

# Numerical Heat Transfer

## Chapter 13 Application examples of Fluent for flow and heat transfer problem



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**Xi'an Jiaotong University**

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# 数值传热学

## 第 13 章 求解流动换热问题的Fluent软件应用举例



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西安交通大学能源与动力工程学院  
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2021年12月22日, 西安

# Class intermediate

**13. A1 Single phase flow and heat transfer in manifold microchannel**

(歧管微通道中流动换热)

**13. A2 Flow and heat transfer in porous media**

(多孔介质流动换热)

**13. A3 Boiling heat transfer using the Volume of Fluid method (池沸腾传热VOF方法模拟)**

**For each example, the general content of the lecture is as follows:**

**1: Using slides to explain in detail the general **10 steps** for Fluent simulation! (PPT讲解)**

- |                          |                              |
|--------------------------|------------------------------|
| 1. Read mesh             | 2. scale domain              |
| 3. Choose model          | 4. define material           |
| 5. define zone condition | 6. define boundary condition |
| 7. Solution              | 8. Initialization            |
| 9. Run the simulation    | 10. Post-processing          |

**2: Operating the Fluent software to simulate the example and post-process the results. (运行软件)**

## 13. A1

# Flow and heat transfer in manifold

## (歧管) microchannel

(歧管微通道中流动换热)

1. What is microchannel?

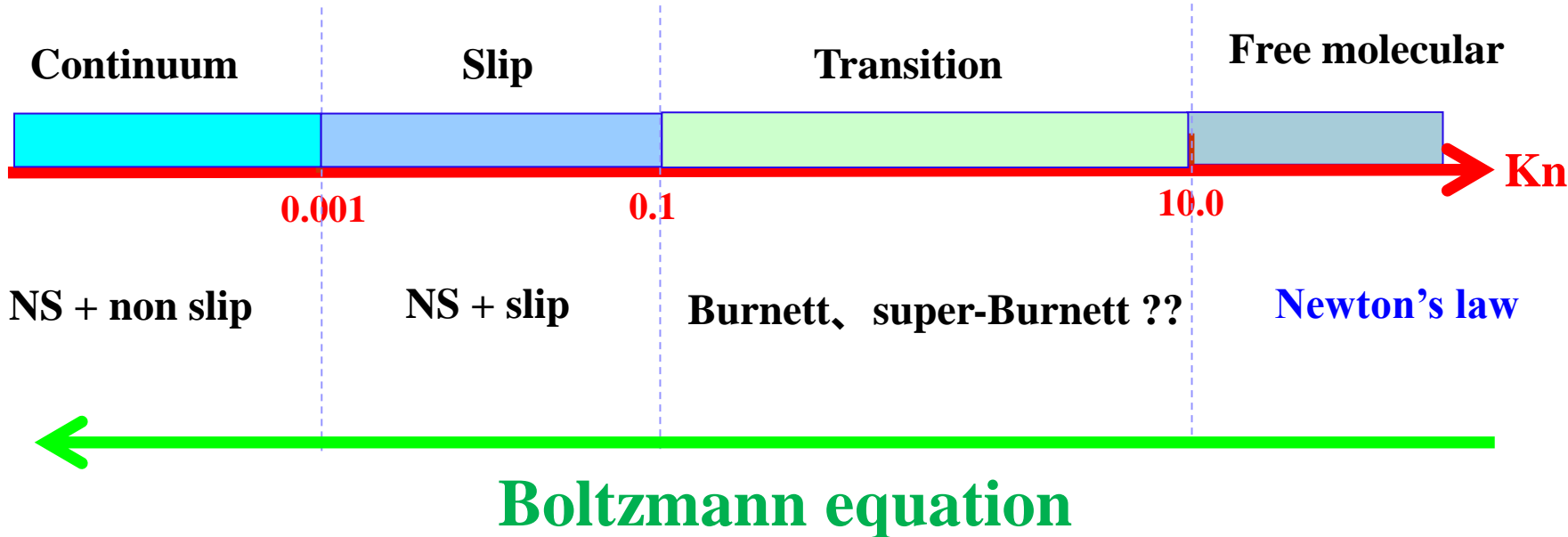
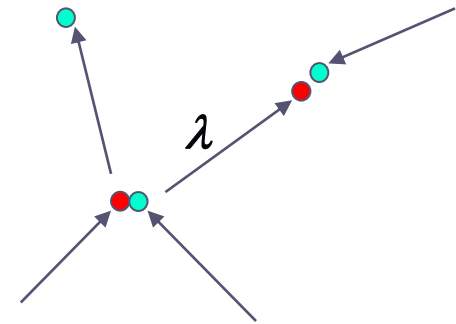
2. What is manifold?

# What is “Microscale” ?

1. The continuum assumption (连续介质假设) does not stand.

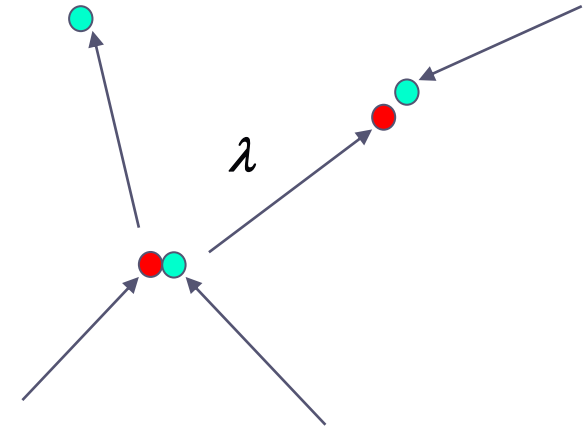
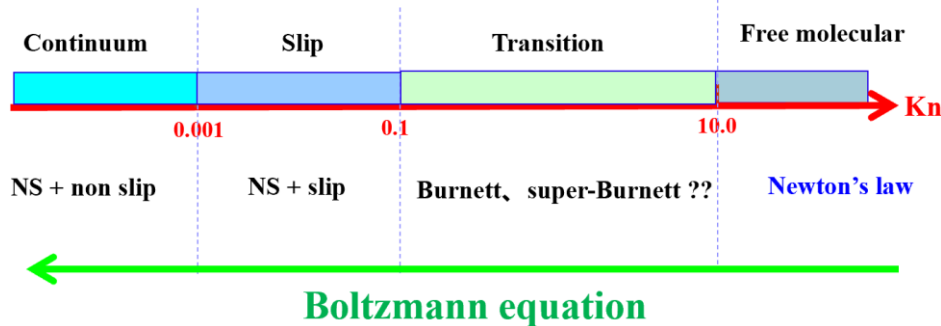
H.-S. Tsien, 1946

Knudsen:  $Kn = \lambda/L$



At normal pressure and temperature, the mean free path for air is 70 nm.

$$Kn = \lambda/L = 70/L$$



## slip flow

$$Kn = 0.001 \sim 0.1: \quad L = 700 \text{ nm} \sim 70 \text{ } \mu\text{m}$$

## Transition flow

$$Kn = 0.1 \sim 10: \quad L = 700 \text{ nm} \sim 7 \text{ nm}$$

# What is “Microscale” ?

## 2. The relative importance of affecting factors changes.

Fluid flow is controlled by different forces such as viscous force, gravitational force, surface tension force...

These force can be classified into two kinds: **body force and surface tension force.**

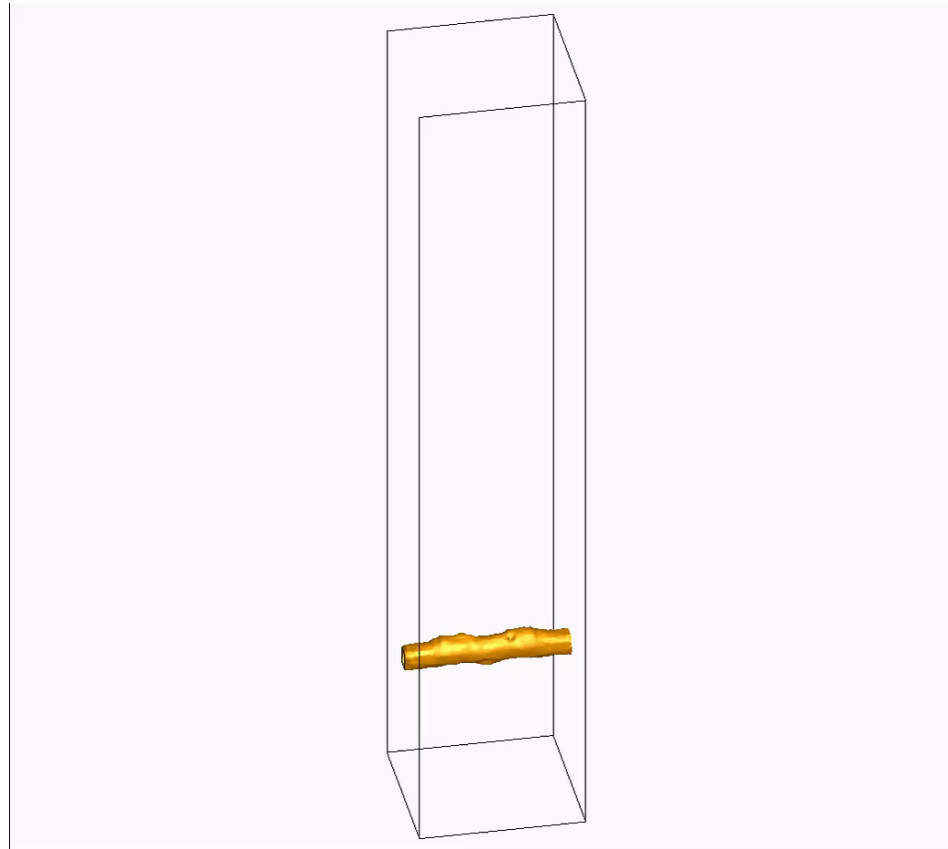
**body forces:  $\sim m^3$**

**surface forces:  $\sim m^2$**

**surface forces/body forces:  $\sim m^{-1}$ ; surface force becomes stronger as length scale decreases.**



# Multiphase heat transfer in microchannel



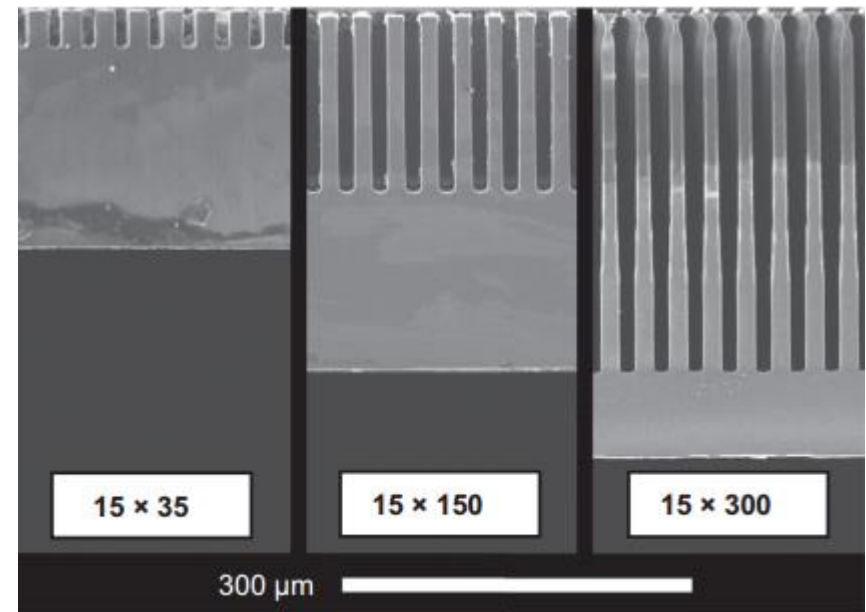
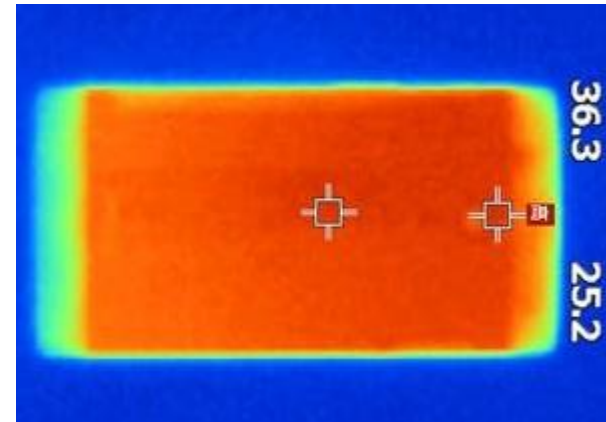
Provided by graduated student Yi Yuan

1. Body force such as **gravity force** can be neglected.
2. Pressure and surface tension force are dominant (主导).

Because of the **integration**(集成化) of electron component (电子元件), the heat flux of a EC greatly increases, even reaches  **$MW \cdot m^{-2}$**  order of magnitude.

Traditional cooling techniques cannot meet the cooling demand of such high heat flux.

**Microchannel** is a promising technique for cooling.



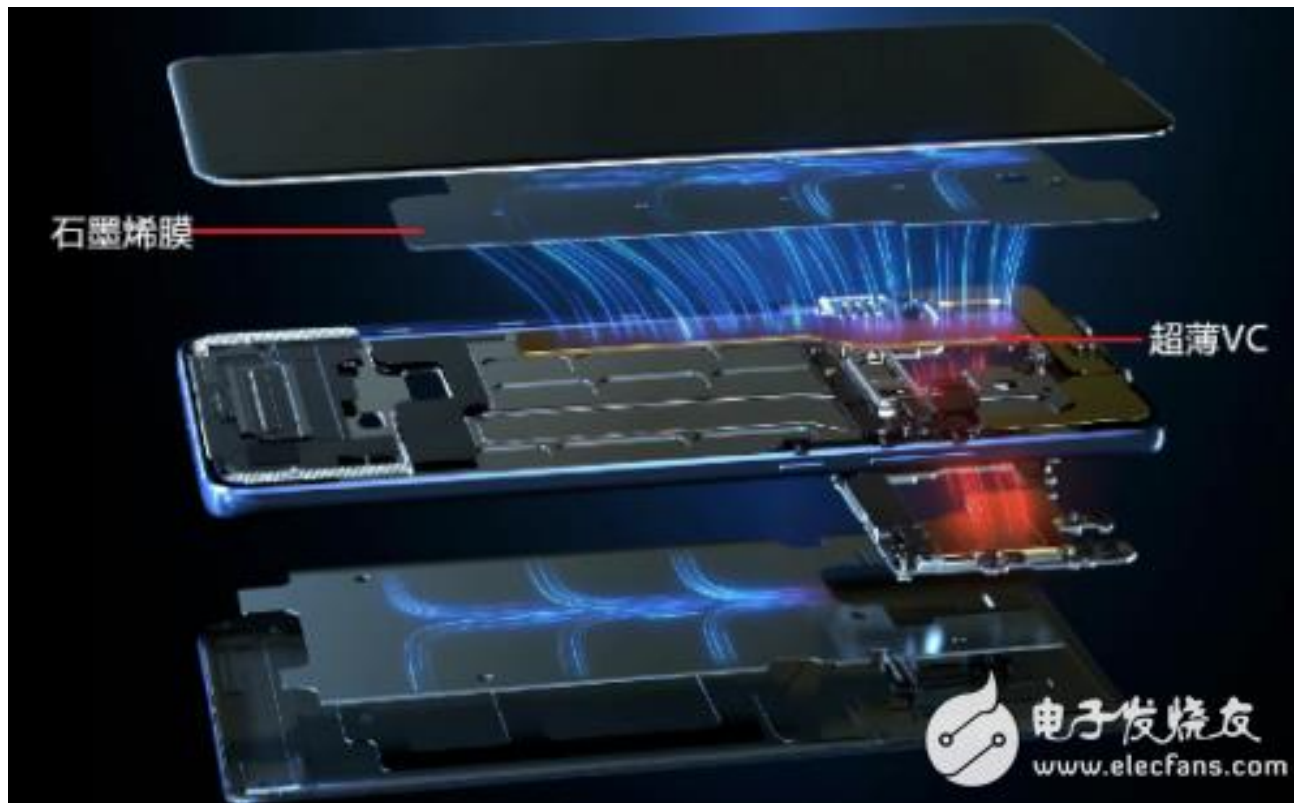
SEM images of channel (Si) cross-sections.(a)( $15\mu m \times 35\mu m$ ), (b)( $15\mu m \times 150\mu m$ ), and (c) ( $15\mu m \times 300\mu m$ )



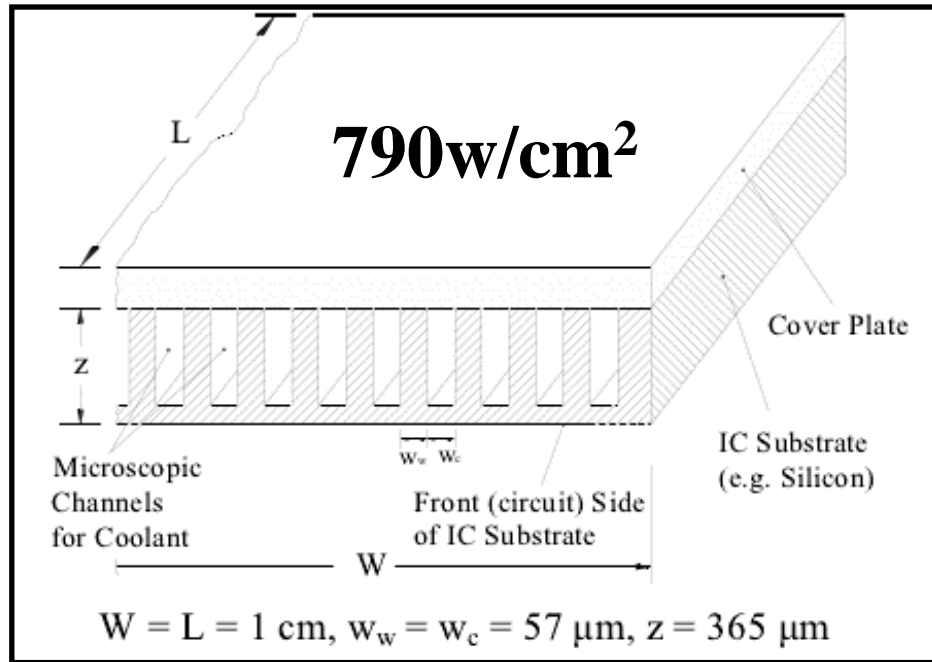
**Zheng-Fei Ren, CEO of Huawei**

**Huawei Technologies Co., Ltd.**, It designs, develops, and sells telecommunication equipment and consumer electronics.

There are three most important key labs in Huawei, including **Advance structural material Lab**, **Advance thermal technique lab** and **Noah's Ark Lab** (诺亚方舟实验室, for AI) 。

