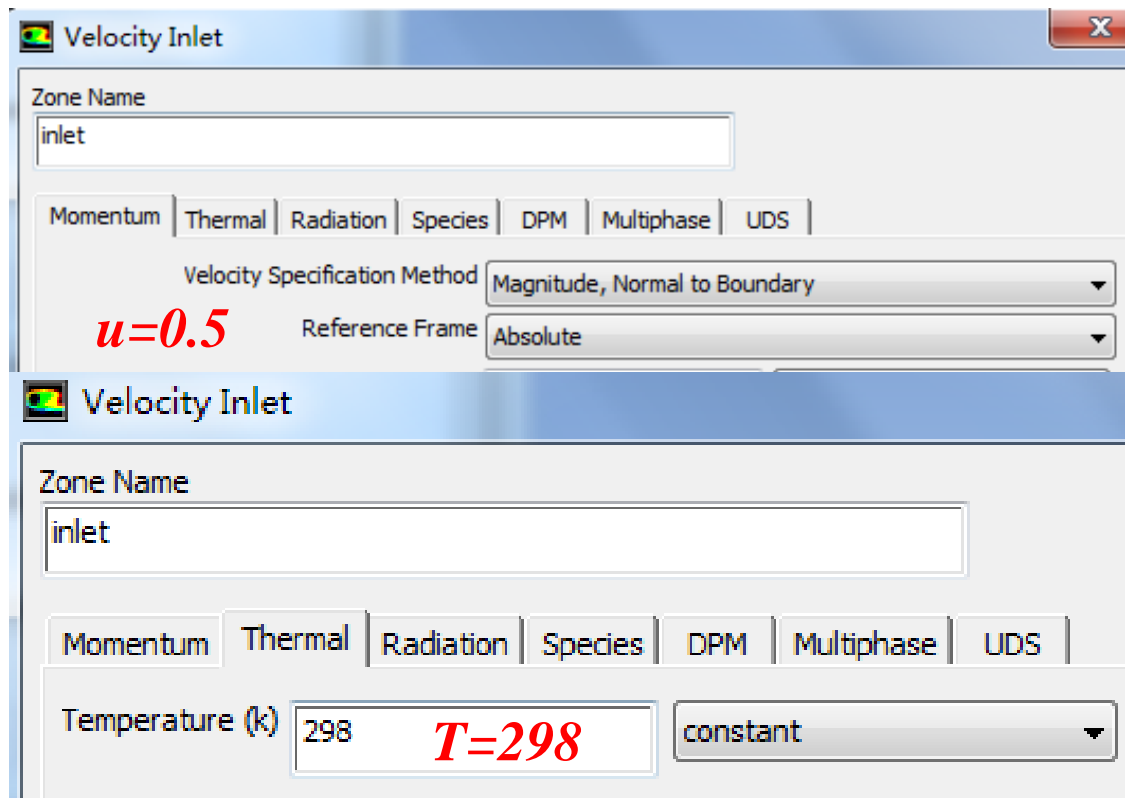
Assign different regions with the corresponding materials.