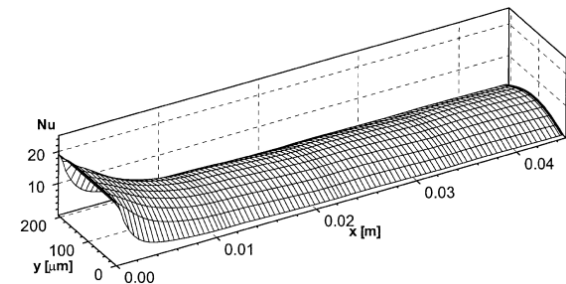
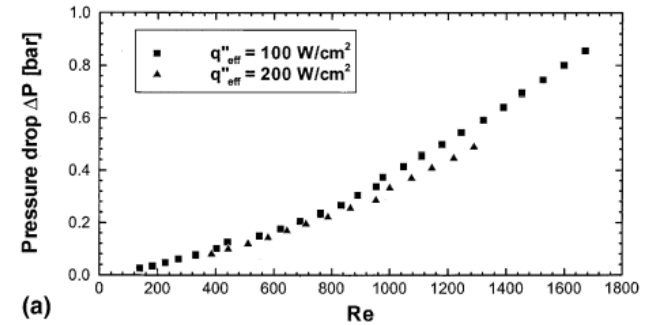
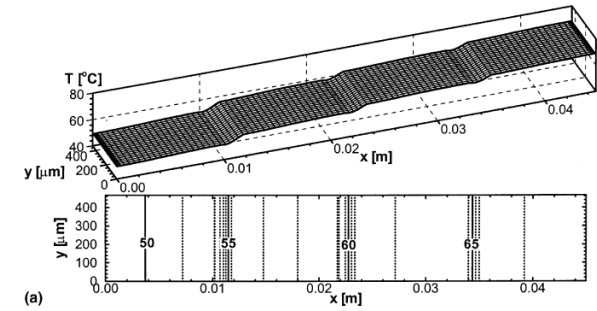


# Traditional microchannel

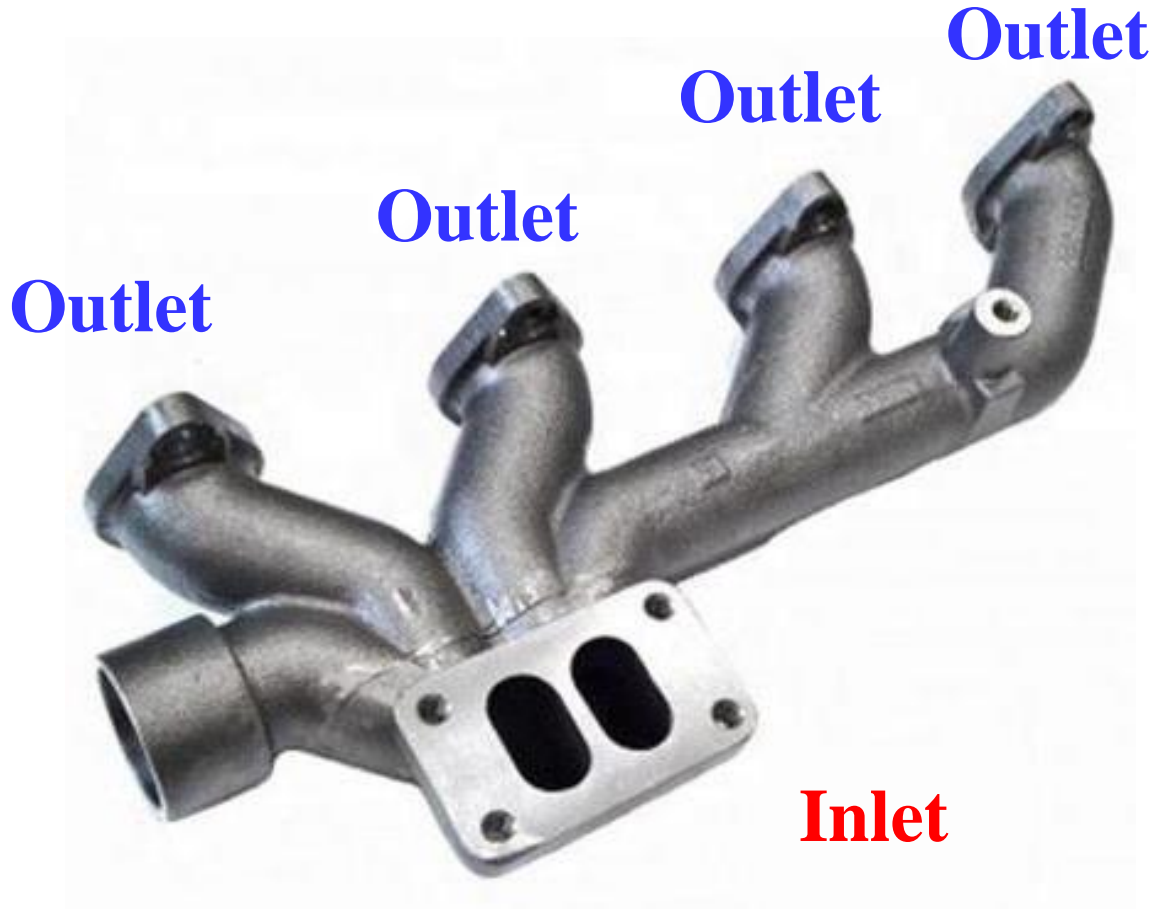


D.B. Tuckerman, R.F.W. Pease, High-performance Heat Sinking for VLSI. IEEE Electron Device Letters 1981, 2(5) 126-129.

1. From the inlet to the outlet, temperature increases.
2. Pressure drop is high.
3. Inlet effect is not significant.

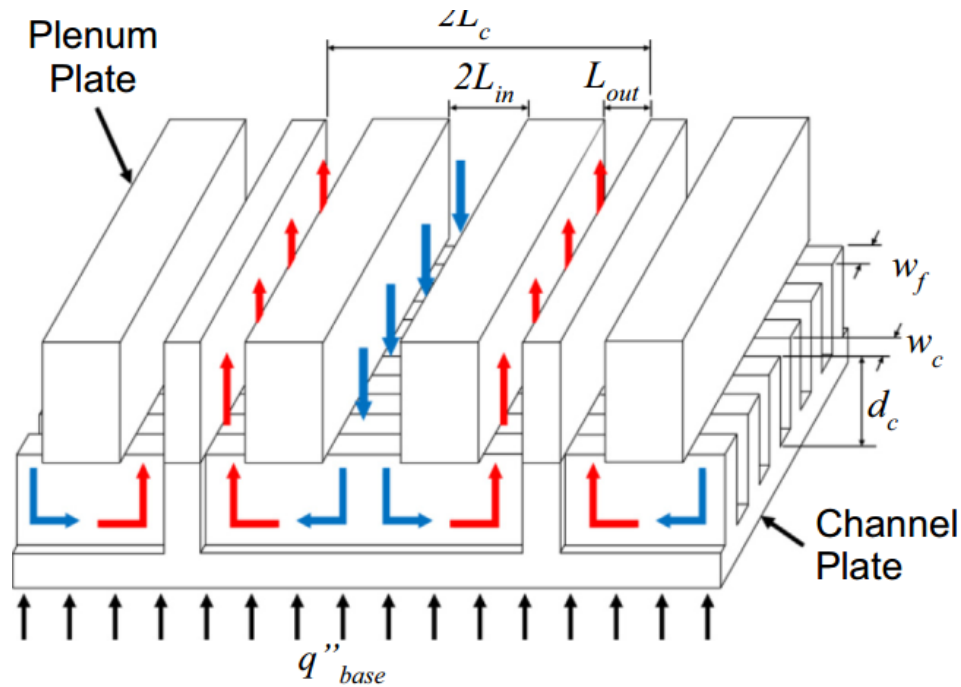


# What is “manifold” ?



**A kind of structure that adopted to distribute fluid.**

# Manifold microchannel



1. Inlet effect is strong.
2. Pressure drop decreases.
3. Temperature distribution is more uniform.





Contents lists available at ScienceDirect

## International Journal of Heat and Mass Transfer

journal homepage: [www.elsevier.com/locate/hmt](http://www.elsevier.com/locate/hmt)

## Numerical study on flow and heat transfer in a multi-jet microchannel heat sink



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Numerical simulation

## ABSTRACT

A multi-jet microchannel (MJMC) heat sink with coolant flowing through alternative inlet and outlet jets in the direction normal to the heated surface is studied. Three dimensional flow and heat transfer processes in the MJMC are numerically simulated using the SIMPLE-type finite volume method (FVM). Compared with traditional microchannels, the MJMC combines the advantages of impinging jet flow and entrance effects of microchannels, and thus its cooling performance overwhelms showing less pumping power, lower thermal resistance and improved uniformity of temperature at the bottom surface. Effects of various geometrical parameters including jet numbers, channel aspect ratio, the fin width to channel width ratio and the width of the outlet on the performance of the MJMC are analyzed in detail. It is found that the MJMC with more jets, wider outlet and smaller fin width to channel width ratio offers better cooling performance. While the cooling performance exhibits a non-monotonic trend with the channel aspect ratio, the optimum structure is obtained with an aspect ratio around 6. Under the range of parameters studied, the MJMC heat sink with 7 jets, aspect ratio of 6 and fin width to channel width ratio of 0.5 obtains the best cooling performance.



# Nature paper

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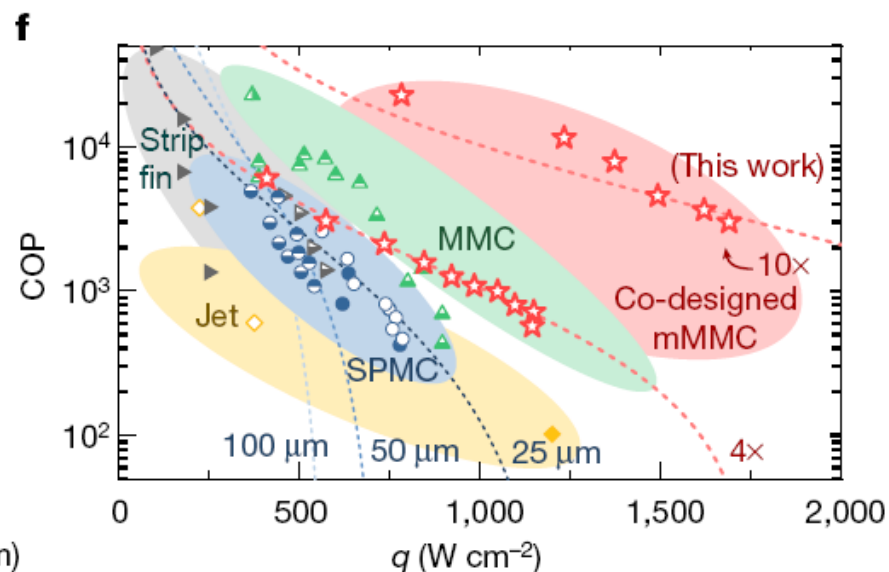
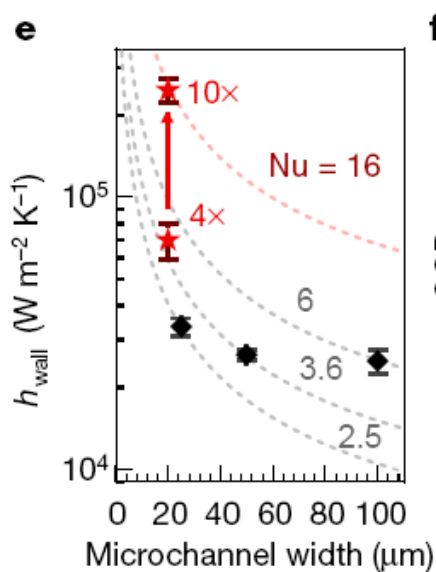
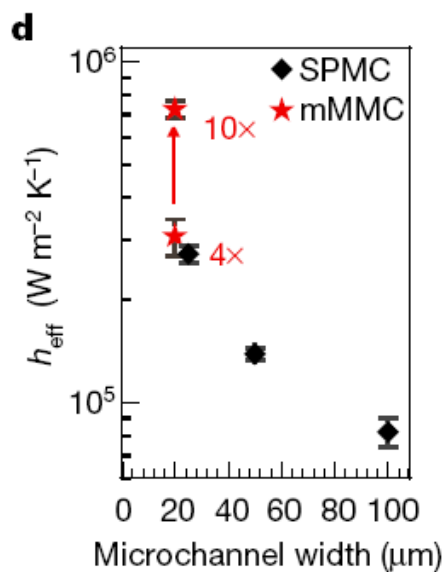
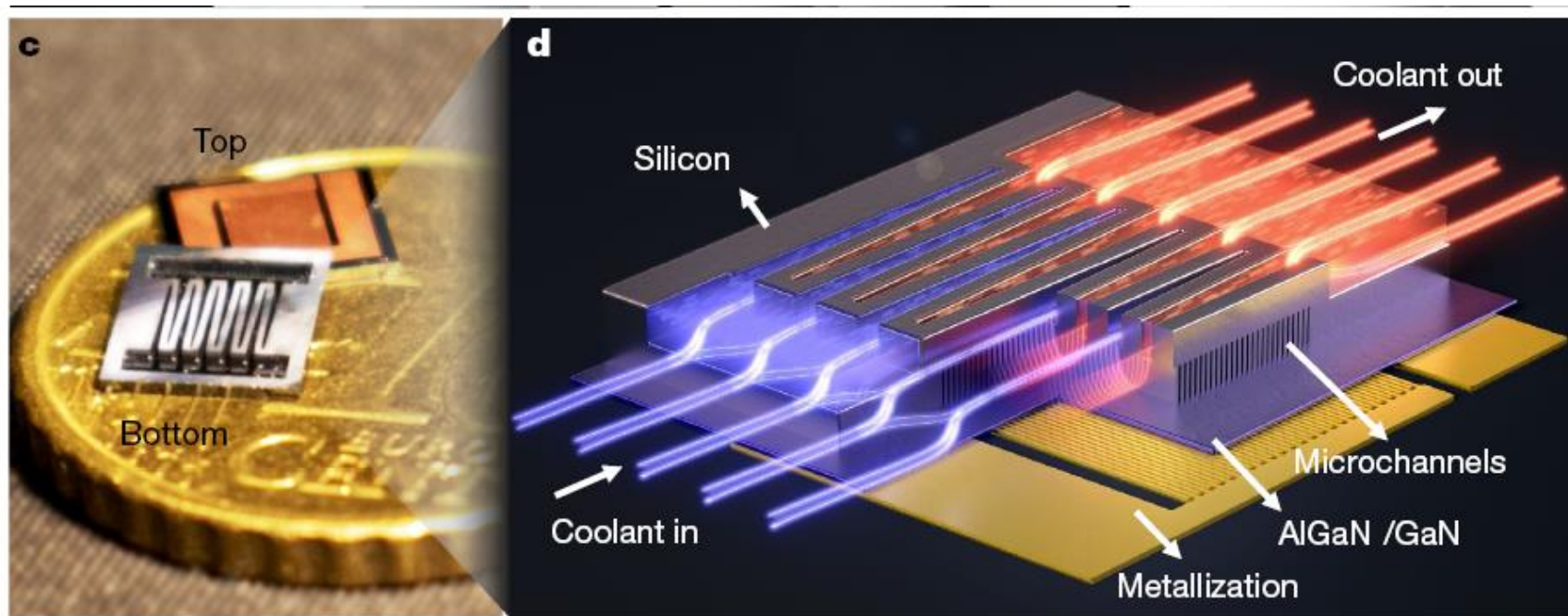
Article | [Published: 09 September 2020](#)

## **Co-designing electronics with microfluidics for more sustainable cooling**

[Remco van Erp](#), [Reza Soleimanzadeh](#), [Luca Nela](#), [Georgios Kampitsis](#) & [Elison Matioli](#) 

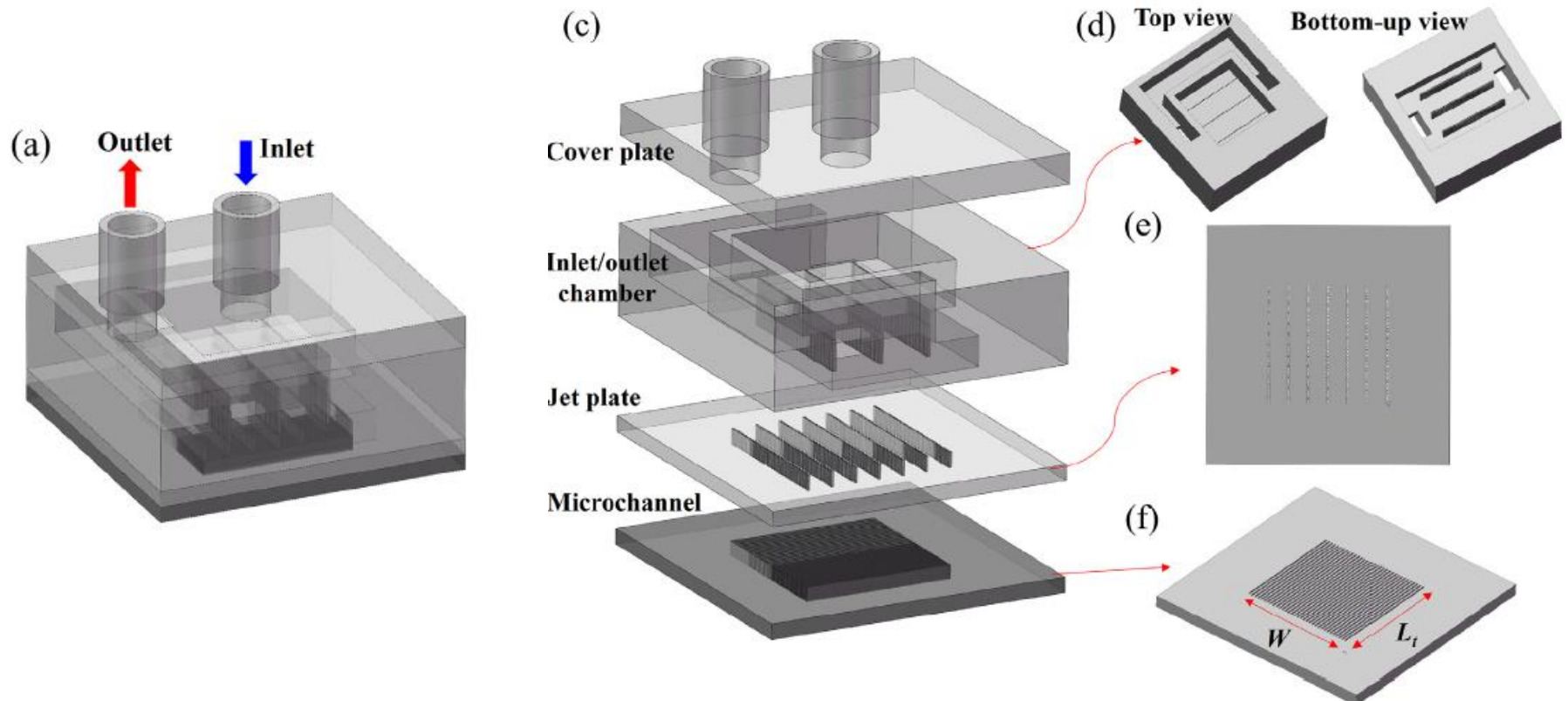
*Nature* **585**, 211–216(2020) | [Cite this article](#)

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## ■ Example 13 A1. Known

Steady single phase fluid flow and heat transfer of water in a manifold microchannel, as shown in Fig. 1



**Fig. 1 Schematic of the manifold microchannel channel**



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journal homepage: [www.elsevier.com/locate/hmt](http://www.elsevier.com/locate/hmt)

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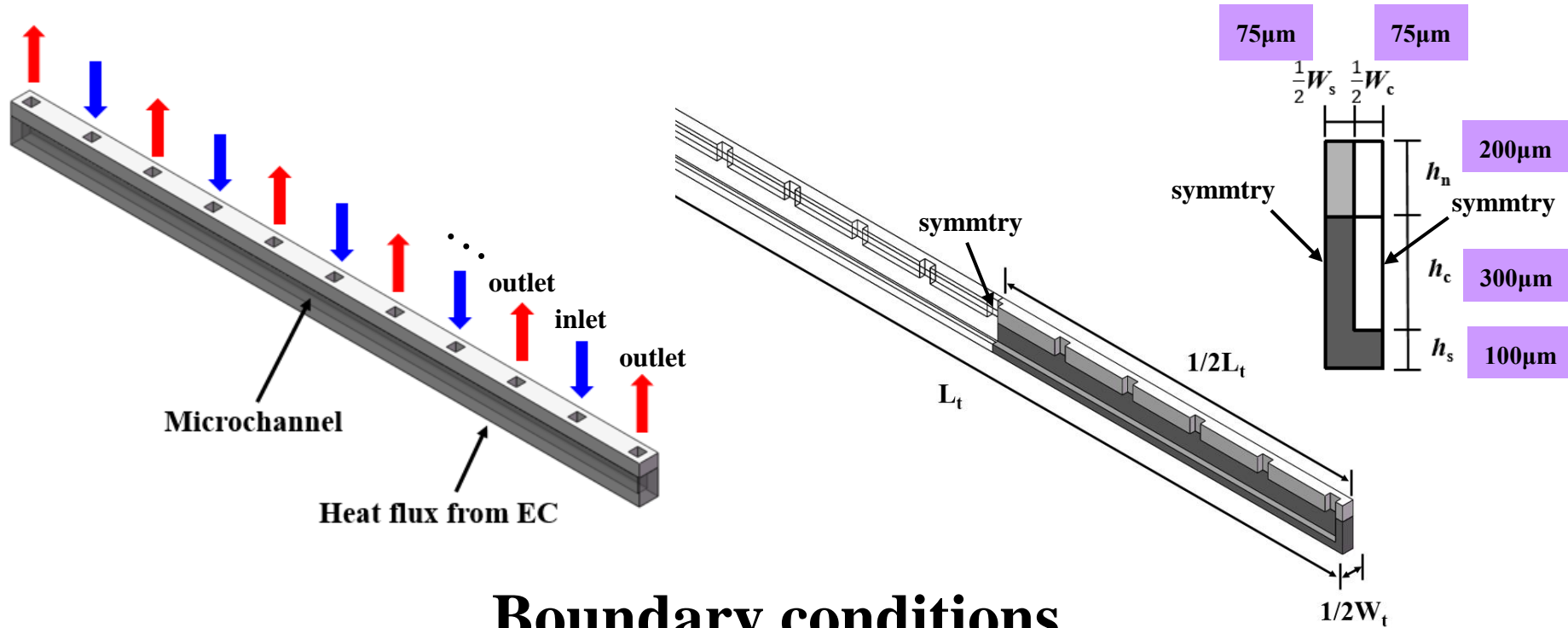
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## Boundary conditions

Inlet	Velocity inlet; 293.15K
Outlet	Pressure out: 1atm
Bottom	Heat flux( $1 \times 10^6 \text{ W} \cdot \text{m}^{-2}$ )
Up	Adiabatic wall
Side	Symmetry & adiabatic

■ **Find:** Temperature of bottom surface ( $T_b$ ), thermal resistance ( $\theta$ ) and pressure drop ( $\Delta P$ ) at different Reynolds number (44, 88, 132, 176 and 220).

■ **Assumptions:**

- (1) When  $Kn$  is less than  $10^{-3}$ , N-S Eqs still can be used;
- (2) Laminar, incompressible, Newtonian fluid;
- (3) Physical parameters are constant;
- (4) The gravity and viscous dissipation can be ignored;
- (5) The thermal radiation can be ignored.



**Remark: develop reasonable physical model and write down the right governing equation, BC and IC is the first and most important step before using software Fluent.**

**Fluent is just a tool for solving above problem !**

**Background of NHT helps you better use the tool.**

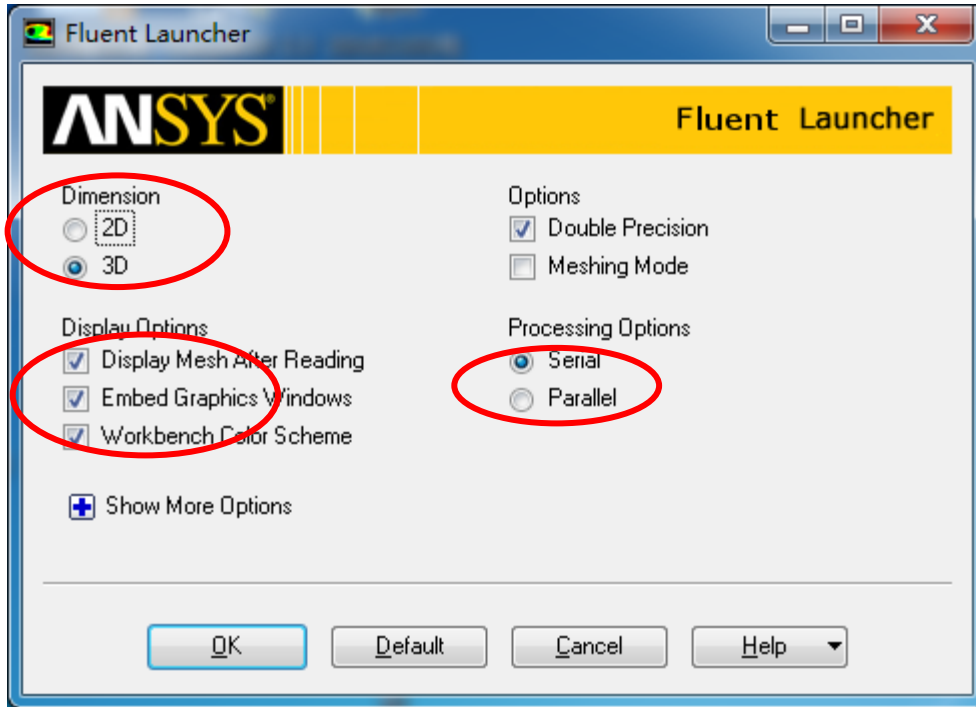
## ■ Governing equations:

Continuum equation  $\nabla u = 0$

Momentum equation  $\nabla(\rho u u) = -\nabla p + \eta \nabla^2 u$

Energy equation  $\nabla(\rho c_p u T_f) = \nabla \lambda_f \nabla T_f \quad 0 = \nabla \lambda_s \nabla T_s$

# Start the Fluent software



1. Choose **3-Dimension**
2. Choose display options
3. Choose **Serial processing** option or parallel to choose different number of processors

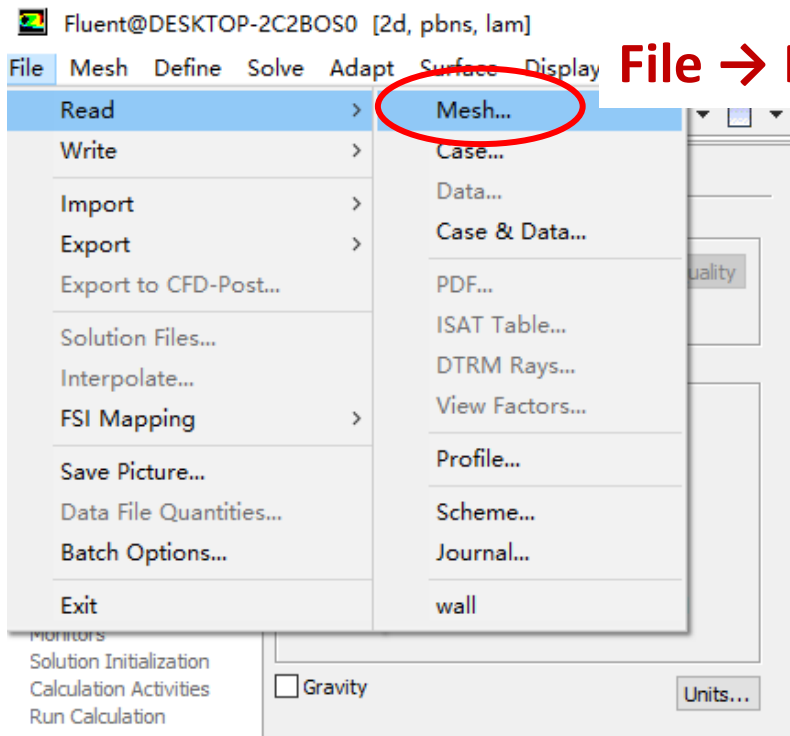
**Note: Double precision or Single precision**

Sometimes the single precision version of Fluent is sufficient. For example, for heat transfer problem, **if the thermal conductivity between different components are high**, it is recommended to use **Double Precision Version**.



## Step 1: **Read** and check the mesh

- The mesh is generated by pre-processing software such as **ICEM** and **GAMBIT**. The document is with suffix (后缀名) “**.msh**”
- This step is similar to the **Grid subroutine (UGRID, Setup1)** in our general teaching code.



```

Building...
  mesh
Slitting wall zone 29 into a coupled wall.
  materials,
  interface,
  domains,
  zones,
    inter_surface_sf-shadow
    down_wall_s
    up_wall_s
    up_wall_f
    inter_surface_sf
    wall_left_f
    wall_left_s
    wall_right_f
    wall_right_s
    out_s
    out_f
    in_s
    in_f
    int_fluid
    int_solid
    fluid
    solid

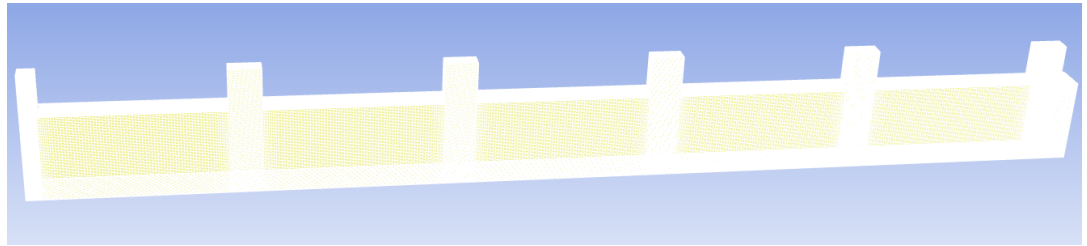
Done.

Preparing mesh for display...
Done.
    
```

# Step 1: Read and **check** the mesh

## Mesh→Check

- Check the **quality** and **topological information** (拓扑信息) of the mesh



- Sometimes this step will be failed if the quality is not good or there is a problem with the mesh.

Face area statistics:  
WARNING: invalid or face with too small area exists.  
minimum face area (m2): 0.000000e+00  
maximum face area (m2): 5.081937e-03

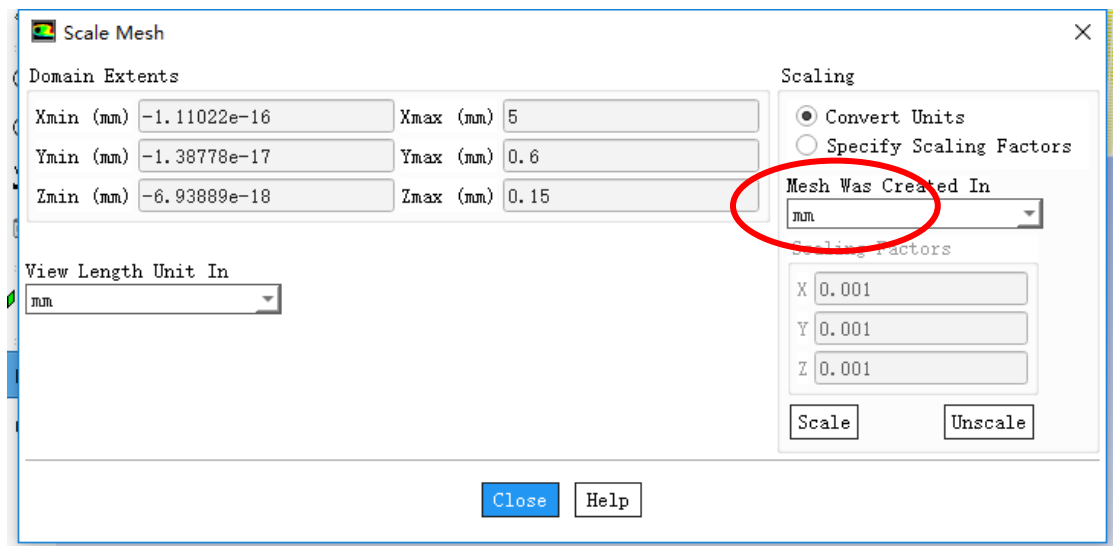
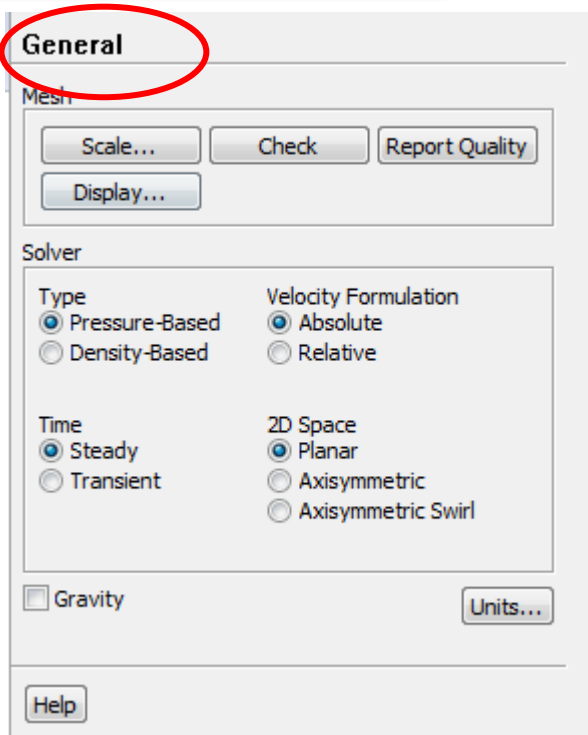
WARNING: Mesh check failed.

WARNING: The mesh contains high aspect ratio quadrilateral, hexahedral, or polyhedral cells.

## Step 2: Scale the domain size (缩放)

General → Scale

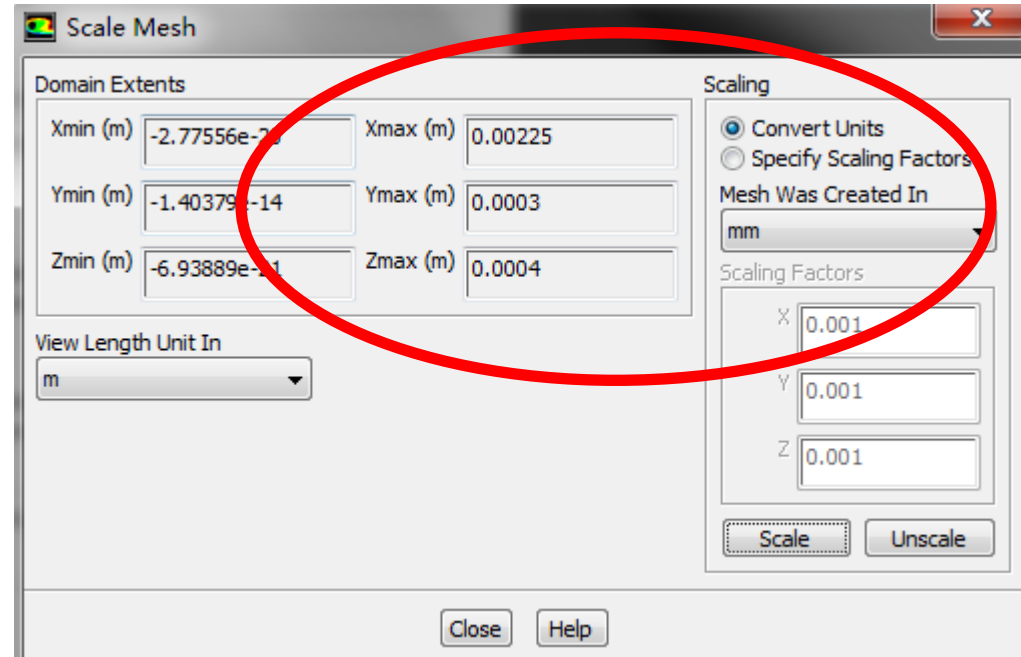
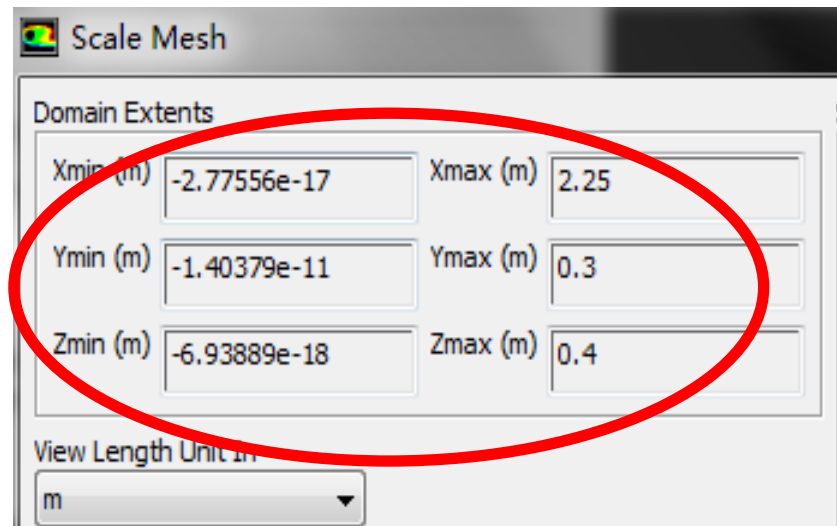
Make sure the unit is right.



- You can scale the domain size use “Convert Units” or “Specify Scaling Factors” command.

**Remark:** Fluent thought you create the mesh in units of m. However, if your mesh is created in a different unit, such as cm, you **must** use **Convert Units Command** to **scale the mesh into the right size**. The values will be multiplied by the Scaling Factor.

**ICEM: 1 mm -> Fluent: 1m -> Scale: mm, factor: 1/1000**



## Step 3: Choose the physic model

Based on the governing equations you are going to solve, select the related models in Fluent.

**Remark:** Understand the problem you are going to solve, and write down the right governing equations is the first and most important step for numerical simulation. Without background of “Fluid mechanics”, “Heat Transfer” and “Numerical heat transfer”, it is hard to complete this step for fluid flow and heat transfer problem.