For the chip, there is a source term with value of  $904055 \text{ W/m}^3$



## Step 6: Define the boundary condition

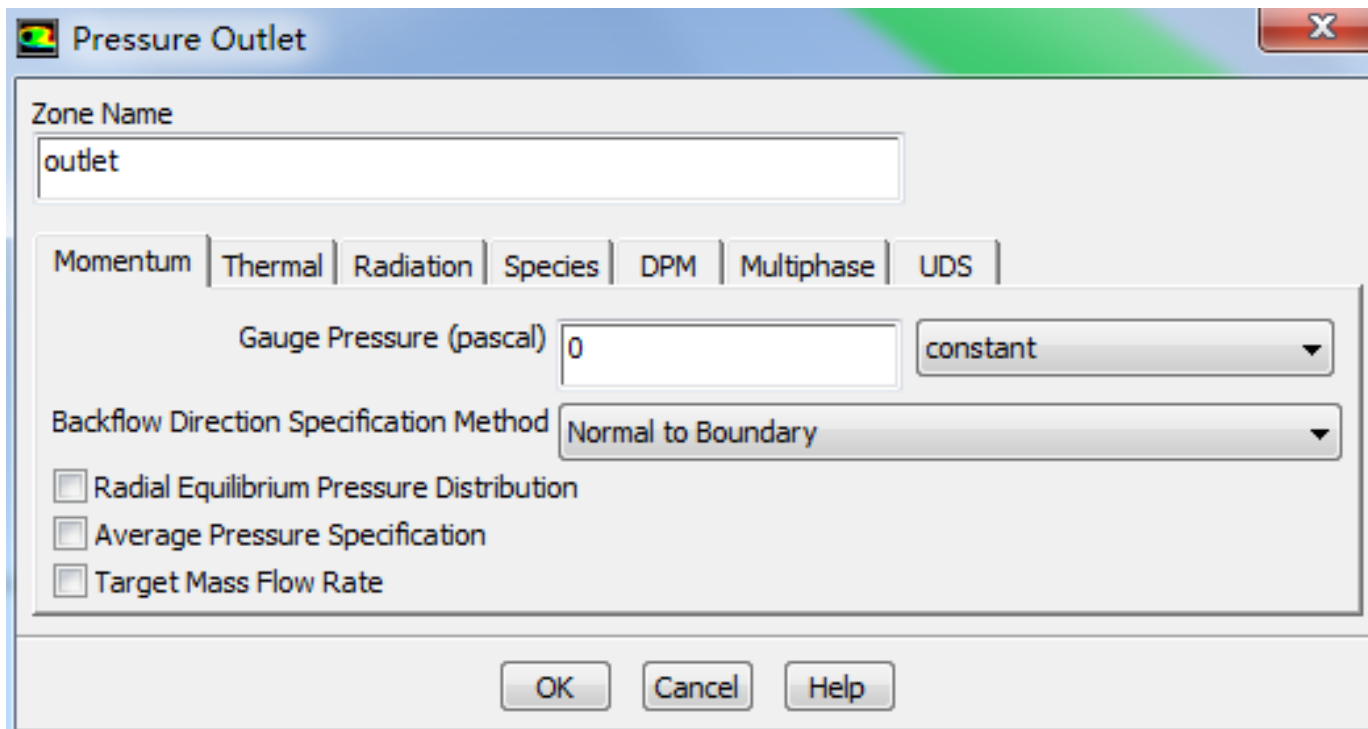
Inlet:  $u$  and  $T$  are specified.





## Step 6: Define the boundary condition

**Outlet: pressure outlet, Gauge pressure as 0.**



## Step 6: Define the boundary condition

### Top and bottom wall: convective boundary condition

The screenshot shows a 'Wall' dialog box with the following settings:

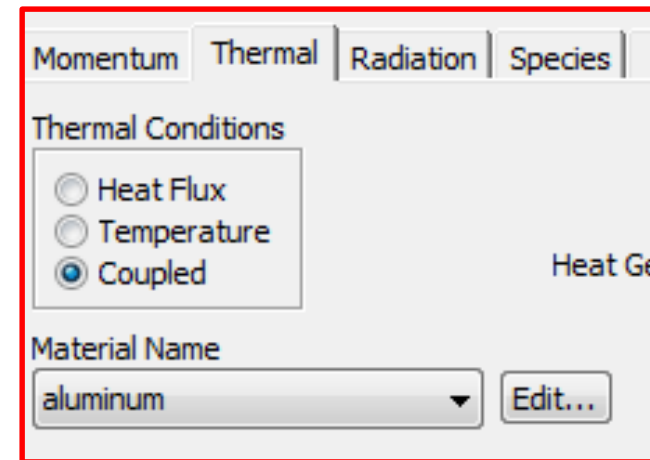
- Zone Name: wall-board-bottom
- Adjacent Cell Zone: cont-solid-board
- Thermal Conditions:  Convection
- Heat Transfer Coefficient (w/m<sup>2</sup>-k): 1.5, constant
- Free Stream Temperature (k): 298, constant
- Wall Thickness (in): 0
- Material Name: aluminum
- Heat Generation Rate (w/m<sup>3</sup>): 0, constant
- Shell Conduction:  Shell Conduction Define...