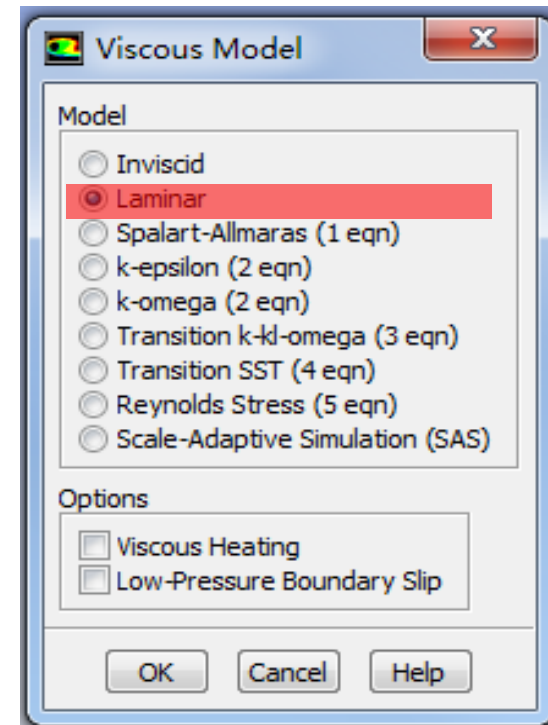
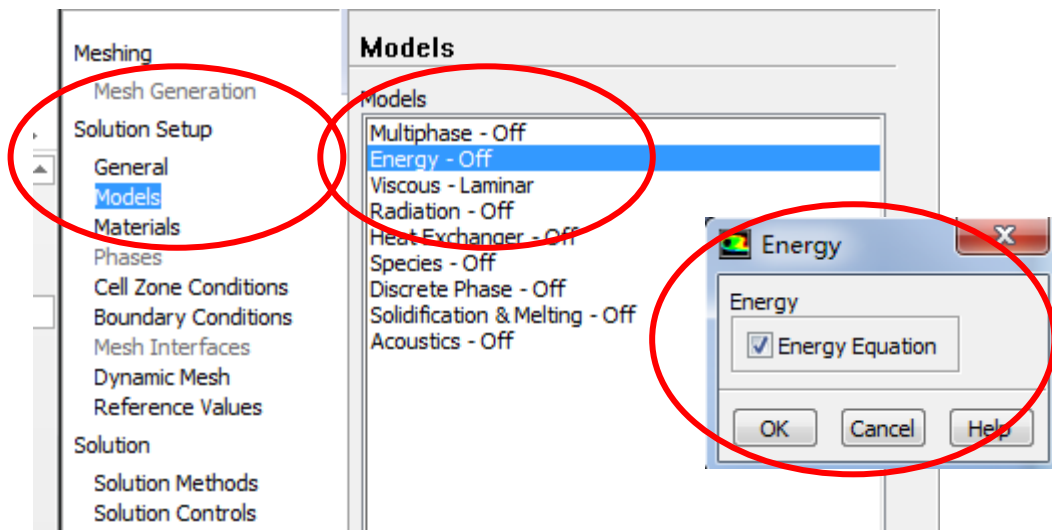


**Fluent is just a tool!**

## Step 3: Choose the physicochemical model

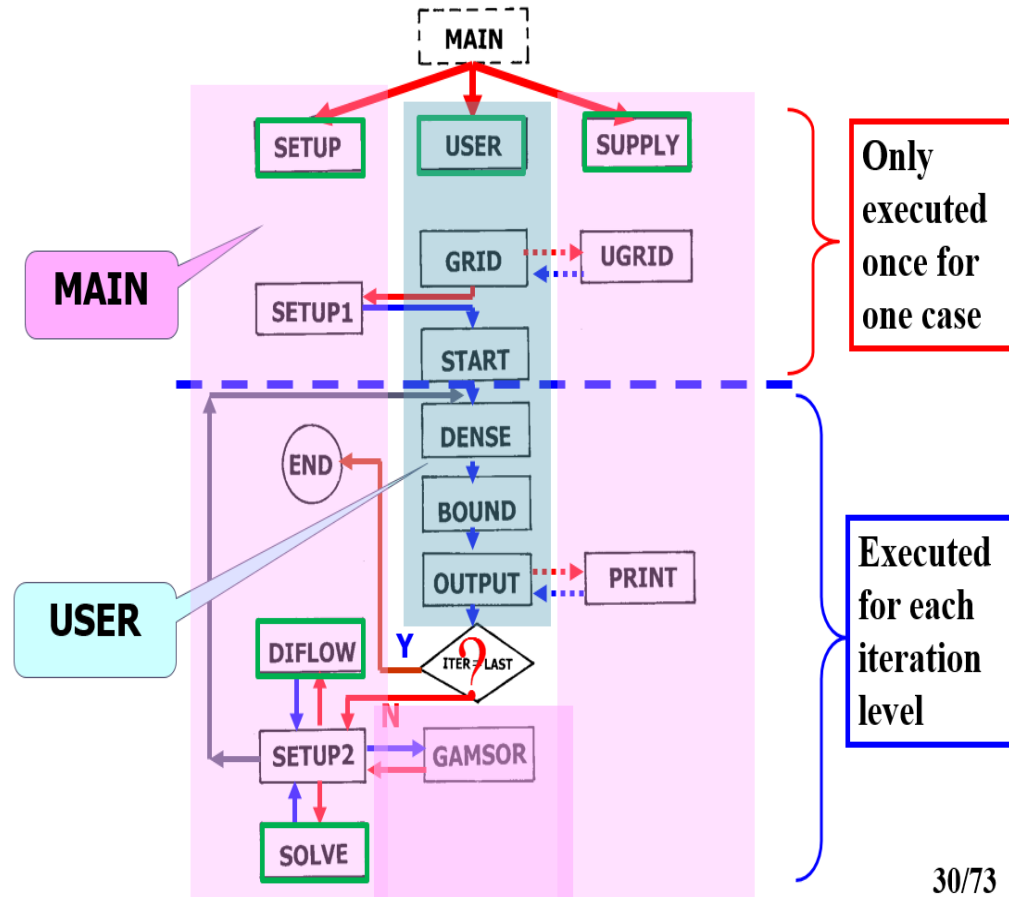
To select the model, the command is as follows:

**Solution Setup → Model**



**Remark:** In our general teaching code

In SETUP2, Visit NF from 1 to NFMAX in order; If LSOLVE(NF)=.T. , this variable is solved; Similarly in PRINT SUBROUTINE NF is visited form 1 to NFX4(=14) in order , as long as LPRINT(NF)=.T., the variable is printed out.



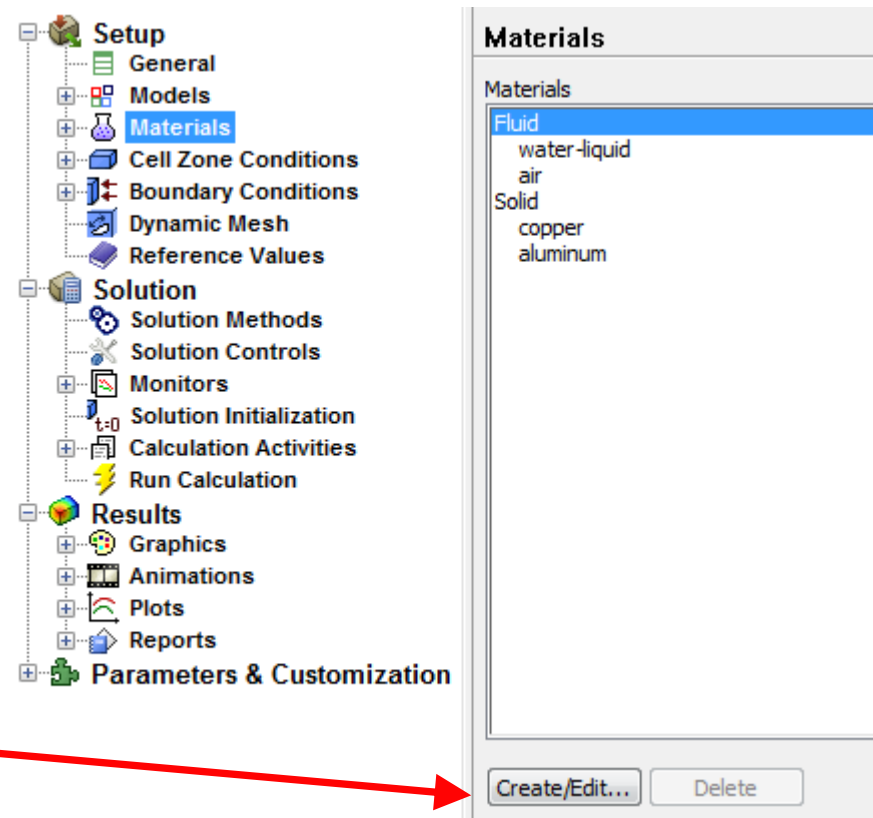
## Step 4: Define the material properties

Define the properties required for modeling! For fluid flow and heat transfer problem studied here,  $\rho$ ,  $c_p$  and  $\lambda$  should be defined.

Solution Setup  $\rightarrow$  Materials

In Fluent, the default fluid is air and the default solid is Al.

Click the Create/Edit button to add copper and liquid water in our case.





### Create/Edit Materials

Name: water-liquid

Material Type: fluid

Order Materials by:  
 Name  
 Chemical Formula

Chemical Formula: h2o<l>

Fluent Fluid Materials: water-liquid (h2o<l>)

Mixture: none

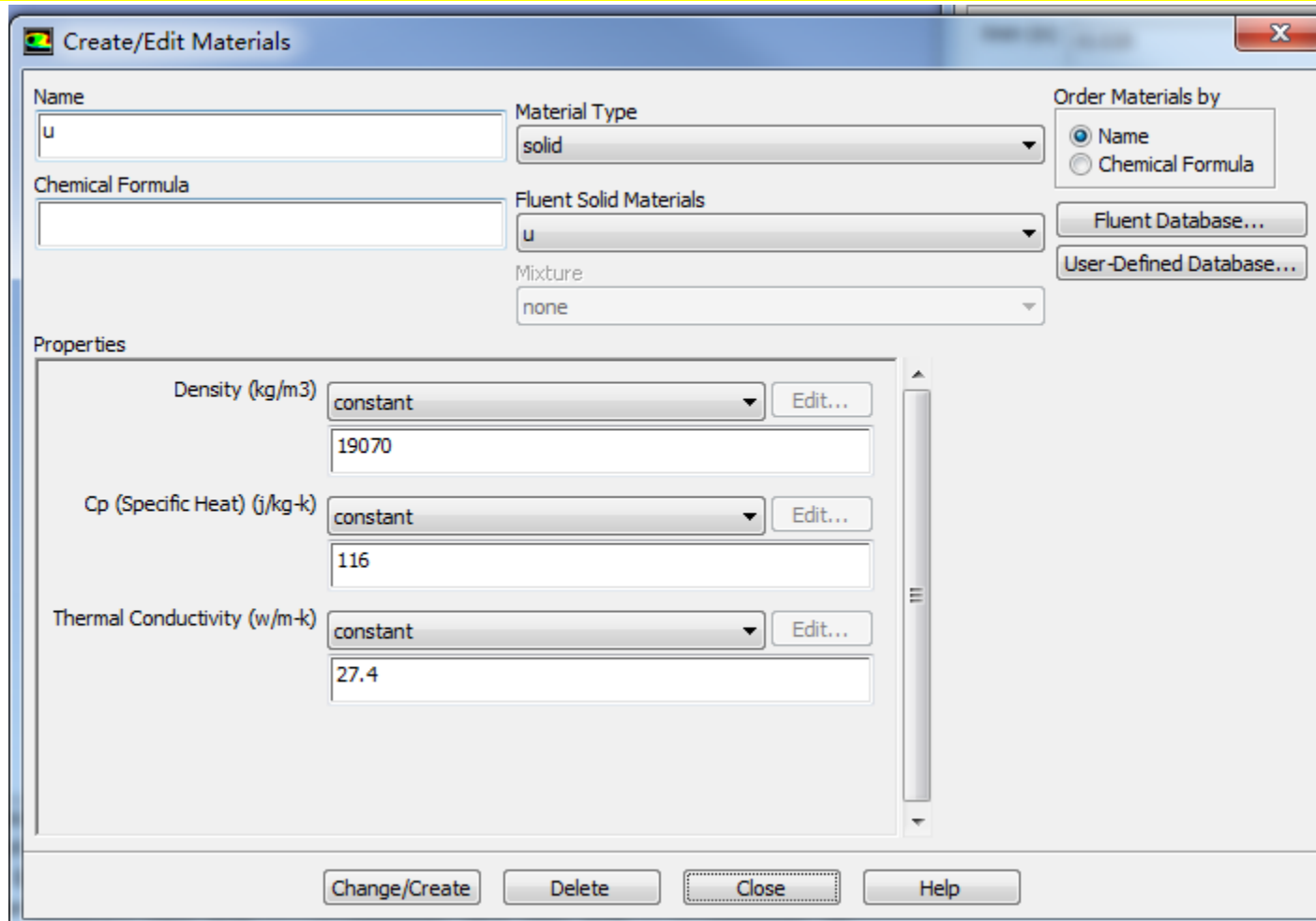
Fluent Database...  
User-Defined Database...

#### Properties

Density (kg/m3)	constant	Edit...
	998.2	
Cp (Specific Heat) (j/kg-k)	constant	Edit...
	4182	
Thermal Conductivity (w/m-k)	constant	Edit...
	0.6	
Viscosity (kg/m-s)	constant	Edit...
	0.001003	

Change/Create   Delete   Close   Help

**However, it will happen that the material you need is not in the database. You can input it manually.**

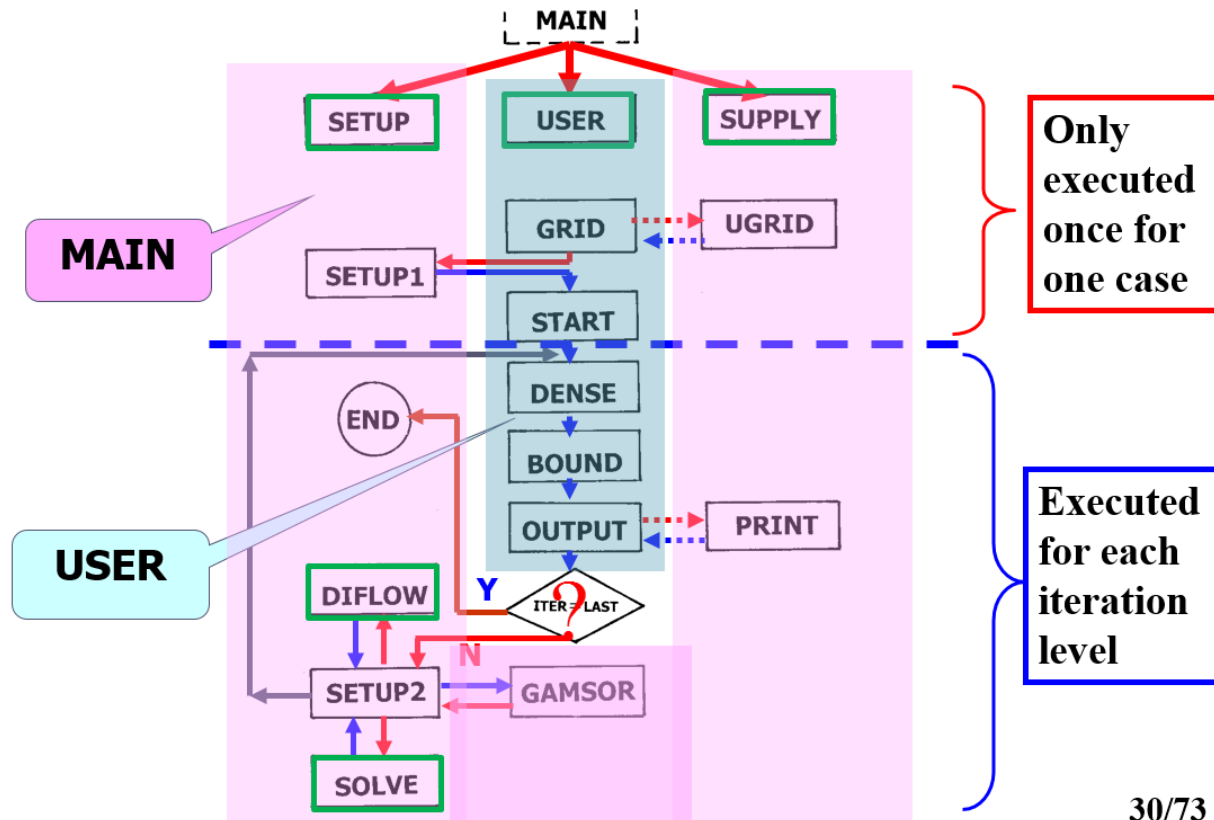


# Our general Code:

## 12. GAMSOR

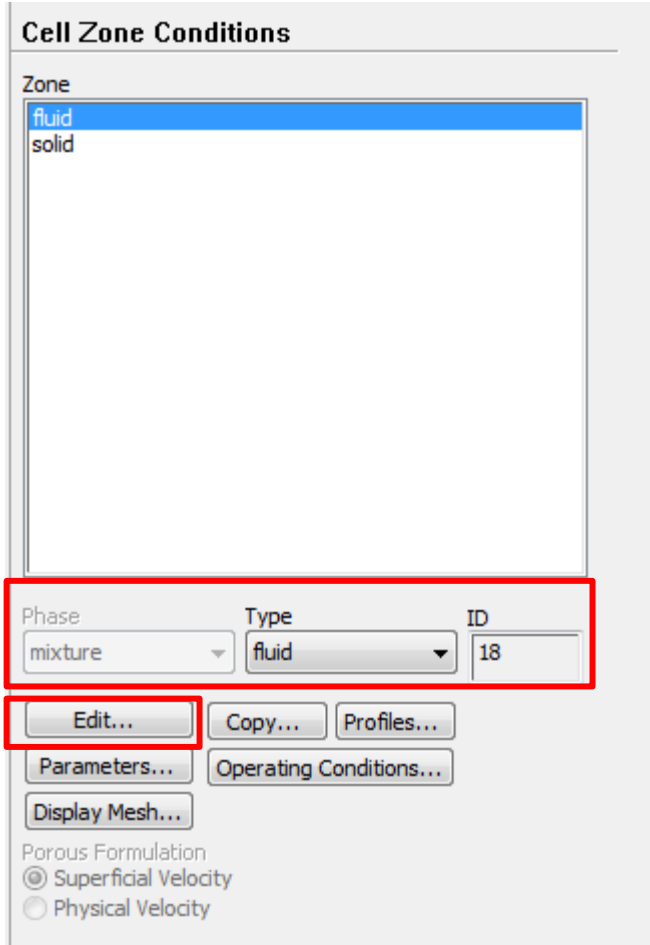
(1) Determine  $\Gamma_\phi$  for different variables:

$$u, v - \eta ; T - \lambda$$



# Step 5: Define zone condition

## Solution Setup → Cell Zone Condition



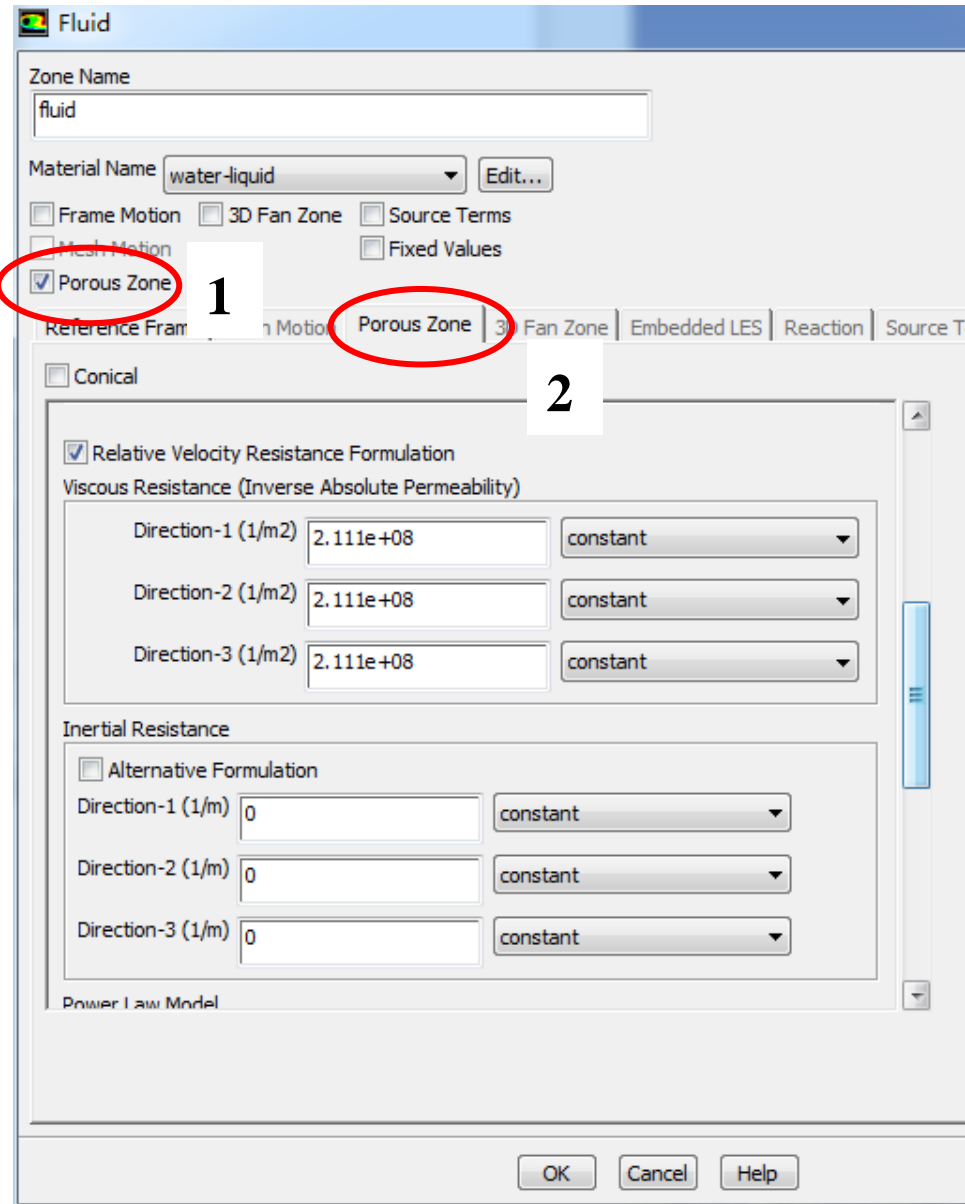
Each zone has its ID.

Each zone should be assigned a type, either fluid or solid.

**Phase** is not activated here. It can be edited under other cases, for example multiphase (多相流) flow model is activated. [See Example A3.](#)

Click Edit to define the zone condition of each zone.

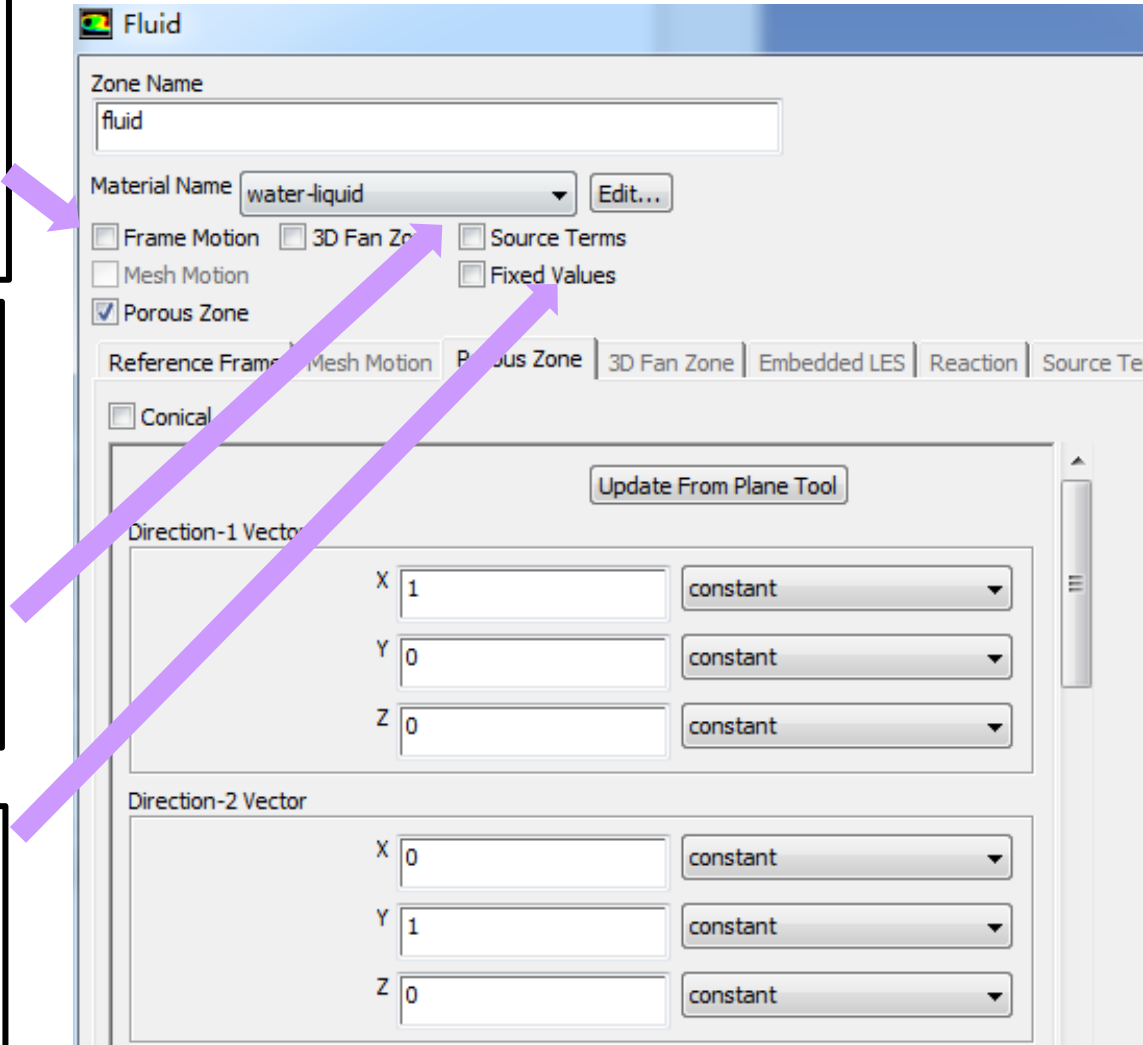
**Porous media is treated as a type of fluid zone, in which parameters related to porous media should be given such as porosity, permeability (渗透率), etc. We will discuss it in Example A2.**



Frame motion and Mesh motion is used if the solid or the frame is moving.

Source term is needed as a constant value or by user defined with .c file compiled if you need.

If  $T$  of the zone is fixed, you can select the Fixed value button.



## Step 6: Define the boundary condition

Boundary condition definition is one of the most important and difficult step during Fluent simulation. General boundary conditions in Fluent can be divided into two kinds:

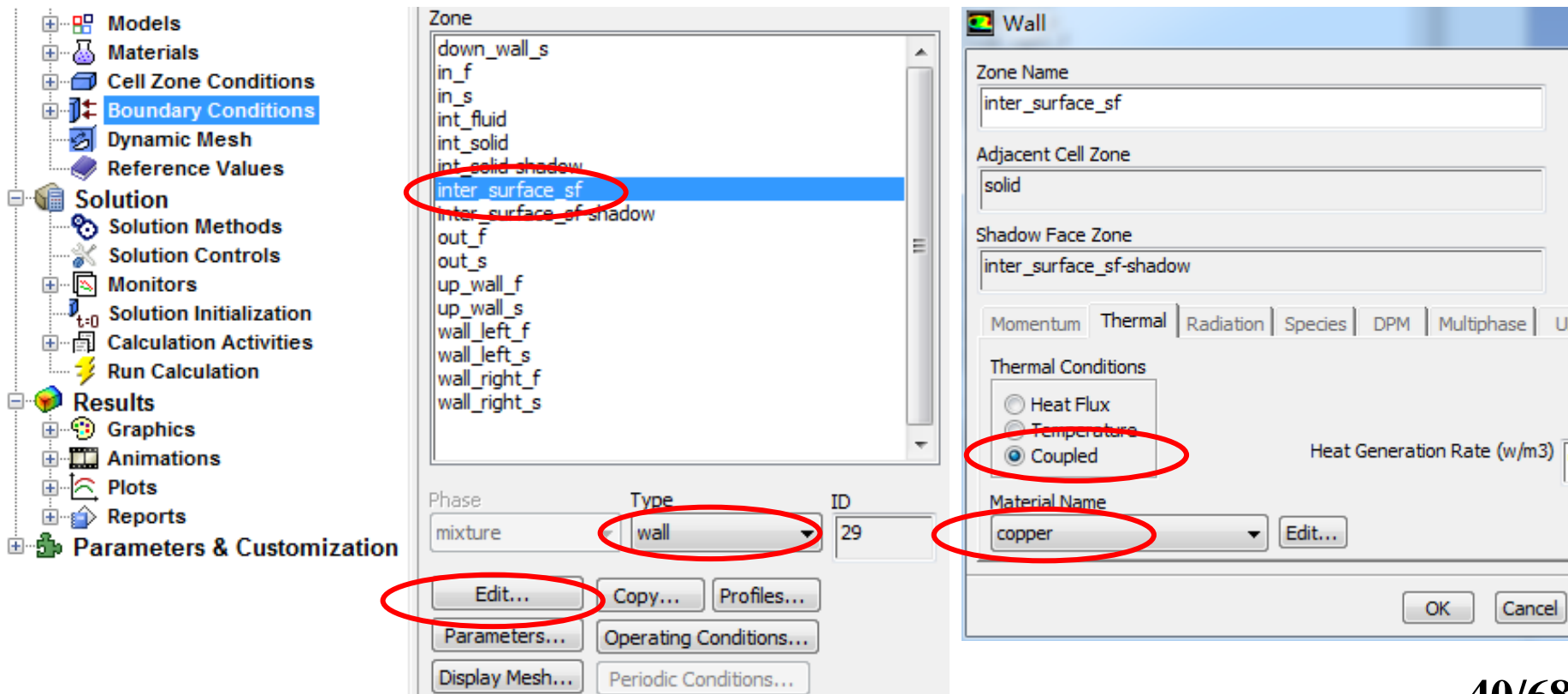
**1. BC at inlet and outlet:** pressure, velocity, mass flow rate, outflow...

**2. BC at wall:** wall, periodic, symmetric...

**Remark:** Interior cell zone and interior interface will also shown in the BC Window.

For example, **inter\_surface\_sf: 29** is listed here. It is the interface between fluid and solid zones.

It is treated as **coupled, conjugate condition** (流固耦合)



The screenshot displays the ANSYS Fluent software interface. On the left is the 'Tree Outline' showing the 'Boundary Conditions' folder expanded. The main window shows the 'Zone' list with 'inter\_surface\_sf' selected and circled in red. Below the list, a table shows the zone details:

Phase	Type	ID
mixture	wall	29

The 'Edit...' button for this zone is also circled in red. To the right, the 'Wall' properties dialog is open, showing the 'inter\_surface\_sf' zone name and 'solid' as the adjacent cell zone. Under 'Thermal Conditions', the 'Coupled' radio button is selected and circled in red. The 'Material Name' is set to 'copper', which is also circled in red. The 'Heat Generation Rate (w/m3)' field is empty.



For example, **inter\_surface\_sf: 29** is listed here. It is the interface between fluid and solid zones.

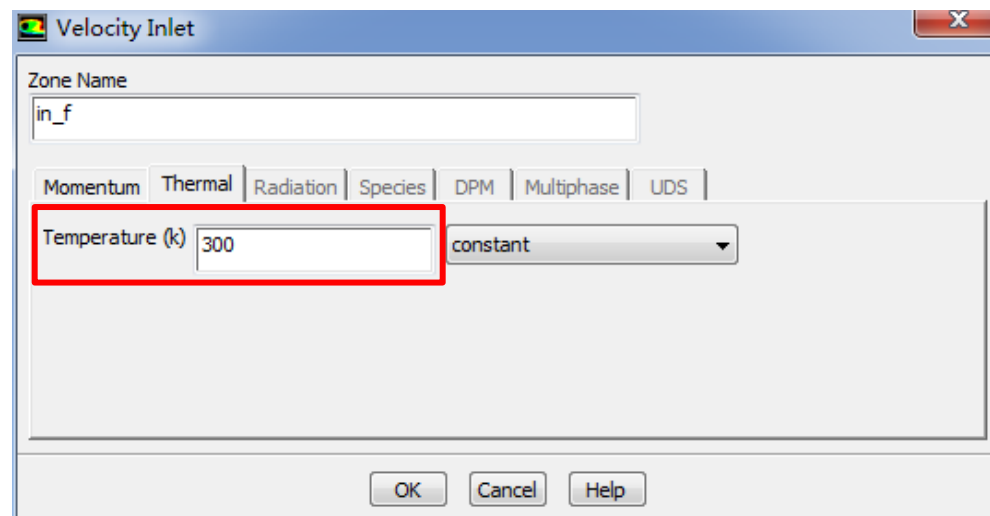
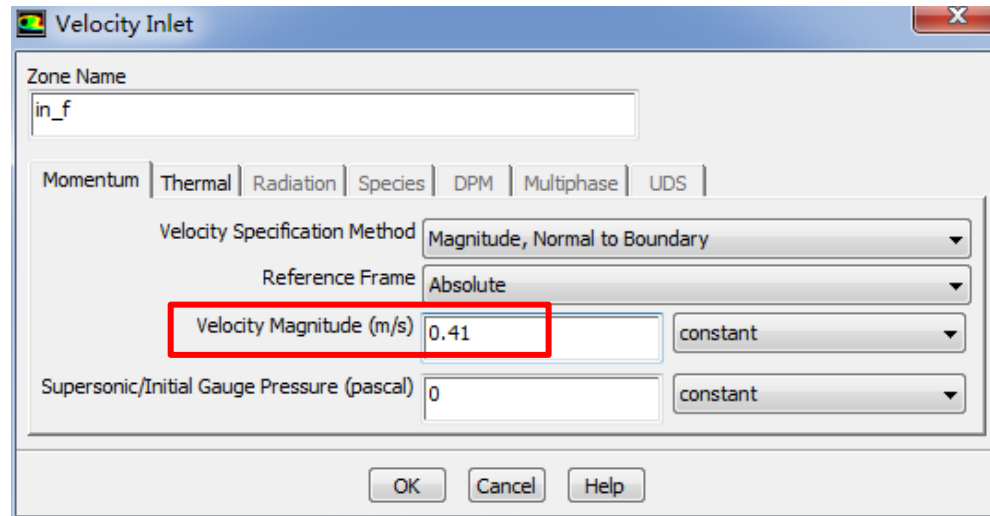
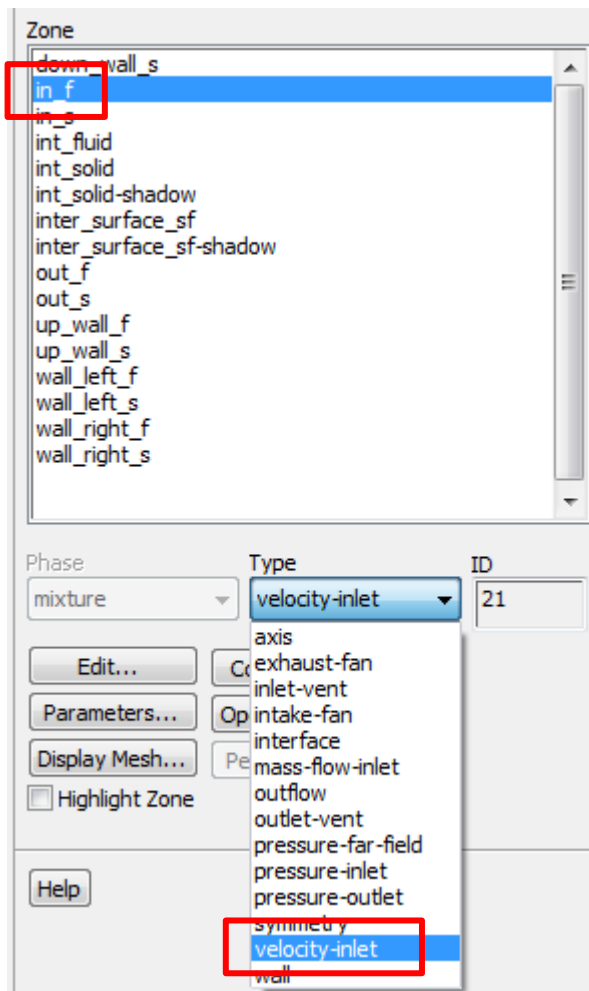
It is treated as **coupled, conjugate condition** (流固耦合)

$$T_f = T_s$$
$$-\lambda_f \frac{\partial(T)_f}{\partial n_f} = \lambda_s \frac{\partial(T)_s}{\partial n_s}$$



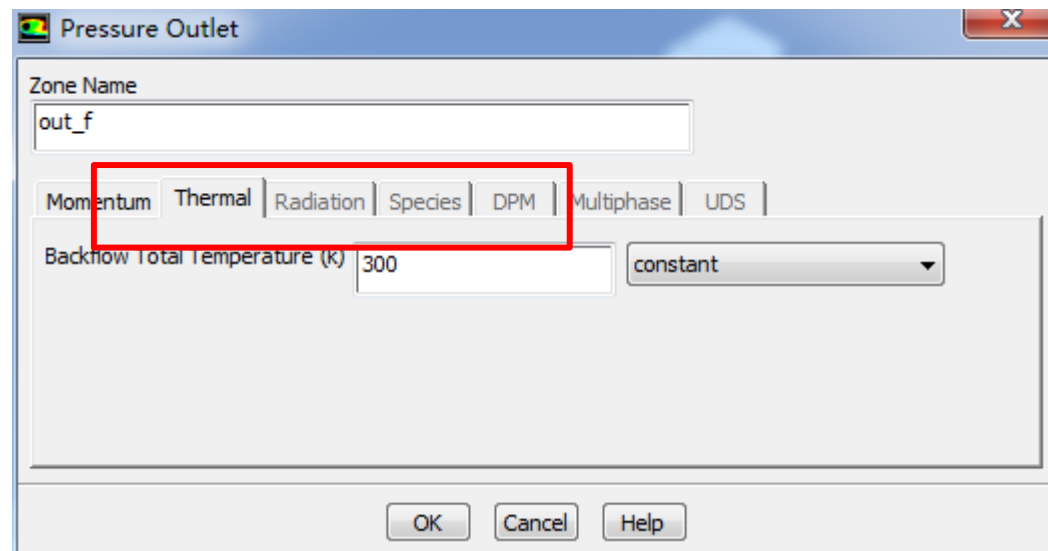
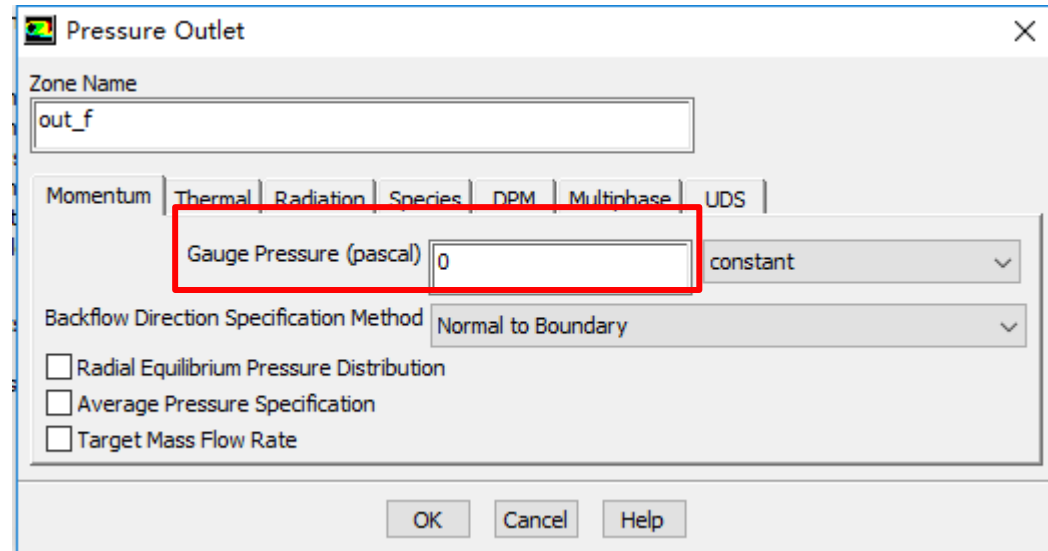
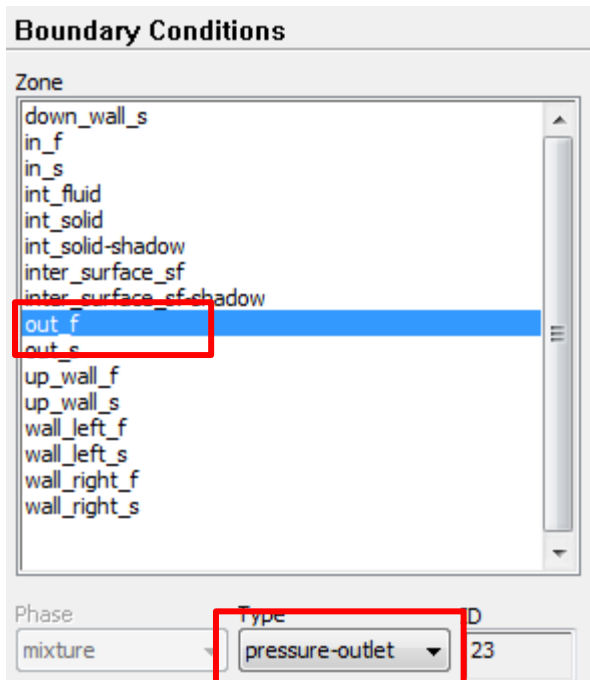
# Other BCs are as follows:

## For fluid inlet: velocity inlet



# Other BCs are as follows:

## For fluid outlet: pressure outlet



## Seven kinds of Pressure in Fluent

1. Atmospheric pressure (大气压)
2. Gauge pressure (表压): the difference between the true pressure and the Atmospheric pressure.
3. Absolute pressure (真实压力): the true pressure  
**= Atmospheric pressure + Gauge pressure**
4. Operating pressure (操作压力) : the same as the reference pressure (参考压力) in our teaching code



## Pressure in Fluent

**Absolute pressure (真实压力):** the true pressure

**= Reference Pressure + Relative Pressure**

**5. Static pressure (静压):** the difference between true pressure and operating pressure.

**The same as relative pressure.**

**6. Dynamic pressure (动压):** calculated by  $0.5\rho U^2$   
**is related to the velocity.**

**7. Total pressure (动压):**

**= Static pressure + dynamic pressure**

# Other BCs are as follows:

## For bottom surface: constant heat flux

**Boundary Conditions**

Zone

- down\_wall\_s
- in\_f
- in\_s
- int\_fluid
- int\_solid
- int\_solid-shadow
- inter\_surface\_sf
- inter\_surface\_sf-shadow
- out\_f
- out\_s
- up\_wall\_f
- up\_wall\_s
- wall\_left\_f
- wall\_left\_s
- wall\_right\_f
- wall\_right\_s

Phase: mixture    Type: wall    ID: 32

Buttons: Edit... Copy... Profiles... Parameters... Operating Conditions... Display Mesh... Periodic Conditions... Highlight Zone

**Wall**

Zone Name: down\_wall\_s

Adjacent Cell Zone: solid

Momentum | **Thermal** | Radiation | Species | DPM | Multiphase | UDS | Wall Film

This page is not applicable under current settings.

**Wall**

Zone Name: down\_wall\_s

Adjacent Cell Zone: solid

Momentum | **Thermal** | Radiation | Species | DPM | Multiphase | UDS

**Thermal Conditions**

- Heat Flux
- Temperature
- Convection
- Radiation
- Mixed
- via System Coupling
- via Mapped Interface

Heat Flux (w/m<sup>2</sup>): 1000000    constant

Wall Thickness (m): 0

Heat Generation Rate (w/m<sup>3</sup>): 0    constant

Shell Conduction    1 Layer    Edit...

Material Name: aluminum    Edit...

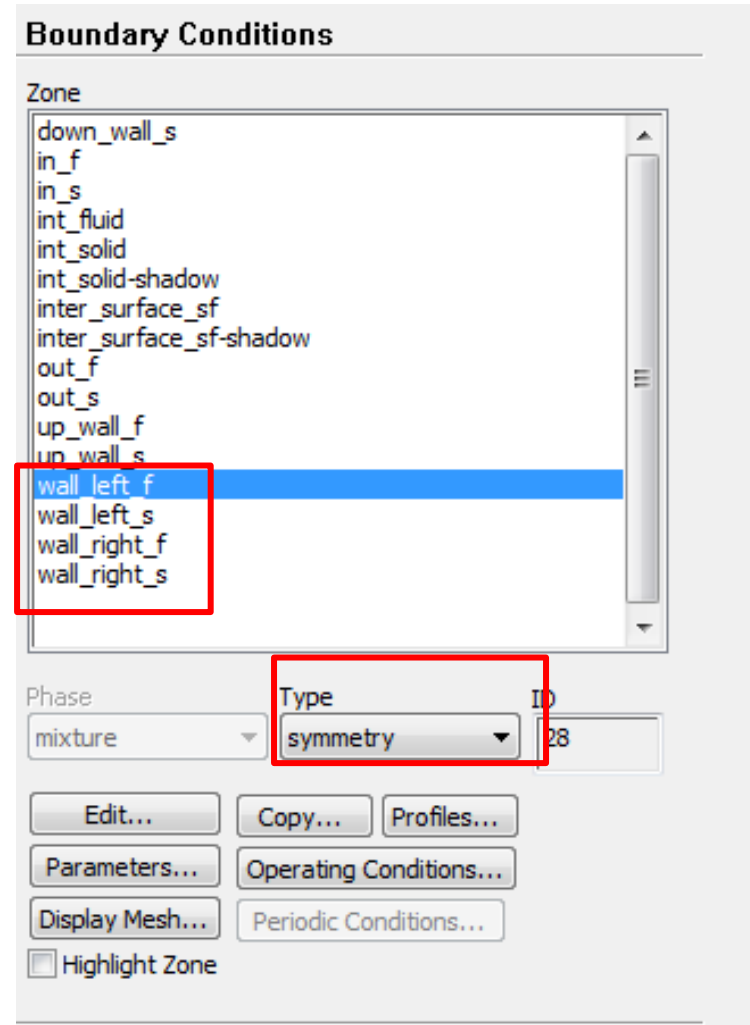
Buttons: OK Cancel Help

**Take care of the unit of heat flux**

Other BCs are as follows:

For left and right fluid surfaces: symmetry

The left and right boundary for solid and fluid are set as **symmetry**. Because the calculation domain is a **typical part** extracted from the total district, which can **represent** the heat transfer and fluid flow characteristics.





# Other BCs are as follows:

For top surface, solid in and out surfaces: adiabatic and non-slipping wall

The image shows the ANSYS Fluent software interface for setting boundary conditions. On the left, the 'Boundary Conditions' panel lists various zones, with 'up\_wall\_f' selected. The 'Wall' dialog box is open, showing the following settings:

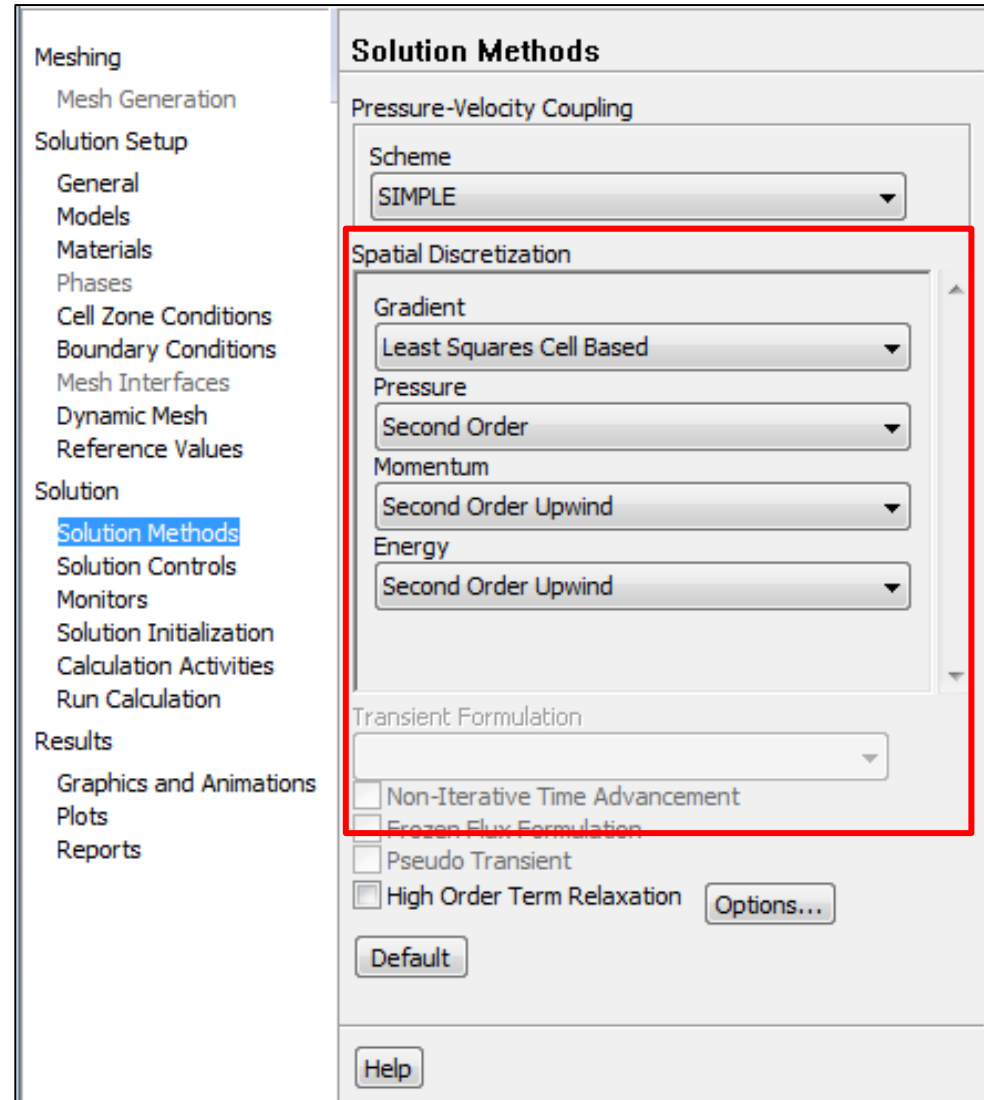
- Zone Name:** up\_wall\_f
- Adjacent Cell Zone:** fluid
- Wall Motion:** Stationary Wall (selected)
- Shear Condition:** No Slip (selected)
- Thermal Conditions:** Heat Flux (selected) with a value of 0.
- Material Name:** aluminum

A yellow box highlights the text **Adiabatic wall**.

# Step 7: Solution setup: algorithm and scheme

**Remark:** In Fluent, for the SIMPLE series algorithms, only **SIMPLE** and **SIMPLEC** are included.

**Review:** What is the difference between SIMPLE, SIMPLEC and SIMPLER?



**Gradient calculation,**  
**There are three schemes.**

Gradient

Least Squares Cell Based

Green-Gauss Cell Based

Green-Gauss Node Based

Least Squares Cell Based

$\nabla \phi$

1. Green-Gauss Cell-Based (格林-高斯基于单元法)
2. Green-Gauss Node-Based (格林-高斯基于节点法)
3. Least-Squares Cell Based 基于单元体的最小二乘法  
It is the default scheme for gradient calculation.

### Green-Gauss Theory:

The averaged gradient over a control domain is:

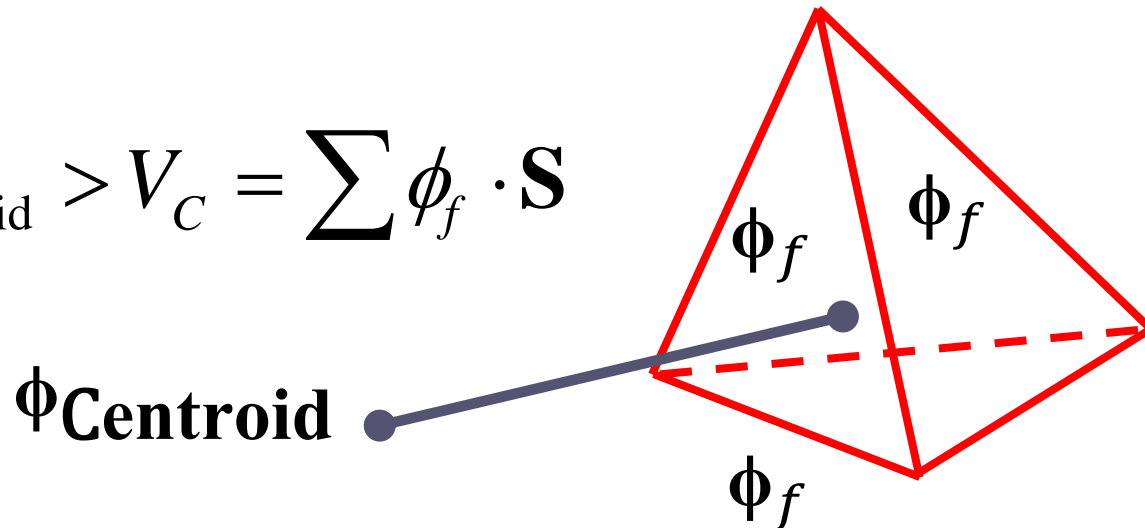
$$\langle \nabla \phi \rangle = \frac{1}{V_C} \int_{V_C} \nabla \phi dV$$

Using the **Gauss integration theory** (高斯定理), the **volume integral** (体积分) is transformed into a **surface integral** (面积分) :

$$\langle \nabla \phi \rangle = \frac{1}{V_C} \int_{V_C} \nabla \phi dV = \frac{1}{V_C} \oint \phi \cdot \mathbf{n} dS$$

In the presence of discrete faces, the above equation can be written as:

$$\langle \nabla \phi_{\text{centroid}} \rangle V_C = \sum \phi_f \cdot \mathbf{S}$$



$$\nabla \phi_{\text{centroid}} V_C = \sum \phi_f \cdot \mathbf{n} S$$

The problem of calculating gradient is transferred into the following equation:

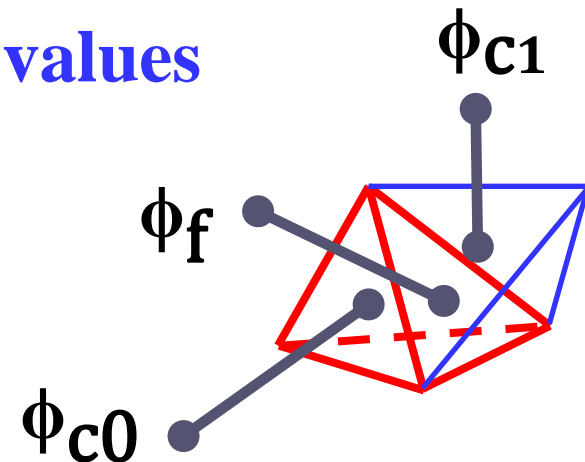
**How to determine  $\phi_f$  at the face?**

### 1. Green-Gauss Cell-Based (格林-高斯基于单元法)

Calculate  $\phi_f$  using cell centroid values

(网格中心点) .

$$\phi_f = \frac{\phi_{C0} + \phi_{C1}}{2}$$

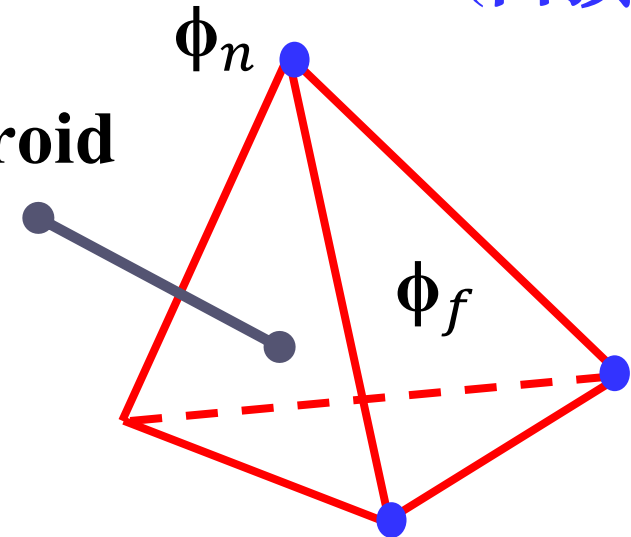


## 2. Green-Gauss Node-Based (格林-高斯基于节点法)

Calculate  $\phi_f$  by the average of the node values. (面顶点的代数平均值)

$$\phi_f = \frac{1}{N_f} \sum \phi_n$$

$$\phi_n = \sum_i^{N_{\text{cells}}(n)} \phi_{c_i} w_{c_i, n}$$



$N_f$ : number of nodes on the face,  $\phi_n$ : node value.

$\phi_n$ , is calculated by weighted average of the cell values surrounding the nodes  $\phi_{c_i}$ .