Buttons: OK, Cancel, Help

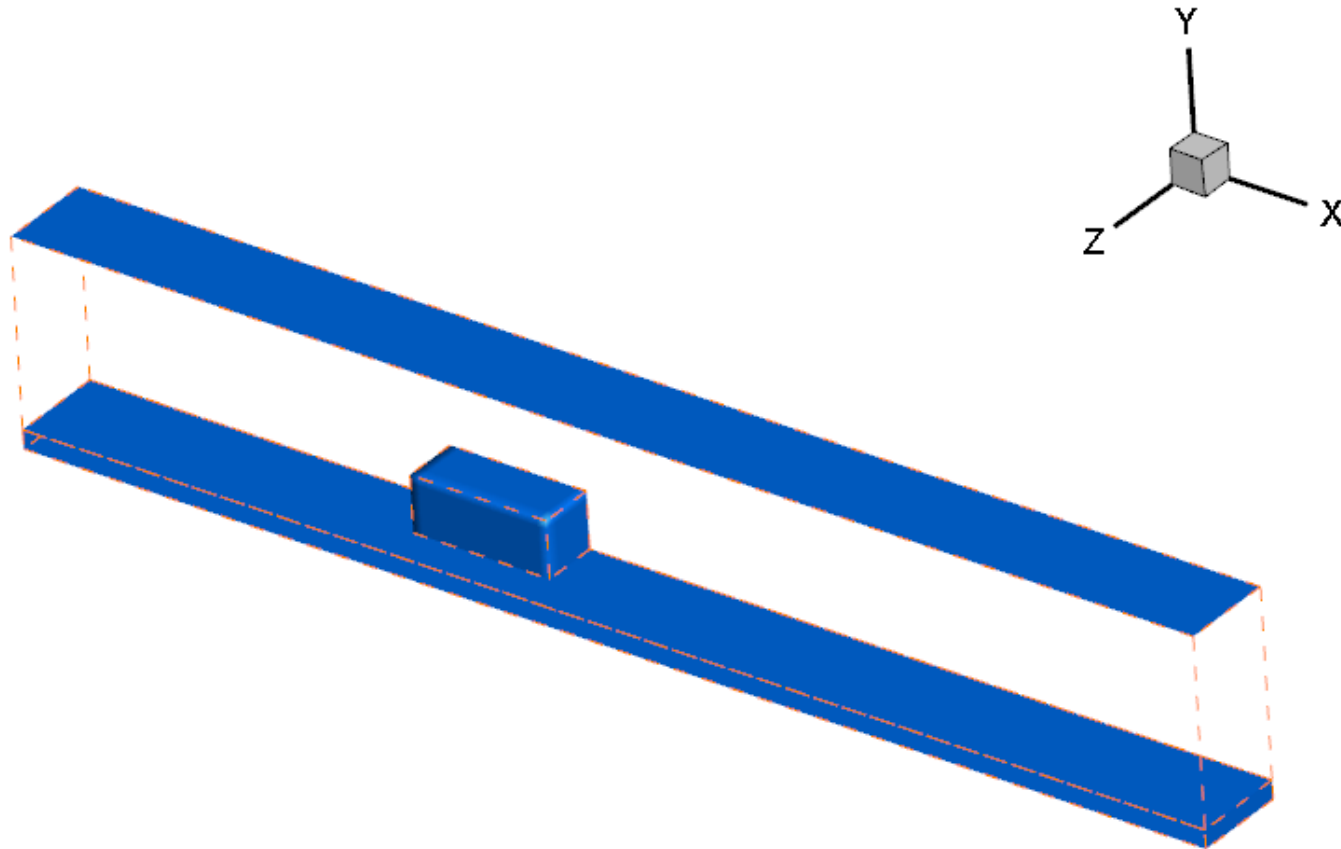
## Step 6: Define the boundary condition

For the front and back boundaries, keep the default set up of **Symmetry**.

For all the other “two-side-walls” boundaries in the domain, keep the default set up for thermal conditions, namely “**Coupled**”. *For details of “Coupled” and “uncoupled” conditions, refer to Example 3 in Chapter 13.*

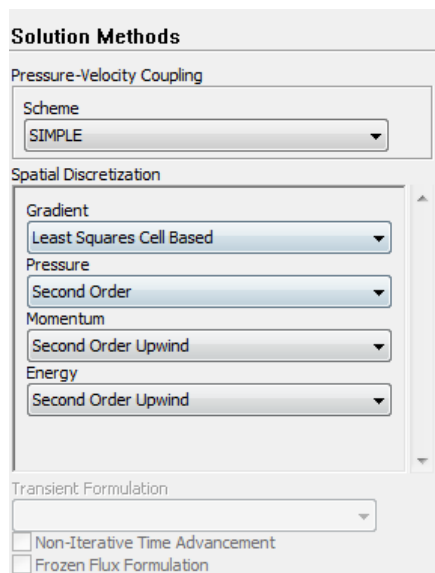


There are many **two-sided-wall** in this Example.



## 7st step: Define the solution

For algorithm and schemes, keep it as default. For more details of this step, one can refer to **Example 1** of Chapter 13.



**Algorithm:** simple

**Gradient:** Least Square Cell Based

**Pressure:** second order

**Momentum:** second order upwind

**Energy:** second order Upwind



## 7st step: **Define the solution**

For under-relaxation factor, keep it default. For more details, refer to **Example 1**.