**Review:** the node-based method is more accurate than the cell-based method.

### 3. Least-Squares Cell Based 基于单元体的最小二乘法

**It is the default scheme for gradient calculation.**

The basic idea is as follows. Consider two cell centroid  $C_0$  and  $C_i$ , and their distance vector as  $\delta r$ . Then, the following equation

$$\phi_{C_i} = \phi_{C_0} + (\nabla \phi) \cdot (\mathbf{r}_{C_i} - \mathbf{r}_{C_0})$$

is exact only when the solution field is linear! **In other words, there is no second-order term for Taylor expansion of  $\phi$ !**

For a cell centroid  $\mathbf{C}_0$  with  $N$  neighboring nodes  $\mathbf{C}_i$ ,

$$\Phi_{C_i} = \phi_{C_i} - \left[ \phi_{C_0} + (\nabla \phi) \cdot (\mathbf{r}_{C_i} - \mathbf{r}_{C_0}) \right]$$

**True value**

**Calculated value**

Making summation of all these  $\Phi_{C_i}$  with a weighting factor  $w_i$

$$\xi = \sum_{i=1}^N w_i \Phi_{C_i} = \sum_{i=1}^N \left\{ w_i \left( \phi_{C_i} - \left[ \phi_{C_0} + (\nabla \phi) \cdot (\mathbf{r}_{C_i} - \mathbf{r}_{C_0}) \right] \right)^2 \right\}$$

$$= \sum_{i=1}^N \left\{ w_i \left( \phi_{C_i} - \phi_{C_0} - \left[ \frac{\partial \phi}{\partial x} \Delta x_i + \frac{\partial \phi}{\partial y} \Delta y_i + \frac{\partial \phi}{\partial z} \Delta z_i \right] \right)^2 \right\}$$



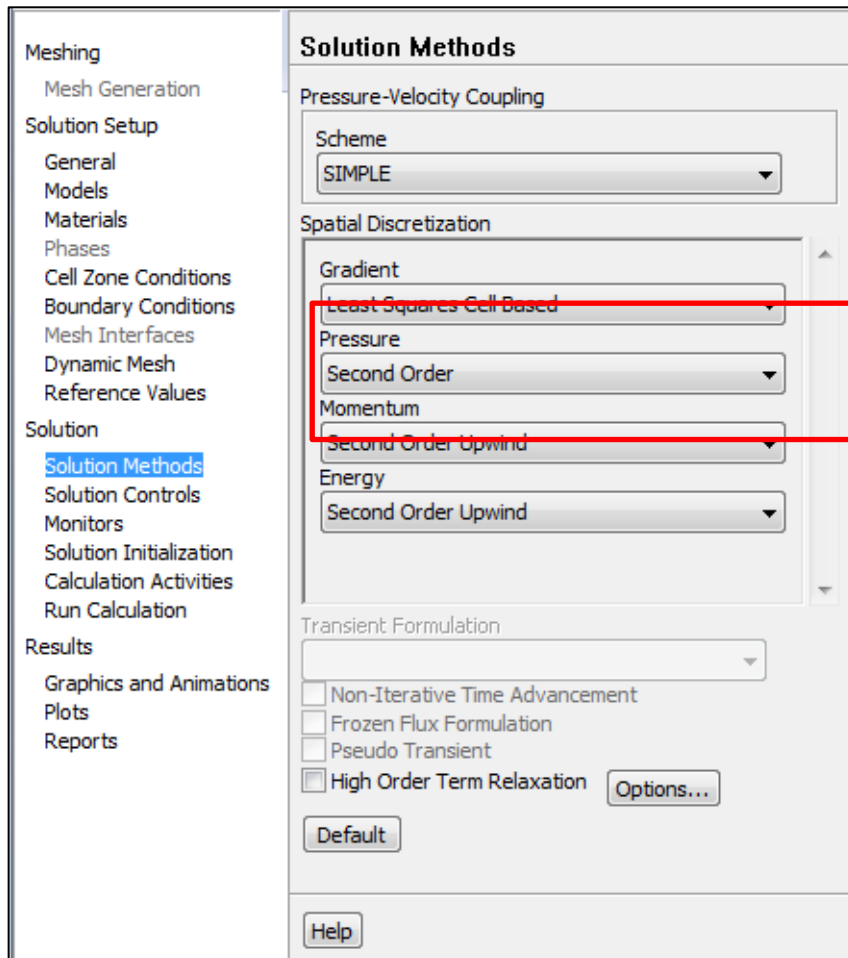
Therefore, to calculate the gradient  $\nabla\phi$  is to find the one leading to the minimum  $\xi$ !

$$\xi = \sum_{i=1}^N \left\{ w_i \left( \phi_{Ci} - \phi_{C0} - \left[ \frac{\partial\phi}{\partial x} \Delta x_i + \frac{\partial\phi}{\partial y} \Delta y_i + \frac{\partial\phi}{\partial z} \Delta z_i \right] \right)^2 \right\}$$

This is the idea of **Least-Squares method**.

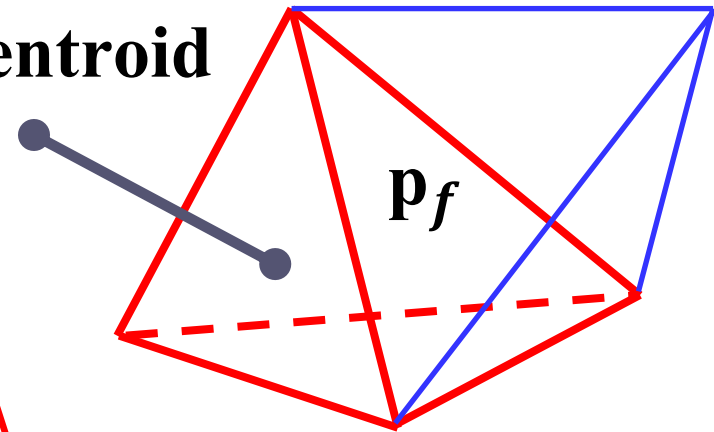
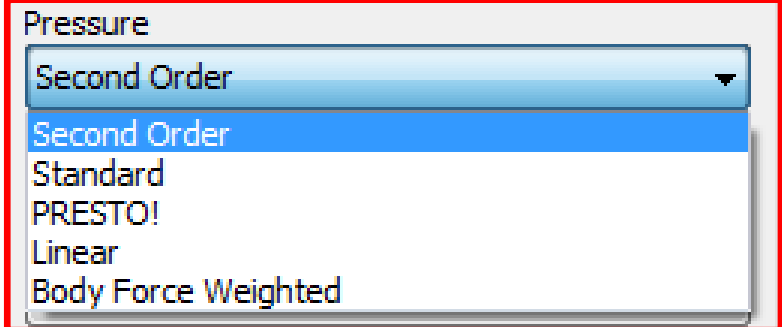
**Remark:** On irregular (不规则) unstructured meshes, the accuracy of the least-squares gradient method is comparable to that of the node-based gradient. However, it is more computational efficient compared with the node-based gradient.

# Pressure calculation: to calculate the pressure value at the interface using centroid value.



The screenshot shows the 'Solution Methods' panel in ANSYS Fluent. The 'Pressure-Velocity Coupling' section has 'Scheme' set to 'SIMPLE'. The 'Spatial Discretization' section has 'Gradient' set to 'Least Squares Cell Based', 'Pressure' set to 'Second Order', and 'Momentum' set to 'Second Order Upwind'. The 'Energy' section has 'Second Order Upwind' selected. The 'Transient Formulation' section has 'Non-Iterative Time Advancement', 'Frozen Flux Formulation', 'Pseudo Transient', and 'High Order Term Relaxation' all unchecked. There are 'Default' and 'Help' buttons at the bottom.

**P**Centroid

A close-up of the 'Pressure' dropdown menu in the software. The 'Second Order' option is selected and highlighted in blue. Other options visible are 'Standard', 'PRESTO!', 'Linear', and 'Body Force Weighted'.

## 1. Linear scheme

Compute the face pressure use the average of the pressure values in the adjacent cells.

$$P_f = \frac{P_{C0} + P_{C1}}{2}$$

## 2. Standard scheme

Interpolate the pressure using momentum equation coefficient.

$$P_f = \frac{\frac{P_{c0}}{a_{P,c0}} + \frac{P_{c1}}{a_{P,c1}}}{\frac{1}{a_{P,c0}} + \frac{1}{a_{P,c1}}}$$

### 3. Second Order

Calculate the pressure value using a central difference scheme

$$P_f \approx \frac{P_{C0} + \nabla P_{C0} \mathbf{r}_{C0} + P_{C1} + \nabla P_{C1} \mathbf{r}_{C1}}{2}$$

### 4. Body Force Weighted scheme

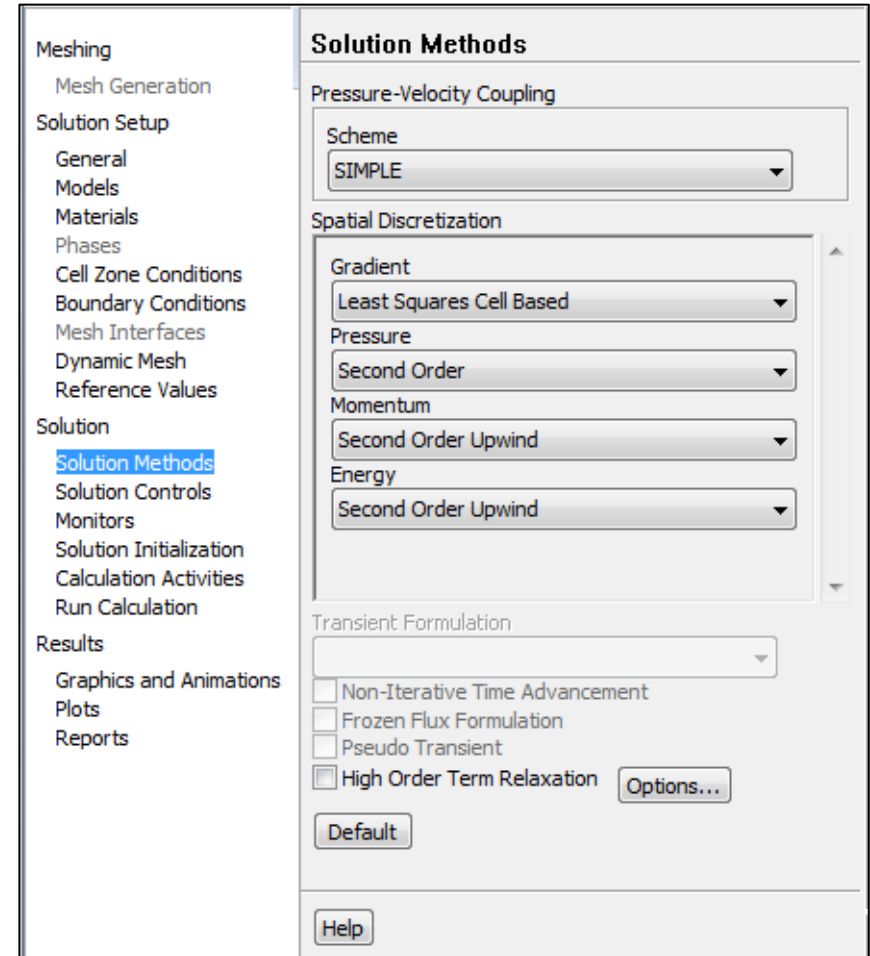
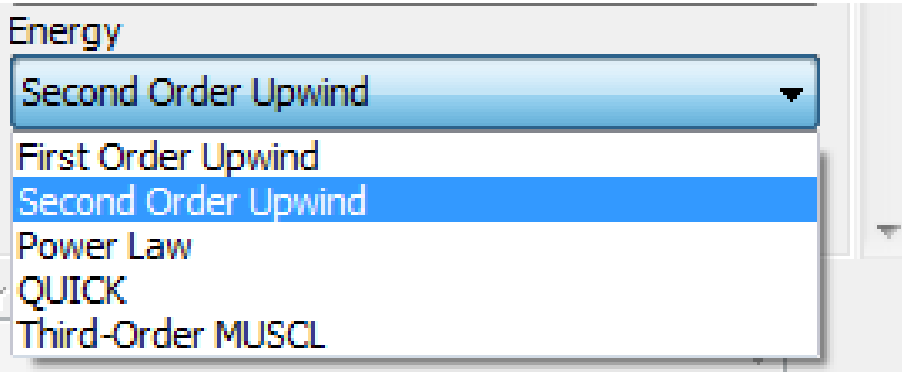
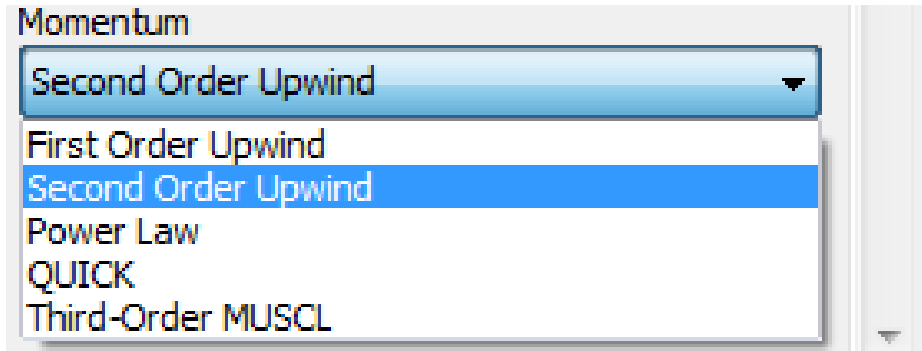
Calculate the pressure according to the body force.

- ✓ Multiphase flow such as VOF (Volume of Fluid, 体积函数法) or LS (Level Set, 水平集): **recommended**.
- ✓ For porous media: **not recommended!**

### 5. PRESTO! (Pressure Staggering Option) scheme

For problem with high pressure gradient.

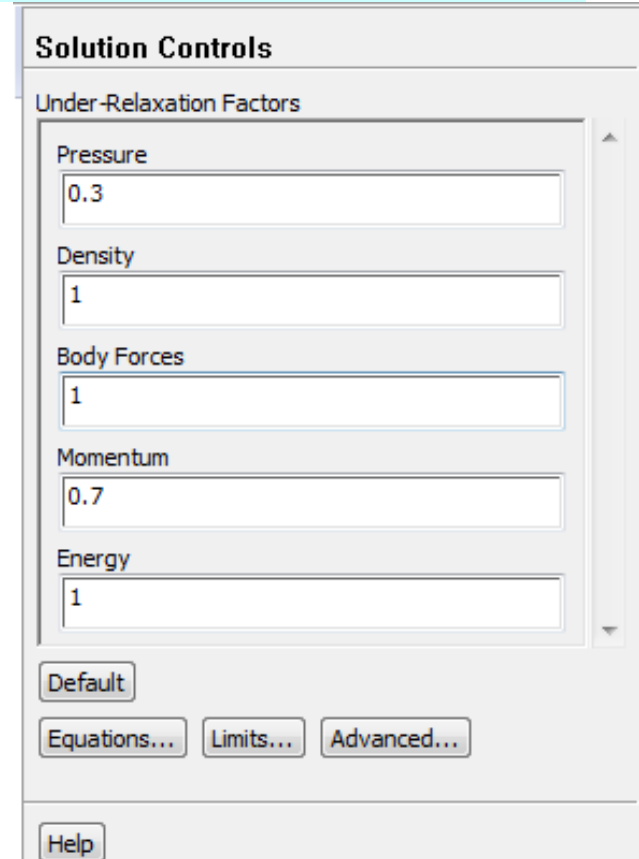
# For convective term scheme, we are very familiar!



## Step 7: Solution setup: relaxation

Under-relaxation is adopted to control the change rate of simulated variables in subsequent iterations.

The relaxation factor  $\alpha$  for each variable has been optimized for the largest possible.



**Solution Controls**

Under-Relaxation Factors

Pressure	0.3
Density	1
Body Forces	1
Momentum	0.7
Energy	1

Default

Equations... Limits... Advanced...

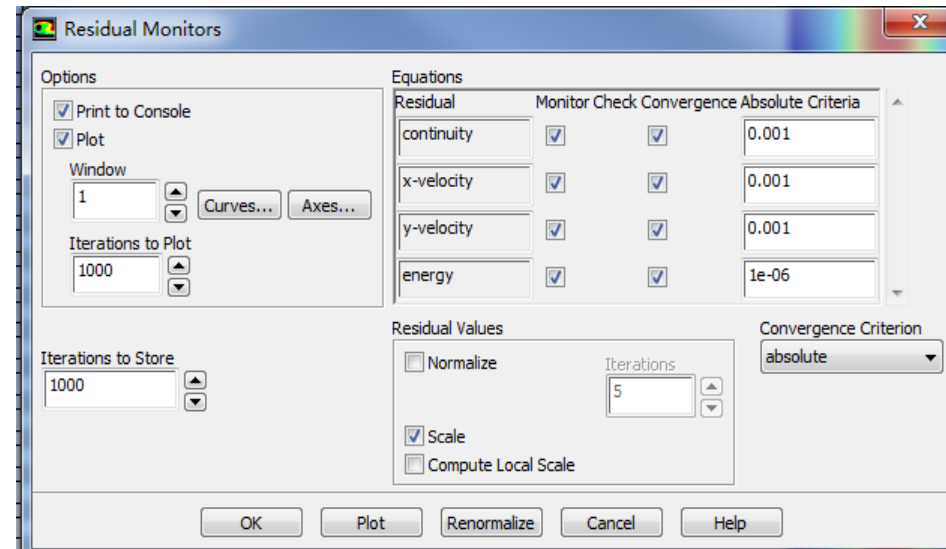
Help

In some cases, if your simulation is not converged, and you are sure there is no problem with other setting, you can try to reduce  $\alpha$ !

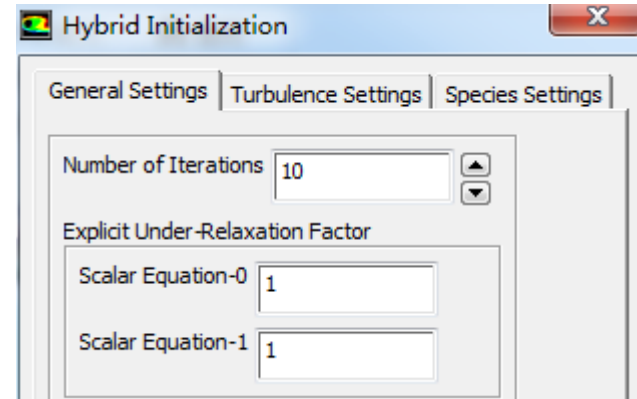
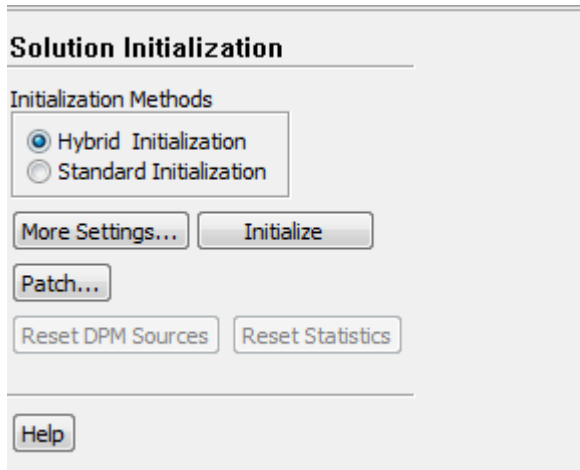
## Step 7: Solution setup: monitors

Similar to “Print” function in our teaching code, you can use Monitors in Fluent to setup a certain number of variables to monitor the iteration process of the simulation.

The Residuals are the most important values to be monitored. You can set the related values.



## Step 8: Initialization



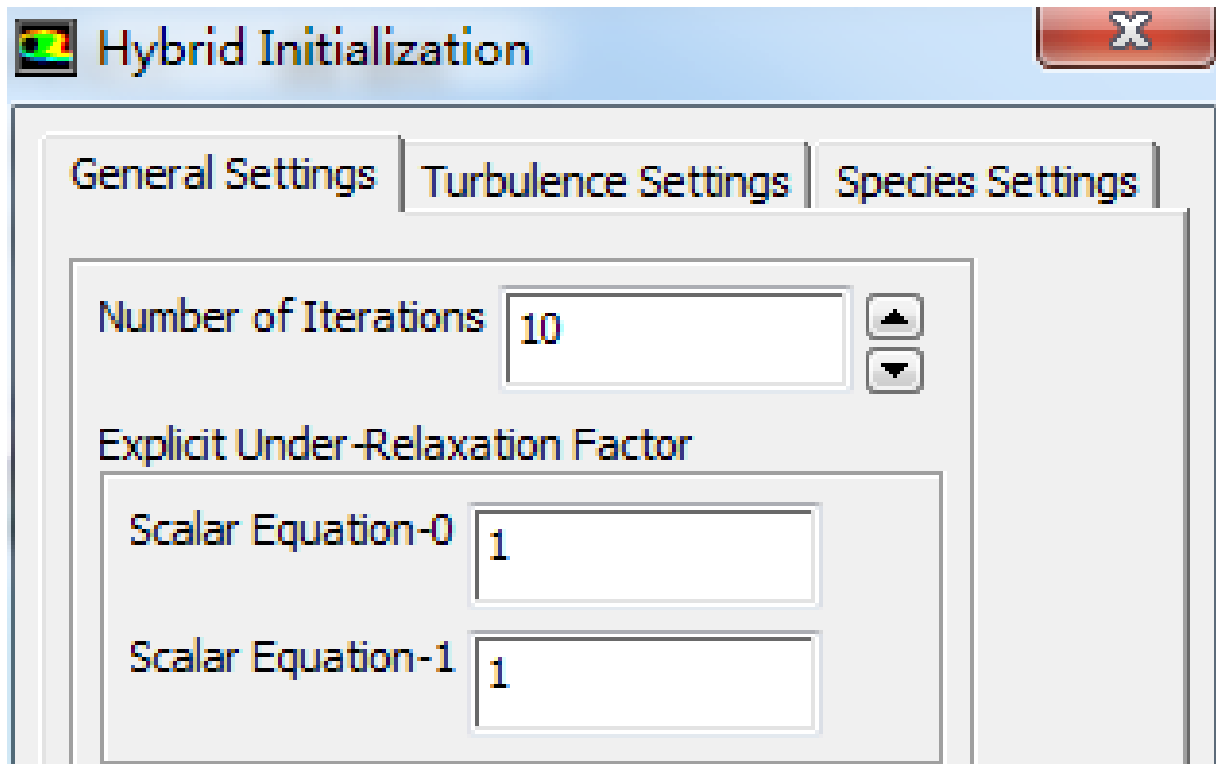
The default selection is Hybrid initialization (混合初始化).

The initial pressure and velocity field you give usually are not consistent, in other words, not meet the NS equation.

In SIMPLER algorithm, we solved an additional Poisson equation for pressure based on given velocity.

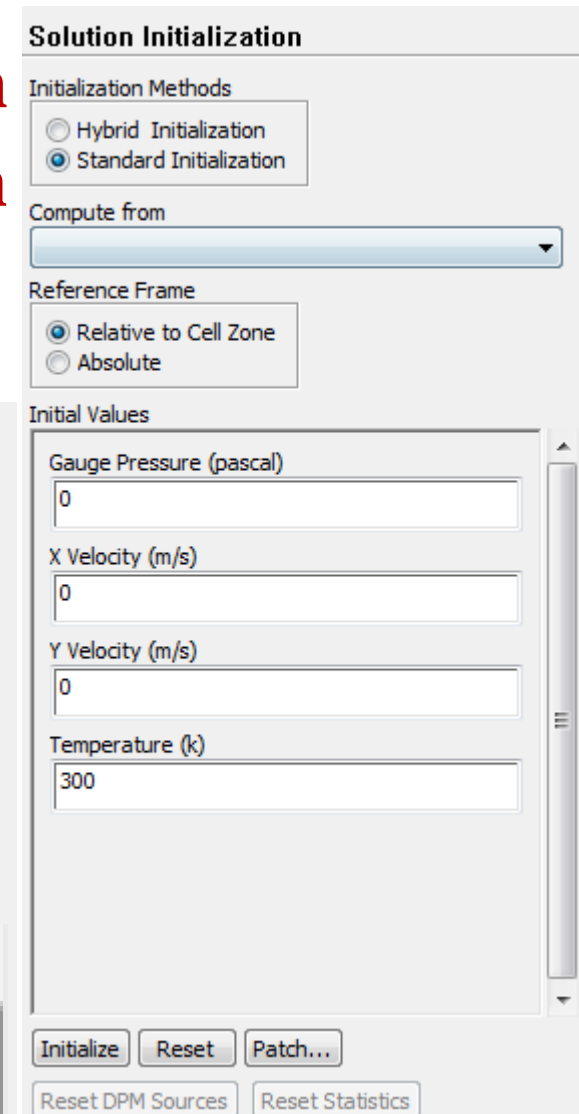
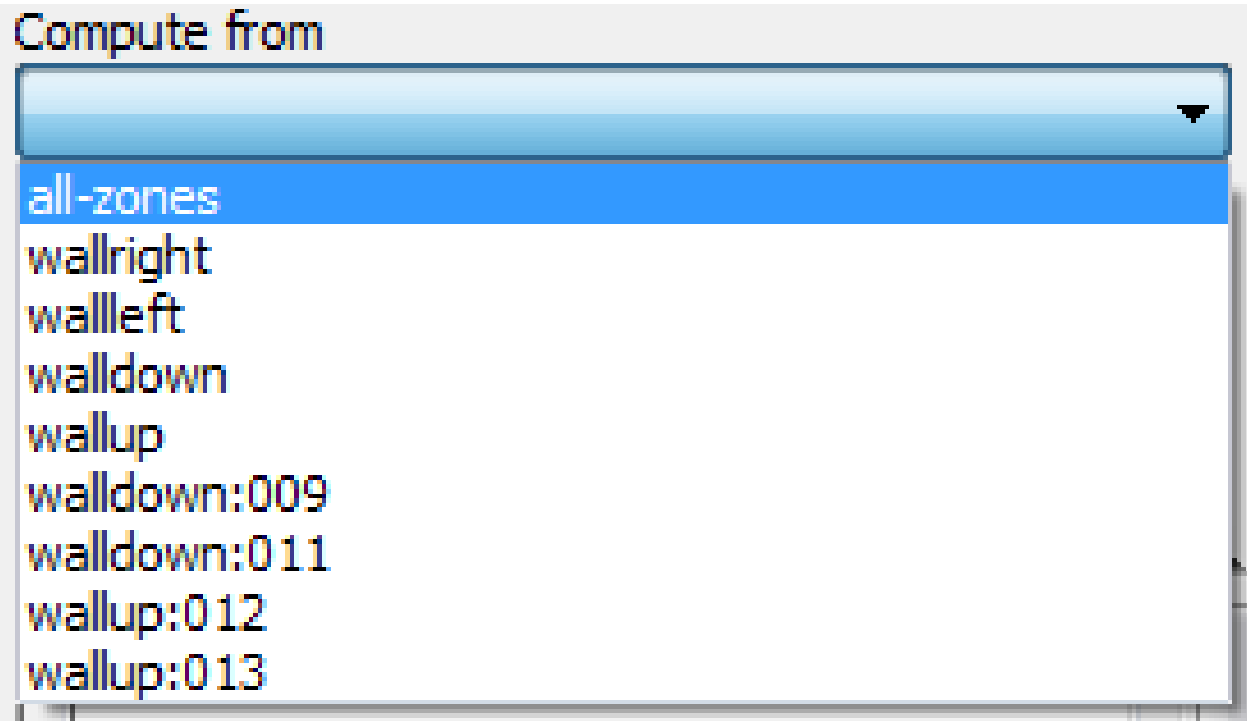


The Hybrid initialization method is similar that Poisson equation is solved to initialize the velocity and pressure equation. You can set the number of iterations to make sure the initial velocity and pressure are consistent.



Or you can simply chose Standard initialization method.

Click Compute from, the drop-down list will show, and you can select an region.

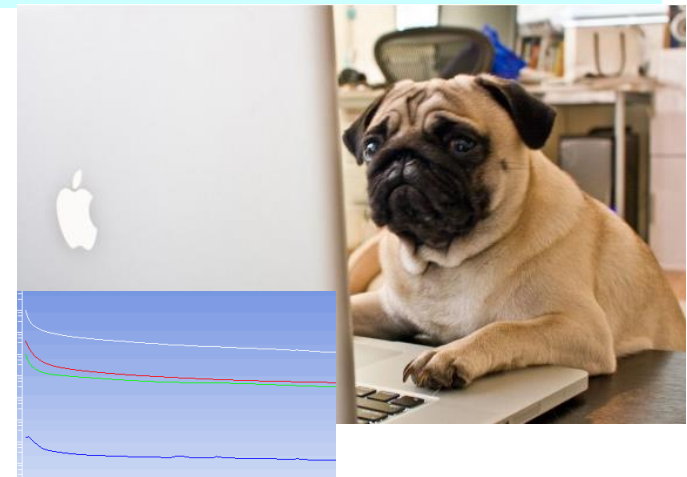


**The eight steps for preparing a Fluent simulation have been completed!**

1. Read mesh
2. scale domain
3. Choose model
4. define material
5. define zone condition
6. define boundary condition
7. Solution step
8. Initialization
9. Run the simulation.
10. Post-process

## **Step 9: Run the simulation**

**What should you do in this step?  
Just stare at the monitor to hope  
that the residual curves are going  
down for a steady problem.**



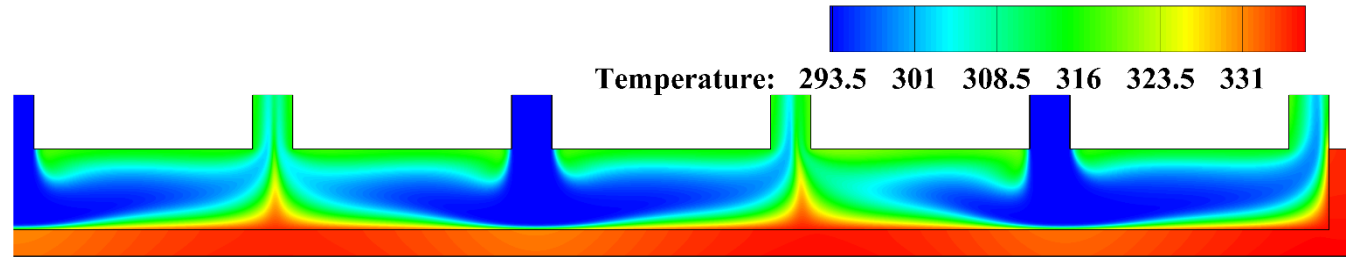
**Diverged? Go back to Steps 1 to 8.**

## **Review: The 10 steps for a Fluent simulation:**

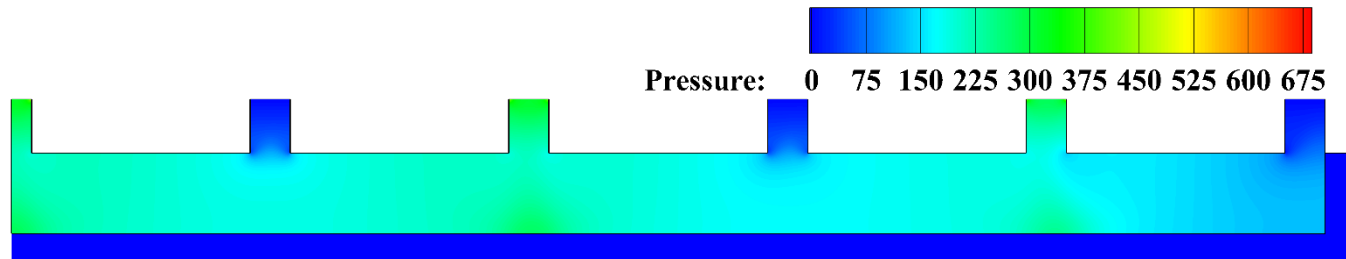
- 1. Read and check the mesh: mesh quality.**
- 2. Scale domain: make sure the domain size is right.**
- 3. Choose model: write down the right governing equation is very important.**
- 4. Define material: the solid and fluid related to your problem.**
- 5. Define zone condition: material of each zone and source term**
- 6. Define boundary condition: very important**
- 7. Solution step: algorithm and scheme. Have a background of NHT.**
- 8. Initialization: initial condition**
- 9. Run the simulation: monitor the residual curves and certain variable.**
- 10. Post-process: analyze the results.**

Re=44

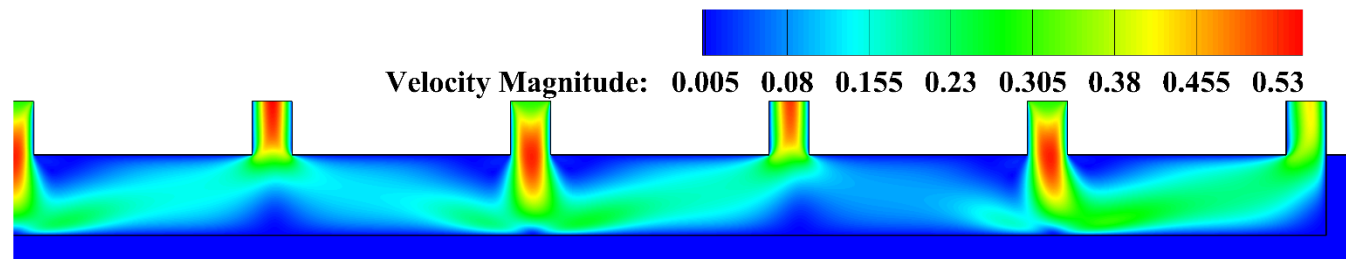
Temperature distribution



Pressure distribution



Streamline and velocity distribution



## Step 10: Post-process: Data reduction

The Reynolds number ( $Re$ ) is expressed as follow:

$$Re = \frac{\rho u_m D_h}{\mu}$$

$$D_h = \frac{2H_c W_c}{H_c + W_c}$$

$u$ (m/s)	0.3	0.6	0.9	1.2	1.5
$Re$	44	88	132	176	220

## Friction factor

$$f = \frac{2D_h \Delta P}{L_t \rho u_m^2}$$

## Heat transfer coefficient

$$h_{ave} = \frac{q_w A_s}{A_{con} (T_{w,ave} - T_{f,ave})}$$

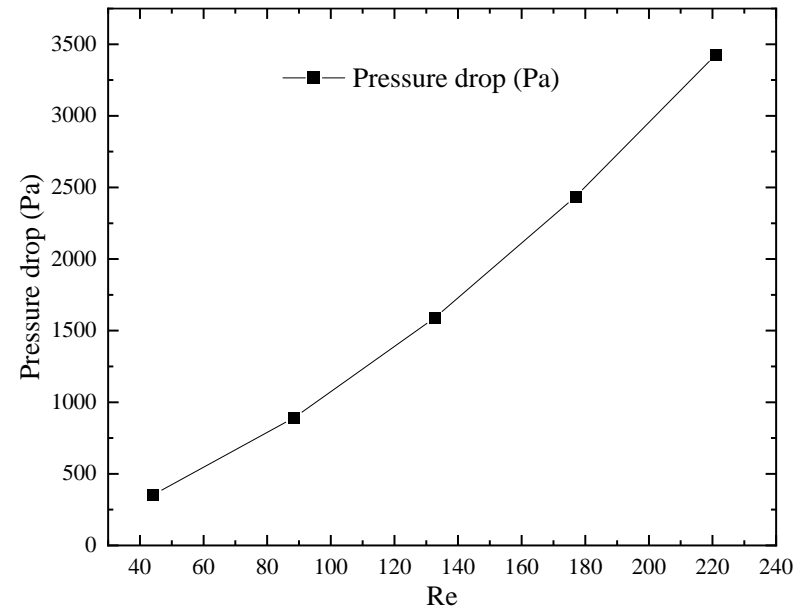
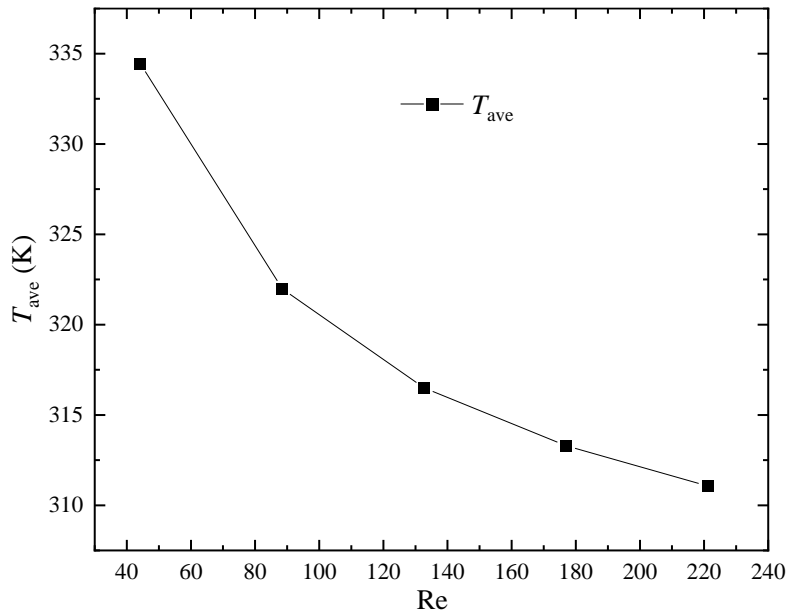
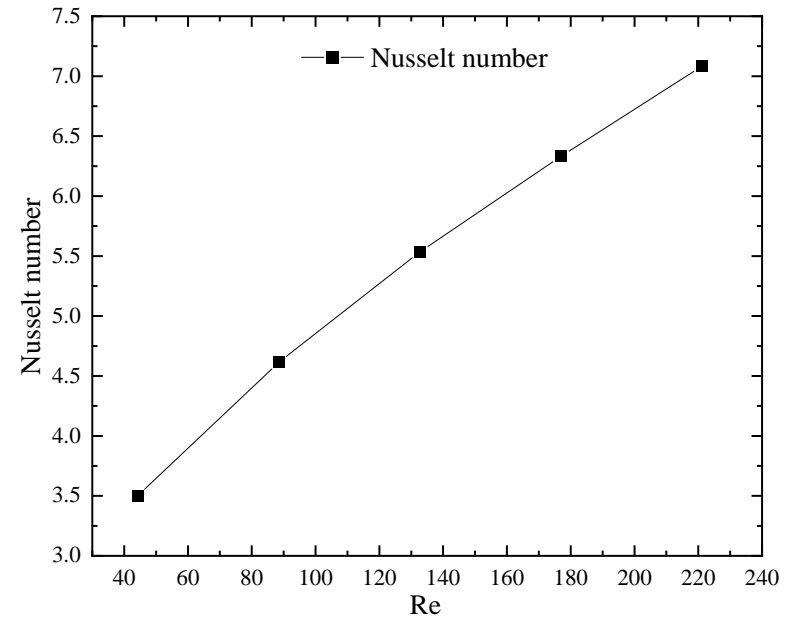
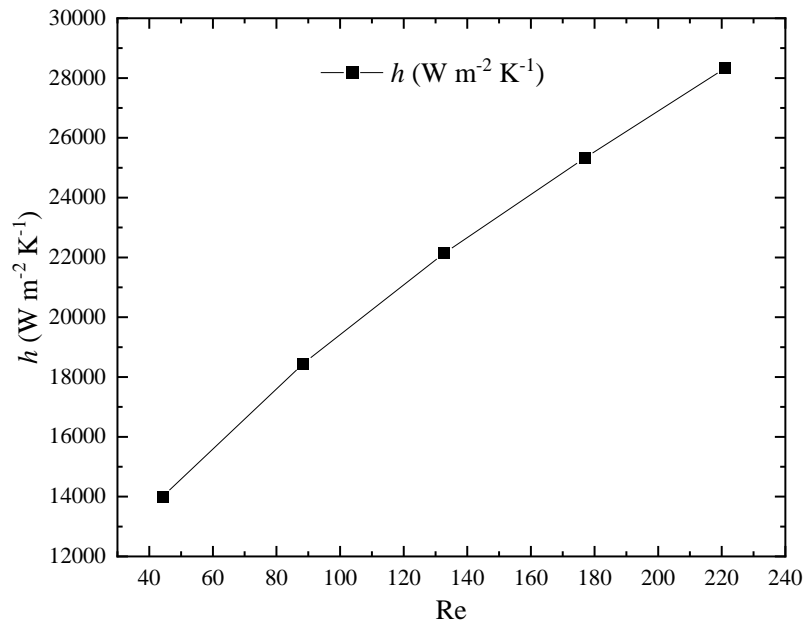
$$q_w A_s = h A_{con} \Delta T_m = C_p M (T'' - T')$$

## Average Nusselt number

$$Nu_{ave} = \frac{h_{ave} D_h}{\lambda_f}$$

$Re$	44	88	132	176	220
$h$ ( $\text{Wm}^{-2}\text{K}^{-1}$ )	13999.6	18453.6	22140	25323.2	28336
$Nu$	3.5	4.6	5.5	6.3	7.1
$\Delta P$ (Pa)	354	892.8	1590	2436.6	3428
$T_w$ (K)	334.45	321.98	316.5	313.3	311.1







**Wanzhou Meng, daughter of Zhengfei Ren, was arrested on 1th Dec. 2018 by Canada, required by USA.**



Detained by

1028 days