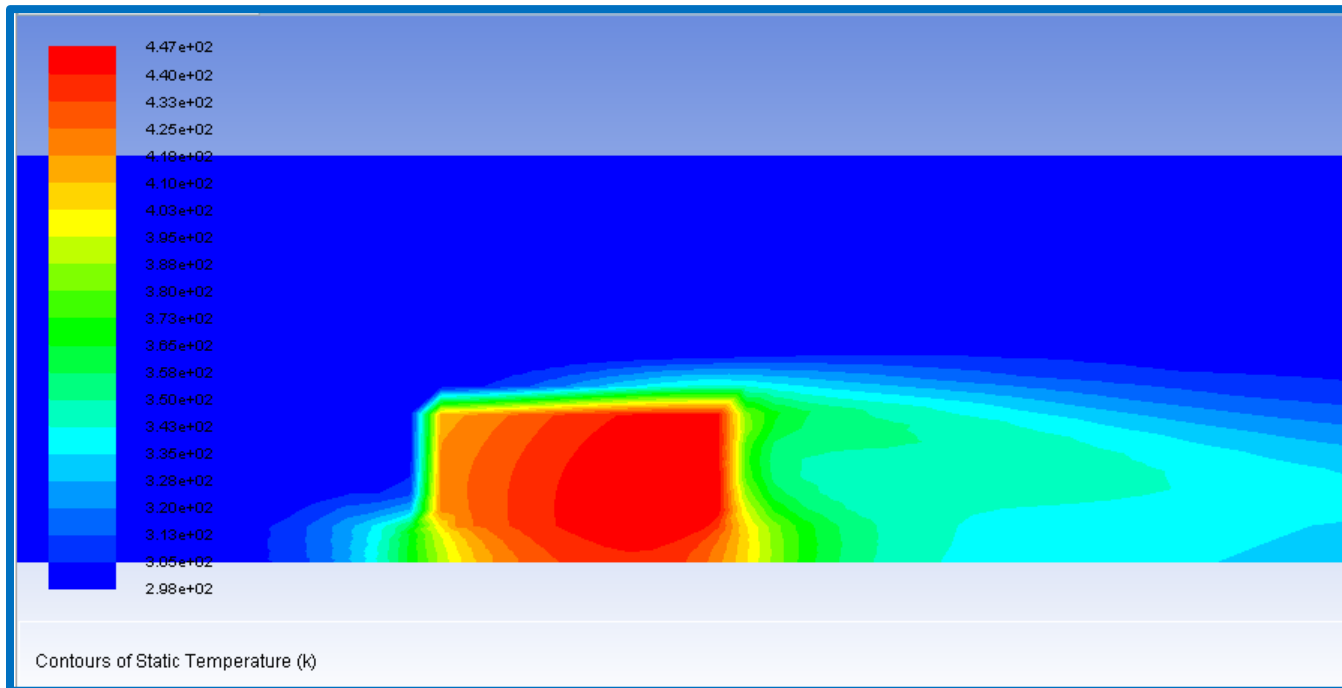
## 8st step: Initialization

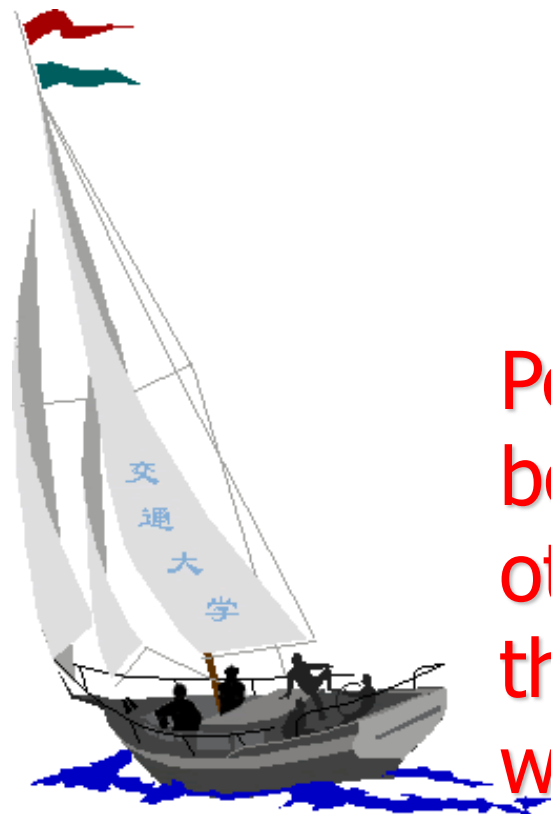
Use the standard initialization, for more details of Hybrid initialization, refer to Example 1.

## Step 9: Run the simulation

## Step 10: Post-processing results

## Static Temperature(K) of back boundary





# 同舟共济 渡彼岸!

People in the same  
boat help each  
other to cross to  
the other bank,  
where....